

Fig. 1

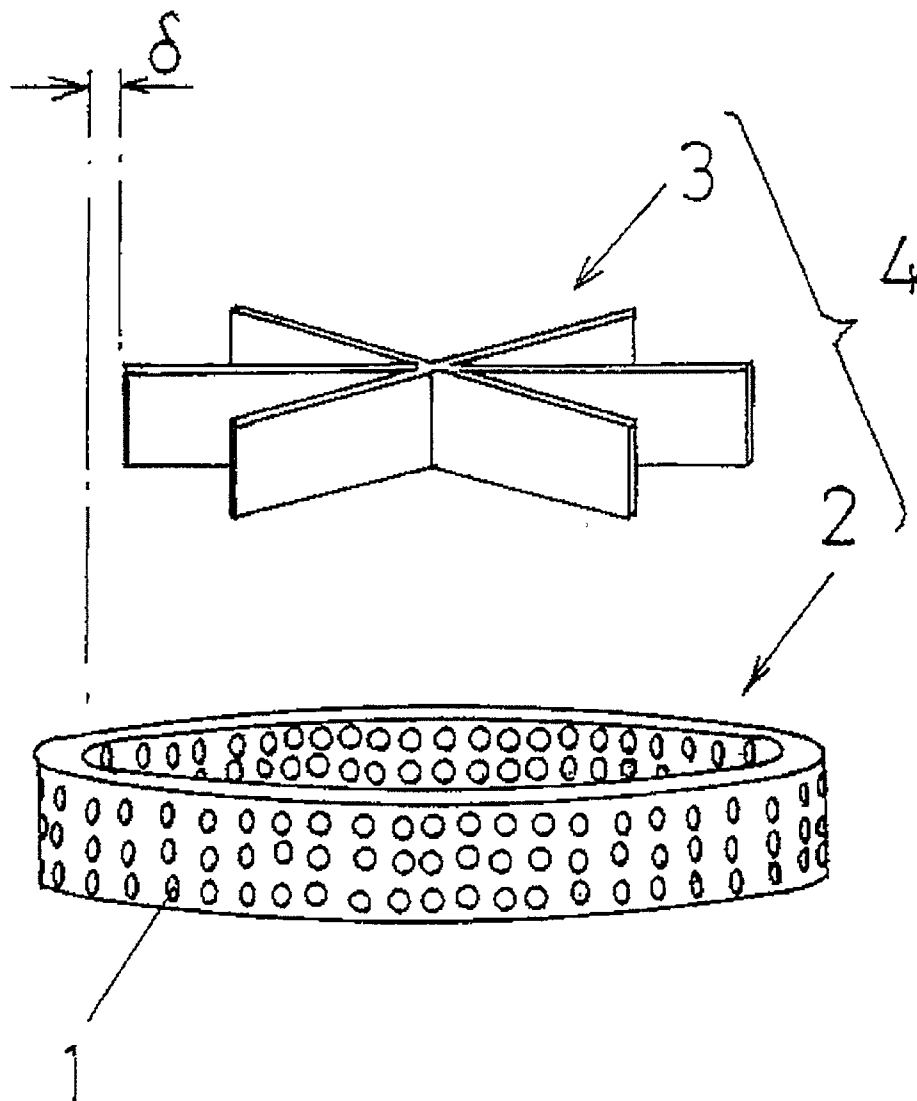
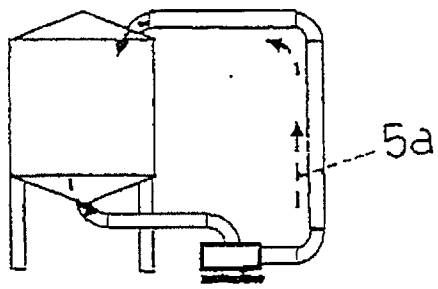


Fig. 2

External Circulation



Internal Circulation

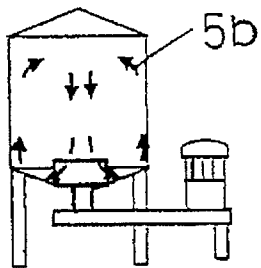


Fig. 3

Mixer (Rotor-Stator Type)

