

DESCRIPTION

FILTRATION MEMBRANE TREATMENT DEVICE, MEMBRANE FILTRATION
DEVICE, AND FILTRATION MEMBRANE TREATMENT METHOD

5 TECHNICAL FIELD

[0001] The present disclosure relates to a filtration
membrane treatment device, a membrane filtration device, and
a filtration membrane treatment method that enable ozone
treatment of a filtration membrane with a small variation.

10

BACKGROUND ART

[0002] If a treatment-target liquid is subjected to
separation by a filtration membrane, the filtration membrane
may be clogged with impurities and microorganisms in water.

15 Such clogging can be prevented by improving the water
permeability of such a filtration membrane in treatment of
the filtration membrane. As methods for improving the water
permeability of a filtration membrane, there are methods such
as a method in which a produced filtration membrane is
20 chemically treated and hydrophilized.

[0003] For example, Patent Document 1 describes a method
including: treating a polyvinylidene-based resin porous
membrane with a base, and then treating the polyvinylidene-
based resin porous membrane with an aqueous solution that
25 contains hydrogen peroxide or ozone; and further treating the

polyvinylidene-based resin porous membrane with an aqueous solution that contains at least one type of salt selected from among perchloric acid salts, perbromates, and periodic acid salts, to perform hydrophilization. Furthermore, for
5 example, Patent Document 2 describes a method including stopping passage of ozone water if a difference in pressure reaches a predetermined value when a membrane module is being cleaned with the ozone water, to perform hydrophilization.

10 CITATION LIST

PATENT DOCUMENT

[0004] Patent Document 1: Japanese Laid-Open Patent
Publication No. 2004-230280

Patent Document 2: Japanese Laid-Open Patent
15 Publication No. 2004-249168

SUMMARY OF THE INVENTION

PROBLEMS TO BE SOLVED BY THE INVENTION

[0005] Conventional filtration membrane treatment devices
20 and filtration membrane treatment methods involve:
hydrophilizing a membrane under a certain fixed condition
that, for example, the membrane is treated by being immersed
for 100 hours in ozone water having a concentration of 10
ppm; and evaluating the degree of hydrophilization with use
25 of, as an index of hydrophilization, the ratio between the

permeation amount of pure water after hydrophilization and the permeation amount of pure water before hydrophilization. In this method, a membrane is hydrophilized under a fixed condition. Thus, this method takes into account neither the
5 fact that there is an individual difference among membranes nor the fact that even identical polyvinylidene-based resin porous membranes have different characteristics depending on the manufacturer of the membranes. Therefore, a problem arises in that there is a variation in the degree of
10 hydrophilization among membranes and appropriate treatment of the membranes cannot be efficiently performed.

[0006] The present disclosure has been made to solve the above problem, and an object of the present disclosure is to provide a filtration membrane treatment device, a membrane
15 filtration device, and a filtration membrane treatment method that enable ozone treatment of a filtration membrane with a small variation.

SOLUTION TO THE PROBLEMS

20 [0007] A filtration membrane treatment device according to the present disclosure is a filtration membrane treatment device which performs ozone treatment on a filtration membrane, the filtration membrane treatment device including:
a first supply portion which supplies an ozone-
25 containing fluid to the filtration membrane;

a measurement portion which measures a measurement value based on a pressure to the filtration membrane; and

a control portion which adjusts, on the basis of a change in the measurement value measured by the measurement portion, a supply amount of the ozone-containing fluid to be supplied by the first supply portion.

A membrane filtration device according to the present disclosure is a membrane filtration device which treats a treatment-target liquid with use of the above-described filtration membrane treatment device, the membrane filtration device including:

a storage tank which stores the treatment-target liquid and in which the filtration membrane is immersed; and

a transfer portion which transfers, to outside of the storage tank, the treatment-target liquid having been filtered by the filtration membrane, wherein

the control portion causes the transfer portion to stop and causes the first supply portion to supply the ozone-containing fluid to the filtration membrane immersed inside the storage tank.

A filtration membrane treatment method according to the present disclosure is a filtration membrane treatment method including:

a supply step of supplying an ozone-containing fluid to a filtration membrane;

a measurement step of measuring a measurement value based on a pressure to the filtration membrane; and

a control step of adjusting a supply amount of the ozone-containing fluid on the basis of a change in the measurement value.

EFFECT OF THE INVENTION

[0008] The filtration membrane treatment device, the membrane filtration device, and the filtration membrane treatment method according to the present disclosure enable ozone treatment of a filtration membrane with a small variation.

BRIEF DESCRIPTION OF THE DRAWINGS

15 [0009] [FIG. 1] FIG. 1 is a diagram showing a configuration of a filtration membrane treatment device according to embodiment 1.

[FIG. 2] FIG. 2 is a flowchart of a filtration membrane treatment method by the filtration membrane treatment device shown in FIG. 1.

[FIG. 3] FIG. 3 is a diagram showing a configuration of another filtration membrane treatment device according to embodiment 1.

[FIG. 4] FIG. 4 is a diagram showing a configuration of another filtration membrane treatment device

according to embodiment 1.

[FIG. 5] FIG. 5 is a diagram showing a configuration of another filtration membrane treatment device according to embodiment 1.

5 [FIG. 6] FIG. 6 is a diagram showing a configuration of another filtration membrane treatment device according to embodiment 1.

[FIG. 7] FIG. 7 is a diagram showing a configuration of another filtration membrane treatment device
10 according to embodiment 1.

[FIG. 8] FIG. 8 is a diagram showing a configuration of a filtration membrane treatment device according to embodiment 2.

[FIG. 9] FIG. 9 is a diagram showing a
15 configuration of another filtration membrane treatment device according to embodiment 2.

[FIG. 10] FIG. 10 is a diagram showing a configuration of a filtration membrane treatment device according to embodiment 3.

20 [FIG. 11] FIG. 11 is a flowchart of a filtration membrane treatment method by the filtration membrane treatment device shown in FIG. 10.

[FIG. 12] FIG. 12 is a diagram showing a configuration of another filtration membrane treatment device
25 according to embodiment 3.

[FIG. 13] FIG. 13 is a diagram showing a configuration of a membrane filtration device in which a filtration membrane treatment device is used, according to embodiment 4.

5 [FIG. 14] FIG. 14 is a table showing the specifications of filtration membrane treatment devices used in Example 1, Comparative Example 1, and Comparative Example 2.

[FIG. 15] FIG. 15 is a table showing results of
10 Example 1.

[FIG. 16] FIG. 16 is a table showing results of Comparative Example 1 and Comparative Example 2.

DESCRIPTION OF EMBODIMENTS

15 [0010] Embodiment 1

FIG. 1 is a diagram showing a configuration of a filtration membrane treatment device according to embodiment 1. FIG. 2 is a flowchart of a filtration membrane treatment method by the filtration membrane treatment device shown in
20 FIG. 1. FIG. 3 to FIG. 7 are diagrams showing configurations of other filtration membrane treatment devices according to embodiment 1. In each drawing, the filtration membrane treatment device is for performing ozone treatment on a filtration membrane 1 to purge the filtration membrane 1
25 having treated a treatment-target liquid, thereby using the

filtration membrane 1 for treatment of the treatment-target liquid again.

