

Double metal cyanide catalysts for the preparation of polyether polyols

The invention relates to novel double metal cyanide (DMC) catalysts for the preparation of polyether polyols by polyaddition of alkylene oxides to starter compounds containing active hydrogen atoms.

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Double metal cyanide (DMC) catalysts for the polyaddition of alkylene oxides to starter compounds containing active hydrogen atoms are known (see, for example, US 3 404 109, US 3 829 505, US 3 941 849 and US 5 158 922). The use of those DMC catalysts for the preparation of polyether polyols brings about in particular a reduction in the proportion of monofunctional polyethers having terminal double bonds, so-called monools, in comparison with the conventional preparation of polyether polyols by means of alkali catalysts, such as alkali hydroxides. The polyether polyols so obtained can be processed to high-quality polyurethanes (e.g. elastomers, foams, coatings). DMC catalysts are usually obtained by reacting an aqueous solution of a metal salt with the aqueous solution of a metal cyanide salt in the presence of an organic complex ligand, for example an ether. In a typical catalyst preparation, for example, aqueous solutions of zinc chloride (in excess) and potassium hexacyanocobaltate are mixed, and dimethoxyethane (glyme) is then added to the suspension formed. After filtration and washing of the catalyst with aqueous glyme solution, an active catalyst of the general formula

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is obtained (see, for example, EP 700 949).

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From JP 4 145 123, US 5 470 813, EP 700 949, EP 743 093, EP 761 708 and WO 97/40086 there are known DMC catalysts which, by the use of tert.-butanol as organic complex ligand (alone or in combination with a polyether (EP 700 949, EP 761 708, WO 97/40086)), further reduce the proportion of monofunctional polyethers having terminal double bonds in the preparation of polyether polyols.

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Moreover, the use of those DMC catalysts reduces the induction time in the polyaddition reaction of the alkylene oxides with appropriate starter compounds and increases the catalyst activity.

- 5 The object of the present invention was to make available further improved DMC catalysts for the polyaddition of alkylene oxides to appropriate starter compounds, which catalysts exhibit increased catalyst activity as compared with the catalyst types known hitherto. By shortening the alkoxylation times, this leads to an improvement in the process for preparing polyether polyols in terms of economy.
- 10 Ideally, as a result of the increased activity, the catalyst can then be used in such low concentrations (25 ppm or less) that the very expensive separation of the catalyst from the product is no longer necessary and the product can be used directly for the preparation of polyurethanes.
- 15 Surprisingly, it has now been found that DMC catalysts that contain a polyalkylene glycol sorbitan ester as complex ligand possess greatly increased activity in the preparation of polyether polyols.

Accordingly, the present invention provides a double metal cyanide (DMC) catalyst
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- a) one or more, preferably one, double metal cyanide compound(s),
- b) one or more, preferably one, organic complex ligand(s) other than c), and
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- c) one or more, preferably one, polyalkylene glycol sorbitan ester(s).

The catalyst according to the invention may optionally contain d) water, preferably from 1 to 10 wt.%, and/or e) one or more water-soluble metal salts, preferably from
30 5 to 25 wt.%, of formula (I) $M(X)_n$ from the preparation of the double metal cyanide compounds a). In formula (I), M is selected from the metals Zn(II), Fe(II), Ni(II), Mn(II), Co(II), Sn(II), Pb(II), Fe(III), Mo(IV), Mo(VI), Al(III), V(V), V(IV), Sr(II),

W(IV), W(VI), Cu(II) and Cr(III). Zn(II), Fe(II), Co(II) and Ni(II) are especially preferred. The substituents X are identical or different, preferably identical, and represent an anion, preferably selected from the group consisting of halides, hydroxides, sulfates, carbonates, cyanates, thiocyanates, isocyanates, isothiocyanates, carboxylates, oxalates and nitrates. The value of n is 1, 2 or 3.

The double metal cyanide compounds a) contained in the catalysts according to the invention are the reaction products of water-soluble metal salts and water-soluble metal cyanide salts.

