

PARAFFINIC PRODUCTS, A METHOD FOR PRODUCING PARAFFINIC PRODUCTS AND A USE OF PARAFFINIC PRODUCTS

FIELD OF THE INVENTION

5 The present invention relates to an electrotechnical composition comprising paraffin fractions obtained from renewable raw materials, to a method for producing said composition and to a use of said composition.

BACKGROUND

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Liquid or gaseous electrotechnical fluids are used in electrical apparatuses such as transformers, capacitors, switchgears, bushings, etc. Electrotechnical fluids typically act as an electrically insulating medium separating the high voltage and grounded parts within the apparatus and
15 functioning as a cooling medium to transfer the heat generated in the apparatus. In addition to the above mentioned basic function the electrotechnical fluid should comply with other necessary and desired requirements such as long operational life time, operation in wide range of temperatures, suitable kinematic viscosity and minimal environmental impact.

20 There is a growing end need for sustainable, biosourced and recycled alternatives in the field of electrotechnical fluids.

In the electrotechnical fluids segment, there is a clear end user need to develop solutions that offer low conductivity combined with other improved characteristics. Current solutions do not typically meet the criteria.

25 WO2014128227 discloses a renewable hydrocarbon based insulating fluid which comprises more than 70 % isoparaffins. This disclosure does not teach how to produce a fluid which meets the required performance or the composition of a fluid which meets the required performance.

WO2018078024 discloses an electrotechnical fluid for an electric
30 vehicle, having a boiling point in the range of from 200 °C to 400 °C and a boiling range below 80 °C, said fluid comprising more than 95% isoparaffins and less than 3% naphthens by weight, a biocarbon content of at least 95% by weight, containing less than 100ppm aromatics by weight. This disclosure does not teach how to produce a fluid which meets the required performance or the
35 composition of a fluid which meets the required performance.

SUMMARY

An object of the present invention is to provide a hydrocarbon composition which is suitable as electrotechnical fluid and which alleviates the disadvantages discussed above. The present invention also relates to a method
5 of making an electrotechnical fluid having low conductivity combined with other improved characteristics. In addition, the invention relates to the use of an electrotechnical fluid.

More specifically the composition according to present invention comprises more than 90 wt-% paraffins in the C17-C18 range, based on the total
10 weight of the composition, wherein the ratio of the amount of C18 i-paraffins to the amount of C18 n-paraffins is more than 40, based on the weight of the C18 i-paraffins and the weight of the C18 n-paraffins in the composition.

The experimental part shows surprisingly good properties of the electrotechnical fluid according to present invention.

15 DETAILED DESCRIPTION OF EMBODIMENTS

The following embodiments are exemplary. Although the specification may refer to “an”, “one”, or “some” embodiment(s) in several locations, this does not necessarily mean that each such reference is to the same embodiment(s), or that the feature only applies to a single embodiment.
20 Single features of different embodiments may also be combined to provide other embodiments. Furthermore, words “comprising”, “containing” and “including” should be understood as not limiting the described embodiments to consist of only those features that have been mentioned and such embodiments may contain also features/structures that have not been specifically mentioned.

25 All standards referred herein are the latest revisions available, unless otherwise mentioned.

The present invention relates to a paraffinic hydrocarbon product which has surprisingly good performance as an electrotechnical fluid.

The present invention discloses a method for production of an
30 electrotechnical fluid, an electrotechnical fluid and use of an electrotechnical fluid. More specifically, the present invention discloses a method for production of electrotechnical fluid comprising hydrodeoxygenation and isomerization of renewable feedstock to obtain a renewable paraffinic feed; and

35 subjecting the obtained renewable paraffinic feed to at least one separation, or fractionation, process to recover a hydrocarbon composition

having a boiling range within a range from about 275 °C to about 300 °C (EN ISO3405:2011), preferably within a range from about 280 °C to about 300 °C, which is useful as an electrotechnical fluid. The present invention discloses also uses of the electrotechnical fluid.

5 The renewable paraffinic feed may be obtained by hydrodeoxygenation and isomerization of renewable (biosourced) raw material. The renewable paraffinic feed thus obtained has a carbon number distribution in the range of C8-C22 or C10 to C20, preferably in the range of C15 to C18, and a boiling range within 140 °C–340 °C, preferably within a range of 180 °C–
10 320 °C. The renewable paraffinic feed comprises mainly n-paraffins and i-paraffins.

In an embodiment, the renewable paraffinic feed for the separation/fractionation is provided by catalytic hydrotreatment and catalytic isomerization of renewable raw material.

15 In another embodiment, the hydrotreatment is catalytic hydrodeoxygenation.

In another embodiment, the separation process comprises distillation.

20 The boiling range covers a temperature interval from the initial boiling point, IBP, defined as the temperature at which the first drop of distillation product is obtained, to a final boiling point, FBP, when the highest-boiling compounds evaporate.

EN ISO 3405:2011 and ASTM D86:2015 standards "Standard Test Method for Distillation of Petroleum Products and Liquid Fuels at Atmospheric
25 Pressure", as well as ASTM D7345:2017 standard "Standard Test Method for Distillation of Petroleum Products and Liquid Fuels at Atmospheric Pressure (Micro Distillation Method)" describe a distillation method for measuring the boiling point distribution of liquid fuel products having boiling range within a range from 0 °C to 400 °C (ASTM D7345: 20°C to 400°C). Using ASTM D86 or
30 ASTM D7345, boiling points are measured at 25 vol-% distilled. The points may also be reported at 88% distilled.