[0011] Thus, the filtration membrane 1 is inevitably formed of a material having ozone resistance. In addition, the filtration membrane 1 is formed of a material that is hydrophilized by ozone. Specifically, it is possible to use, for example, a material formed of a fluorine-based macromolecule. Representative examples of the material are polyvinylidene difluoride (PVDF) and polytetrafluoroethylene (PTFE).

[0012] The shape of the filtration membrane 1 is not particularly limited, and, for example, a hollow fiber membrane, a flat membrane, or a tubular membrane can be used. In addition, a module type of the filtration membrane 1 is not particularly limited, and, for example, an internal pressure type module or an external pressure type module accommodated in a cylindrical container, or an immersion type module, can be used. Here, description will be given with an example in which a hollow fiber membrane module of an immersion type is used.

[0013] The filtration membrane treatment device includes a first supply portion 3, a measurement portion 8, and a control portion 11. The first supply portion 3 supplies an ozone-containing fluid to the filtration membrane 1. The measurement portion 8 measures a measurement value H based on

a pressure to the filtration membrane 1. The control portion 11 adjusts, on the basis of a change in the measurement value H measured by the measurement portion 8, a supply amount of the ozone-containing fluid to be supplied by the first supply
5 portion 3.

[0014] Here, the filtration membrane 1 is a hollow fiber membrane module of an immersion type and thus filters the treatment-target liquid from a primary side to a secondary side. In addition, since a hollow fiber membrane module of
10 an immersion type is used as the filtration membrane 1, the ozone-containing fluid will be described using an example of a pouring method similar to so-called "reverse-pressure cleaning" in which the ozone-containing fluid is poured from the secondary side toward the primary side.

15 [0015] The filtration membrane 1 is accommodated inside the accommodating tank 2. The accommodating tank 2 is filled with a liquid 4 which is, for example, water. Thus, the filtration membrane 1 is immersed in the liquid 4. This is because the filtration membrane 1 is a hollow fiber membrane
20 module of an immersion type and performance deterioration thereof due to drying has to be prevented. Therefore, a filtration membrane 1 in which performance deterioration due to drying does not occur does not necessarily need to be subjected to ozone treatment in a state of being immersed in
25 the liquid 4 inside the accommodating tank 2.

[0016] The filtration membrane 1, the measurement portion 8, and the first supply portion 3 are connected by a first pipe 7. The first supply portion 3 includes: a first reservoir 5 which stores the ozone-containing fluid; and a first pump 6 which is for supplying ozone from the first reservoir 5 through the first pipe 7 to the filtration membrane 1. As for the ozone-containing fluid, for example, use of one or more types of ozone gas, ozone water produced by dissolving ozone in a solvent such as water, or mixed water obtained by mixing, with ozone water, a substance that promotes generation of radicals due to decomposition of ozone, is assumed.

[0017] The measurement portion 8 includes, as a constituent for measuring the measurement value H based on the pressure to the filtration membrane 1, a pressure gauge 9 which measures a pressure value in the first pipe 7 as a pipe through which the fluid (here, ozone-containing fluid) to be supplied to the filtration membrane 1 flows. The specifications of the pressure gauge 9 is not limited as long as the pressure gauge 9 is of a type that allows the measured pressure value to be sent to the control portion 11. The control portion 11 receives the measurement value H from the pressure gauge 9 of the measurement portion 8 and controls, by means of the first pump 6, the supply amount of the ozone-containing fluid to be supplied through the first pipe 7, on

the basis of a change in the measurement value H. The accommodating tank 2 is provided with a first discharge portion 10 by which an excess portion of the ozone-containing fluid or the liquid 4 is discharged to outside.

5 [0018] Next, a filtration membrane treatment method by the filtration membrane treatment device according to embodiment 1 configured as described above, will be described. First, the filtration membrane treatment device according to the present embodiment 1 is configured as described above, and
10 the change in the measurement value H based on the pressure at the time of supplying the ozone-containing fluid to the filtration membrane 1 is observed so that the degree of ozone treatment is quantified and a timing of completion of ozone treatment is determined.

15 [0019] Regarding this, earnest studies by the present inventors led to the following findings. When the ozone-containing fluid is brought into contact with the filtration membrane 1, a hydrophilic functional group such as a hydroxyl group is added onto the molecular chain of the material that
20 forms the filtration membrane 1 and that is hydrophilized by ozone. Thus, the hydrophilicity of the filtration membrane 1 is improved. Therefore, the water permeability (i.e., the easiness of passage of water) of the filtration membrane 1 is improved. Judging from this, it can be determined that the
25 filtration membrane 1 is purged by ozone treatment.

[0020] The present inventors further found that, if the ozone-containing fluid is supplied to the filtration membrane 1 and ozone treatment of the filtration membrane 1 is monitored and evaluated on the basis of the change in the measurement value H based on the pressure, determination can be performed by interpretation as an index of the water permeability (the easiness of passage of water) of the filtration membrane 1. Moreover, the present inventors found that: if ozone treatment of the filtration membrane 1 is performed by supplying the ozone-containing fluid, the measurement value H based on the pressure to the filtration membrane 1 gradually decreases; and, if the ozone treatment is completed, the change in the measurement value H becomes very small. The reason for this was found to be as follows, as a result of earnest studies by the present inventors. There is a limit to the amount of a hydrophilic group that can be added onto the aforementioned molecular chain of the filtration membrane 1, and, if the limit is exceeded, the change in the degree of hydrophilization becomes very small even when the ozone-containing fluid is supplied to the filtration membrane 1.

[0021] Consequently, the present inventors found that determination based on the change in the measurement value H leads to decision of a breakpoint of the ozone treatment of the filtration membrane 1, i.e., a point at which the ozone

treatment should be completed. As described above, the ozone treatment of the filtration membrane 1 is synonymous with hydrophilization of the filtration membrane 1. Therefore, the present inventors found a limit of the hydrophilization of the filtration membrane 1, i.e., a point at which the hydrophilization should be completed. It is noted that the above described findings apply also to the other embodiments, and description thereof is omitted, as appropriate.

[0022] Hereinafter, the filtration membrane treatment method will be described with reference to the flowchart in FIG. 2 in consideration of these findings. First, the control portion 11 drives the first pump 6, to perform a supply step of supplying the ozone-containing fluid from the first reservoir 5 of the first supply portion 3 through the first pipe 7 to the filtration membrane 1 (step ST1 in FIG. 2). It is noted that the ozone-containing fluid continues to be supplied such that the supply amount thereof is a fixed amount.

[0023] Next, a measurement step of measuring the measurement value H based on the pressure to the filtration membrane 1, is performed while the supply step is continued. First, the measurement portion 8 measures, as the measurement value H, a first measurement value H1 after the first supply portion 3 supplies the ozone-containing fluid for a first time period T1, and the measurement portion 8 sends the first

measurement value H1 to the control portion 11 (step ST2 in FIG. 2). Then, a second measurement value H2 after the ozone-containing fluid is supplied for a second time period T2 which is longer than the first time period T1, is measured
5 and sent to the control portion 11 (step ST3 in FIG. 3).