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Water-soluble metal salts suitable for the preparation of double metal cyanide compounds a) preferably have the general formula (I) $M(X)_n$, wherein M is selected from the metals Zn(II), Fe(II), Ni(II), Mn(II), Co(II), Sn(II), Pb(II), Fe(III), Mo(IV), Mo(VI), Al(III), V(V), V(IV), Sr(II), W(IV), W(VI), Cu(II) and Cr(III). Zn(II), Fe(II), Co(II) and Ni(II) are especially preferred. The substituents X are identical or different, preferably identical, and represent an anion, preferably selected from the group consisting of halides, hydroxides, sulfates, carbonates, cyanates, thiocyanates, isocyanates, isothiocyanates, carboxylates, oxalates and nitrates. The value of n is 1, 2 or 3.

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Examples of suitable water-soluble metal salts are zinc chloride, zinc bromide, zinc acetate, zinc acetylacetonate, zinc benzoate, zinc nitrate, iron(II) sulfate, iron(II) bromide, iron(II) chloride, cobalt(II) chloride, cobalt(II) thiocyanate, nickel(II) chloride and nickel(II) nitrate. Mixtures of various water-soluble metal salts may also be used.

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Water-soluble metal cyanide salts suitable for the preparation of double metal cyanide compounds a) preferably have the general formula (II) $(Y)_a M'(CN)_b (A)_c$, wherein M' is selected from the metals Fe(II), Fe(III), Co(II), Co(III), Cr(II), Cr(III), Mn(II), Mn(III), Ir(III), Ni(II), Rh(III), Ru(II), V(IV) and V(V). M' is selected especially from the metals Co(II), Co(III), Fe(II), Fe(III), Cr(III), Ir(III) and Ni(II). The water-soluble metal cyanide salt may contain one or more of those metals. The

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substituents Y are identical or different, preferably identical, and represent an alkali metal ion or an alkaline earth metal ion. The substituents A are identical or different, preferably identical, and represent an anion selected from the group consisting of halides, hydroxides, sulfates, carbonates, cyanates, thiocyanates, isocyanates, isothiocyanates, carboxylates, oxalates and nitrates. a as well as b and c are integers, the values for a, b and c being so selected that the metal cyanide salt is electroneutral; a is preferably 1, 2, 3 or 4; b is preferably 4, 5 or 6; c preferably has the value 0. Examples of suitable water-soluble metal cyanide salts are potassium hexacyanocobaltate(III), potassium hexacyanoferrate(II), potassium hexacyanoferrate(III), calcium hexacyanocobaltate(III) and lithium hexacyanocobaltate(III).

Preferred double metal cyanide compounds a) contained in the catalysts according to the invention are compounds of the general formula (III)

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wherein M is as defined in formula (I) and

M' is as defined in formula (II) and

20 x, x', y and z are integers and are so selected that the double metal cyanide compound has electro neutrality.

Preferably,

x = 3, x' = 1, y = 6 and z = 2,

25 M = Zn(II), Fe(II), Co(II) or Ni(II) and

M' = Co(III), Fe(III), Cr(III) or Ir(III).

30 Examples of suitable double metal cyanide compounds a) are zinc hexacyanocobaltate(III), zinc hexacyanoiridate(III), zinc hexacyanoferrate(III) and cobalt(II) hexacyanocobaltate(III). Further examples of suitable double metal cyanide compounds will be found in, for example, US 5 158 922 (column 8, lines 29-66). The use of zinc hexacyanocobaltate(III) is especially preferred.

The organic complex ligands b) contained in the DMC catalysts according to the invention are in principle known and are described in detail in the prior art (see, for example, US 5 158 922, especially column 6, lines 9-65, US 3 404 109, US 3 829 505, US 3 941 849, EP 700 949, EP 761 708, JP 4 145 123, US 5 470 813, EP 743 093 and WO 97/40086). Preferred organic complex ligands are water-soluble organic compounds having hetero atoms, such as oxygen, nitrogen, phosphorus or sulfur, which are able to form complexes with the double metal cyanide compound a). Suitable organic complex ligands are, for example, alcohols, aldehydes, ketones, ethers, esters, amides, ureas, nitriles, sulfides and mixtures thereof. Preferred organic complex ligands are water-soluble aliphatic alcohols, such as ethanol, isopropanol, n-butanol, isobutanol, sec.-butanol and tert.-butanol. Tert.-butanol is especially preferred.