Description of the process

35 By the term "hydrotreatment" is meant a catalytic process of organic material by all means of molecular hydrogen. Preferably, hydrotreatment removes oxygen from organic oxygen compounds as water i.e. by

hydrodeoxygenation (HDO). Additionally/alternatively, hydrotreatment may remove sulphur from organic sulphur compounds as dihydrogen sulphide (H_2S), i.e. by hydrodesulphurisation, (HDS), remove nitrogen from organic nitrogen compounds as ammonia (NH_3), i.e. by hydrodenitrofication (HDN), and/or
5 remove halogens, for example chlorine, from organic chloride compounds as hydrochloric acid (HCl), i.e. by hydrodechlorination (HDCI).

By the term "hydrodeoxygenation" (HDO), of for example triglycerides or other fatty acid derivatives or fatty acids, is meant the removal of for example carboxyl oxygen as water by means of molecular hydrogen under the influence
10 of a catalyst.

Reaction conditions and catalysts suitable for the hydrodeoxygenation of renewable raw material and the isomerization of resultant n-paraffins are known. Examples of such processes are presented in FI100248, Examples 1–3, and in WO 2015/101837 A2.

15 By the term "deoxygenation" is meant removal of oxygen from organic molecules, such as fatty acid derivatives, alcohols, ketones, aldehydes and/or ethers, by any means previously described, or decarboxylation or decarbonylation.

20 Renewable raw material

Renewable raw material (or renewable oil and/or fat) refers to a feedstock derived from a biological raw material component containing oils and/or fats, usually containing lipids (e.g. fatty acids or glycerides), such as plant oil/fats, vegetable oil/fats, animal oil/fats, fish oil/fats and algae oil/fats, or oil/fats
25 from other microbial processes, for example, genetically manipulated algae oil/fats, genetically manipulated oil/fats from other microbial processes and also genetically manipulated vegetable oil/fats. Components or derivatives of such materials may also be used, for example, alkyl esters (typically C1-C5 alkyl esters, such as methyl, ethyl, propyl, iso-propyl, butyl, sec-butyl esters) or
30 olefins. Renewable specifically excludes fossil sources, however recycled fossil material may be utilized.

The renewable oils and/or fats may include a single kind of oil, a single kind of fat, mixtures of different oils, mixtures of different fats, mixtures of oil(s) and fat(s), fatty acids, glycerol, and/or mixtures of the afore-mentioned.

35 These oils and/or fats typically comprise C10-C24 fatty acids and derivatives thereof, including esters of fatty acids, glycerides, i.e. glycerol esters

of fatty acids. The glycerides may specifically include monoglycerides, diglycerides and triglycerides.

Carbon atoms of renewable or biological origin comprise a higher number of unstable radiocarbon (^{14}C) atoms compared to carbon atoms of fossil origin. Therefore, it is possible to distinguish between carbon compounds derived from renewable or biological sources or raw material and carbon compounds derived from fossil sources or raw material by analysing the ratio of ^{12}C and ^{14}C isotopes. Thus, a particular ratio of said isotopes can be used as a “tag” to identify renewable carbon compounds and differentiate them from non-renewable carbon compounds. The isotope ratio does not change in the course of chemical reactions. Examples of a suitable method for analysing the content of carbon from biological or renewable sources are DIN 51637 (2014), ASTM D6866 (2020) and EN 16640 (2017). As used herein, the content of carbon from biological or renewable sources is expressed as the biogenic carbon content meaning the amount of biogenic carbon in the material as a weight percent of the total carbon (TC) in the material (in accordance with ASTM D6866 (2020) or EN 16640 (2017)).

Feedstock or raw material of biological origin means material having typically only biogenic carbon content.

Typically hydrocarbons made from 100% palm oil have a biogenic carbon content of about 100 wt-%.

Typically hydrogenated animal fat has a biogenic carbon content of about 100 wt-%.

Typically fossil crude oil based diesel fuel has a biogenic carbon content of about 0 wt-%.

In an embodiment the biogenic carbon content of the feedstock or renewable raw material, or a renewable paraffinic feed obtainable therefrom, is more than 50 wt-%, preferably the biogenic carbon content is more than 90 wt-% and most preferably the biogenic carbon content is more than 99 wt-%.

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Renewable paraffinic feed and preparation thereof

The preparation of a renewable paraffinic feed often involves reactions removing oxygen from the renewable feedstock, and there are a number of strategies for doing this. The deoxygenation may comprise one or more of following reactions:

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1) hydrodeoxygenation (HDO), hydrogenation of oxygen bonds – removing oxygen as H₂O,

2) decarboxylation where oxygen is removed in the form of CO₂, and

3) decarbonylation where oxygen is removed in the form of CO.

5 Process conditions for hydrodeoxygenation are known in the art. For example, the hydrodeoxygenation of renewable raw material may be carried out on a metal sulphide catalyst. The metal may be one or more Group VI metals, such as Mo or W, or one or more Group VIII non-noble metals such as Co or Ni. The catalyst may be supported on any convenient support, such as alumina,
10 silica, zirconia, titania, amorphous carbon, molecular sieves or combinations thereof. Usually the metal is impregnated or deposited on the support as metal oxides. They are then typically converted into their sulphides. Examples of typical catalysts for hydrodeoxygenation are molybdenum containing catalysts, NiMo, CoMo, or NiW catalysts, supported on alumina or silica, but many other
15 hydrodeoxygenation catalysts are known in the art, and have been described together with or compared to NiMo and/or CoMo catalysts. The hydrodeoxygenation is preferably carried out under the influence of sulphided NiMo or sulphided CoMo catalysts in the presence of hydrogen gas.