[0024] Preferable ranges of the first time period T1 and a time period from the end of the first time period T1 to the start of the second time period T2, for the measurement performed as described above, are 1 minute to 20 minutes. If
10 the time periods are shorter than 1 minute, ozone treatment has hardly progressed, and the difference from a previous measurement value H or from an initial-state value is unclear, whereby there is a possibility that completion of the ozone treatment cannot be determined. Meanwhile, if the
15 time periods are longer than 20 minutes, the time period to the next measurement is elongated, whereby there is a possibility that, even though the ozone treatment has actually been completed, determination of the completion is delayed and the ozone treatment is unnecessarily continued.
20 It is noted that the first time period T1 and the time period from the end of the first time period T1 to the start of the second time period T2 may be equal to each other or may be individually set. For example, it can also be assumed that: each time period is initially set to be long at the start of
25 the ozone treatment; and the time period is set to be short

at approximation to a time point at which the treatment is ordinarily considered to end.

[0025] Then, a control step of adjusting the supply amount of the ozone-containing fluid on the basis of a change in the measurement value H , is performed. The control portion 11 determines whether or not a change ratio α in the following expression 1 between the first measurement value $H1$ and the second measurement value $H2$ is equal to or smaller than a threshold value $\alpha1$ (the following expression 2) (step ST4 in FIG. 2).

[0026] $|H1-H2| \div |H1| = \alpha$... expression 1

[0027] $\alpha \leq \alpha1$... expression 2

[0028] If the change ratio α is equal to or smaller than the threshold value $\alpha1$ (YES), the supply of the ozone-containing fluid by the first supply portion 3 is suppressed. Here, the control portion 11 causes the first pump 6 to stop, to end the supply of the ozone-containing fluid to the filtration membrane 1 (step ST5 in FIG. 2).

[0029] Meanwhile, if the change ratio α is larger than the threshold value $\alpha1$ (NO), the supply of the ozone-containing fluid by the first supply portion 3 is continued, and the process from step ST3 is repeated. If the operation is repeated from step ST3, the previously measured second measurement value $H2$ at the elapse of the second time period $T2$ is regarded as a first measurement value $H1$ at the elapse

of the first time period T1 for the repetition. Then, a second measurement value H2 at the subsequent elapse of the second time period T2, is newly measured, and the method described above is repeated. That is, the first measurement value H1 at the elapse of the first time period T1 is the previous measurement value H, and the second measurement value H2 at the elapse of the second time period T2 is the present measurement value H.

[0030] A preferable range of the threshold value $\alpha 1$ for the change ratio α is 0 to 0.5. If the threshold value $\alpha 1$ is larger than 0.5, there is a possibility that ozone treatment is determined to have been completed even though there is room for the ozone treatment to progress.

[0031] In the above-described embodiment 1, an example in which the pressure value in the first pipe 7 is used as the measurement value H has been described. However, the present disclosure is not limited to this example. For example, the trans-membrane pressure (TMP) value between the primary side and the secondary side of the filtration membrane 1 may be measured and used as the measurement value H. In this case, for example, pressure gauges may be disposed respectively on the primary side and the secondary side of the filtration membrane 1, and a trans-membrane pressure value may be calculated from the values at the pressure gauges and used as the measurement value H. Alternatively, if a filtration

membrane 1 of an immersion type such as one in FIG. 1 is used, a TMP may be calculated from a liquid level inside the accommodating tank 2 and the pressure value at the pressure gauge 9 and used as the measurement value H.

5 [0032] In addition, in the above-described embodiment 1, an example in which the first supply portion 3 includes the first reservoir 5 for storing the ozone-containing fluid and supplies the ozone-containing fluid, has been described. Although the ozone-containing fluid has not been particularly
10 described, another case can be assumed in which ozone gas is used as the ozone-containing fluid. As shown in FIG. 3, a first supply portion 3 includes an ozone gas generator 12. The control portion 11 controls the amount of ozone gas to be generated from the ozone gas generator 12. The ozone gas is
15 supplied through the first pipe 7 directly to the filtration membrane 1, whereby the filtration membrane can be treated in the same manner as in the above-described embodiment 1.

[0033] In the case where ozone gas is used as the ozone-containing fluid, the concentration of the ozone gas is
20 preferably 1 ppm to 1000 ppm. The reason is as follows. If the concentration of the ozone gas is lower than 1 ppm, the ozone treatment effect is low and it takes time to complete ozone treatment. Meanwhile, if the concentration of the ozone gas is higher than 1000 ppm, a member forming the
25 filtration membrane 1, the first pipe 7, or the like may be

degraded.

[0034] Another example of using ozone gas is shown in FIG. 4 in which a first supply portion 3 includes the ozone gas generator 12, the first reservoir 5, and the first pump 6. The control portion 11 controls the amount of ozone gas to be generated from the ozone gas generator 12. The generated ozone gas is stored as an ozone-containing fluid in the first reservoir 5, and the stored ozone gas is supplied via the first pump 6 to the filtration membrane 1, whereby the filtration membrane can be treated in the same manner as in the above-described embodiment 1. In this case, the inside of the first reservoir 5 may be filled with a porosity such as silica gel as an adsorbent so that the ozone gas is stored while being adsorbed and condensed.

[0035] As another example, a case can be assumed in which ozone water is used as the ozone-containing fluid. As shown in FIG. 5, a first supply portion 3 includes the ozone gas generator 12, a first reservoir 50, and the first pump 6. The first reservoir 50 includes: a second pipe 13 through which a solvent such as water for dissolving ozone gas is supplied; and a second discharge portion 14 by which excess ozone gas in the first reservoir 5 is discharged to outside. Through the second pipe 13, for example, water is supplied to the first reservoir 50. Then, ozone gas is supplied from the ozone gas generator 12 into the first reservoir 50, and ozone

water is produced and stored in the first reservoir 5. The stored ozone water is supplied via the first pump 6 to the filtration membrane 1, whereby the filtration membrane can be treated in the same manner as in the above-described embodiment 1.

[0036] In the case where ozone water is used as the ozone-containing fluid, the concentration of the dissolved ozone contained in the ozone water to be supplied to the filtration membrane 1 is preferably 1 mg/L to 100 mg/L. The reason is as follows. If the concentration of the dissolved ozone is lower than 1 mg/L, the ozone treatment effect is low and it takes time to complete the treatment. Meanwhile, if the concentration of the dissolved ozone is higher than 100 mg/L, there is a possibility that a large amount of oxygen gas bubbles is generated owing to decomposition of ozone and hinder the supply of the ozone water to the filtration membrane 1.

[0037] In the case where ozone water is used as the ozone-containing fluid, a pH adjuster such as hydrochloric acid or sulfuric acid may be added to the ozone water. The pH of the ozone water to be supplied to the filtration membrane 1 is not particularly limited as long as the pH is within a range corresponding to the pH resistance of the filtration membrane 1. For example, in a case where polyvinylidene difluoride (PVDF) is used for the filtration membrane 1, any pH can be

selected from between 1 pH to 14 pH as the pH of the ozone water.

[0038] As another example, a case can be assumed in which mixed water obtained by mixing, with ozone water, a substance
5 that promotes generation of radicals due to decomposition of ozone (hereinafter, abbreviated as a promoter) is used as the ozone-containing fluid. In this case, the mixed water produced by mixing the ozone water and the promoter in advance is stored in the first reservoir 5 shown in FIG. 1,
10 and the stored mixed water is supplied via the first pump 6 to the filtration membrane 1, whereby the filtration membrane can be treated in the same manner as in the above-described embodiment 1.