The organic complex ligand is added either during preparation of the catalyst or immediately after precipitation of the double metal cyanide compound a). The organic complex ligand is usually employed in excess.

The DMC catalysts according to the invention contain the double metal cyanide compounds a) in amounts of from 20 to 90 wt.%, preferably from 25 to 80 wt.%, based on the amount of finished catalyst, and the organic complex ligands b) in amounts of from 0.5 to 30 wt.%, preferably from 1 to 25 wt.%, based on the amount of finished catalyst. The DMC catalysts according to the invention usually contain from 1 to 80 wt.%, preferably from 1 to 40 wt.%, based on the amount of finished catalyst, of polyalkylene glycol sorbitan ester.

Polyalkylene glycol sorbitan esters suitable for the preparation of the catalysts according to the invention are, for example, alkoxylated mono-, di- or tri-esters of sorbitans with carboxylic acids.

Sorbitans (monoanhydrosorbitols) are tetrahydric tetrahydrofuran alcohols which are formed by the removal of one molecule of water from sorbitol, such as, for example, 1,4-sorbitan, 3,6-sorbitan, 1,5-sorbitan (pyrogalite) or 2,5-anhydro-L-iditol.

- 5 There are suitable as the carboxylic acid component aryl-, aralkyl- and alkyl-carboxylic acids having from 2 to 30 carbon atoms, preferably from 4 to 24 carbon atoms and especially from 6 to 20 carbon atoms, preferably aralkyl- and alkyl-carboxylic acids, especially alkylcarboxylic acids.
- 10 There are suitable as the polyalkylene glycol components polyethylene glycols and polypropylene glycols having from 2 to 40 alkylene oxide units.

- 15 Polyalkylene glycol sorbitan esters that are preferably used are the polyethylene glycol sorbitan esters (polysorbates), which are generally obtained by esterification of sugar alcohols, such as sorbitol or sorbitan, by fatty acids, such as butyric acid, isovaleric acid, caproic acid, caprylic acid, capric acid, lauric acid, myristic acid, palmitic acid, stearic acid, oleic acid, linoleic acid or linolenic acid, in the presence of acids, and reaction with ethylene oxide.

- 20 Special preference is given to polyethylene glycol sorbitan mono-, di- and tri-esters of fatty acids having from 6 to 18 carbon atoms and from 2 to 40 moles of ethylene oxide.

- 25 Methods for the preparation of polyalkylene glycol sorbitan esters are generally well known and are described in detail, for example, in "Kirk-Othmer, Encyclopedia of Chemical Technology", Vol. 23, 4th edition, 1997, p. 100 ff; "Römpf, Lexikon Chemie", 9th edition, Stuttgart/New York, 1992, p. 3570, 4217; "Ullmann, Encyclopedia of Industrial Chemistry", Vol. A25, 5th edition, 1994, p. 418 ff.

- 30 It is also possible to use any desired mixtures of the above-mentioned polyalkylene glycol sorbitan esters.

Analysis of the catalyst composition is usually carried out by means of elemental analysis, thermogravimetry or removal by extraction of the polyalkylene glycol sorbitan ester content, with subsequent gravimetric determination.

- 5 The catalysts according to the invention may be crystalline, partially crystalline or amorphous. Analysis of the crystallinity is usually carried out by powder X-ray diffraction.

Preference is given to catalysts according to the invention containing

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- a) zinc hexacyanocobaltate(III),
- b) tert.-butanol and
- 15 c) a polyalkylene glycol sorbitan ester.

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Preparation of the DMC catalysts according to the invention is usually carried out in aqueous solution by reacting α) metal salts, especially of formula (I), with metal cyanide salts, especially of formula (II), β) organic complex ligands b) other than polyalkylene glycol sorbitan esters, and γ) polyalkylene glycol sorbitan esters.

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In the preparation it is preferable first to react the aqueous solutions of the metal salt (e.g. zinc chloride used in stoichiometric excess (at least 50 mol %, based on the metal cyanide salt)) and of the metal cyanide salt (e.g. potassium hexacyanocobaltate) in the presence of the organic complex ligand b) (e.g. tert.-butanol), there being formed a suspension which contains the double metal cyanide compound a) (e.g. zinc hexacyanocobaltate), water d), excess metal salt e) and the organic complex ligand b).