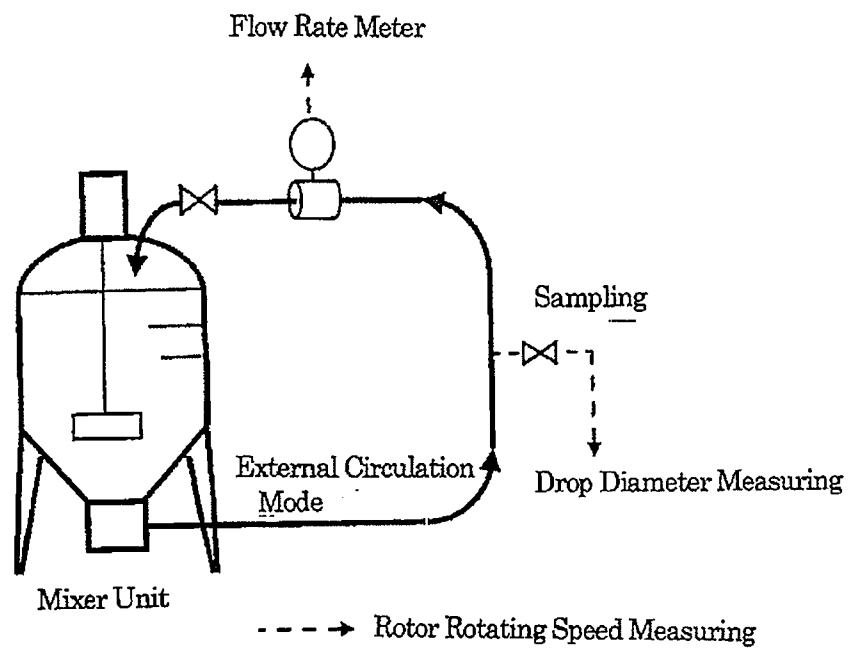


Fig. 4

[図4]