 The hydrodeoxygenation may be performed under a hydrogen
20 pressure from 10 to 200 barg (bar gauge), at temperatures from 200 °C to 400 °C, and liquid hourly space velocities of 0.2 h⁻¹ to 10 h⁻¹. During the hydrodeoxygenation step using a sulfided catalyst, the sulfided state of the catalyst may be maintained by the addition of sulphur in the gas phase or by using a feedstock having sulphur containing mineral oil blended with the
25 renewable feedstock. The sulphur content of the total feed being subjected to hydrodeoxygenation may be, for example, in the range of 50 wppm (ppm by weight) to 20 000 wppm, preferably in the range of 100 wppm to 1000 wppm.

 Effective conditions for hydrodeoxygenation may reduce the oxygen content of the feedstock to less than 1 wt-%, such as less than 0.5 wt-% or less
30 than 0.2 wt-%. In some cases, the conditions may be selected to yield partial hydrodeoxygenation corresponding to a deoxygenation of at least 40 wt-%, at least 50 wt-% or at least 75 wt-%.

 The renewable paraffinic feed usable in the present invention may be provided by isomerizing a hydrotreated renewable raw material obtained from
35 the renewable raw material. Generally, the renewable paraffinic feed may be produced from the renewable raw material using any known method. Specific

examples of a method for producing the renewable paraffinic feed are provided in the European patent application EP 1741768 A1. Also other methods may be employed, particularly another BTL (Biomass-To-Liquid) method may be chosen, for example biomass gasification followed by a Fischer-Tropsch method.

In a preferred embodiment, preparing a renewable paraffinic feed from a renewable raw material comprises subjecting the renewable raw material to a deoxygenation treatment. Most renewable raw materials comprise materials having a high oxygen content. In one embodiment, the renewable feedstock comprises fatty acids, or fatty acid derivatives, such as triglycerides, or a combination thereof.

In the present invention, the deoxygenating method is not particularly limited and any suitable deoxygenating method may be employed. Suitable methods are, for example, hydrotreatment, such as hydrodeoxygenation (HDO), catalytic hydrodeoxygenation (catalytic HDO), catalytic cracking (CC), or a combination thereof. Other suitable methods include decarboxylation and decarbonylation reactions, either alone or in combination with hydrotreatment.

In a preferred embodiment, the deoxygenation treatment, to which the renewable raw material is subjected, is hydrotreatment. Preferably, the renewable raw material is subjected to hydrodeoxygenation (HDO) which preferably uses a HDO catalyst. Catalytic HDO is the most common way of removing oxygen and has been extensively studied and optimized. However, the present invention is not limited thereto. As the HDO catalyst, a HDO catalyst comprising hydrogenation metal supported on a carrier may be used. Examples include a HDO catalyst comprising a hydrogenation metal selected from a group consisting of Pd, Pt, Ni, Co, Mo, Ru, Rh, W, or a combination of these. Alumina or silica is suited as a carrier, among others. The hydrodeoxygenation step may, for example, be conducted at a temperature of 100-500 °C and at a pressure of 10-150 bar (absolute).

Preparing a hydrotreated raw material from the renewable raw material may comprise a step of hydrocracking hydrocarbons in the renewable hydrocarbon raw material. Thus, the chain length of the renewable hydrocarbon raw material may be adjusted and the product distribution of the produced mixture of biohydrocarbons can be indirectly controlled.

Isomerization treatment

The renewable paraffinic feed of the present invention may be provided by subjecting at least straight chain hydrocarbons in the hydrotreated raw material to an isomerization treatment to prepare the renewable paraffinic feed. The renewable paraffinic feed and its preparation is described above.

The isomerization treatment causes branching of hydrocarbon chains, i.e. isomerization, of the hydrotreated raw material. Branching of hydrocarbon chains improves cold properties, i.e. the isomeric composition formed by the isomerization treatment has better cold properties compared to the hydrotreated raw material.

The isomerization step may be carried out in the presence of an isomerization catalyst, and optionally in the presence of hydrogen added to the isomerisation process. Suitable isomerisation catalysts contain a molecular sieve and/or a metal selected from Group VIII of the periodic table and optionally a carrier. Preferably, the isomerization catalyst contains SAPO-11, or SAPO-41, or ZSM-22, or ZSM-23, or ferrierite, and Pt, Pd, or Ni, and Al_2O_3 , or SiO_2 . Typical isomerization catalysts are, for example, Pt/SAPO-11/ Al_2O_3 , Pt/ZSM-22/ Al_2O_3 , Pt/ZSM-23/ Al_2O_3 , and Pt/SAPO-11/ SiO_2 . The catalysts may be used alone or in combination. The presence of added hydrogen is particularly preferable to reduce catalyst deactivation. In a preferred embodiment, the isomerization catalyst is a noble metal bifunctional catalyst, such as Pt-SAPO and/or Pt-ZSM-catalyst, which is used in combination with hydrogen. The isomerization step may, for example, be conducted at a temperature of 200-500 °C, preferably 280-400 °C, and at a pressure of 10-150 bar, preferably 30-100 bar (absolute). The isomerization step may comprise further intermediate steps such as a purification step and a fractionation step. The isomerization may be performed e.g. at 300 °C to 350 °C.

Incidentally, the isomerization treatment is a step which predominantly serves to isomerize the hydrotreated raw material. That is, while most thermal or catalytic conversions (such as HDO) result in a minor degree of isomerization (usually less than 5 wt-%), the isomerization step which may be employed in the present invention is a step which leads to a significant increase in the content of isoparaffins.