[0039] Another example of the case of using the mixed
15 water is shown in FIG. 6 in which a first supply portion 3 includes the ozone gas generator 12, the first reservoir 50, the first pump 6, and an adding portion 15. The adding portion 15 is for adding the promoter. A third pipe 16 connecting the adding portion 15 and the first pipe 7 to each
20 other is provided. The control portion 11 controls the amount of the promoter to be added by the adding portion 15.

[0040] The promoter is supplied from the adding portion 15 through the third pipe 16 to the first pipe 7, the promoter is mixed with the ozone water in the first pipe 7, and the
25 obtained mixed water is supplied to the filtration membrane

1, whereby the filtration membrane can be treated in the same manner as in the above-described embodiment 1. As the promoter, for example, oxidizing agents such as hydrogen peroxide water and sodium hypochlorite and alkalis such as caustic soda and potassium hydroxide, can be used. Among them, one type may be selected, or a plurality of types may be used.

[0041] In the above-described embodiment 1, an example in which the first supply portion 3 pours the ozone-containing fluid from the secondary side to the primary side of the filtration membrane 1, has been described. However, the present disclosure is not limited to this example. An example in which the first supply portion 3 supplies the ozone-containing fluid from the primary side to the secondary side of the filtration membrane 1, will be described. As shown in FIG. 7, the ozone-containing fluid is supplied from the first pump 6 through the first pipe 7 to the accommodating tank 2. The ozone-containing fluid is suctioned via a suction pump 30 from the first pipe 7 connected to the filtration membrane 1, and the ozone-containing fluid is supplied to the filtration membrane 1, so that ozone treatment is performed on the filtration membrane 1. Then, the ozone-containing fluid suctioned via the suction pump 30 is discharged to outside by the first discharge portion 10. Also with this configuration, the

filtration membrane can be treated in the same manner as in the above-described embodiment 1. It is noted that, in this case, the pressure value measured by the pressure gauge 9 is a negative value. However, since values are calculated with absolute values as indicated in the above-described expression 1, the calculation can be performed in the same manner.

[0042] The filtration membrane treatment device according to embodiment 1 configured as described above is a filtration membrane treatment device which performs ozone treatment on a filtration membrane, the filtration membrane treatment device including:

- a first supply portion which supplies an ozone-containing fluid to the filtration membrane;
- a measurement portion which measures a measurement value based on a pressure to the filtration membrane; and
- a control portion which adjusts, on the basis of a change in the measurement value measured by the measurement portion, a supply amount of the ozone-containing fluid to be supplied by the first supply portion.

The filtration membrane treatment method according to embodiment 1 includes:

- a supply step of supplying an ozone-containing fluid to a filtration membrane;
- a measurement step of measuring a measurement value

based on a pressure to the filtration membrane; and

a control step of adjusting a supply amount of the ozone-containing fluid on the basis of a change in the measurement value.

5 Thus, if the ozone-containing fluid is supplied to the filtration membrane and ozone treatment of the filtration membrane is monitored and evaluated on the basis of the change in the measurement value based on the pressure, determination can be performed by interpretation as an index
10 of the water permeability (the easiness of passage of water) of the filtration membrane. Consequently, the point of completion of ozone treatment of the filtration membrane can be determined according to improvement in the water permeability due to progression of hydrophilization of the
15 filtration membrane. Therefore, hydrophilization potential latently belonging to the filtration membrane is maximized, and ozone treatment can be assuredly completed regardless of a variation based on an individual difference dependent on the types, the properties, or manufacturing of filtration
20 membranes.

[0043] The filtration membrane filters a treatment-target liquid from a primary side to a secondary side, and

the first supply portion is configured to either pour the ozone-containing fluid from the secondary side to
25 the primary side of the filtration membrane, or suction or

inject the ozone-containing fluid from the primary side to the secondary side of the filtration membrane. Thus, ozone treatment can be performed according to the configuration of the filtration membrane.

5 [0044] The measurement portion measures, as the measurement value, each of a first measurement value H1 after the first supply portion supplies the ozone-containing fluid for a first time period and a second measurement value H2 after the supply is performed for a second time period which
10 is longer than the first time period.

The control portion causes the first supply portion to continue the supply of the ozone-containing fluid if a change ratio α in expression 1 between the first measurement value H1 and the second measurement value H2 is equal to or
15 smaller than a threshold value α_1 , and causes the first supply portion to suppress the supply of the ozone-containing fluid if the change ratio α is larger than the threshold value α_1 .

The measurement step includes measuring each of a
20 first measurement value H1 after the ozone-containing fluid is supplied for a first time period and a second measurement value H2 after the supply is performed for a second time period which is longer than the first time period.

The control step includes: continuing the supply of
25 the ozone-containing fluid if a change ratio α in expression

1 between the first measurement value H1 and the second
measurement value H2 is equal to or smaller than a threshold
value α_1 ; and suppressing the supply of the ozone-containing
fluid if the change ratio α is larger than the threshold
5 value α_1 .

Thus, it is possible to more assuredly control
ozone treatment of the filtration membrane on the basis of a
change between the measurement values which are the first
measurement value and the second measurement value based on
10 the pressures to the filtration membrane.

[0045] The control portion causes the first supply portion
to end the supply of the ozone-containing fluid if the change
ratio α between the measurement values is larger than the
threshold value α_1 . Thus, wasteful supply of the ozone-
15 containing fluid can be reduced in ozone treatment of the
filtration membrane.

[0046] The first supply portion supplies, as the ozone-
containing fluid, at least one of ozone gas, ozone water
obtained by dissolving ozone, or ozone-mixed water obtained
20 by mixing, with ozone water, a substance that promotes
generation of radicals due to decomposition of ozone. Thus,
the filtration membrane can be assuredly subjected to ozone
treatment.

[0047] Regarding the measurement value from the
25 measurement portion, a pressure value in a pipe through which

a fluid being supplied to the filtration membrane is flowing
is measured as the measurement value, or a trans-membrane
pressure value between inside and outside of the filtration
membrane at a time of passage of the fluid through the
5 filtration membrane is measured as the measurement value.
Thus, the measurement value regarding the filtration membrane
can be assuredly measured, whereby the filtration membrane
can be assuredly subjected to ozone treatment.

[0048] The filtration membrane is formed of a material
10 that is hydrophilized by ozone, and
the control portion determines a degree of
hydrophilization of the filtration membrane on the basis of
the change in the measurement value. Thus, the degree of
hydrophilization can be determined through ozone treatment of
15 the filtration membrane according to the configuration of the
filtration membrane.

[0049] Embodiment 2

FIG. 8 and FIG. 9 are diagrams showing
configurations of filtration membrane treatment devices
20 according to embodiment 2. In the above-described embodiment
1, an example has been described in which the pressure value
of the fluid in the first pipe 7 or the trans-membrane
pressure (TMP) value of the filtration membrane 1 is used as
the measurement value H based on the pressure to the
25 filtration membrane 1. Meanwhile, in the present embodiment

2, a case will be described in which a value obtained in consideration of a flow rate value of the fluid in the first pipe 7 in addition to these measurement values is used as the measurement value H based on the pressure to the filtration
5 membrane 1.