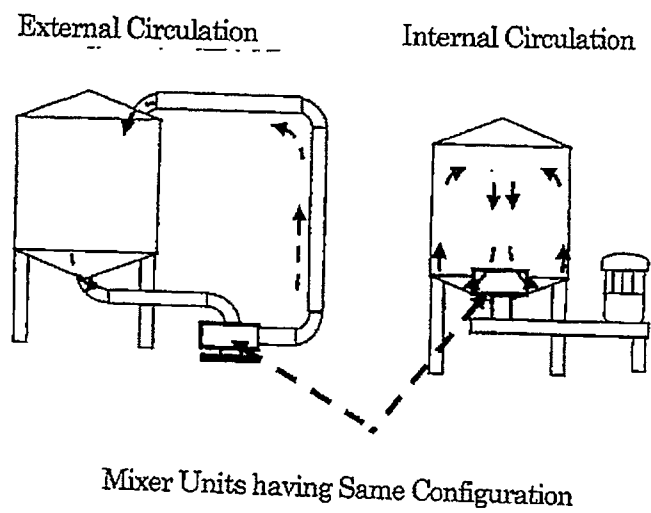


Fig. 5

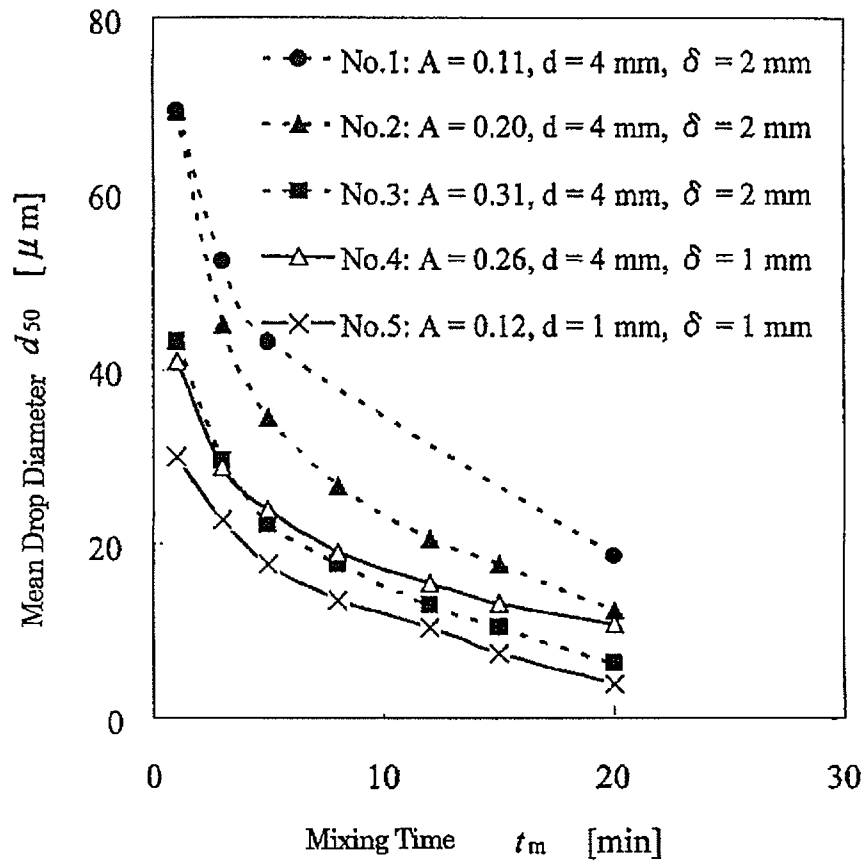


Fig. 5 Relationship between Mixing Time and Drop Diameter for Mixers A

Fig. 6

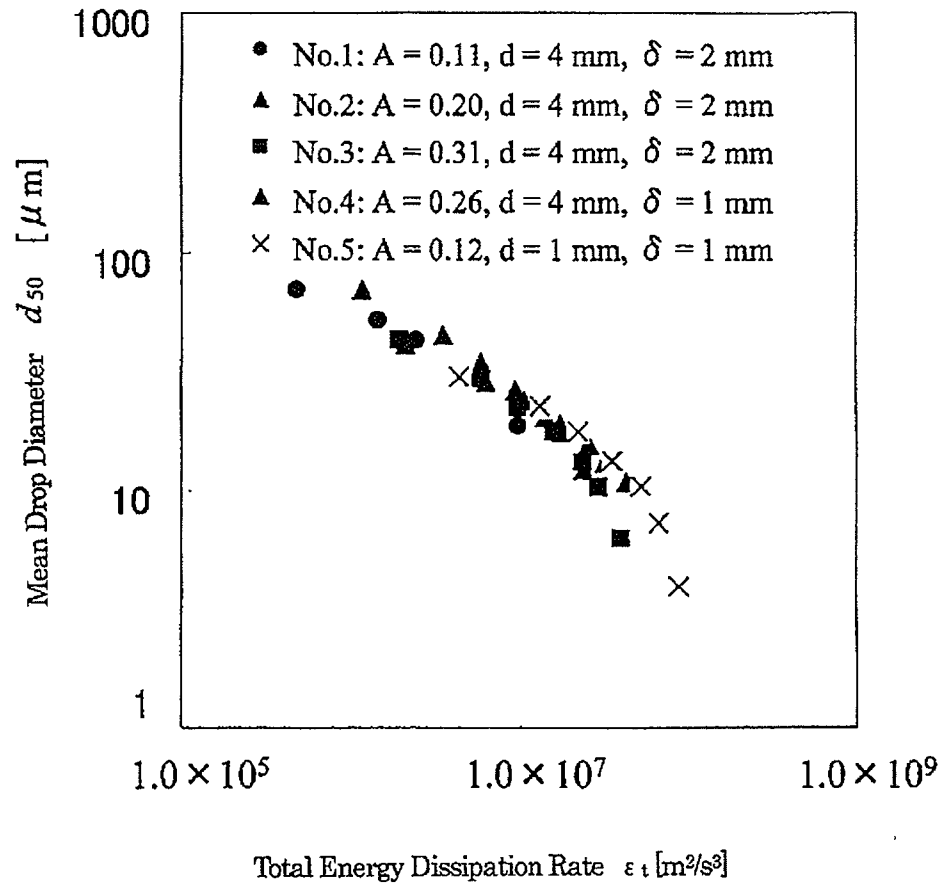