Thus the renewable raw material may be subjected at least to a hydrodeoxygenation reaction in the presence of hydrogen and a hydrodeoxygenation catalyst and optionally to an isomerisation reaction in the

presence of an isomerisation catalyst, for obtaining the renewable paraffinic feed. When a hydrodeoxygenation step and an isomerisation step are applied, these may be performed either simultaneously or in sequence. The hydrodeoxygenation reaction may be performed in the presence of hydrogen gas and a hydrodeoxygenation catalyst, such as CoMo, NiMo, NiW, CoNiMo, on a support, for example, an alumina support, zeolite support, or a mixed support. The hydrodeoxygenation reaction may, for example, be conducted at a temperature in the range from 250 to 400 °C, and at a pressure in the range from 20 to 80 barg, at a WHSV (weight hourly space velocity, i.e. mass flow/catalyst mass) in the range from 0.5 to 3 h⁻¹, and a H₂/oil ratio of 350-900 nl/l, using a catalyst, such as NiMo, optionally on an alumina support.

The product of the hydrodeoxygenation step, i.e. the hydrotreated renewable raw material, may be subjected to an isomerization step in the presence of hydrogen and an isomerization catalyst. The isomerisation catalyst may be a noble metal bifunctional catalyst such as Pt-SAPO or Pt-ZSM catalyst or NiW. The isomerization reaction may, for example, be conducted at a temperature of 250-400 °C and at a pressure of 10-60 barg. The isomerisation reaction may, for example, be conducted at a temperature of 250-400 °C, at a pressure of between 10 and 60 barg, at a WHSV of 0.5-3 h⁻¹, and at a H₂/oil ratio of 100-800 nl/l.

The hydrodeoxygenation and hydroisomerisation steps may be carried out in a single step on the same catalyst bed using a single catalyst for this combined step, e.g. NiW, or a Pt catalyst, such as Pt/SAPO in a mixture with a Mo catalyst on a support, e.g. NiMo on alumina.

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Fractionation step

Any known separation / fractionation method, or combination thereof, may be used in the production of an electrotechnical fluid composition according to the present invention from the renewable paraffinic feed to recover a hydrocarbon composition having a boiling range within a range from about 275 °C to about 300 °C (EN ISO3405:2011), preferably within a range from about 280 °C to about 300 °C. Exemplary boiling ranges include about 275 °C to about 300 °C, and about 280 °C to about 300 °C (EN ISO3405:2011). Preferably the separation is selected so that a majority of the C18 normal paraffins end up in the residue, and majority of the C18 i-paraffins end up in the recovered hydrocarbon composition. By selecting the final boiling point in this way, it is

possible to control the viscosity of the recovered hydrocarbon composition. Also the amount of impurities may be reduced as they typically concentrate in the heavier hydrocarbon bottom.

5 In one embodiment an electrotechnical fluid composition is produced by subjecting the renewable paraffinic feed to at least one separation process comprising distillation.

In one embodiment the initial boiling point of the electrotechnical fluid composition, IBP, is about 275 °C and preferably about 280 °C and the final boiling point, FBP, is about 300 °C (EN-ISO3405:2011).

10 In one embodiment the process comprises two or more separation steps.

Selection of renewable feedstock regarding favourable characteristics, such as selecting a renewable feedstock having a high amount of compounds having carbon chain length longer than or equal to C16, may be used to increase the yield of the electrotechnical fluid composition.

The yield of electrotechnical fluid composition may be increased also by the selection of the process conditions in the renewable paraffinic feed production process.

15 In an embodiment an electrotechnical fluid composition comprises more than 90 wt-% paraffins in the C17-C18 range, based on the total weight of the composition, wherein the ratio of the amount of C18 i-paraffins to the amount of C18 n-paraffins is more than 40, based on the weight of the C18 i-paraffins and the weight of the C18 n-paraffins in the composition. This composition has surprisingly good performance. The high share of C17-C18 paraffins increases the flash point of the composition, while the high weight ratio of C18 i-paraffins to C18 n-paraffins provides lower viscosity and thus better fluidity, this combination ensuring safe use in broad range of different electrotechnical fluid applications, over a wide temperature range. The better fluidity ensures e.g. more efficient heat transfer which improves for example efficiency of transformers and decreases their operating temperature, which in turn allows higher power output. Also risk of local hot spots is reduced, thereby improving life-time of the electrotechnical fluid, and safety. More efficient cooling may also allow smaller transformer designs reducing cost and need for space.

20 In one embodiment the electrotechnical fluid composition comprises less than 95 wt-% paraffins in C17- C18 range, based on the total weight of the composition. This composition denotes good performance.

In one embodiment the electrotechnical fluid composition has a total isoparaffinic content of more than 90 wt-%, based on the total weight of the composition. This improves cold performance, including enhanced fluidity at low temperatures.

5 In one embodiment the electrotechnical fluid composition has a pour point less than -50 °C, preferably less than -55 °C, more preferably less than -60 °C or less than -65°C (ASTMD5950).

In one embodiment the electrotechnical fluid composition comprises less than 2 wt-% C15 and lighter paraffins and less than 2 wt-% C20 and heavier
10 paraffins, based on the total weight of the composition. This composition denotes good performance.

In one embodiment the electrotechnical fluid composition has a flash point of at least 135 °C, preferably at least 140 °C, more preferably at least 145 °C (ENISO2719:2016).

15 In one embodiment the electrotechnical fluid composition comprises at most 2 wt-% C19 paraffins, such as between 1 wt-% and 2 wt-% C19 paraffins, based on the total weight of the composition. This composition denotes good performance.

In one embodiment the electrotechnical fluid composition comprises
20 at most 10 wt-% C16 paraffins, such as between 2 wt-% and 10 wt-% C16 paraffins, preferably at most 6 wt-% C16 paraffins, such as between 2 wt-% and 6 wt-% C16 paraffins, based on the total weight of the composition. This composition denotes good performance.

In one embodiment the electrotechnical fluid composition comprises
25 more than 37 wt-% C17 paraffins, based on the total weight of the composition. This composition denotes good performance.

In one embodiment the electrotechnical fluid composition comprises less than 42 wt-% C17 paraffins, based on the total weight of the composition. This composition denotes good performance.

