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TRANSPORT OF SOLUTIONS OF CELLULOSE THROUGH PIPES

This invention relates to the transport of solutions of cellulose in a tertiary amine N-oxide, in particular N-methylmorpholine N-oxide, through pipes.

5 It is known that cellulose fibre can be made by extrusion of a solution of cellulose in a suitable solvent into a coagulating bath. One example of such a process is described in US Patent 4,416,698 (McCorsley III), the contents of which are incorporated herein by way of reference. Cellulose is
10 dissolved in a solvent containing a tertiary amine N-oxide (which may also be called for brevity an amine oxide), for example N-methylmorpholine N-oxide (NMMO). The solvent may also contain a proportion of a non-solvent for cellulose, for example water. The resulting solution is extruded through a
15 suitable die to produce filaments, which are coagulated, washed in water to remove the solvent, and dried. This process of extrusion and coagulation is referred to as "solvent-spinning", and the cellulose fibre produced thereby is referred to as "solvent-spun" cellulose fibre. It is also
20 known that cellulose fibre can be made by extrusion of a solution of a cellulose derivative into a regenerating and coagulating bath. One example of such a process is the viscose process, in which the cellulose derivative is cellulose xanthate. Solvent-spinning has a number of
25 advantages over other known processes for the manufacture of cellulose fibre such as the viscose process, for example reduced environmental emissions.

US Patent 4,416,698 describes a method of preparing a solution of cellulose in a tertiary amine N-oxide and a method
30 for preparing a shaped article such as a fibre from such a solution. A mixture of the tertiary amine N-oxide containing the preferred amount of water and the cellulose are ground to the same predetermined particle size and charged simultaneously to the barrel of an extruder. The preferred
35 temperature range in the barrel of the extruder for processing

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the mixture of cellulose and solvent thereby dissolving the cellulose is from about 90°C to about 140°C. Degradation of the cellulose can be avoided or substantially reduced by dissolving the cellulose in the barrel of the extrusion
5 apparatus, extruding the solution to form a film or filament and promptly precipitating the cellulose before degradation of the cellulose.

US Patent 4,426,228 (Brandner et al), the contents of which are incorporated herein by way of reference, describes
10 a solution of cellulose in a solvent which is a tertiary amine N-oxide optionally mixed with a non-solvent for the cellulose and a method of preparing the same. The solution may contain up to 25% by weight of the non-solvent, for example water. The solution additionally comprises an additive which limits
15 polymer decomposition at elevated temperatures so that the solution is only slightly coloured and cellulose articles made there from exhibit improved properties such as strength. One example of such an additive is propyl gallate used at 0.01 to 5% by weight relative to the solvent. US Patent 4,426,228
20 also describes a method of preparing such a solution in which the cellulose and the solvent are processed at temperatures between 70°C and 190°C until the cellulose has been dissolved. A solution containing 5 to 8% by weight cellulose is particularly appropriately prepared by processing at
25 temperatures between 70°C and 100°C. In order to hold the processing time as low as possible and to attain high production rates, temperatures between 100°C and 150°C or between 115°C and 130°C may be used.

It is known that the solutions of cellulose in a tertiary
30 amine N-oxide exhibit high viscosity, particularly those solutions which contain more than about 10% by weight, for example 10 to 25% by weight, cellulose. Solutions containing such relatively high concentrations of cellulose are desirably used in the commercial manufacture of fibre and film both to
35 reduce processing costs and in particular because extrusion of such solutions leads to the production of fibre and film

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with improved physical properties, for example tensile strength. It is also known that the viscosity of such solutions decreases as their temperature is raised. It is therefore desirable to transport such solutions at high temperature in order to reduce the pumping costs associated with transporting high viscosity solutions.

It is also known that solutions of cellulose in a tertiary amine N-oxide such as NMMO are liable to degradation when stored at elevated temperatures. Such solutions may become discoloured when stored at temperatures above about 130°C. It is also known that uncontrolled exothermic reaction may occur when such solutions are stored at temperatures above about 170°C. It has further been observed that such uncontrolled exothermic reaction may occur even when such solutions are stored for extended periods of time at temperatures considerably below 170°C. This fact has hampered the commercial development and utilisation of solvent-spinning processes, because the risk of uncontrolled exothermic reaction is not acceptable in industrial-scale plant. The risk has previously been minimised on the laboratory or pilot plant scale by extruding the solution immediately after its preparation, so minimising the time during which the solution is stored. However, this solution is less than satisfactory for industrial-scale production, both because it is desirable to submit the solution to intermediate processing operations such as filtration between preparation and extrusion, and because it is not possible to assemble the elements of industrial-scale plant in as close a spatial relationship as the elements of laboratory or pilot plant apparatus.

The invention provides in a first aspect a method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of the solution in the centre of the pipe being controlled at no more than

1000 / (X + 0.19 x $\sqrt{D}$),

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where D represents the internal diameter of the pipe in millimetres and X represents a numerical value. The value of X may be equal to or greater than 5.0, in preferred embodiments of the invention the value of X is 5.25 or 5.75, 5 and in a particularly preferred embodiment the value of X is 5.5. If the internal diameter of the pipe is measured in inches the value 0.19 in the above-noted expression should be replaced by 0.98.

The invention further provides in a second aspect a 10 method for transporting a solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of the solution at the interior wall of the pipe being controlled at no more than

$$1000 / (Y + 0.23 \times \sqrt{D}),$$

15 where D represents the internal diameter of the pipe in millimetres and Y represents a numerical value. The value of Y may be equal to or greater than 5.4, in preferred embodiments of the invention the value of Y is 5.65 or 6.15, and in a particularly preferred embodiment the value of Y is 20 5.9. If the internal diameter of the pipe is measured in inches, the value 0.23 in the above-noted expression should be replaced by 1.15.

The solution of cellulose in N-methylmorpholine N-oxide may be referred to hereinafter alternatively as the "dope".

25 The dope may for example comprise by weight 10 to 25%, preferably 13 to 17%, cellulose and 7 to 13% water, with the balance being largely NMMO. The dope preferably contains an additive which limits polymer decomposition at elevated temperatures, as described for example in US Patent 4,426,228, 30 for example propyl gallate. The dope preferably contains 0.01 to 0.5%, more preferably 0.05 to 0.2%, by weight propyl gallate. It has been found that the presence of such an additive increases the temperature at which the dope may be



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stored and transported without undergoing exothermic decomposition by several degrees Centigrade, for example by 5 to 10°C.

Use of the value 5.5 for X or of the value 5.9 for the value Y is believed to give a safety margin of at least about 10°C between the temperature of the dope in the centre of the pipe and the temperature at which spontaneous exothermic decomposition may occur during operation when the dope contains an additive as hereinbefore described.

10 The pipe is generally at least 0.5 or 1 inch (12.5 or 25 mm) in external diameter, preferably at least 2, 3 or 4 inches (50, 75 or 100 mm) in external diameter. The pipe may be up to 12 inches (300 mm) in external diameter, but is generally no more than 10 or 8 inches (250 or 200 mm) in external
15 diameter. Pipes of 6 inches (150 mm) external diameter may also be used. Pipes of 4 to 8 inches (100 to 200 mm) external diameter may be preferred. It will be noted that the equations defined in the methods of the invention relate the temperature of the dope to the internal diameter of the pipe,
20 whereas the preceding numbers refer to the nominal external diameter of the pipe. Pipework is generally specified and sold commercially by reference to its nominal external diameter.

The flow rate of the dope through the pipe may be for
25 example in the range 0.1 to 10 m/min, preferably 1 to 5 m/min.

The methods of the invention have been found to be generally less satisfactory for vessels of large diameter than for pipes of about 12 inches (300 mm) diameter or below, for example filters and tanks having internal diameters in the
30 range about 20 to about 40 inches (500 mm to 1000 mm). Such filters and tanks may in general be operated at a temperatures several degrees above those according to the method of the invention, at least during continuous operation.

The temperature of the dope in the pipe both at the wall of the pipe and in the centre of the pipe may be controlled by equipping the pipe with a thermostatic jacket, for example a hollow jacket containing a circulating heat transfer fluid 5 such as water. The temperature of the thermostatic jacket is generally maintained below the temperature of the dope at the centre of the pipe to provide some external cooling and thereby remove any heat generated by any exothermic reaction which may take place in the dope. The temperature of the 10 thermostatic jacket is essentially the same as that of the dope at the wall of the pipe. It has been found that slow exothermic reaction may take place in dope stored at temperatures considerably below 170°C, the temperature in which spontaneous decomposition is known to occur. Use of 15 such external cooling means is therefore preferred. It will be understood from the above that the value of Y is generally higher than the value of X. In particular it may be preferred that the value of (Y-X) is about 0.4. The temperature of the dope in the centre of the pipe is generally about 10 to about 20 15°C, preferably about 11 to about 14°C, higher than the temperature of the dope at the wall of the pipe, although it will be understood that this preferred temperature difference is to some extent dependent on the internal diameter of the pipe. The temperature of the dope may be controlled by 25 suitably varying the flow rate or the temperature of the heat transfer fluid acting as cooling medium.