Fig. 6 Relationship between Mixing Time and Drop Diameter for Mixer A

Fig. 7

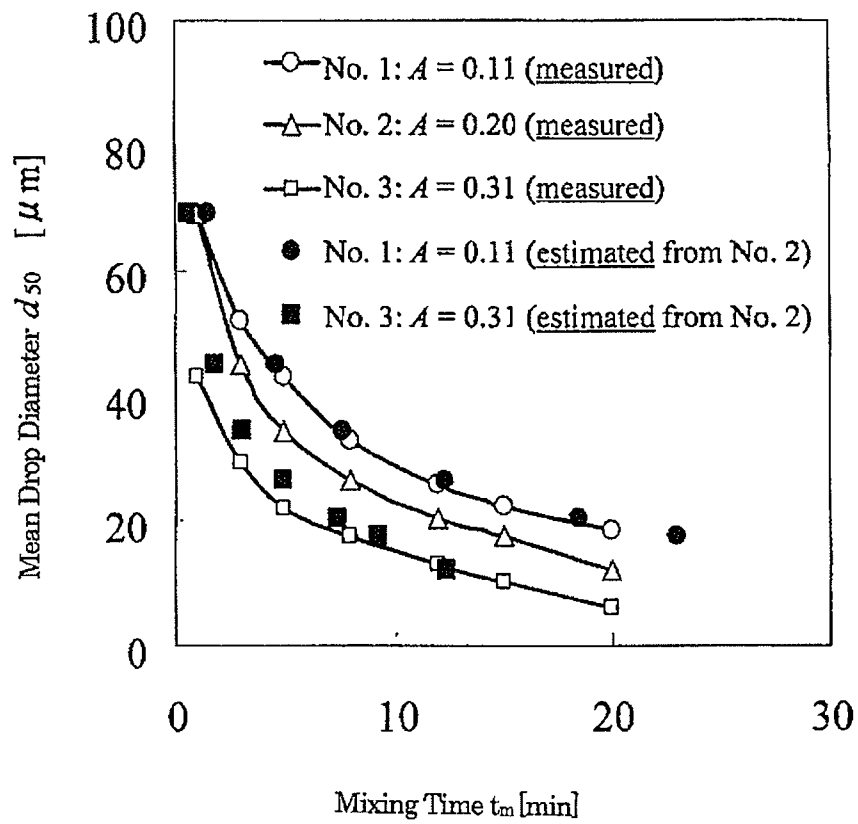


Fig. 7 Relationship between Mixing Time and Drop Diameter for Stator Nos. 1 through 3 and Estimated Values for Stator Nos. 1 and 3