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The organic complex ligand b) may be present in the aqueous solution of the metal salt and/or of the metal cyanide salt, or it is added directly to the suspension obtained after precipitation of the double metal cyanide compound a). It has proved

advantageous to mix the aqueous solutions and the organic complex ligand b), with vigorous stirring. The suspension formed is then usually treated with the polyalkylene glycol sorbitan ester c). The polyalkylene glycol sorbitan ester c) is preferably used in a mixture with water and organic complex ligand b).

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The catalyst is then isolated from the suspension by known techniques, such as centrifugation or filtration. In a preferred variant, the isolated catalyst is then washed with an aqueous solution of the organic complex ligand b) (e.g. by being re-suspended and subsequently isolated again by filtration or centrifugation). In that manner it is possible to remove, for example, water-soluble by-products, such as potassium chloride, from the catalyst according to the invention.

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The amount of organic complex ligand b) in the aqueous washing solution is preferably from 40 to 80 wt.%, based on the total solution. Furthermore, it is advantageous to add to the aqueous washing solution a small amount of polyalkylene glycol sorbitan ester, preferably in the range of from 0.5 to 5 wt.%, based on the total solution.

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It is also advantageous to wash the catalyst more than once. To that end, the first washing procedure may be repeated, for example. It is, however, preferred to use non-aqueous solutions for further washing procedures, for example a mixture of organic complex ligand and polyalkylene glycol sorbitan ester.

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The washed catalyst, optionally after pulverisation, is then dried at temperatures of generally from 20 to 100°C and at pressures of generally from 0.1 mbar to normal pressure (1013 mbar).

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The present invention relates also to the use of the DMC catalysts according to the invention in a process for the preparation of polyether polyols by polyaddition of alkylene oxides to starter compounds containing active hydrogen atoms.

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There are used as alkylene oxides preferably ethylene oxide, propylene oxide, butylene oxide and mixtures thereof. The synthesis of the polyether chains by alkoxylation may be carried out, for example, with only one monomeric epoxide or in a random or block manner with 2 or 3 different monomeric epoxides. Further
5 details will be found in "Ullmanns Encyclopädie der industriellen Chemie", English language edition, 1992, Vol. A21, pages 670-671.

There are preferably used as starter compounds containing active hydrogen atoms compounds having molecular weights of from 18 to 2000 and having from 1 to 8
10 hydroxyl groups. There may be mentioned by way of example: ethylene glycol, diethylene glycol, triethylene glycol, 1,2-propylene glycol, 1,4-butanediol, hexamethylene glycol, bisphenol A, trimethylolpropane, glycerol, pentaerythritol, sorbitol, cane sugar, decomposed starch or water.

15 Advantageously, the starter compounds containing active hydrogen atoms that are used are those which have been prepared, for example, by conventional alkali catalysis from the above-mentioned low molecular weight starters and which are oligomeric alkoxylation products having molecular weights of from 200 to 2000.

20 The polyaddition, catalysed by the catalysts according to the invention, of alkylene oxides to starter compounds containing active hydrogen atoms is generally carried out at temperatures of from 20 to 200°C, preferably in the range of from 40 to 180°C, especially at temperatures of from 50 to 150°C. The reaction may be carried out at total pressures of from 0 to 20 bar. The polyaddition may be carried out
25 without a solvent or in an inert organic solvent, such as toluene and/or THF. The amount of solvent is usually from 10 to 30 wt.%, based on the amount of polyether polyol to be prepared.

The catalyst concentration is so selected that good control of the polyaddition
30 reaction under the given reaction conditions is possible. The catalyst concentration is generally in the range of from 0.0005 wt.% to 1 wt.%, preferably in the range of

from 0.001 wt.% to 0.1 wt.%, especially in the range of from 0.001 to 0.0025 wt.%, based on the amount of polyether polyol to be prepared.

5 The molecular weights of the polyether polyols prepared by the process according to the invention are in the range of from 500 to 100,000 g/mol, preferably in the range of from 1000 to 50,000 g/mol, especially in the range of from 2000 to 20,000 g/mol.

The polyaddition may be carried out continuously or discontinuously, for example in a batch or semi-batch process.