The minimum temperature of the dope in the centre of the pipe is preferably at least 100°C, more preferably at least 105°C. It has been found that the viscosity of the dope is 30 sufficiently low for the dope to be pumped through pipes in a commercial scale factory when it has at least such a minimum temperature. A dope containing about 15% by weight cellulose may exhibit a viscosity of about 2000 Pa.s (20,000 poise) at a shear rate of 1 sec⁻¹ at 100°C, 1500 Pa.s (15,000 poise) at 35 110°C and 1000 Pa.s (10,000 poise) at 120°C. The first aspect of the invention provides for a dope temperature in the sensor of the pipe which may be 105°C or higher for all pipe sizes



up to at least about 12 inches (300 mm) internal diameter. The preferred temperature of the dope in the centre of the pipe is between the minimum and maximum temperatures hereinbefore mentioned.

5 Processing of cellulose and solvent to dissolve the cellulose may provide dope at a higher temperature than that required by the methods of the invention, and in such a case the hot dope may be cooled to the desired temperature shortly after dissolution by passage through a suitable heat
10 exchanger. It may be desired to extrude the dope to form fibre or film at a higher temperature than that required by the methods of the invention, for example to obtain optimum tensile properties, and in such a case the dope can be warmed to the desired temperature shortly before extrusion by passage
15 through a suitable heat exchanger. One example of a suitable type of heat exchanger is a shell-and-tube heat exchanger in which the dope passes through the tubes, the tubes being equipped with static mixers which serve to mix the dope and so improve the efficiency of the heat exchange, and the heat
20 transfer medium passes through the shell, as available for example from Kenics Corporation. Another example of a suitable type of heat exchanger consists of a chamber containing a sinuous tube, the heat transfer medium passing through the sinuous tube, and the dope passing through the
25 chamber over the tube, as available for example from Gebrueder Sulzer Ag under the Trade Mark "Sulzer SMR".

Use of the methods of the invention permits solvent-spinning of cellulose to be carried out safely on the industrial scale. The methods of the invention have the
30 advantage that additional process items, for example filters, mixers and buffer tanks, can be interposed between the dissolution apparatus and the extrusion apparatus. They have the further advantage that pipes containing dope do not need to be emptied if dope transport is stopped for any reason, for
35 example to allow plant maintenance such as filter changes. The dope in the pipe is advantageously cooled to lower

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temperature, for example around 80°C, during such a stoppage by circulation of cool heat transfer fluid through the thermostatic jacket. The dope so cooled can be warmed to the required temperature for transport after the stoppage by 5 increasing the temperature of the heat transfer fluid. Nevertheless, such additional process items are preferably emptied during such a stoppage and refilled afterwards.

Practical experience and experiment bears out the value of the methods of the invention, in particular in reducing the 10 occurrence of uncontrolled exothermic reaction to an acceptably very low value. This is especially remarkable in that the equations upon which they rely they have no apparent theoretical basis. In particular, it is surprising that they should involve the square root of a linear dimension, namely 15 the internal diameter of the pipe, rather than either the dimension itself or its square or cube, which are proportional to surface area and volume respectively.

The invention will now be more particularly explained with reference to the accompanying drawing, in which:

20 Figure 1 is a graph of $1000/T$ against $\sqrt{D}$, where T is dope temperature in °C and D is the internal pipe diameter, and

Figure 2 is a graph of T against D , where T and D have the same meanings as in Figure 1.

25 Referring to Figure 1, line 1 corresponds to the equation

$$1000/T = 5.5 + 0.98 \times \sqrt{D}$$

representing the relationship between a preferred maximum temperature of the dope in the centre of the pipe and the internal diameter of the pipe. Line 2 corresponds to the 30 equation

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$$1000/T = 5.9 + 1.15 \times \sqrt{D}$$

representing the relationship between a preferred maximum temperature of the dope at the wall of the pipe and the internal diameter of the pipe. Line 3 corresponds to 105°C, which is a preferred minimum temperature for the dope in the centre of the pipe. The data points represented by squares correspond to dope temperature in the centre of the pipe and the data points represented by crosses to dope temperature at the wall of the pipe as recorded in Table 1 below:

Table 1

<u>D inches</u>	<u>Centre °C</u>	<u>Wall °C</u>
2	146	133
3	140	127
4	133	121
6	125.5	114
8	121	109
10	117	105

The data points in Table 1 have been determined empirically to provide a safety margin of at least 10°C between the dope temperature in the centre of the pipe and the temperature at which spontaneous exothermic reaction may take place when the dope contains about 0.05 to about 0.2% by weight propyl gallate. It will be observed that the agreement between the relevant equations and the data points is excellent.

Referring to Figure 2, line 1 relates dope temperature in the centre of the pipe to internal pipe diameter when $X = 5.5$, line 2 relates dope temperature at the wall of the pipe to internal pipe diameter when $Y = 5.9$, and line 3 corresponds to 105°C. The data points of Table 1 are represented by squares and crosses as in Figure 1.

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CLAIMS

1. A method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of said solution
5 in the centre of said pipe being controlled at

$$1000 / (X + 0.19 \times \sqrt{D}),$$

where D represents the internal diameter of said pipe in millimetres and X represents a value equal to or greater than 5.0.

10 2. A method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of said solution at the interior wall of said pipe being controlled at

$$1000 / (Y + 0.23 \times \sqrt{D}),$$

15 where D represents the internal diameter of said pipe in millimetres and Y represents a value equal to or greater than 5.4.

3. A method according to claim 1, wherein X represents a value equal to or greater than 5.25.

20 4. A method according to claim 1, wherein X represents a value equal to or greater than 5.5.

5. A method according to claim 2, wherein Y represents a value equal to or greater than 5.65.

25 6. A method according to claim 2, wherein Y represents a value equal to or greater than 5.9.

7. A method according to any one of the preceding claims, wherein said solution comprises 10 to 25 percent by weight cellulose and 7 to 13 percent by weight water.

30 8. A method according to any one of the preceding claims, wherein said solution comprises an additive which



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limits decomposition at elevated temperatures.

9. A method according to claim 8, wherein said additive is propyl gallate at a concentration of 0.05 to 0.2 percent by weight.

5 10. A method according to any one of the preceding claims, wherein the nominal external diameter of said pipe is at least 50 mm.

11. A method according to claim 10, wherein the nominal external diameter of said pipe is no more than 300 mm.

10 12. A method according to claim 10, wherein the nominal external diameter of said pipe is in the range 100 to 200 mm.

13. A method according to any one of the preceding claims, wherein the temperature of said solution in said centre of the pipe is at least 100°C.

15 14. A method according to claim 13, wherein the temperature of said solution in said centre of the pipe is at least 105°C.

15 15. A method according to any one of the preceding claims, wherein the temperature of said solution in said centre of said pipe is 10 to 15°C higher than the temperature of said solution at said interior wall of said pipe.

16. A method according to any one of the preceding claims, wherein said pipe is equipped with a thermostatic jacket.

25 17. A method according to claim 16, wherein said thermostatic jacket is a hollow jacket through which water is circulated.

18. A method according to any one of the preceding



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claims, wherein the flow rate of said solution of cellulose through said pipe is in the range 0.1 to 10 m/min.

19. A method according to claim 18, wherein the flow rate of said solution of cellulose through said pipe is in the range 1 to 5 m/min.

20. A method of manufacturing a shaped cellulosic product which includes the steps of dissolving cellulose in an aqueous N-methylmorpholine N-oxide to form a solution, transporting the solution through at least one pipe and passing the solution into a coagulation bath to form the shaped cellulosic product, characterised in that the solution is transported through the pipe in accordance with the method of any one of the preceding claims.

21. A method as claimed in claim 20, characterised in that the shaped cellulosic product is a cellulosic fibre.

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ABSTRACT

A method for transporting a solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees centigrade of said solution in the centre of said pipe being controlled at $1000/(X + 0.19 \times \sqrt{D})$ and/or the temperature of said solution at the interior wall of said pipe being controlled at $1000/(Y + 0.23 \times \sqrt{D})$ where D represents the internal diameter of the pipe in millimetres, X represents a value equal to or greater than 5.0, and Y represents a value equal to or greater than 5.4.