30 In one embodiment the electrotechnical fluid composition comprises more than 45 wt-%, preferably more than 48 wt-%, more preferably more than 50 wt-% C18 paraffins, based on the total weight of the composition. This composition denotes good performance.

In one embodiment the electrotechnical fluid composition comprises
35 less than 57 wt-% C18 paraffins, based on the total weight of the composition. This composition denotes good performance.

In preferred embodiments the electrotechnical fluid composition comprises more than 90 wt-% paraffins in the C17-C18 range, based on the total weight of the composition, wherein the ratio of the amount of C18 i-paraffins to the amount of C18 n-paraffins is more than 40, based on the weight of the C18 i-paraffins and the weight of the C18 n-paraffins in the composition, and more than 45 wt-%, preferably more than 48 wt-%, more preferably more than 50 wt-% C18 paraffins, based on the total weight of the composition.

In one embodiment the ratio of the amount of C17 i-paraffins to the amount of C17 n-paraffins is more than 20, and preferably less than 30, based on the weight of the C17 i-paraffins and the weight of the C17 n-paraffins in the composition. This composition denotes good performance.

In one embodiment the electrotechnical fluid composition comprises 0.01-1 wt-% aromatics, preferably 0.01-0.5 wt-% aromatics, based on the total weight of the composition. This denotes good performance.

In one embodiment the electrotechnical fluid composition comprises 3-4 wt-% C16 i-paraffins, 35-40 wt-% C17 i-paraffins, 50-55 wt-% C18 i-paraffins, 1-3 wt-% C19 i-paraffins, 0.1-1 wt-% C16 n-paraffins, 0.5-2 wt-% C17 n-paraffins, 0.5-2 wt-% C18 n-paraffins and 0.01-1 wt-% C19 n-paraffins, based on the total weight of the composition. This denotes good performance.

In one embodiment the total isoparaffinic content of the composition is more than 90 wt-% and less than 98 wt-%, based on the total weight of the composition. This denotes good performance, especially in terms of reduced viscosity or enhanced fluidity, over a broad temperature range.

In one embodiment the ratio of the amount of C18 i-paraffins to the amount of C18 n-paraffins is between 42 and 47, based on the weight of the C18 i-paraffins and the weight of the C18 n-paraffins in the composition. This denotes good performance.

In one embodiment a conductivity at 22 °C (ISO6297:1997) is less than 1 pS/m and NOACK150 (ASTMD5800-15a B) is 8.5 wt-% or less. This denotes good performance.

In one embodiment the electrotechnical fluid composition has a density at 20 °C (EN ISO12185) between 782 and 784 kg/m³, and a cloud point (ASTMD7689:2017) lower than -32 °C. This denotes good performance.

In one embodiment the electrotechnical fluid composition has a biogenic carbon content more than 50 wt-%, preferably a biogenic carbon

content more than 90 wt-% and most preferably a biogenic carbon content more than 99 wt-%. This reflects the origin of the raw material.

Preferably the electrotechnical fluid composition is classified as readily biodegradable according to OECD Test Guideline 301 F.

5 In one embodiment the electrotechnical fluid composition meets at least one specification defined in Table 2 General Specifications of standard IEC 60296:2012. In some embodiments the electrotechnical fluid composition may meet even all of the specifications defined in Table 2 General Specifications of standard IEC 60296:2012.

10 In some embodiments the electrotechnical fluid composition may further comprise one or more additives, for example selected from antioxidant additives, metal passivators, pour point depressants, additives decreasing gassing tendency, and any other additives commonly used in electrochemical fluids.

15 In one embodiment a method of producing an electrotechnical fluid composition, comprising:

 conducting at least one hydrodeoxygenation reaction and at least one isomerization reaction of a renewable raw material to obtain a renewable paraffinic feed; and

20 subjecting the renewable paraffinic feed to at least one separation process to recover a hydrocarbon composition having a boiling range within a range from about 275 °C to about 300 °C (EN ISO3405:2011) preferably within a range from about 280 °C to about 300 °C . Preferably the recovered hydrocarbon composition has a boiling range from about 275 °C to about 300 °C (EN ISO3405:2011), more preferably from about 280 °C to about 300 °C.

25 In one embodiment any of above mentioned compositions is used in an electrical device.

 In one embodiment any of above mentioned compositions is used as a battery coolant, an insulating oil or a cable oil.

30 In one embodiment any of above mentioned compositions is used as an electric vehicle battery coolant.

 In one embodiment any of above mentioned compositions is used as transformer oil or as a component of transformer oil.

35 In one embodiment any of above mentioned compositions is used as a server farm coolant.

The embodiments of the present disclosure may be combined, in whole or in part, with each other to form further embodiment(s) of the present disclosure. Further, the particular features or characteristics illustrated or described in connection with various embodiments may be combined, in whole or in part, with the features or characteristics of one or more other embodiments without limitation. Such modifications and variations are intended to be included within the scope of the present disclosure. A composition, a method or a use, to which the present disclosure is related, may comprise at least one of the embodiments of the present disclosure described in this specification.

EXAMPLE 1 (COMPARATIVE)

Table 1 summarizes physical and chemical properties of the composition of Example 1 (Comparative).

Table 2 summarizes carbon number distribution of the composition of Example 1 (Comparative)

The sample composition of Example 1 was produced by hydrodeoxygenation and isomerization of feedstock of renewable origin as explained above. The isomerization step was followed by a distillation step to recover a hydrocarbon composition having an initial boiling point (IBP) 275.4 °C and a final boiling point (FBP) 321.0 °C.