[0050] In the drawings, the same portions as those in the above-described embodiment 1 will be denoted by the same reference characters, and description thereof is omitted. A measurement portion 8 in FIG. 8 includes: the pressure gauge
10 9; and a flowmeter 17 provided to the first pipe 7. A measurement portion 8 in FIG. 9 includes: the pressure gauge 9; and the flowmeter 17 and a thermometer 170 provided to the first pipe 7. A filtration membrane treatment method by the filtration membrane treatment devices shown in FIG. 8 and
15 FIG. 9 is performed according to the flowchart shown in FIG. 2 in the same manner as in the above-described embodiment 1. However, the filtration membrane treatment device shown in FIG. 8 according to the present embodiment 2 is different in that a value obtained by calculating the ratio between a
20 pressure value in the first pipe 7 obtained by the pressure gauge 9 and a flow rate value in the first pipe 7 obtained by the flowmeter 17, is used as the measurement value H.

[0051] That is, in the present embodiment 2, the value calculated according to the following expression 3 is used as
25 the measurement value H.

[0052] $H=Q \div P$... expression 3

H: measurement value (L/h/kPa)

Q: flow rate value (L/h)

P: pressure value (kPa) or trans-membrane pressure
5 value (kPa)

[0053] The filtration membrane treatment method is performed in the same manner as in the above-described embodiment 1 with use of this measurement value H.

[0054] If the effective area of the filtration membrane 1
10 is known, the value calculated according to the following expression 4 is used as the measurement value H.

[0055] $H=Q \div A \div P$... expression 4

A: effective area of filtration membrane 1 (m²)

[0056] The filtration membrane treatment method is
15 performed in the same manner as in the above-described embodiment 1 with use of this measurement value H.

[0057] Meanwhile, in the filtration membrane treatment device shown in FIG. 9 according to the present embodiment 2, a correction based on the temperature of the ozone-containing
20 fluid in addition to the above-described flow rate value is applied to the measurement value H. Specifically, the measurement value H obtained according to the above-described expression 3 or the above-described expression 4 is subjected to a process as in the following expression 5, whereby a
25 measurement value H' after the correction is obtained.

[0058] $H' = H \times (\mu_t \div \mu_s)$... expression 5

H' : measurement value after correction based on temperature

μ_s : viscosity value of ozone-containing fluid at
5 any reference temperature

μ_t : viscosity value of ozone-containing fluid at temperature at time of measurement of measurement value

[0059] It is noted that, in the case of using water as a solvent for ozone, the viscosity of the ozone-containing
10 fluid is equal to the viscosity of the water, and thus the publicly-known viscosities of water can be used as μ_s and μ_t .
In determining μ_s , a reference temperature needs to be arbitrarily selected but is not particularly limited. For example, the reference temperature may be set, as
15 appropriate, to any normal temperature from 15°C to 30°C.
The filtration membrane treatment method is performed in the same manner as in the above-described embodiment 1 with use of this measurement value H' .

[0060] In each filtration membrane treatment device
20 according to embodiment 2 configured as described above, the same advantageous effects as those in the above-described embodiment 1 are exhibited, as a matter of course, and in addition, regarding the measurement value from the measurement portion, a ratio between the pressure value or
25 the trans-membrane pressure value and a flow rate value of

the fluid being supplied to the filtration membrane is measured as the measurement value, and thus

a measurement value can be detected with excellent accuracy without being influenced by the flow rate of the
5 ozone-containing fluid, whereby ozone treatment of the filtration membrane can be optimally controlled.

[0061] Embodiment 3

FIG. 10 is a diagram showing a configuration of a filtration membrane treatment device according to embodiment
10 3. FIG. 11 is a flowchart of a filtration membrane treatment method by the filtration membrane treatment device shown in FIG. 10. FIG. 12 is a diagram showing a configuration of another filtration membrane treatment device according to embodiment 3. In the drawings, the same portions as those in
15 the above-described embodiments are denoted by the same reference characters, and description thereof is omitted. In the above-described embodiments, examples have been described in which the measurement value H based on the pressure to the filtration membrane 1 is measured while the ozone-containing
20 fluid is being supplied to the filtration membrane 1. Meanwhile, in the present embodiment 3, a case will be described in which, when the measurement value H based on the pressure to the filtration membrane 1 is measured, the ozone-containing fluid to the filtration membrane 1 is temporarily
25 stopped for the measurement.

[0062] In the drawings, the same portions as those in the above-described embodiments are denoted by the same reference characters, and description thereof is omitted. A second supply portion 18 which supplies a measurement fluid
5 different from the ozone-containing fluid to the filtration membrane 1, is provided. The second supply portion 18 includes a second reservoir 20 and a second pump 19. The second reservoir 20 stores the measurement fluid. As long as the measurement fluid is different from the ozone-containing
10 fluid, the measurement fluid is not particularly limited, and any fluid containing no substance that causes contamination of the filtration membrane 1 can be used. For example, use of tap water, pure water, ultrapure water, an alkaline chemical such as caustic soda, or an acidic chemical such as
15 hydrochloric acid, sulfuric acid, or citric acid, is assumed.

[0063] The second pump 19 supplies the measurement fluid from the second reservoir 20 through a fourth pipe 21 to the first pipe 7 and the filtration membrane 1. The first pipe 7 is provided with a valve 23, and the fourth pipe 21 is
20 provided with a valve 22.

[0064] When the measurement portion 8 measures the measurement value H, the control portion 11 causes the valve 23 of the first pipe 7 to close and causes the first pump 6 to stop, thereby causing the first supply portion 3 to stop
25 the supply of the ozone-containing fluid. Meanwhile, the

control portion 11 causes the valve 22 of the fourth pipe 21 to open and drives the second pump 19, thereby causing the measurement fluid to be supplied from the second reservoir 20 of the second supply portion 18 through the fourth pipe 21 to the first pipe 7 and the filtration membrane 1. When the measurement portion 8 ends measuring the measurement value H, the control portion 11 causes the valve 22 of the fourth pipe 21 to close and causes the second pump 19 to stop, thereby causing the second supply portion 18 to stop the supply of the measurement fluid. Meanwhile, the control portion 11 causes the valve 23 of the first pipe 7 to open and drives the first pump 6, thereby causing the ozone-containing fluid to be supplied from the first reservoir 5 of the first supply portion 3 through the first pipe 7 to the filtration membrane 1.

[0065] Next, the filtration membrane treatment method by the filtration membrane treatment device according to embodiment 3 configured as described above will be described with reference to the flowchart in FIG. 11. First, the control portion 11 drives the first pump 6, to perform a supply step of supplying the ozone-containing fluid from the first reservoir 5 of the first supply portion 3 through the first pipe 7 to the filtration membrane 1 (step ST11 in FIG. 11).

[0066] Then, after the supply is performed for the first

time period T1, the control portion 11 causes the first pump 6 to stop and causes the valve 23 of the first pipe 7 to close, thereby causing the supply of the ozone-containing fluid to the filtration membrane 1 to stop and interrupting the ozone treatment of the filtration membrane 1 (step ST12 in FIG. 11). Then, the control portion 11 causes the valve 22 of the fourth pipe 21 to open and drives the second pump 19, thereby causing the measurement fluid to be supplied from the second reservoir 20 of the second supply portion 18 through the fourth pipe 21 to the first pipe 7 and the filtration membrane 1. Then, the measurement step of measuring the measurement value H based on the pressure to the filtration membrane 1 is performed while the measurement fluid continues to be supplied. The measurement portion 8 measures, as the measurement value H, a first measurement value H1 after the ozone-containing fluid is supplied to the filtration membrane 1 for the first time period T1, and the measurement portion 8 sends the first measurement value H1 to the control portion 11 (step ST13 in FIG. 11).