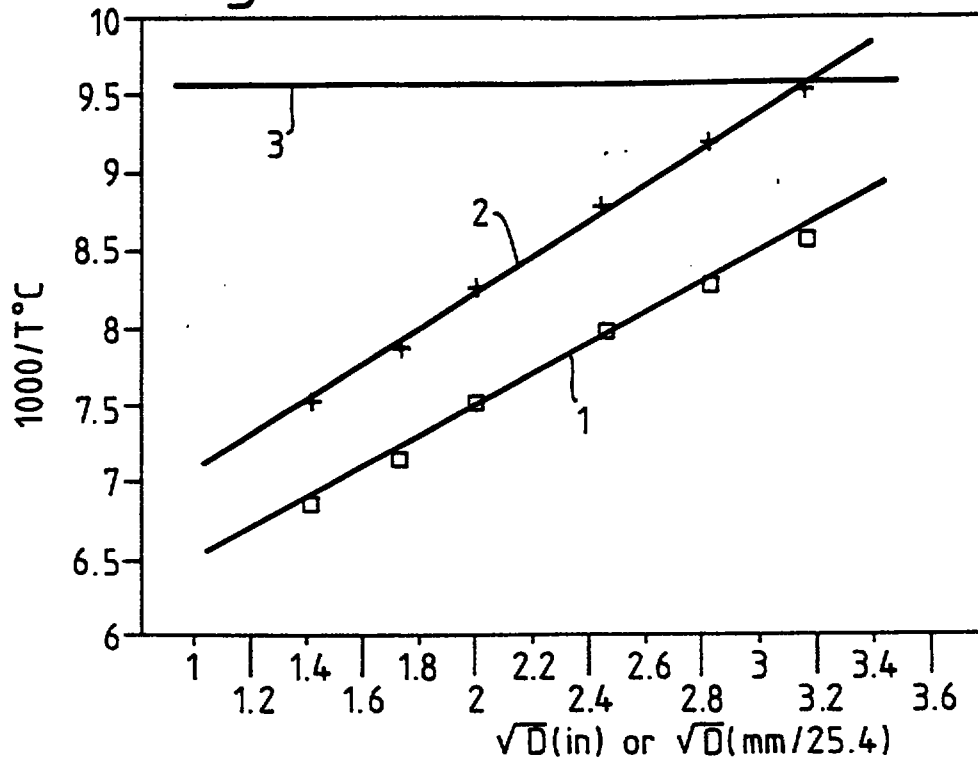
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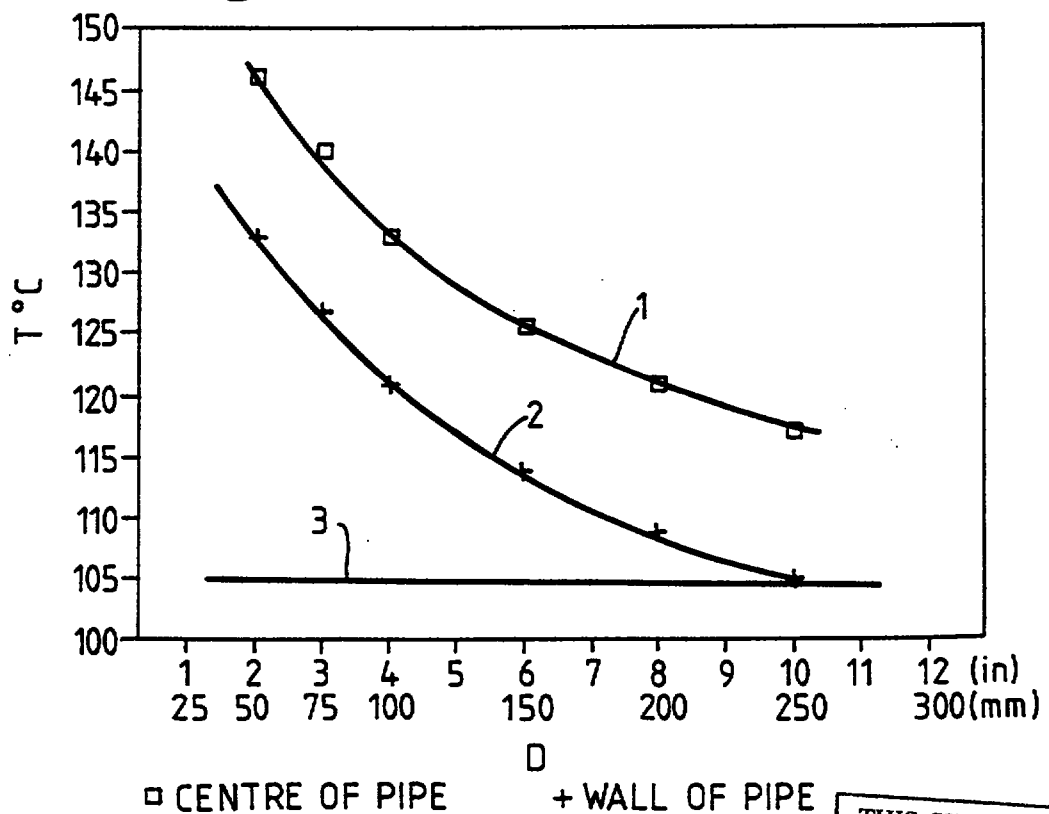
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Fig. 1.



□ CENTRE OF PIPE + WALL OF PIPE

Fig. 2.



□ CENTRE OF PIPE + WALL OF PIPE

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TRANSPORT OF SOLUTIONS OF CELLULOSE THROUGH PIPES

This invention relates to the transport of solutions of cellulose in a tertiary amine N-oxide, in particular N-methylmorpholine N-oxide, through pipes.

5 It is known that cellulose fibre can be made by extrusion of a solution of cellulose in a suitable solvent into a coagulating bath. One example of such a process is described in US Patent 4,416,698 (McCorsley III), the contents of which are incorporated herein by way of reference. Cellulose is
10 dissolved in a solvent containing a tertiary amine N-oxide (which may also be called for brevity an amine oxide), for example N-methylmorpholine N-oxide (NMMO). The solvent may also contain a proportion of a non-solvent for cellulose, for example water. The resulting solution is extruded through a
15 suitable die to produce filaments, which are coagulated, washed in water to remove the solvent, and dried. This process of extrusion and coagulation is referred to as "solvent-spinning", and the cellulose fibre produced thereby is referred to as "solvent-spun" cellulose fibre. It is also
20 known that cellulose fibre can be made by extrusion of a solution of a cellulose derivative into a regenerating and coagulating bath. One example of such a process is the viscose process, in which the cellulose derivative is cellulose xanthate. Solvent-spinning has a number of
25 advantages over other known processes for the manufacture of cellulose fibre such as the viscose process, for example reduced environmental emissions.

US Patent 4,416,698 describes a method of preparing a solution of cellulose in a tertiary amine N-oxide and a method
30 for preparing a shaped article such as a fibre from such a solution. A mixture of the tertiary amine N-oxide containing the preferred amount of water and the cellulose are ground to the same predetermined particle size and charged simultaneously to the barrel of an extruder. The preferred
35 temperature range in the barrel of the extruder for processing

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the mixture of cellulose and solvent thereby dissolving the cellulose is from about 90°C to about 140°C. Degradation of the cellulose can be avoided or substantially reduced by dissolving the cellulose in the barrel of the extrusion apparatus, extruding the solution to form a film or filament and promptly precipitating the cellulose before degradation of the cellulose.

US Patent 4,426,228 (Brandner et al), the contents of which are incorporated herein by way of reference, describes a solution of cellulose in a solvent which is a tertiary amine N-oxide optionally mixed with a non-solvent for the cellulose and a method of preparing the same. The solution may contain up to 25% by weight of the non-solvent, for example water. The solution additionally comprises an additive which limits polymer decomposition at elevated temperatures so that the solution is only slightly coloured and cellulose articles made there from exhibit improved properties such as strength. One example of such an additive is propyl gallate used at 0.01 to 5% by weight relative to the solvent. US Patent 4,426,228 also describes a method of preparing such a solution in which the cellulose and the solvent are processed at temperatures between 70°C and 190°C until the cellulose has been dissolved. A solution containing 5 to 8% by weight cellulose is particularly appropriately prepared by processing at temperatures between 70°C and 100°C. In order to hold the processing time as low as possible and to attain high production rates, temperatures between 100°C and 150°C or between 115°C and 130°C may be used.

It is known that the solutions of cellulose in a tertiary amine N-oxide exhibit high viscosity, particularly those solutions which contain more than about 10% by weight, for example 10 to 25% by weight, cellulose. Solutions containing such relatively high concentrations of cellulose are desirably used in the commercial manufacture of fibre and film both to reduce processing costs and in particular because extrusion of such solutions leads to the production of fibre and film



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with improved physical properties, for example tensile strength. It is also known that the viscosity of such solutions decreases as their temperature is raised. It is therefore desirable to transport such solutions at high temperature in order to reduce the pumping costs associated with transporting high viscosity solutions.