The carbon number distribution of the composition of Example 1 is presented in table 2. The composition comprises 96.05 % i-paraffins and 3.95 % n-paraffins. 97.19 wt-% of all paraffins are in the C16-C20 range. The ratio of the amount of C18 i-paraffins to the amount of C18 n-paraffins is 31.9 based on the weight of the C18 i-paraffins and the weight of the C18 n-paraffins in the composition.

As can be seen in table 1, conductivity of the composition is 161 pS/m, which means that the composition is not suitable for certain electrotechnical applications.

Table 1. Physical and chemical properties of a composition according to Example 1 (Comparative)

Method	Property	Unit	
PHYSICAL & CHEMICAL PROPERTIES			
ENISO12185	DENSITY	kg/m ³	787,6
ENISO12185	DENS20°C	kg/m ³	784,1
ISO2049	COLOUR		L 0,5
ASTMD4176-1	APPEARANCE		CLEAR
ENISO2592	Flash point-COC	°C	146
ENISO2719	Flash point-PM	°C	125
EN14522	AUTOIGNITION TEMP	°C	211
IP529	Freezing point -AUT	°C	-26
ASTMD7689	Cloud point-EXACT	°C	-31
ASTMD5950	Pour point-ISL	°C	-48
ENISO20846	SULPHUR	mg/kg	<1
ENISO12937	WATER	mg/kg	18
ENISO2160	Copper Corrosion 3H/50°C	no	1a
EN12662	SEDIMENT-TOT	mg/kg	6,5
ISO2977	ANILINEPOINT	°C	100,3
ASTMD1133	KAURIBUTANOL		18,5
ASTMD1218	Refractive index-20		1,4395
UOP495	AROMATICS	wt-%	0,37
ASTMD3242	ACIDITY-TAN	mg KOH/g	0,001
ISO6297	CONDUCTIVITY at 22oC	pS/m	161
IP387	FBT		6,83
NM490A	N-PARAFFINS	wt-%	3,95
ASTMD5800-B	NOACK150	wt-%	8,6
ASTMD971M	SURFACE-TENSION	mN/m	27
ASTMD971	INTERFAC-TENSION	mN/m	46
ASTMD971	TEMPERATURE	°C	25

VISCOSITY			
ENISO3104	VISCO100C	mm ² /s	1
ENISO3104	VISCO40C	mm ² /s	4
ENISO3104	VISCO20C	mm ² /s	6
ENISO3104	VISCO10°C	mm ² /s	9
ENISO3104	VISCO-0C	mm ² /s	12
ENISO3104	VISCO-10	mm ² /s	18
ENISO3104	VISCO-20C	mm ² /s	30
ENISO3104	VISCO-30C	mm ² /s	55
METALS			
NM534	BORON	mg/kg	<1
NM534	SODIUM	mg/kg	<0,10
NM534	MAGNESIUM	mg/kg	<0,10
NM534	ALUMINIUM	mg/kg	<0,10
NM534	SILICON	mg/kg	0,19
NM534	PHOSPHOROUS	mg/kg	<0,10
NM534	POTASSIUM	mg/kg	0,23
NM534	CALCIUM	mg/kg	<0,10
NM534	TITANIUM	mg/kg	<0,10
NM534	VANADINIUM	mg/kg	<0,10
NM534	CHROMIUM	mg/kg	<0,10
NM534	MANGANESE	mg/kg	<0,10
NM534	IRON	mg/kg	<0,10
NM534	NICKEL	mg/kg	<0,10
NM534	COPPER	mg/kg	<0,10
NM534	ZINC	mg/kg	<0,10
NM534	MOLYBDENIUM	mg/kg	<0,10
NM534	CADMIUM	mg/kg	<0,10
NM534	TIN	mg/kg	<0,10
NM534	BARIUM	mg/kg	<0,10
NM534	LEAD	mg/kg	<0,10

DISTILLATION			
ENISO3405	DIS-IBP	°C	275,4
ENISO3405	DIS-05	°C	291,7
ENISO3405	DIS-10	°C	292,2
ENISO3405	DIS-20	°C	292,8
ENISO3405	DIS-30	°C	293,2
ENISO3405	DIS-40	°C	293,7
ENISO3405	DIS-50	°C	294,2
ENISO3405	DIS-60	°C	294,7
ENISO3405	DIS-70	°C	295,5
ENISO3405	DIS-80	°C	296,7
ENISO3405	DIS-90	°C	299,4
ENISO3405	DIS-95	°C	306,5
ENISO3405	DIS-FBP	°C	321
ENISO3405	DIS-RECOVERY	vol-%	97,2

Table 2. Carbon number distribution of the composition of Example 1 (comparative)

Carbon number	i-paraffins	n-paraffins	Total paraffins
3	0,00	0,00	0,00
4	0,00	0,00	0,00
5	0,00	0,00	0,00
6	0,00	0,00	0,00
7	0,05	0,03	0,08
8	0,08	0,02	0,10
9	0,04	0,01	0,05
10	0,03	0,00	0,03
11	0,02	0,00	0,02
12	0,01	0,00	0,01
13	0,01	0,00	0,01
14	0,01	0,00	0,01
15	0,30	0,08	0,38
16	4,01	0,12	4,12
17	33,31	1,91	35,22
18	51,62	1,62	53,24
19	3,05	0,08	3,13
20	1,44	0,04	1,48
21	0,47	0,02	0,49
22	0,24	0,01	0,25
23	0,12	0,00	0,13
24	0,07	0,00	0,07
25-29	0,78	0,00	0,78
30-36	0,39	0,00	0,39
>C36	0,00	0,00	0,00
Total paraffins	96,05	3,95	100,00

5

EXAMPLE 2

Table 3 summarizes physical and chemical properties of the composition of Example 2.

Table 4 summarizes the carbon number distribution of the composition of Example 2.