[0067] Then, the control portion 11 causes the second pump 19 to stop and causes the valve 22 of the fourth pipe 21 to close, thereby causing the supply of the measurement fluid to the filtration membrane 1 to stop. Meanwhile, the control portion 11 drives the first pump 6, thereby causing the ozone-containing fluid to be supplied from the first

reservoir 5 of the first supply portion 3 through the first pipe 7 to the filtration membrane 1, whereby ozone treatment of the filtration membrane 1 is restarted (step ST14 in FIG. 11).

5 [0068] Then, after the supply is performed for the second time period T2, the control portion 11 causes the first pump 6 to stop and causes the valve 23 of the first pipe 7 to close, thereby causing the supply of the ozone-containing fluid to the filtration membrane 1 to stop and interrupting
10 the ozone treatment of the filtration membrane 1 (step ST15 in FIG. 11). Then, the control portion 11 causes the valve 22 of the fourth pipe 21 to open and drives the second pump 19, thereby causing the measurement fluid to be supplied from the second reservoir 20 of the second supply portion 18
15 through the fourth pipe 21 to the first pipe 7 and the filtration membrane 1.

[0069] Then, the measurement step of measuring the measurement value H based on the pressure to the filtration membrane 1 is performed while the measurement fluid continues
20 to be supplied. The measurement portion 8 measures, as the measurement value H, a second measurement value H2 after the ozone-containing fluid is supplied to the filtration membrane 1 for the second time period T2, and the measurement portion 8 sends the second measurement value H2 to the control
25 portion 11 (step ST16 in FIG. 11). Then, the control step of

adjusting the supply amount of the ozone-containing fluid on the basis of the change in the measurement value H is performed in the same manner as in the above-described embodiment 1 (step ST17 and step ST18 in FIG. 11).

5 [0070] In the above-described embodiment 3, at least the first pump 6 is stopped and the valve 23 is closed, whereby the supply of the hydrophilization fluid to the filtration membrane is stopped. In the case where, for example, ozone
10 generator 12 may be stopped, or a bypass pipe or the like may be separately provided above the first pipe 7 and flow paths may be switched so that the supply of the ozone gas to the filtration membrane 1 is temporarily interrupted.

[0071] Also in the case where the first supply portion 3
15 supplies the ozone-containing fluid from the primary side to the secondary side of the filtration membrane 1 as shown in FIG. 7 for the above-described embodiment 1, measurement with the measurement fluid from the second supply portion 18 in the above-described embodiment 3 can be performed in the same
20 manner. For example, as shown in FIG. 12, another filtration membrane treatment device according to embodiment 3 is configured by combining the configuration in FIG. 7 described in the above-described embodiment 1 and the configuration in FIG. 10 described in the present embodiment 3. That is, in
25 the same manner as in the above-described embodiment 3, the

control portion 11 causes the valve 22 of the fourth pipe 21 to open and drives the second pump 19, thereby causing the measurement fluid to be supplied from the second reservoir 20 of the second supply portion 18 through the fourth pipe 21 and the first pipe 7 to the accommodating tank 2.

[0072] Then, the measurement fluid is suctioned via the suction pump 30 from the first pipe 7 connected to the filtration membrane 1, and the measurement fluid suctioned via the suction pump 30 is discharged to outside by the first discharge portion 10. Also with this configuration, the filtration membrane treatment method can be performed in the same manner as in the above-described embodiment 3. It is noted that, in this case, the pressure value measured by the pressure gauge 9 is a negative value. However, since values with respect to pressure values are calculated with absolute values as indicated in the above-described expressions, the calculation can be performed in the same manner.

[0073] The filtration membrane treatment device according to embodiment 3 configured as described above exhibits the same advantageous effects as those in the above-described embodiments, as a matter of course, and in addition, includes

a second supply portion which supplies a measurement fluid which is different from the ozone-containing fluid to the filtration membrane, wherein at a time of measurement by the measurement

portion, the control portion causes the first supply portion to stop, causes the second supply portion to supply the measurement fluid to the filtration membrane, and causes the measurement portion to measure the measurement value.

5 Consequently, if the measurement value is measured with use of the measurement fluid, no ozone treatment is performed on the filtration membrane during the measurement since the measurement fluid is different from the ozone-containing fluid. Thus, the measurement value can be stabilized, and a
10 more accurate measurement value can be measured, whereby control of ozone treatment of the filtration membrane is further improved.

[0074] In addition, the filtration membrane filters a treatment-target liquid from a primary side to a secondary
15 side, and

the second supply portion is configured to either pour the measurement fluid from the secondary side to the primary side of the filtration membrane, or suction or inject the measurement fluid from the primary side to the secondary
20 side of the filtration membrane. Consequently, ozone treatment can be performed according to the configuration of the filtration membrane.

[0075] Embodiment 4

FIG. 13 is a diagram showing a configuration of a
25 membrane filtration device in which a filtration membrane

treatment device is used, according to embodiment 4. In the present embodiment 4, the filtration membrane 1 of any of the filtration membrane treatment devices according to the above-described embodiments is used for membrane filtration, and both filtration of a treatment-target fluid by the filtration membrane 1 and cleaning of the filtration membrane 1 can be performed. That is, if the filtration membrane 1 is contaminated by performing filtration such as waste water treatment or water cleaning treatment on the treatment-target liquid with use of the filtration membrane 1, the ozone-containing fluid is supplied to the filtration membrane 1, whereby dirt having adhered on the filtration membrane 1 can be separated and decomposed by the ozone-containing fluid. Thus, the filtration membrane 1 is hydrophilized while the filtration membrane 1 is cleaned.

[0076] As an example of this configuration, FIG. 13 shows a configuration in which the filtration membrane treatment device is incorporated in the membrane filtration device. In the drawing, the same portions as those in the above-described embodiments are denoted by the same reference characters, and description thereof is omitted. The membrane filtration device shown in FIG. 13 is, for example, a membrane separation bioreactor and includes: an aeration tank as a storage tank which stores active sludge 26; and a fifth pipe 24 through which the treatment-target fluid is

supplied to the active sludge 26 in the aeration tank 25.
The aeration tank 25 functions also as the accommodating tank
2 of the above-described filtration membrane treatment
devices. By the first discharge portion 10, an excess
5 portion of the active sludge 26 in the aeration tank 25 is
discharged. The first pipe 7 is connected to a sixth pipe
28, and the sixth pipe 28 is provided with a third pump 27 as
a transfer portion. The sixth pipe 28 is provided with a
valve 29. The third pump 27 is connected to a third
10 discharge portion 31.