It is also known that solutions of cellulose in a tertiary amine N-oxide such as NMMO are liable to degradation when stored at elevated temperatures. Such solutions may become discoloured when stored at temperatures above about 130°C. It is also known that uncontrolled exothermic reaction may occur when such solutions are stored at temperatures above about 170°C. It has further been observed that such uncontrolled exothermic reaction may occur even when such solutions are stored for extended periods of time at temperatures considerably below 170°C. This fact has hampered the commercial development and utilisation of solvent-spinning processes, because the risk of uncontrolled exothermic reaction is not acceptable in industrial-scale plant. The risk has previously been minimised on the laboratory or pilot plant scale by extruding the solution immediately after its preparation, so minimising the time during which the solution is stored. However, this solution is less than satisfactory for industrial-scale production, both because it is desirable to submit the solution to intermediate processing operations such as filtration between preparation and extrusion, and because it is not possible to assemble the elements of industrial-scale plant in as close a spatial relationship as the elements of laboratory or pilot plant apparatus.

The invention provides in a first aspect a method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of the solution in the centre of the pipe being controlled at no more than

1000 / (X + 0.19 x $\sqrt{D}$),

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where D represents the internal diameter of the pipe in millimetres and X represents a numerical value. The value of X may be equal to or greater than 5.0, in preferred embodiments of the invention the value of X is 5.25 or 5.75, 5 and in a particularly preferred embodiment the value of X is 5.5. If the internal diameter of the pipe is measured in inches the value 0.19 in the above-noted expression should be replaced by 0.98.

The invention further provides in a second aspect a 10 method for transporting a solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of the solution at the interior wall of the pipe being controlled at no more than

$$1000 / (Y + 0.23 \times \sqrt{D}),$$

15 where D represents the internal diameter of the pipe in millimetres and Y represents a numerical value. The value of Y may be equal to or greater than 5.4, in preferred embodiments of the invention the value of Y is 5.65 or 6.15, and in a particularly preferred embodiment the value of Y is 20 5.9. If the internal diameter of the pipe is measured in inches, the value 0.23 in the above-noted expression should be replaced by 1.15.

The solution of cellulose in N-methylmorpholine N-oxide may be referred to hereinafter alternatively as the "dope".

25 The dope may for example comprise by weight 10 to 25%, preferably 13 to 17%, cellulose and 7 to 13% water, with the balance being largely NMMO. The dope preferably contains an additive which limits polymer decomposition at elevated temperatures, as described for example in US Patent 4,426,228, 30 for example propyl gallate. The dope preferably contains 0.01 to 0.5%, more preferably 0.05 to 0.2%, by weight propyl gallate. It has been found that the presence of such an additive increases the temperature at which the dope may be

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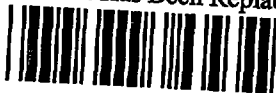
stored and transported without undergoing exothermic decomposition by several degrees Centigrade, for example by 5 to 10°C.

Use of the value 5.5 for X or of the value 5.9 for the value Y is believed to give a safety margin of at least about 10°C between the temperature of the dope in the centre of the pipe and the temperature at which spontaneous exothermic decomposition may occur during operation when the dope contains an additive as hereinbefore described.

10 The pipe is generally at least 0.5 or 1 inch (12.5 or 25 mm) in external diameter, preferably at least 2, 3 or 4 inches (50, 75 or 100 mm) in external diameter. The pipe may be up to 12 inches (300 mm) in external diameter, but is generally no more than 10 or 8 inches (250 or 200 mm) in external
15 diameter. Pipes of 6 inches (150 mm) external diameter may also be used. Pipes of 4 to 8 inches (100 to 200 mm) external diameter may be preferred. It will be noted that the equations defined in the methods of the invention relate the temperature of the dope to the internal diameter of the pipe,
20 whereas the preceding numbers refer to the nominal external diameter of the pipe. Pipework is generally specified and sold commercially by reference to its nominal external diameter.

The flow rate of the dope through the pipe may be for
25 example in the range 0.1 to 10 m/min, preferably 1 to 5 m/min.

The methods of the invention have been found to be generally less satisfactory for vessels of large diameter than for pipes of about 12 inches (300 mm) diameter or below, for example filters and tanks having internal diameters in the
30 range about 20 to about 40 inches (500 mm to 1000 mm). Such filters and tanks may in general be operated at a temperatures several degrees above those according to the method of the invention, at least during continuous operation.



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The temperature of the dope in the pipe both at the wall of the pipe and in the centre of the pipe may be controlled by equipping the pipe with a thermostatic jacket, for example a hollow jacket containing a circulating heat transfer fluid such as water. The temperature of the thermostatic jacket is generally maintained below the temperature of the dope at the centre of the pipe to provide some external cooling and thereby remove any heat generated by any exothermic reaction which may take place in the dope. The temperature of the thermostatic jacket is essentially the same as that of the dope at the wall of the pipe. It has been found that slow exothermic reaction may take place in dope stored at temperatures considerably below 170°C , the temperature in which spontaneous decomposition is known to occur. Use of such external cooling means is therefore preferred. It will be understood from the above that the value of Y is generally higher than the value of X. In particular it may be preferred that the value of $(Y-X)$ is about 0.4. The temperature of the dope in the centre of the pipe is generally about 10 to about 15°C , preferably about 11 to about 14°C , higher than the temperature of the dope at the wall of the pipe, although it will be understood that this preferred temperature difference is to some extent dependent on the internal diameter of the pipe. The temperature of the dope may be controlled by suitably varying the flow rate or the temperature of the heat transfer fluid acting as cooling medium.

The minimum temperature of the dope in the centre of the pipe is preferably at least 100°C , more preferably at least 105°C . It has been found that the viscosity of the dope is sufficiently low for the dope to be pumped through pipes in a commercial scale factory when it has at least such a minimum temperature. A dope containing about 15% by weight cellulose may exhibit a viscosity of about 2000 Pa.s (20,000 poise) at a shear rate of 1 sec^{-1} at 100°C , 1500 Pa.s (15,000 poise) at 110°C and 1000 Pa.s (10,000 poise) at 120°C . The first aspect of the invention provides for a dope temperature in the sensor of the pipe which may be 105°C or higher for all pipe sizes

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up to at least about 12 inches (300 mm) internal diameter. The preferred temperature of the dope in the centre of the pipe is between the minimum and maximum temperatures hereinbefore mentioned.

5 Processing of cellulose and solvent to dissolve the cellulose may provide dope at a higher temperature than that required by the methods of the invention, and in such a case the hot dope may be cooled to the desired temperature shortly after dissolution by passage through a suitable heat
10 exchanger. It may be desired to extrude the dope to form fibre or film at a higher temperature than that required by the methods of the invention, for example to obtain optimum tensile properties, and in such a case the dope can be warmed to the desired temperature shortly before extrusion by passage
15 through a suitable heat exchanger. One example of a suitable type of heat exchanger is a shell-and-tube heat exchanger in which the dope passes through the tubes, the tubes being equipped with static mixers which serve to mix the dope and so improve the efficiency of the heat exchange, and the heat
20 transfer medium passes through the shell, as available for example from Kenics Corporation. Another example of a suitable type of heat exchanger consists of a chamber containing a sinuous tube, the heat transfer medium passing through the sinuous tube, and the dope passing through the
25 chamber over the tube, as available for example from Gebrueder Sulzer Ag under the Trade Mark "Sulzer SMR".

Use of the methods of the invention permits solvent-spinning of cellulose to be carried out safely on the industrial scale. The methods of the invention have the
30 advantage that additional process items, for example filters, mixers and buffer tanks, can be interposed between the dissolution apparatus and the extrusion apparatus. They have the further advantage that pipes containing dope do not need to be emptied if dope transport is stopped for any reason, for
35 example to allow plant maintenance such as filter changes. The dope in the pipe is advantageously cooled to lower

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temperature, for example around 80°C, during such a stoppage by circulation of cool heat transfer fluid through the thermostatic jacket. The dope so cooled can be warmed to the required temperature for transport after the stoppage by increasing the temperature of the heat transfer fluid. Nevertheless, such additional process items are preferably emptied during such a stoppage and refilled afterwards.

Practical experience and experiment bears out the value of the methods of the invention, in particular in reducing the occurrence of uncontrolled exothermic reaction to an acceptably very low value. This is especially remarkable in that the equations upon which they rely they have no apparent theoretical basis. In particular, it is surprising that they should involve the square root of a linear dimension, namely the internal diameter of the pipe, rather than either the dimension itself or its square or cube, which are proportional to surface area and volume respectively.