Fig. 8

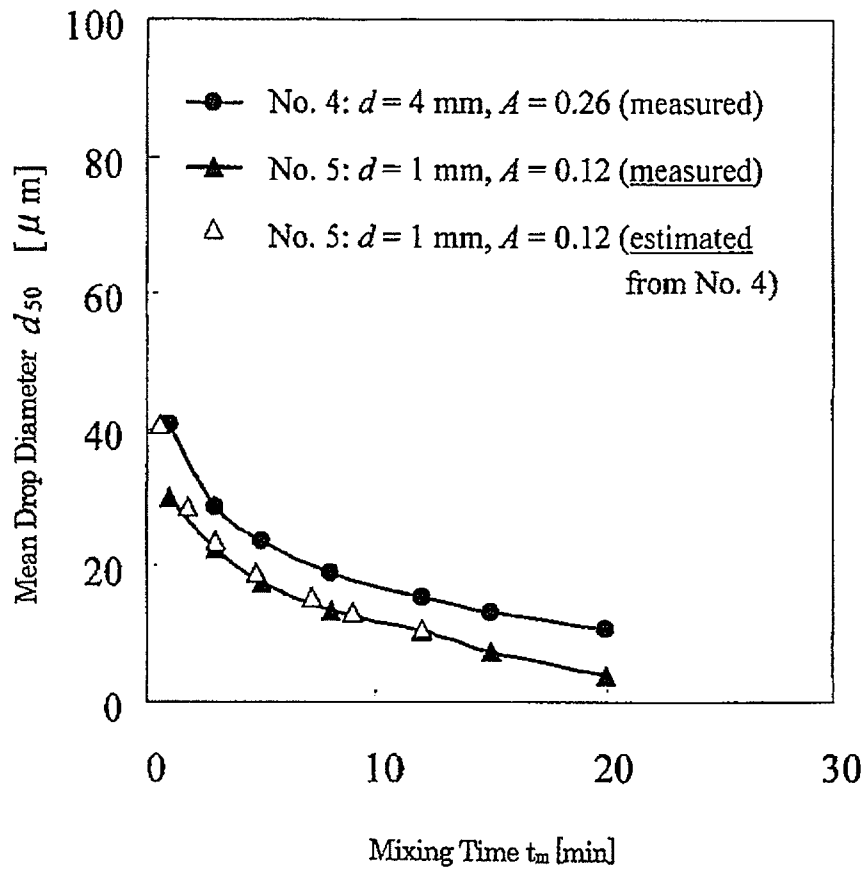
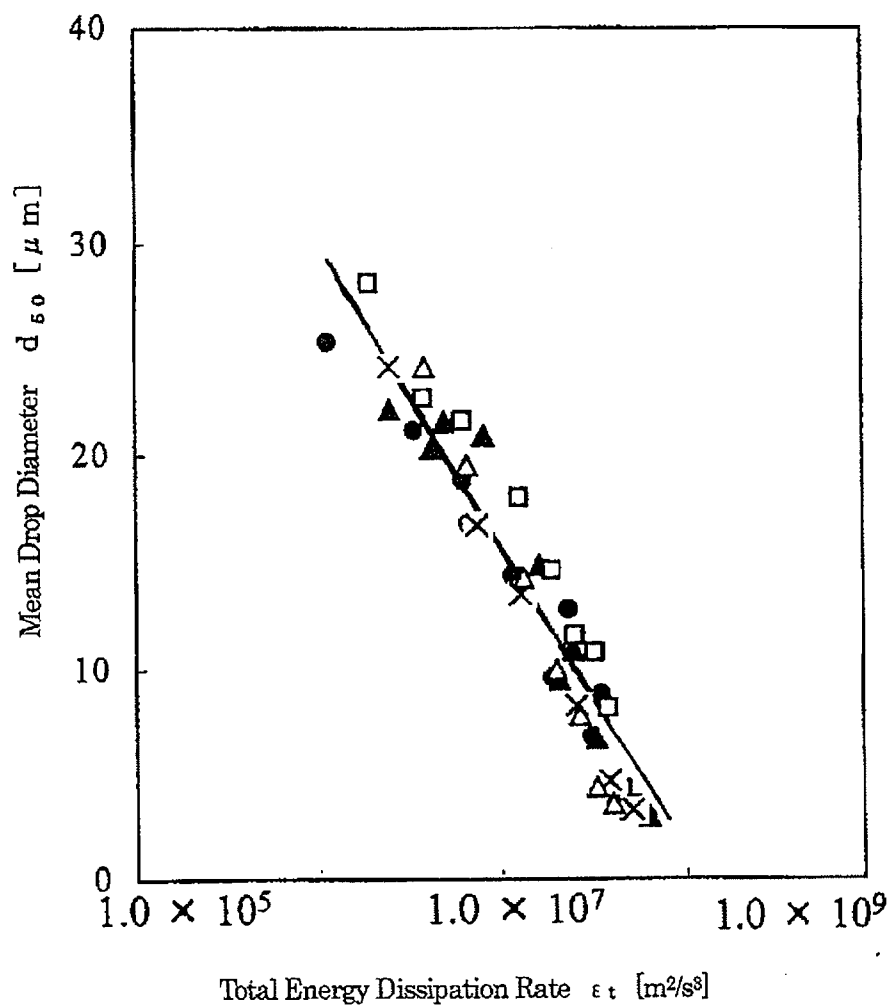