[0077] Next, an operation of the membrane filtration
device according to embodiment 4 configured as described
above will be described. First, the treatment-target liquid
is supplied from the fifth pipe 24 to the aeration tank 25.
15 Then, the active sludge 26 stored in the aeration tank 25 and
the treatment-target liquid are mixed with each other.
Organic matter contained in the treatment-target liquid is
adsorbed and decomposed by the active sludge 26. At the same
time, the control portion 11 causes the valve 29 to open, and
20 the third pump 27 is driven. Then, the active sludge 26 is
filtered by the filtration membrane 1. A filtered-out fluid
obtained by the filtration is discharged through the first
pipe 7 and the sixth pipe 28 to the outside of the device by
the third discharge portion 31. At this time, the valve 23
25 of the first pipe 7 is in a closed state. The filtration

operation does not necessarily need to be continuously performed but may be intermittently performed.

[0078] If dirt such as organic matter adheres on the filtration membrane 1 in association with the filtration operation, the trans-membrane pressure value of the filtration membrane 1 increases. Ozone treatment of the filtration membrane 1 is performed by stopping the filtration operation in a case where the trans-membrane pressure value reaches a predetermined value, in a case where the filtration is performed for a predetermined time period, or at an arbitrarily-selected timing.

[0079] The control portion 11 causes the third pump 27 to stop and causes the valve 29 to close, thereby ending the filtration operation. Then, the control portion 11 causes the valve 23 of the first pipe 7 to open and drives the first pump 6, thereby causing the ozone-containing fluid to be supplied to the filtration membrane 1, whereby the filtration membrane 1 is subjected to ozone treatment. The filtration membrane treatment method can be performed in the same manner as in the above-described embodiments, and thus description thereof is omitted, as appropriate. If the ozone treatment of the filtration membrane 1 is ended, the control portion 11 causes the first pump 6 to stop and causes the valve 23 of the first pipe 7 to close, whereby the treatment of the filtration membrane is ended. Then, the control portion 11

causes the valve 29 of the sixth pipe 28 to open and drives the third pump 27, whereby filtration treatment by the filtration membrane 1 is restarted.

[0080] It is noted that ozone treatment of the filtration
5 membrane 1 does not need to be performed each time of
cleaning of the filtration membrane 1, and instead, whether
ozone treatment needs to be performed may be determined and
ozone treatment may be performed each time it is determined
that ozone treatment needs to be performed. Alternatively,
10 filtration of the active sludge 26 may be started after ozone
treatment is performed in advance before the start of
filtration of the active sludge 26.

[0081] The membrane filtration device according to
embodiment 4 configured as described above exhibits the same
15 advantageous effects as those in the above-described
embodiments, as a matter of course, and in addition,
includes:

a storage tank which stores the treatment-target
liquid and in which the filtration membrane is immersed; and
20 a transfer portion which transfers, to outside of
the storage tank, the treatment-target liquid having been
filtered by the filtration membrane, wherein

the control portion causes the transfer portion to
stop and causes the first supply portion to supply the ozone-
25 containing fluid to the filtration membrane immersed inside

the storage tank. Thus, if the filtration membrane treatment device is incorporated in the membrane filtration device for the treatment-target liquid and both filtration by the filtration membrane and cleaning and hydrophilization of the filtration membrane are performed, the cleaning of the filtration membrane can be prevented from being excessively or insufficiently performed.

[0082] Example 1

Hereinafter, Example 1 and Comparative Examples 1 and 2 will be described. Here, description will be given on the basis of results of performing ozone treatment on the filtration membrane 1 with use of the same device as the filtration membrane treatment device shown in FIG. 8. The main specifications of the filtration membrane treatment device used in the present Example 1 is as shown in the table in FIG. 14. In the present Example 1, before the start of ozone treatment, pure water was poured from the secondary side to the primary side of the filtration membrane 1 at 3(L/h), and an initial measurement value H was obtained in advance with use of expression 4 on the basis of the flow rate value of the pure water, a pressure value at this time, and the effective area of the filtration membrane 1 (membrane area). Ozone treatment was performed according to the procedure of the flowchart shown in FIG. 2.

[0083] Ozone water was started to be supplied as the

ozone-containing fluid to the filtration membrane 1 at 3(L/h). Then, a first measurement value H_1 regarding the filtration membrane 1 was measured after the elapse of 10 minutes which was the first time period T_1 . The first measurement value H_1 was calculated with use of expression 4. Then, a second measurement value H_2 was calculated after the elapse of the second time period T_2 which was 10 minutes from the elapse of the first time period T_1 . Then, a change ratio α between the first measurement value H_1 and the second measurement value H_2 was calculated on the basis of expression 1 in a first determination. Here, the threshold value α_1 was set as follows: $\alpha_1=0.2$. The change ratio α and the threshold value α_1 were compared with each other with use of expression 2.

[0084] As shown in the table in FIG. 15, the change ratio α in the first determination was 0.4 and larger than the threshold value α_1 , i.e., 0.2. Thus, the measurement value H was measured again after the elapse of 10 minutes, and a second determination was performed in the same manner as the above-described first determination. In the second determination, the second measurement value H_2 in the first determination was used as a first measurement value H_1 , and a second measurement value H_2 after the elapse of the second time period T_2 , i.e., after the elapse of 30 minutes as a cumulative treatment time period from the start of the ozone

treatment, was newly measured. The change ratio α at this time was 0.38 and larger the threshold value α_1 , i.e., 0.2. Thus, the measurement value H was measured again after the elapse of 10 minutes, and a third determination was performed in the same manner as the above-described determinations. The change ratio α in the third determination was 0.28. Thus, the measurement value H was measured again after the elapse of 10 minutes, and a fourth determination was performed in the same manner as the above-described determinations. The change ratio α in the fourth determination was 0.08 and equal to or smaller than the threshold value α_1 , i.e., 0.2. Thus, the ozone treatment was ended.

[0085] Meanwhile, in Comparative Example 1 shown in FIG. 16, the filtration membrane treatment device used in Example 1 was used, and ozone treatment of the filtration membrane was also performed under the same condition. In Comparative Example 1, a measurement value was obtained only at the time point at which 30 minutes of pouring of ozone water at 3(L/h) as ozone treatment was ended. No measurement value was measured before the time point. Meanwhile, in Comparative Example 2 shown in FIG. 16, the filtration membrane was subjected to ozone treatment with use of the filtration membrane treatment device used in Example 1. In Comparative Example 2, hydrophilization merely involved 90 minutes of

pouring of ozone water at 3(L/h), and no measurement value was measured before the elapse of 90 minutes. Each measurement value was calculated with use of expression 4 on the basis of a pressure value, a flow rate value, and the effective area of the filtration membrane in the same manner as in the above-described Example 1.

[0086] The results of Example 1 are as shown in the table in FIG. 15. The change ratio α 50 minutes after the start of the ozone treatment was smaller than the threshold value α_1 , i.e., 0.2, and the ozone treatment was completed. At this time, the measurement value had increased from 11 (L/m²/h/kPa) which was an initial measurement value to 33.3 (L/m²/h/kPa). Thus, it can be confirmed that ozone treatment was sufficiently performed and hydrophilization was promoted.

[0087] Meanwhile, the results of Comparative Examples 1 and 2 are as shown in the table in FIG. 16. In Comparative Example 1, the measurement value in ozone treatment is 23 (L/m²/h/kPa). Since the measurement value in Example 1 is 33 (L/m²/h/kPa), ozone treatment was stopped while there was room for ozone treatment, in Comparative Example 1.