The invention will now be more particularly explained with reference to the accompanying drawing, in which:

Figure 1 is a graph of $1000/T$ against $\sqrt{D}$, where T is dope temperature in °C and D is the internal pipe diameter, and

Figure 2 is a graph of T against D , where T and D have the same meanings as in Figure 1.

Referring to Figure 1, line 1 corresponds to the equation

$$1000/T = 5.5 + 0.98 \times \sqrt{D}$$

representing the relationship between a preferred maximum temperature of the dope in the centre of the pipe and the internal diameter of the pipe. Line 2 corresponds to the equation

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$$1000/T = 5.9 + 1.15 \times \sqrt{D}$$

representing the relationship between a preferred maximum temperature of the dope at the wall of the pipe and the internal diameter of the pipe. Line 3 corresponds to 105°C, which is a preferred minimum temperature for the dope in the centre of the pipe. The data points represented by squares correspond to dope temperature in the centre of the pipe and the data points represented by crosses to dope temperature at the wall of the pipe as recorded in Table 1 below:

Table 1

<u>D inches</u>	<u>Centre °C</u>	<u>Wall °C</u>
2	146	133
3	140	127
4	133	121
6	125.5	114
8	121	109
10	117	105

The data points in Table 1 have been determined empirically to provide a safety margin of at least 10°C between the dope temperature in the centre of the pipe and the temperature at which spontaneous exothermic reaction may take place when the dope contains about 0.05 to about 0.2% by weight propyl gallate. It will be observed that the agreement between the relevant equations and the data points is excellent.

Referring to Figure 2, line 1 relates dope temperature in the centre of the pipe to internal pipe diameter when $X = 5.5$, line 2 relates dope temperature at the wall of the pipe to internal pipe diameter when $Y = 5.9$, and line 3 corresponds to 105°C. The data points of Table 1 are represented by squares and crosses as in Figure 1.

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CLAIMS

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1. A method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of said solution 5 in the centre of said pipe being controlled at
- $$1000 / (X + 0.19 \times \sqrt{D}),$$
- where D represents the internal diameter of said pipe in millimetres and X represents a value equal to or greater than 5.0.
- 10 2. A method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of said solution at the interior wall of said pipe being controlled at
- $$1000 / (Y + 0.23 \times \sqrt{D}),$$
- 15 where D represents the internal diameter of said pipe in millimetres and Y represents a value equal to or greater than 5.4.
3. A method according to claim 1, wherein X represents a value equal to or greater than 5.25.
- 20 4. A method according to claim 1, wherein X represents a value equal to or greater than 5.5.
5. A method according to claim 2, wherein Y represents a value equal to or greater than 5.65.
6. A method according to claim 2, wherein Y represents 25 a value equal to or greater than 5.9.
7. A method according to any one of the preceding claims, wherein said solution comprises 10 to 25 percent by weight cellulose and 7 to 13 percent by weight water.
8. A method according to any one of the preceding 30 claims, wherein said solution comprises an additive which



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limits decomposition at elevated temperatures.

9. A method according to claim 8, wherein said additive is propyl gallate at a concentration of 0.05 to 0.2 percent by weight.

5 10. A method according to any one of the preceding claims, wherein the nominal external diameter of said pipe is at least 50 mm.

11. A method according to claim 10, wherein the nominal external diameter of said pipe is no more than 300 mm.

10 12. A method according to claim 10, wherein the nominal external diameter of said pipe is in the range 100 to 200 mm.

13. A method according to any one of the preceding claims, wherein the temperature of said solution in said centre of the pipe is at least 100°C.

15 14. A method according to claim 13, wherein the temperature of said solution in said centre of the pipe is at least 105°C.

15 15. A method according to any one of the preceding claims, wherein the temperature of said solution in said 20 centre of said pipe is 10 to 15°C higher than the temperature of said solution at said interior wall of said pipe.

16. A method according to any one of the preceding claims, wherein said pipe is equipped with a thermostatic jacket.

25 17. A method according to claim 16, wherein said thermostatic jacket is a hollow jacket through which water is circulated.

18. A method according to any one of the preceding



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claims, wherein the flow rate of said solution of cellulose through said pipe is in the range 0.1 to 10 m/min.

19. A method according to claim 18, wherein the flow rate of said solution of cellulose through said pipe is in the 5 range 1 to 5 m/min.

20. A method of manufacturing a shaped cellulosic product which includes the steps of dissolving cellulose in an aqueous N-methylmorpholine N-oxide to form a solution,
10 transporting the solution through at least one pipe and passing the solution into a coagulation bath to form the shaped cellulosic product, characterised in that the solution is transported through the pipe in accordance with the method of any one of the preceding claims.

15 21. A method as claimed in claim 20, characterised in that the shaped cellulosic product is a cellulosic fibre.

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ABSTRACT

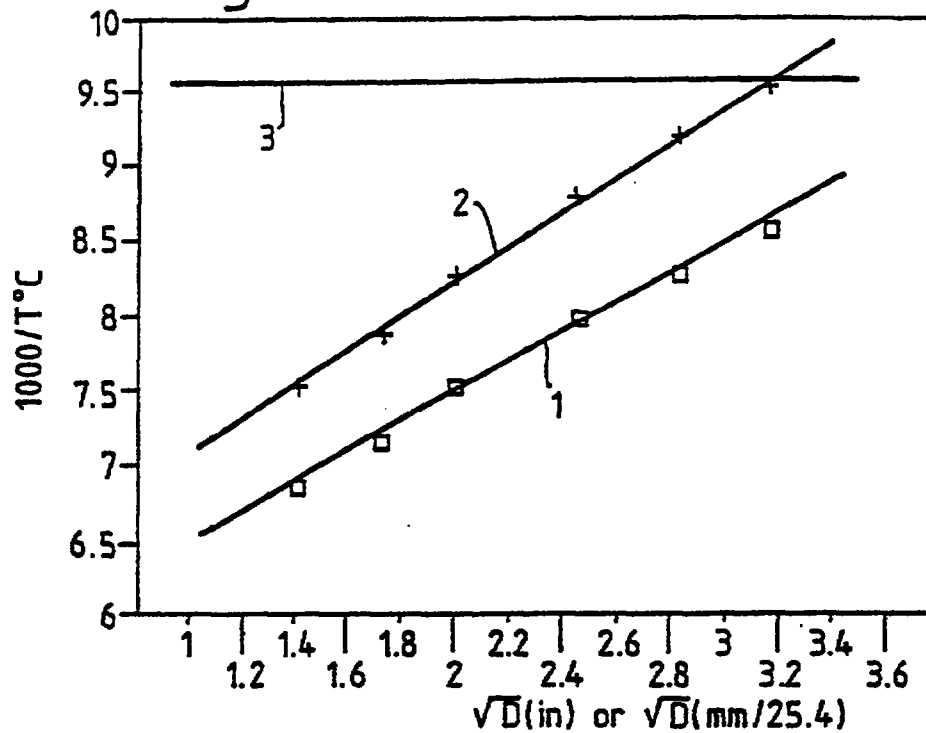
A method for transporting a solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees centigrade of said solution in the centre of said pipe being controlled at $1000/(X + 0.19 \times \sqrt{D})$ and/or the temperature of said solution at the interior wall of said pipe being controlled at $1000/(Y + 0.23 \times \sqrt{D})$ where D represents the internal diameter of the pipe in millimetres, X represents a value equal to or greater than 5.0, and Y represents a value equal to or greater than 5.4.

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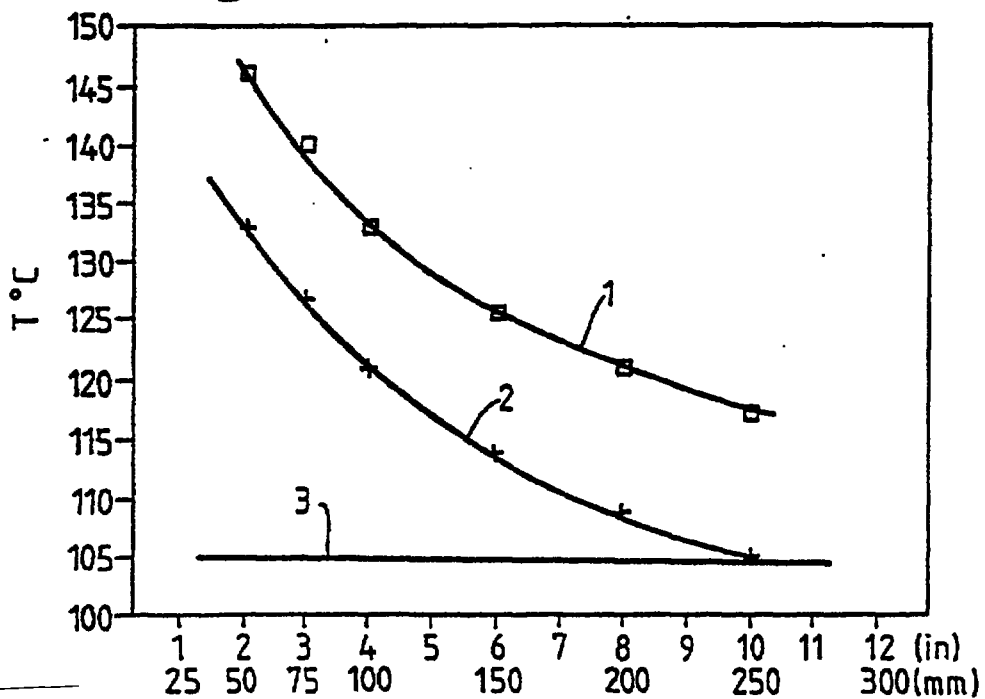
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Fig. 1.