Fig. 8 Relationship between Mixing Time and Drop Diameter for Stator Nos. 4 and 5 and Estimated Values for Stator No. 5

Fig. 9



- No. 1: $V = 200 \text{ L}$, $N = 27 \text{ s}^{-1}$
 - ▲ No. 2: $V = 300 \text{ L}$, $N = 27 \text{ s}^{-1}$
 - No. 3: $V = 500 \text{ L}$, $N = 27 \text{ s}^{-1}$
 - No. 4: $V = 300 \text{ L}$, $N = 21 \text{ s}^{-1}$
 - ▲ No. 5: $V = 7000 \text{ L}$, $N = 15 \text{ s}^{-1}$
 - × No. 6: $V = 7000 \text{ L}$, $N = 16 \text{ s}^{-1}$
 - △ No. 7: $V = 7000 \text{ L}$, $N = 17 \text{ s}^{-1}$
- $d_{50} = a \cdot \ln(\epsilon_t) + b$
- $a = -6.2465$
- $b = 116.42$
- $R^2 = 0.91$

Relationship between Mean Drop Diameter and Total Energy Dissipation Rate for Medium and Large Scale Mixers

Fig. 10

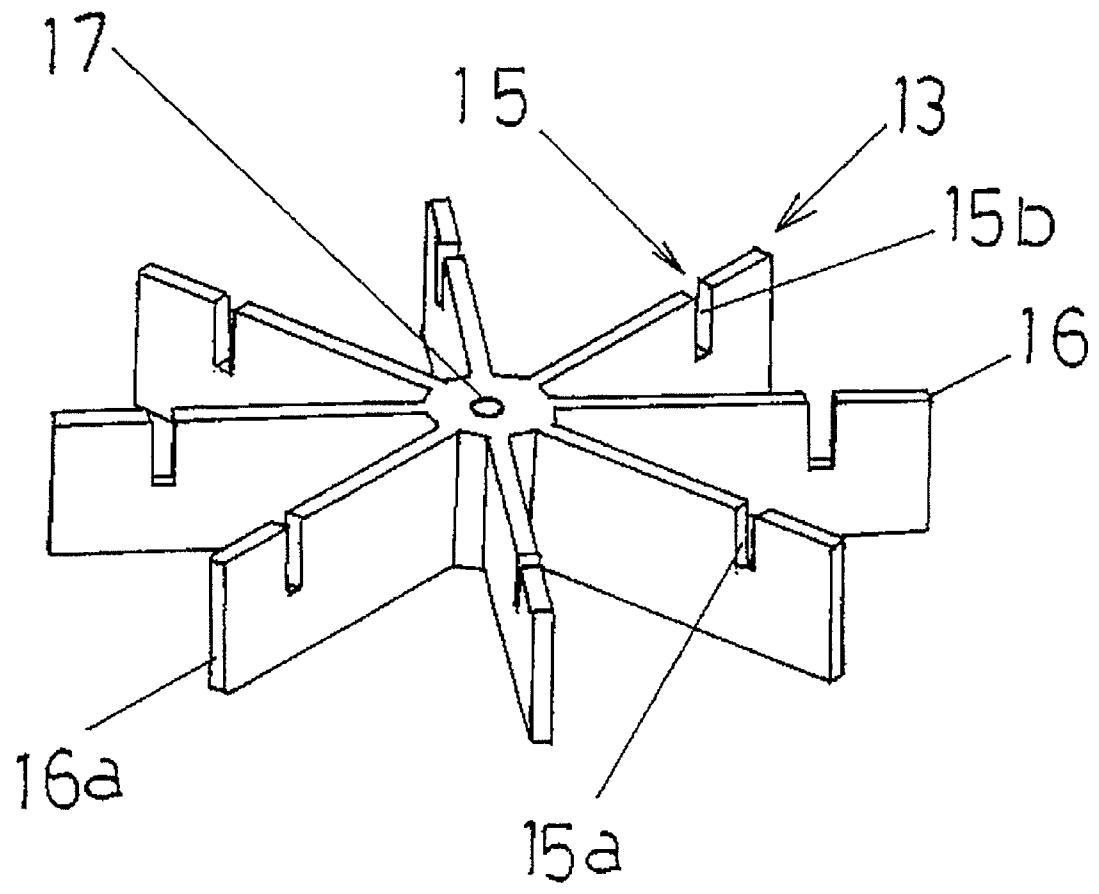


Fig. 11

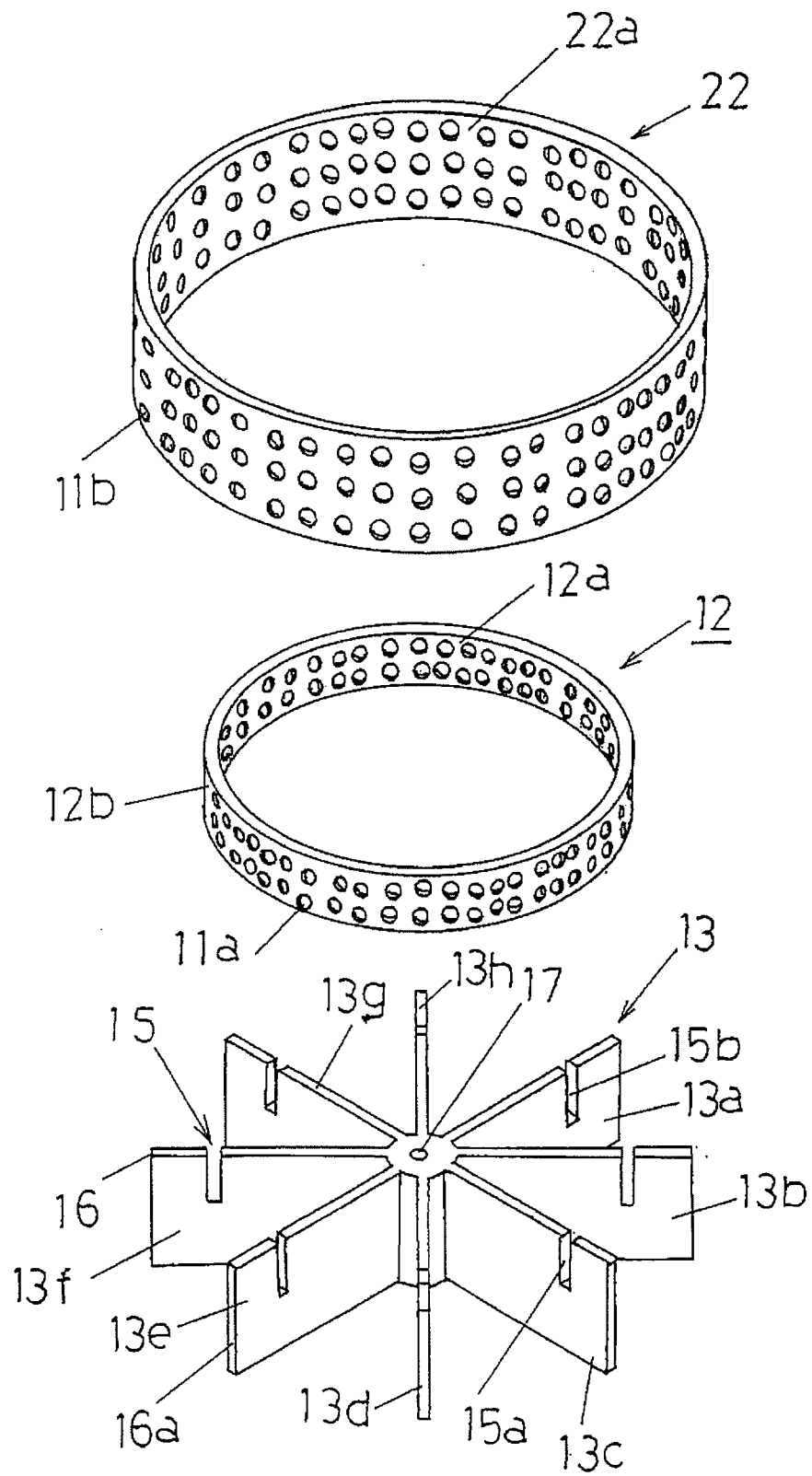


Fig. 12

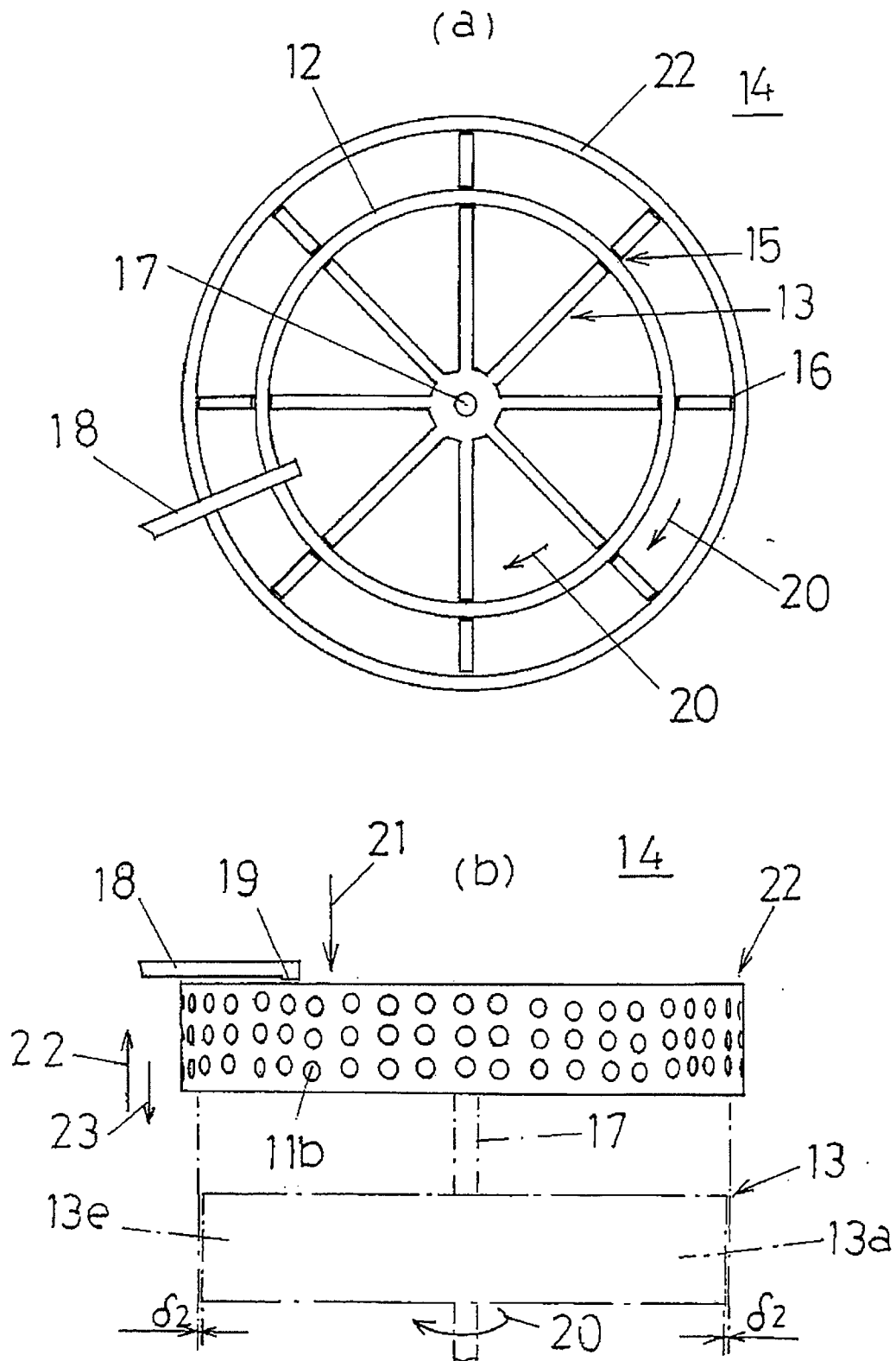


Fig. 13

Relationship between ε_t and Particle Size Diameter
(MEIBALANCE HP 1.0)