The sample composition of Example 2 was produced by conducting a distillation step to the sample composition of Example 1 to recover a hydrocarbon composition having an initial boiling point (IBP) 283.5 °C and final boiling point (FBP) 298.5 °C.

The carbon number distribution of the composition of Example 2 is presented in Table 4. The composition comprises 96.75 % i-paraffins and 3.25 % n-paraffins. 99.08 wt-% of all the paraffins are in the C16-C19 range. The ratio of the amount of C18 i-paraffins to the amount of C18 n-paraffins is 45.52 based on the weight of the C18 i-paraffins and the weight of the C18 n-paraffins in the composition.

The composition comprises 0.31 wt-% C15 and lighter paraffins and 0.62 wt-% C20 and heavier paraffins.

Table 3 summarizes physical and chemical properties of the composition of Example number 2. As can be seen from table 1, conductivity of this composition is less than 1 pS/m, which means that the composition is suitable for various electrotechnical applications. Surprisingly, even the composition of Example 2 comprises lighter paraffins compared to the composition of comparative example 1, and the volatility (NOACK150) of the composition of Example 2 is less than the volatility of the composition of comparative Example 1.

This surprising performance is the result of the distillation final boiling point selection, so that the majority of C18 normal paraffins of the composition of Example 2 have ended up in the distillation residue, as can be seen from table 4. By selecting the distillation final boiling point as described above, also the low temperature performance of the product has been substantially improved. The viscosity of the product also fulfils the requirements on such products.

Additionally biodegradability of the composition was tested according to OECD Test Guideline 301 F, and the composition was found readily biodegradable.

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Table 3. Physical and chemical properties of a composition according to Example 2

PHYSICAL & CHEMICAL PROPERTIES			
ENISO12185	DENSITY	kg/m ³	786,6
ENISO12185	DENS20°C	kg/m ³	783,2
ISO2049	COLOUR		L 0,5
ASTMD4176-1	APPEARANCE		C&B
ENISO2592	Flash point-COC	°C	149
ENISO2719	Flash point-PM	°C	145
EN14522	AUTOIGNITION TEMP	°C	211
IP529	Freezing point -AUT	°C	-22
ASTMD7689	Cloud point-EXACT	°C	-34
ASTMD5950	Pour point-ISL	°C	-69
ENISO20846	SULPHUR	mg/kg	<1
ENISO12937	WATER	mg/kg	17
ENISO2160	Copper Corrosion 3H/50°C	no	1a
EN12662	SEDIMENT-TOT	mg/kg	
ISO2977	ANILINEPOINT	°C	99,9
ASTMD1133	KAURIBUTANOL		18,5
ASTMD1218	Refractive index-20		1,4391
UOP495	AROMATICS	wt-%	0,04
ASTMD3242	ACIDITY-TAN	mg KOH/g	<0,001
ISO6297	CONDUCTIVITY at 22°C	pS/m	<1
IP387	FBT		1,01
NM490A	N-PARAFFINS	wt-%	3,25
ASTMD5800-B	NOACK150	wt-%	8,4
ASTMD971M	SURFACE-TENSION	mN/m	27
ASTMD971	INTERFAC-TENSION	mN/m	51
ASTMD971	TEMPERATURE	°C	25

VISCOSITY			
ENISO3104	VISCO100C	mm ² /s	1
ENISO3104	VISCO40C	mm ² /s	4
ENISO3104	VISCO20C	mm ² /s	6
ENISO3104	VISCO10°C	mm ² /s	8
ENISO3104	VISCO-0C	mm ² /s	12
ENISO3104	VISCO-10	mm ² /s	18
ENISO3104	VISCO-20C	mm ² /s	29
ENISO3104	VISCO-30C	mm ² /s	52
METALS			
NM534	BORON	mg/kg	<1
NM534	SODIUM	mg/kg	<0,10
NM534	MAGNESIUM	mg/kg	<0,10
NM534	ALUMINIUM	mg/kg	<0,10
NM534	SILICON	mg/kg	<0,10
NM534	PHOSPHOROUS	mg/kg	<0,10
NM534	POTASSIUM	mg/kg	<0,10
NM534	CALCIUM	mg/kg	<0,10
NM534	TITANIUM	mg/kg	<0,10
NM534	VANADINIUM	mg/kg	<0,10
NM534	CHROMIUM	mg/kg	<0,10
NM534	MANGANESE	mg/kg	<0,10
NM534	IRON	mg/kg	<0,10
NM534	NICKEL	mg/kg	<0,10
NM534	COPPER	mg/kg	<0,10
NM534	ZINC	mg/kg	<0,10
NM534	MOLYBDENIUM	mg/kg	<0,10
NM534	CADMIUM	mg/kg	<0,10
NM534	TIN	mg/kg	<0,10
NM534	BARIUM	mg/kg	<0,10
NM534	LEAD	mg/kg	<0,10

DISTILLATION			
ENISO3405	DIS-IBP	°C	283,5
ENISO3405	DIS-05	°C	291,1
ENISO3405	DIS-10	°C	291,5
ENISO3405	DIS-20	°C	291,9
ENISO3405	DIS-30	°C	292,2
ENISO3405	DIS-40	°C	292,3
ENISO3405	DIS-50	°C	292,6
ENISO3405	DIS-60	°C	293,1
ENISO3405	DIS-70	°C	293,6
ENISO3405	DIS-80	°C	294,2
ENISO3405	DIS-90	°C	295,2
ENISO3405	DIS-95	°C	296,4
ENISO3405	DIS-FBP	°C	298,5
ENISO3405	DIS-RECOVERY	vol-%	98