□ CENTRE OF PIPE + WALL OF PIPE

Fig. 2.



□ CENTRE OF PIPE + WALL OF PIPE

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TRANSPORT OF SOLUTIONS OF CELLULOSE THROUGH PIPES

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ABSTRACT

A method for transporting a solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees centigrade of said solution in the centre of said pipe being controlled at $1000/(X + 0.19 \times \sqrt{D})$ and/or the temperature of said solution at the interior wall of said pipe being controlled at $1000/(Y + 0.23 \times \sqrt{D})$ where D represents the internal diameter of the pipe in millimetres, X represents a value equal to or greater than 5.0, and Y represents a value equal to or greater than 5.4.

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CLAIMS

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1. A method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of said solution in the centre of said pipe being controlled at

$$1000 / (X + 0.19 \times \sqrt{D}),$$

where D represents the internal diameter of said pipe in millimetres and X represents a value equal to or greater than 5.0.

2. A method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees Centigrade of said solution at the interior wall of said pipe being controlled at

$$1000 / (Y + 0.23 \times \sqrt{D}),$$

where D represents the internal diameter of said pipe in millimetres and Y represents a value equal to or greater than 5.4.

3. A method according to claim 1, wherein X represents a value equal to or greater than 5.25.

4. A method according to claim 1, wherein X represents a value equal to or greater than 5.5.

5. A method according to claim 2, wherein Y represents a value equal to or greater than 5.65.

6. A method according to claim 2, wherein Y represents a value equal to or greater than 5.9.

7. A method according to any one of the preceding claims, wherein said solution comprises 10 to 25 percent by weight cellulose and 7 to 13 percent by weight water.

8. A method according to any one of the preceding claims, wherein said solution comprises an additive which



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limits decomposition at elevated temperatures.

9. A method according to claim 8, wherein said additive is propyl gallate at a concentration of 0.05 to 0.2 percent by weight.

10. A method according to any one of the preceding claims, wherein the nominal external diameter of said pipe is at least 50 mm.

11. A method according to claim 10, wherein the nominal external diameter of said pipe is no more than 300 mm.

12. A method according to claim 10, wherein the nominal external diameter of said pipe is in the range 100 to 200 mm.

13. A method according to any one of the preceding claims, wherein the temperature of said solution in said centre of the pipe is at least 100°C.

14. A method according to claim 13, wherein the temperature of said solution in said centre of the pipe is at least 105°C.

15. A method according to any one of the preceding claims, wherein the temperature of said solution in said centre of said pipe is 10 to 15°C higher than the temperature of said solution at said interior wall of said pipe.

16. A method according to any one of the preceding claims, wherein said pipe is equipped with a thermostatic jacket.

17. A method according to claim 16, wherein said thermostatic jacket is a hollow jacket through which water is circulated.

18. A method according to any one of the preceding



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claims, wherein the flow rate of said solution of cellulose through said pipe is in the range 0.1 to 10 m/min.

19. A method according to claim 18, wherein the flow rate of said solution of cellulose through said pipe is in the range 1 to 5 m/min.

20. A method of manufacturing a shaped cellulosic product which includes the steps of dissolving cellulose in an aqueous N-methylmorpholine N-oxide to form a solution, transporting the solution through at least one pipe and passing the solution into a coagulation bath to form the shaped cellulosic product, characterised in that the solution is transported through the pipe in accordance with the method of any one of the preceding claims.

21. A method as claimed in claim 20, characterised in that the shaped cellulosic product is a cellulosic fibre.

22. A method as claimed in claim 20, characterised in that the shaped cellulosic product film.

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ABSTRACT

A method for transporting a solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees centigrade of said solution in the centre of said pipe being controlled at $1000/(X + 0.19 \times \sqrt{D})$ and/or the temperature of said solution at the interior wall of said pipe being controlled at $1000/(Y + 0.23 \times \sqrt{D})$ where D represents the internal diameter of the pipe in millimetres, X represents a value equal to or greater than 5.0, and Y represents a value equal to or greater than 5.4.

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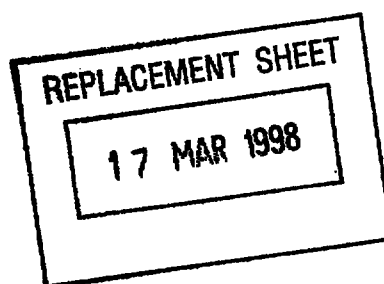


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Transport Of Solutions Of Cellulose Througe PipesABSTRACT

A method for transporting a solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees centigrade of said solution in the centre of said pipe being controlled at $1000/(X + 0.19 \times \sqrt{D})$ and/or the temperature of said solution at the interior wall of said pipe being controlled at $1000/(Y + 0.23 \times \sqrt{D})$ where D represents the internal diameter of the pipe in millimetres, X represents a value equal to or greater than 5.0, and Y represents a value equal to or greater than 5.4.



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TRANSPORT OF SOLUTIONS OF CELLULOSE THROUGH PIPES

This invention relates to the transport of solutions of cellulose in a tertiary amine N-oxide, in particular N-methylmorpholine N-oxide, through pipes.

It is known that cellulose fibre can be made by extrusion of a solution of cellulose in a suitable solvent into a coagulating bath. One example of such a process is described in US Patent 4,416,698 (McCorsley-III). Cellulose is dissolved in a solvent containing a tertiary amine N-oxide (which may also be called for brevity an amine oxide), for example N-methylmorpholine N-oxide (NMMO). The solvent may also contain a proportion of a non-solvent for cellulose, for example water. The resulting solution is extruded through a suitable die to produce filaments, which are coagulated, washed in water to remove the solvent, and dried. This process of extrusion and coagulation is referred to as "solvent-spinning", and the cellulose fibre produced thereby is referred to as "solvent-spun" cellulose fibre. It is also known that cellulose fibre can be made by extrusion of a solution of a cellulose derivative into a regenerating and coagulating bath. One example of such a process is the viscose process, in which the cellulose derivative is cellulose xanthate. Solvent-spinning has a number of advantages over other known processes for the manufacture of cellulose fibre such as the viscose process, for example reduced environmental emissions.

US Patent 4,416,698 describes a method of preparing a solution of cellulose in a tertiary amine N-oxide and a method for preparing a shaped article such as a fibre from such a solution. A mixture of the tertiary amine N-oxide containing the preferred amount of water and the cellulose are ground to the same predetermined particle

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size and charged simultaneously to the barrel of an extruder. The preferred temperature range in the barrel of the extruder for processing the mixture of cellulose and solvent thereby dissolving the cellulose is from about 90°C to about 140°C. Degradation of the cellulose can be avoided or substantially reduced by dissolving the cellulose in the barrel of the extrusion apparatus, extruding the solution to form a film or filament and promptly precipitating the cellulose before degradation of the cellulose.

US Patent 4,426,228 (Brandner et al) describes a solution of cellulose in a solvent which is a tertiary amine N-oxide optionally mixed with a non-solvent for the cellulose and a method of preparing the same. The solution may contain up to 25% by weight of the non-solvent, for example water. The solution additionally comprises an additive which limits polymer decomposition at elevated temperatures so that the solution is only slightly coloured and cellulose articles made therefrom exhibit improved properties such as strength. One example of such an additive is propyl gallate used at 0.01 to 5% by weight relative to the solvent. US Patent 4,426,228 also describes a method of preparing such a solution in which the cellulose and the solvent are processed at temperatures between 70°C and 190°C until the cellulose has been dissolved. A solution containing 5 to 20% by weight cellulose is particularly appropriately prepared by processing at temperatures between 70°C and 100°C. In order to hold the processing time as low as possible and to attain high production rates, temperatures between 100°C and 150°C or between 115°C and 130°C may be used.

