CLAIMS:

1. A method for producing a diesel fuel and a lubricant basestock, comprising: contacting a feedstock having a T95 boiling point of 1100.degree. F. (593.degree. C.) or less and comprising at least 100 wppm of sulfur with a dewaxing catalyst under effective conversion conditions, prior to exposing the feedstock to a hydrotreating catalyst, to produce a converted effluent, the effective conversion conditions being effective for at least 25% conversion of the feedstock relative to a conversion temperature of 370° C., the dewaxing catalyst comprising a unidimensional, 10-member ring pore molecular sieve, at least one Group VI metal, at least one Group VIII metal, and a binder having a binder surface area of 100 m^2/g or less, wherein the effective conversion conditions comprise a temperature of 350° C. to 450° C., a hydrogen partial pressure of from 11.5 MPag to 34.6 MPag (1662 psig to 5000 psig), a hydrogen circulation rate of from 445 m^3/m^3 (2500 SCF/B) to 1781 m^3/m^3 (10,000 scf/B), and an LHSV from 0.2 hr^{-1} to 1 hr^{-1}; contacting at least a portion of the converted effluent with a supported hydrotreating catalyst under effective hydrotreating conditions to produce a product effluent, the hydrotreating catalyst comprising at least one Group VI metal and at least one Group VIII metal; and fractionating the converted, hydrotreated effluent to form at least a distillate fuel product fraction and a lubricant base oil product fraction, wherein the distillate fuel product fraction comprises a diesel product fraction with a sulfur content of less than or equal to 12.4 ppmw.

2. The method of claim 1, wherein the support for the supported hydrotreating catalyst is substantially free of molecular sieve, the support for the supported hydrotreating catalyst is an amorphous support, or a combination thereof.

3. The method of claim 1, wherein the binder has a binder surface area of 80 m^2/g or less.

4. The method of claim 1, further comprising mixing the converted effluent with a quench fluid prior to contacting the converted effluent with the supported hydrotreating catalyst.

5. The method of claim 1, wherein the effective hydrotreating conditions include a temperature at least 10° C. lower than the effective conversion conditions.

6. The method of claim 1, wherein the molecular sieve is EU-1, NU-87, ZSM-22, EU-2, EU-11, ZBM-30, ZSM-48, ZSM-23, or a combination thereof.

7. The method of claim 1, wherein the molecular sieve is ZSM-48, ZSM-23, or a combination thereof.

8. The method of claim 1, wherein the molecular sieve is ZSM-48 with a silica to alumina ratio of 90:1 or less.

9. The method of claim 1, wherein the dewaxing catalyst binder comprises silica, alumina, titania, zirconia, silica-alumina, or a combination thereof.

10. The method of claim 9, wherein the dewaxing catalyst comprises a micropore surface area to total surface area ratio of greater than or equal to 25%, wherein the total surface area equals the surface area of the external zeolite plus the surface area of the binder.

11. The method of claim 1, wherein the dewaxing catalyst comprises Ni as the at least one Group VIII metal and Mo, W, or a combination thereof as the at least one Group VI metal.

12. The method of claim 1, wherein the feedstock comprises at least 1000 wppm of sulfur, the feedstock has a T95 boiling point of 1000° F. (538° C.) or less, or a combination thereof.

13. The method of claim 1, wherein the total conversion of the feedstock, relative to a conversion temperature of 370° C., to form the hydrotreated effluent is at least 45%.

14. The method of claim 1, wherein the hydrotreating catalyst comprises Ni as the at least one Group VIII metal and Mo, W, or a combination thereof as the at least one Group VI metal.

15. The method of claim 1, further comprising hydrofinishing at least a portion of the product

effluent, the distillate fuel product fraction, the lubricant product fraction, or a combination thereof.

16. The method of claim 1, wherein the effective hydrotreating conditions comprise a temperature of 200° C. to 450° C., a pressure of 250 psig (1.8 MPag) to 5000 psig (34.6 MPag), a liquid hourly space velocity (LHSV) of 0.1 hr^{-1} to 10 hr^{-1}, and a hydrogen treat rate of 200 scf/B (35.6 m^3/m^3) to 10,000 scf/B (1781 m^3/m^3).

17. `The method of claim 1, wherein the converted effluent is cascaded to said exposing to the hydrotreating catalyst under effective hydrotreating conditions without intermediate separation.

18. The method of claim 1, wherein the diesel product fraction has a cetane index of at least 50, a cloud point of -20° C. or less, or a combination thereof.

19. The method of claim 1, wherein the lubricant product fraction has a viscosity index of at least 110, a content of aromatics having three or more rings of 1.0 μmole/g or less, or a combination thereof.