Table 4. Carbon number distribution of the composition of Example 2

Carbon number	i-paraffins	n-paraffins	Total paraffins
3	0,00	0,00	0,00
4	0,00	0,00	0,00
5	0,00	0,00	0,00
6	0,00	0,00	0,00
7	0,00	0,00	0,00
8	0,00	0,00	0,00
9	0,00	0,00	0,00
10	0,00	0,00	0,00
11	0,00	0,00	0,00
12	0,00	0,00	0,00
13	0,00	0,00	0,00
14	0,01	0,00	0,02
15	0,22	0,08	0,29
16	3,66	0,42	4,08
17	37,42	1,51	38,93
18	53,27	1,17	54,44
19	1,58	0,04	1,63
20	0,45	0,03	0,48
21	0,10	0,00	0,10
22	0,03	0,00	0,04
23	0,00	0,00	0,00
24	0,00	0,00	0,00
25-29	0,00	0,00	0,00
30-36	0,00	0,00	0,00
>C36	0,00	0,00	0,00
Total paraffins	96,75	3,25	100,00

5 It will be obvious to a person skilled in the art, as the technology advances, that the inventive concept of the present invention can be implemented in various ways. The invention and its embodiments are not limited to the examples described above but may vary within the scope of the claims.

Claims

1. An electrotechnical fluid composition, comprising:
more than 90 wt-% paraffins in the C17- C18 range, based on the total weight
5 of the composition,
wherein the ratio of the amount of C18 i-paraffins to the amount of C18 n-
paraffins is more than 40, based on the weight of the C18 i-paraffins and the
weight of the C18 n-paraffins in the composition.
- 10 2. The electrotechnical fluid composition according to claim 1, wherein the
composition comprises less than 95 wt-% paraffins in C17- C18 range, based
on the total weight of the composition.
- 15 3. The electrotechnical fluid composition according to claim 1 or 2, wherein the
total isoparaffinic content of the composition is more than 90 wt-%, based on
the total weight of the composition.
- 20 4. The electrotechnical fluid composition according to any of claims 1-3,
wherein the composition comprises less than 2 wt-% C15 and lighter paraffins
and less than 2 wt-% C20 and heavier paraffins, based on the total weight of
the composition.
- 25 5. The electrotechnical fluid composition according to any of claims 1-4,
wherein the composition has a flash point according to ENISO2719:2016 of at
least 135 °C, preferably at least 140 °C, more preferably at least 145 °C.
- 30 6. The electrotechnical fluid composition according to any of claims 1-5,
wherein the composition comprises more than 37 wt-% C17 paraffins and/or
comprises less than 42 wt-% C17 paraffins, based on the total weight of the
composition.
- 35 7. The electrotechnical fluid composition according to any of claims 1-6,
wherein the composition comprises more than 45 wt-%, preferably more than
48 wt-%, more preferably more than 50 wt-% C18 paraffins and/or comprises
less than 57 wt-% C18 paraffins, based on the total weight of the composition.

8. The electrotechnical fluid composition according to any of claims 1-7, wherein the ratio of the amount of C17 i-paraffins to the amount of C17 n-paraffins is more than 20, and preferably less than 30, based on the weight of the C17 i-paraffins and the weight of the C17 n-paraffins in the composition.
- 5 9. The electrotechnical fluid composition according to any of claims 1-8, wherein the composition comprises 0.01-1 wt-% aromatics, preferably 0.01-0.5 wt-% aromatics, based on the total weight of the composition.
- 10 10. The electrotechnical fluid composition according to any of claims 1-9, wherein the composition comprises 3-4 wt-% C16 i-paraffins, 35-40 wt-% C17 i-paraffins, 50-55 wt-% C18 i-paraffins, 1-3 wt-% C19 i-paraffins, 0.1-1 wt-% C16 n-paraffins, 0.5-2 wt-% C17 n-paraffins, 0.5-2 wt-% C18 n-paraffins and 0.01-1 wt-% C19 n-paraffins, based on the total weight of the composition.
- 15 11. The electrotechnical fluid composition according to any of claims 1-10, wherein the total isoparaffinic content of the composition is less than 98 wt-%, based on the total weight of the composition.
- 20 12. The electrotechnical fluid composition according to any of claims 1-11, wherein the ratio of the amount of C18 i-paraffins to the amount of C18 n-paraffins is between 42 and 47, based on the weight of the C18 i-paraffins and the weight of the C18 n-paraffins in the composition.
- 25 13. The electrotechnical fluid composition according to any of claims 1-12, wherein the conductivity according to ISO6297:1997 at 22 °C is less than 1 pS/m and NOACK150 according to ASTM D5800-B is 8.5 wt-% or less.
- 30 14. The electrotechnical fluid composition according to any of claims 1-13, wherein the density according to EN ISO12185 at 20 °C is between 782 and 784 kg/m³, and the cloud point according to ASTM D7689:2017 is lower than -32 °C.
- 35 15. The electrotechnical fluid composition according to any of claims 1-14, wherein the composition has a biogenic carbon content of more than 50 wt-%, preferably more than 90 wt-%, and most preferably more than 99 wt-%.

16. A method of producing an electrotechnical fluid composition according to any of claims 1-15, comprising:
- 5 conducting at least one hydrodeoxygenation reaction and at least one isomerization reaction of a renewable raw material to obtain a renewable paraffinic feed; and
- 10 subjecting the renewable paraffinic feed to at least one separation process to recover a hydrocarbon composition having a boiling range according to EN ISO3405:2011 within a range from 275 °C to 300 °C, preferably within a range from about 280 °C to 300 °C.
17. Use of an electrotechnical fluid composition according to any of claims 1-15 in an electrical device, preferably as a battery coolant, an insulating oil, a cable oil, an electric vehicle battery coolant, transformer oil or as a component
- 15 of transformer oil, or as a server farm coolant.