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It is known that the solutions of cellulose in a tertiary amine N-oxide exhibit high viscosity, particularly those solutions which contain more than about 10% by weight, for example 10 to 25% by weight, cellulose. Solutions containing such relatively high concentrations of cellulose are desirably used in the commercial manufacture of fibre and film both to reduce processing costs and in particular because extrusion of such solutions leads to the production of fibre and film with improved physical properties, for example tensile strength. It is also known that the viscosity of such solutions decreases as their temperature is raised. It is therefore desirable to transport such solutions at high temperature in order to reduce the pumping costs associated with transporting high viscosity solutions.

It is also known that solutions of cellulose in a tertiary amine N-oxide such as NMMO are liable to degradation when stored at elevated temperatures. Such solutions may become discoloured when stored at temperatures above about 130°C. It is also known that uncontrolled exothermic reaction may occur when such solutions are stored at temperatures above about 170°C. It has further been observed that such uncontrolled exothermic reaction may occur even when such solutions are stored for extended periods of time at temperatures considerably below 170°C. This fact has hampered the commercial development and utilisation of solvent-spinning processes, because the risk of uncontrolled exothermic reaction is not acceptable in industrial-scale plant. The risk has previously been minimised on the laboratory or pilot plant scale by extruding the solution immediately after its preparation, so minimising the time during which the solution is stored. However, this solution is less than satisfactory for industrial-scale production, both because it is desirable to submit the solution

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to intermediate processing operations such as filtration between preparation and extrusion, and because it is not possible to assemble the elements of industrial-scale plant in as close a spatial relationship as the elements of laboratory or pilot plant apparatus.

The invention provides in a first aspect a method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe of nominal external diameter in the range from 25 to 300 mm the temperature in degrees Centigrade of the solution in the centre of the pipe being controlled at no more than

$$1000 / (X + 0.19 \times \sqrt{D})$$

where D represents the internal diameter of the pipe in millimetres and X represents a numerical value. The value of X may be equal to or greater than 5.0. in preferred embodiments of the invention the value of X is 5.25 or 5.75, and in a particularly preferred embodiment the value of X is 5.5. If the internal diameter of the pipe is measured in inches the value 0.19 in the above-noted expression should be replaced by 0.98.

The invention further provides in a second aspect a method for transporting a solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe of nominal external diameter in the range from 25 to 300 mm, the temperature in degrees Centigrade of the solution at the interior wall of the pipe being controlled at no more than

$$1000 / (Y + 0.23 \times \sqrt{D}).$$

where D represents the internal diameter of the pipe in millimetres and Y represents a numerical value. The value of Y may be equal to or greater than 5.4. in preferred embodiments of the invention the value of Y is 5.65 or

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6.15, and in a particularly preferred embodiment the value of Y is 5.9. If the internal diameter of the pipe is measured in inches, the value 0.23 in the above-noted expression should be replaced by 1.15.

The solution of cellulose in N-methylmorpholine N-oxide may be referred to hereinafter alternatively as the "dope".

The dope may for example comprise by weight 10 to 25%, preferably 13 to 17%, cellulose and 7 to 13% water, with the balance being largely NMMO. The dope preferably contains an additive which limits polymer decomposition at elevated temperatures, as described for example in US Patent 4,426,228, for example propyl gallate. The dope preferably contains 0.01 to 0.5%, more preferably 0.05 to 0.2%, by weight propyl gallate. It has been found that the presence of such an additive increases the temperature at which the dope may be stored and transported without undergoing exothermic decomposition by several degrees Centigrade, for example by 5 to 10°C.

Use of the value 5.5 for X or of the value 5.9 for the value Y is believed to give a safety margin of at least about 10°C between the temperature of the dope in the centre of the pipe and the temperature at which spontaneous exothermic decomposition may occur during operation when the dope contains an additive as hereinbefore described.

The pipe preferably at least 2, 3 or 4 inches (50, 75 or 100 mm) in external diameter. The pipe is generally no more than 10 or 8 inches (250 or 200 mm) in external diameter. Pipes of 6 inches (150 mm) external diameter may also be used. Pipes of 4 to

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8 inches (100 to 200 mm) external diameter may be preferred. It will be noted that the equations defined in the methods of the invention relate the temperature of the dope to the internal diameter of the pipe, whereas the preceding numbers refer to the nominal external diameter of the pipe. Pipework is generally specified and sold commercially by reference to its nominal external diameter.

The flow rate of the dope through the pipe may be for example in the range 0.1 to 10 m/min, preferably 1 to 5 m/min.

The methods of the invention have been found to be generally less satisfactory for vessels of large diameter than for pipes of about 1.2 inches (300 mm) diameter or below, for example filters and tanks having internal diameters in the range about 20 to about 40 inches (500 mm to 1000 mm). Such filters and tanks may in general be operated at a temperatures several degrees above those according to the method of the invention, at least during continuous operation.

The temperature of the dope in the pipe both at the wall of the pipe and in the centre of the pipe may be controlled by equipping the pipe with a thermostatic jacket, for example a hollow jacket containing a circulating heat transfer fluid such as water. The temperature of the thermostatic jacket is generally maintained below the temperature of the dope at the centre of the pipe to provide some external cooling and thereby remove any heat generated by any exothermic reaction which may take place in the dope. The temperature of the thermostatic jacket is essentially the same as that of the dope

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at the wall of the pipe. It has been found that slow exothermic reaction may take place in dope stored at temperatures considerably below 170°C , the temperature in which spontaneous decomposition is known to occur. Use of such external cooling means is therefore preferred. It will be understood from the above that the value of Y is generally higher than the value of X . In particular it may be preferred that the value of $(Y-X)$ is about 0.4. The temperature of the dope in the centre of the pipe is generally about 10 to about 15°C , preferably about 11 to about 14°C , higher than the temperature of the dope at the wall of the pipe, although it will be understood that this preferred temperature difference is to some extent dependent on the internal diameter of the pipe. The temperature of the dope may be controlled by suitably varying the flow rate or the temperature of the heat transfer fluid acting as cooling medium.

The minimum temperature of the dope in the centre of the pipe is preferably at least 100°C , more preferably at least 105°C . It has been found that the viscosity of the dope is sufficiently low for the dope to be pumped through pipes in a commercial scale factory when it has at least such a minimum temperature. A dope containing about 15% by weight cellulose may exhibit a viscosity of about 2000 Pa.s (20,000 poise) at a shear rate of 1 sec^{-1} at 100°C , 1500 Pa.s (15,000 poise) at 110°C and 1000 Pa.s (10,000 poise) at 120°C . The first aspect of the invention provides for a dope temperature in the centre of the pipe which may be 105°C or higher for all pipe sizes up to at least about 12 inches (300 mm) internal diameter. The preferred temperature of the dope in the centre of the pipe is between the minimum and maximum temperatures hereinbefore mentioned.

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Processing of cellulose and solvent to dissolve the cellulose may provide dope at a higher temperature than that required by the methods of the invention, and in such a case the hot dope may be cooled to the desired temperature shortly after dissolution by passage through a suitable heat exchanger. It may be desired to extrude the dope to form fibre or film at a higher temperature than that required by the methods of the invention, for example to obtain optimum tensile properties, and in such a case the dope can be warmed to the desired temperature shortly before extrusion by passage through a suitable heat exchanger. One example of a suitable type of heat exchanger is a shell-and-tube heat exchanger in which the dope passes through the tubes, the tubes being equipped with static mixers which serve to mix the dope and so improve the efficiency of the heat exchange, and the heat transfer medium passes through the shell, as available for example from Kenics Corporation. Another example of a suitable type of heat exchanger consists of a chamber containing a sinuous tube, the heat transfer medium passing through the sinuous tube, and the dope passing through the chamber over the tube, as available for example from Gebrueder Sulzer Ag under the Trade Mark "Sulzer SMR".

Use of the methods of the invention permits solvent-spinning of cellulose to be carried out safely on the industrial scale. The methods of the invention have the advantage that additional process items, for example filters, mixers and buffer tanks, can be interposed between the dissolution apparatus and the extrusion apparatus. They have the further advantage that pipes containing dope do not need to be emptied if dope transport is stopped for any reason, for example to allow plant

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maintenance such as filter changes. The dope in the pipe is advantageously cooled to lower temperature, for example around 80°C , during such a stoppage by circulation of cool heat transfer fluid through the thermostatic jacket. The dope so cooled can be warmed to the required temperature for transport after the stoppage by increasing the temperature of the heat transfer fluid. Nevertheless, such additional process items are preferably emptied during such a stoppage and refilled afterwards.