[0088] Meanwhile, in Comparative Example 2, the measurement value is 33.6 (L/m²/h/kPa), and ozone treatment is considered to have been sufficient. However, this measurement value is hardly different from the final measurement value in Example 1 in which ozone treatment was

performed for 50 minutes. That is, 50 minutes is sufficient for ozone treatment of the filtration membrane 1 used in the present Example 1 and Comparative Example 2. Thus, performing ozone treatment for 90 minutes as in Comparative
5 Example 2 is uneconomical and inefficient.

[0089] As described above, it has been confirmed that: the present filtration membrane treatment method allows finding of a point at which ozone treatment of the filtration membrane is completed; and hydrophilization of the filtration
10 membrane can be assuredly completed by minimum necessary ozone treatment. Judging from the above, the superiority of the present example is obvious.

[0090] Although the disclosure is described above in terms of various exemplary embodiments and implementations, it
15 should be understood that the various features, aspects and functionality described in one or more of the individual embodiments are not limited in their applicability to the particular embodiment with which they are described, but instead can be applied, alone or in various combinations to
20 one or more of the embodiments of the disclosure.

It is therefore understood that numerous modifications which have not been exemplified can be devised without departing from the scope of the specification of the present disclosure. For example, at least one of the
25 constituent parts may be modified, added, or eliminated. At

least one of the constituent parts mentioned in at least one of the preferred embodiments may be selected and combined with the constituent parts mentioned in another preferred embodiment.

5

DESCRIPTION OF THE REFERENCE CHARACTERS

	[0091]	1	filtration membrane
		2	accommodating tank
		3	first supply portion
10		30	suction pump
		4	liquid
		5	first reservoir
		50	first reservoir
		6	first pump
15		7	first pipe
		8	measurement portion
		9	pressure gauge
		10	first discharge portion
		11	control portion
20		12	ozone gas generator
		13	second pipe
		14	second discharge portion
		15	adding portion
		16	third pipe
25		17	flowmeter

	170	thermometer
	18	second supply portion
	19	second pump
	20	second reservoir
5	21	fourth pipe
	22	valve
	23	valve
	24	fifth pipe
	25	aeration tank
10	26	active sludge
	27	third pump
	28	sixth pipe
	29	valve
	30	suction pump
15	31	third discharge portion
	H	measurement value
	H'	measurement value
	H1	first measurement value
	H2	second measurement value
20	T1	first time period
	T2	second time period

CLAIMS

[1] A filtration membrane treatment device which performs ozone treatment on a filtration membrane, the filtration membrane treatment device comprising:

5 a first supply portion which supplies an ozone-containing fluid to the filtration membrane;

a measurement portion which measures a measurement value based on a pressure to the filtration membrane; and

10 a control portion which adjusts, on the basis of a change in the measurement value measured by the measurement portion, a supply amount of the ozone-containing fluid to be supplied by the first supply portion.

[2] The filtration membrane treatment device according to claim 1, wherein

the filtration membrane filters a treatment-target liquid from a primary side to a secondary side, and

20 the first supply portion is configured to either pour the ozone-containing fluid from the secondary side to the primary side of the filtration membrane, or suction or inject the ozone-containing fluid from the primary side to the secondary side of the filtration membrane.

[3] The filtration membrane treatment device according to claim 1 or 2, further comprising a second supply portion

which supplies a measurement fluid which is different from the ozone-containing fluid to the filtration membrane, wherein

at a time of measurement by the measurement
5 portion, the control portion causes the first supply portion to stop, causes the second supply portion to supply the measurement fluid to the filtration membrane, and causes the measurement portion to measure the measurement value.

10 [4] The filtration membrane treatment device according to claim 3, wherein

the filtration membrane filters a treatment-target liquid from a primary side to a secondary side, and

the second supply portion is configured to either
15 pour the measurement fluid from the secondary side to the primary side of the filtration membrane, or suction or inject the measurement fluid from the primary side to the secondary side of the filtration membrane.

20 [5] The filtration membrane treatment device according to any one of claims 1 to 4, wherein

the measurement portion measures, as the measurement value, each of a first measurement value H1 after the first supply portion supplies the ozone-containing fluid
25 for a first time period and a second measurement value H2

after the supply is performed for a second time period which is longer than the first time period, and

the control portion

causes the first supply portion to continue the
5 supply of the ozone-containing fluid if a change ratio α in the following expression 1 between the first measurement value H1 and the second measurement value H2 is larger than a threshold value α_1 , and

causes the first supply portion to suppress the
10 supply of the ozone-containing fluid if the change ratio α is equal to or smaller than the threshold value α_1 ,

$$|H1-H2| \div |H1| = \alpha \cdots \text{expression 1.}$$

[6] The filtration membrane treatment device according
15 to claim 5, wherein the control portion causes the first supply portion to end the supply of the ozone-containing fluid if the change ratio α between the measurement values is larger than the threshold value α_1 .

20 [7] The filtration membrane treatment device according to any one of claims 1 to 6, wherein the first supply portion supplies, as the ozone-containing fluid, at least one of ozone gas, ozone water obtained by dissolving ozone, or ozone-mixed water obtained by mixing, with ozone water, a
25 substance that promotes generation of radicals due to

decomposition of ozone.

[8] The filtration membrane treatment device according to any one of claims 1 to 7, wherein

5 regarding the measurement value from the measurement portion,

a pressure value in a pipe through which a fluid being supplied to the filtration membrane is flowing is measured as the measurement value,

10 a trans-membrane pressure value between inside and outside of the filtration membrane at a time of passage of the fluid through the filtration membrane is measured as the measurement value, or

a ratio between the pressure value or the
15 trans-membrane pressure value and a flow rate value of the fluid being supplied to the filtration membrane is measured as the measurement value.

[9] The filtration membrane treatment device according to any one of claims 1 to 8, wherein

the filtration membrane is formed of a material that is hydrophilized by ozone, and

the control portion determines a degree of hydrophilization of the filtration membrane on the basis of
25 the change in the measurement value.

[10] A membrane filtration device which treats a treatment-target liquid with use of the filtration membrane treatment device according to any one of claims 1 to 9, the
5 membrane filtration device comprising:

a storage tank which stores the treatment-target liquid and in which the filtration membrane is immersed; and

a transfer portion which transfers, to outside of the storage tank, the treatment-target liquid having been
10 filtered by the filtration membrane, wherein

the control portion causes the transfer portion to stop and causes the first supply portion to supply the ozone-containing fluid to the filtration membrane immersed inside the storage tank.

15

[11] A filtration membrane treatment method comprising:

a supply step of supplying an ozone-containing fluid to a filtration membrane;

a measurement step of measuring a measurement value
20 based on a pressure to the filtration membrane; and

a control step of adjusting a supply amount of the ozone-containing fluid on the basis of a change in the measurement value.

25 [12] The filtration membrane treatment method according

to claim 11, wherein

the measurement step includes measuring each of a first measurement value H1 after the ozone-containing fluid is supplied for a first time period and a second measurement value H2 after the supply is performed for a second time period which is longer than the first time period, and

the control step includes:

continuing the supply of the ozone-containing fluid if a change ratio α in the following expression 1 between the first measurement value H1 and the second measurement value H2 is larger than a threshold value α_1 ; and

suppressing the supply of the ozone-containing fluid if the change ratio α is equal to or smaller than the threshold value α_1 ,

$|H1-H2| \div |H1| = \alpha \cdots \text{expression 1.}$