Practical experience and experiment bears out the value of the methods of the invention, in particular in reducing the occurrence of uncontrolled exothermic reaction to an acceptably very low value. This is especially remarkable in that the equations upon which they rely have no apparent theoretical basis. In particular, it is surprising that they should involve the square root of a linear dimension, namely the internal diameter of the pipe rather than either the dimension itself or its square or cube, which are proportional to surface area and volume respectively.

The invention will now be more particularly explained with reference to the accompanying drawing, in which:

Figure 1 is a graph of $1000/T$ against $\sqrt{D}$, where T is dope temperature in $^{\circ}\text{C}$ and D is the internal pipe diameter, and

Figure 2 is a graph of T against D , where T and D have the same meanings as in Figure 1.

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Referring to Figure 1, line 1 corresponds to the equation

$$1000/T = 5.5 + 0.98 \times \sqrt{D}$$

representing the relationship between a preferred maximum temperature of the dope in the centre of the pipe and the internal diameter of the pipe. Line 2 corresponds to the equation

$$1000/T = 5.9 + 1.15 \times \sqrt{D}$$

representing the relationship between a preferred maximum temperature of the dope at the interior wall of the pipe and the internal diameter of the pipe. Line 3 corresponds to 105°C, which is a preferred minimum temperature for the dope in the centre of the pipe. The data points represented by squares correspond to dope temperature in the centre of the pipe and the data points represented by crosses to dope temperature at the wall of the pipe as recorded in Table 1 below:

Table 1

D inches	Centre °C	Wall °C
2	146	133
3	140	127
4	133	121
6	125.5	114
8	121	109
10	117	105
(1in = 2,54 × 10 ⁻² m)		

The data points in Table 1 have been determined

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empirically to provide a safety margin of at least 10°C between the dope temperature in the centre of the pipe and the temperature at which spontaneous exothermic reaction may take place when the dope contains about 0.05 to about 0.2% by weight propyl gallate. It will be observed that the agreement between the relevant equations and the data points is excellent.

Referring to Figure 2, line 1 relates dope temperature in the centre of the pipe to internal pipe diameter when $X = 5.5$. line 2 relates dope temperature at the wall of the pipe to internal pipe diameter when $Y = 5.9$, and line 3 corresponds to 105°C . The data points of Table 1 are represented by squares and crosses as in Figure 1.

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1. A method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe of nominal external diameter in the range from 25 to 300 mm, the temperature in degrees Centigrade of said solution in the centre of said pipe being controlled at

$$1000 / (X + 0.19 \times \sqrt{D}),$$

where D represents the internal diameter of said pipe in millimetres and X represents a value equal to or greater than 5.0.

2. A method for transporting a flowable solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe of nominal external diameter in the range from 25 to 300 mm, the temperature in degrees Centigrade of said solution at the interior wall of said pipe being controlled at

$$1000 / (Y + 0.23 \times \sqrt{D}),$$

where D represents the internal diameter of said pipe in millimetres and Y represents a value equal to or greater than 5.4.

3. A method according to claim 1, wherein X represents a value equal to or greater than 5.25.
4. A method according to claim 1, wherein X represents a value equal to or greater than 5.5.
5. A method according to claim 2, wherein Y represents a value equal to or greater than 5.65.
6. A method according to claim 2, wherein Y represents a value equal to or greater than 5.9.



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7. A method according to any one of the preceding claims, wherein said solution comprises 10 to 25 percent by weight cellulose and 7 to 13 percent by weight water.
8. A method according to any one of the preceding claims, wherein said solution comprises an additive which limits decomposition at elevated temperatures.
9. A method according to claim 5, wherein said additive is propyl gallate at a concentration of 0.05 to 0.2 percent by weight.
10. A method according to any one of the preceding claims, wherein the nominal external diameter of said pipe is at least 50 mm.
11. A method according to any one of the preceding claims, wherein the nominal external diameter of said pipe is in the range 100 to 200 mm.
12. A method according to any one of the preceding claims, wherein the temperature of said solution in said centre of the pipe is at least 100°C.
13. A method according to claim 12 wherein the temperature of said solution in said centre of the pipe is at least 105°C.
14. A method according to any one of the preceding claims, wherein the temperature of said solution in said centre of said pipe is 10 to 15°C higher than the temperature of said solution at said interior wall of said pipe.



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15. A method according to any one of the preceding claims, wherein said pipe is equipped with a thermostatic jacket.
16. A method according to claim 15, wherein said thermostatic jacket is a hollow jacket through which water is circulated.
17. A method according to any one of the preceding claims, wherein the flow rate of said solution of cellulose through said pipe is in the range 0.1 to 10 m/min.
18. A method according to claim 17 wherein the flow rate of said solution of cellulose through said pipe is in the range 1 to 5 m/min.
19. A method of manufacturing a shaped cellulosic product which includes the steps of dissolving cellulose in an aqueous N-methylmorpholine N-oxide to form a solution, transporting the solution through at least one pipe and passing the solution into a coagulation bath to form the shaped cellulosic product, characterised in that the solution is transported through the pipe in accordance with the method of any one of the preceding claims.
20. A method as claimed in claim 19, characterised in that the shaped cellulosic product is a cellulosic fibre.
21. A method as claimed in claim 19, characterised in that the shaped cellulosic product is cellulose film.



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22. A method according to any one of claims 19 to 21, characterised in that the temperature of the solution is lowered by passage through a heat exchanger shortly after the dissolution step and before the transport step.
- 23.. A method according to any one of claims 19 to 22, characterised in that the temperature of the solution is increased by passage through a heat exchanger after the transport step and shortly before the step of passing the solution into the coagulation bath.



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TRANSPORT OF SOLUTIONS OF CELLULOSE THROUGH PIPESABSTRACT

A method for transporting a solution of cellulose in aqueous N-methylmorpholine N-oxide through a pipe, the temperature in degrees centigrade of said solution in the centre of said pipe being controlled at $1000/(X + 0.19 \times \sqrt{D})$ and/or the temperature of said solution at the interior wall of said pipe being controlled at $1000/(Y + 0.23 \times \sqrt{D})$ where D represents the internal diameter of the pipe in millimetres, X represents a value equal to or greater than 5.0, and Y represents a value equal to or greater than 5.4.

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Fig. 1.

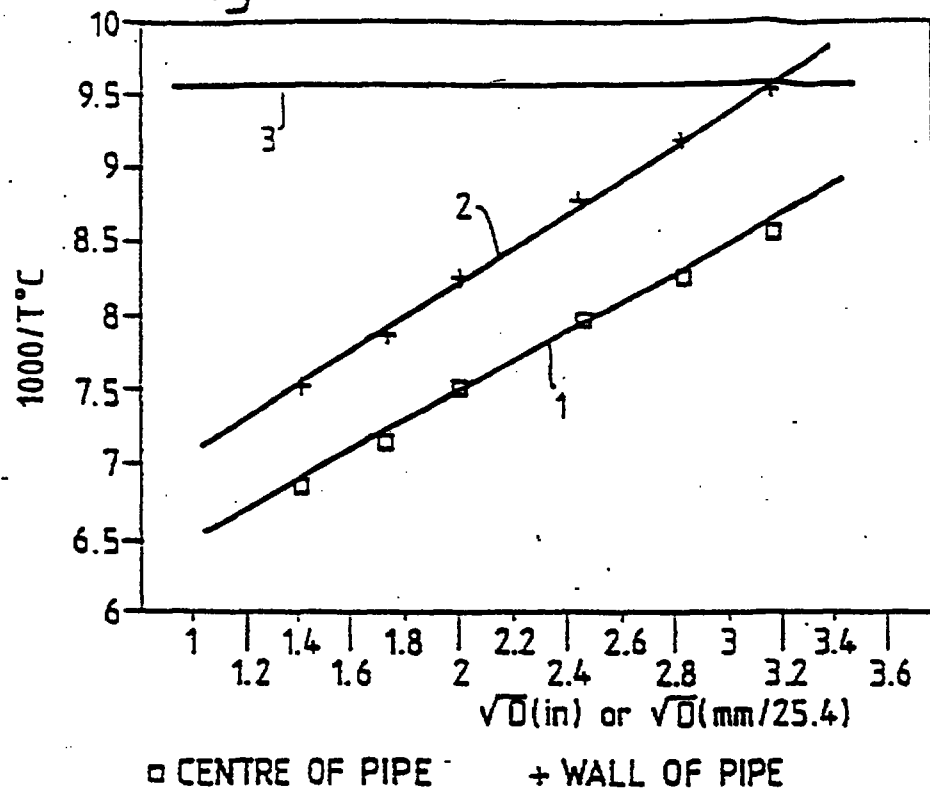


Fig. 2.