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On account of their markedly increased activity, the catalysts according to the invention can be used in very low concentrations (25 ppm and below, based on the amount of polyether polyol to be prepared). If the polyether polyols prepared in the presence of the catalysts according to the invention are used for the preparation of
15 polyurethanes (Kunststoffhandbuch, Vol. 7, Polyurethane, 3rd edition, 1993, p. 25-32 and 57-67), it is possible to dispense with removal of the catalyst from the polyether polyol without the product qualities of the resulting polyurethane being adversely affected.

20 The Examples which follow explain the invention but are not intended to be limiting.

Examples

Catalyst preparation

5 Example A

Preparation of a DMC catalyst using a polyethylene glycol sorbitan monooleate (catalyst A).

10 A solution of 12.5 g (91.5 mmol) of zinc chloride in 20 ml of distilled water is added, with vigorous stirring (24,000 rpm), to a solution of 4 g (12 mmol) of potassium hexacyanocobaltate in 70 ml of distilled water. Immediately thereafter, a mixture of 50 g of tert.-butanol and 50 g of distilled water is added to the suspension which has formed, and vigorous stirring is then carried out for 10 minutes

15 (24,000 rpm). A mixture of 1 g of polyethylene glycol(20) sorbitan monooleate Disponyl SMO 120®, Henkel), 1 g of tert.-butanol and 100 g of distilled water is then added, and stirring is carried out for 3 minutes (1000 rpm). The solid material is isolated by means of filtration, then stirred for 10 minutes (10,000 rpm) with a mixture of 70 g of tert.-butanol, 30 g of distilled water and 1 g of the above

20 polyethylene glycol sorbitan monooleate, and filtered again. Finally, the mixture is stirred for a further 10 minutes (10,000 rpm) with a mixture of 100 g of tert.-butanol and 0.5 g of the above polyethylene glycol sorbitan monooleate. After filtration, the catalyst is dried at 50°C and normal pressure until constant weight is reached.

25 Yield of dry, powdered catalyst: 5.8 g

Elemental analysis, thermogravimetric analysis and extraction:

cobalt = 10.1 %, zinc = 23.5 %, tert.-butanol = 3.3 %, polyethylene glycol sorbitan monooleate = 23.5 %

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Example B

Preparation of a DMC catalyst using a polyethylene glycol sorbitan trioleate (catalyst B).

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The procedure of Example A was followed, but polyethylene glycol(20) sorbitan trioleate (TWEEN 85®, Aldrich) was used instead of the polyethylene glycol sorbitan monooleate from Example A.

10 Yield of dry, powdered catalyst: 5.5 g

Elemental analysis, thermogravimetric analysis and extraction:

cobalt = 11.4 %, zinc = 24.0 %, tert.-butanol = 6.0 %, polyethylene glycol sorbitan trioleate = 12.1 %

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Example C

Preparation of a DMC catalyst using a polyethylene glycol sorbitan monolaurate (catalyst C).

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The procedure of Example A was followed, but polyethylene glycol(20) sorbitan monolaurate (TWEEN 20®, Sigma) was used instead of the polyethylene glycol sorbitan monooleate from Example A.

25 Yield of dry, powdered catalyst: 5.6 g

Elemental analysis, thermogravimetric analysis and extraction:

cobalt = 11.9 %, zinc = 24.9 %, tert.-butanol = 3.6 %, polyethylene glycol sorbitan monolaurate = 14.6 %

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Example D (comparison)

Preparation of a DMC catalyst using tert.-butanol without a polyalkylene glycol sorbitan ester (catalyst D, synthesis according to JP 4 145 123).

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A solution of 10 g (73.3 mmol) of zinc chloride in 15 ml of distilled water is added, with vigorous stirring (24,000 rpm), to a solution of 4 g (12 mmol) of potassium hexacyanocobaltate in 75 ml of distilled water. Immediately thereafter, a mixture of 50 g of tert.-butanol and 50 g of distilled water is added to the suspension which has formed, and vigorous stirring is then carried out for 10 minutes (24,000 rpm). The solid material is isolated by means of filtration, then stirred for 10 minutes (10,000 rpm) with 125 g of a mixture of tert.-butanol and distilled water (70/30; w/w), and filtered again. Finally, the mixture is stirred for a further 10 minutes (10,000 rpm) with 125 g of tert.-butanol. After filtration, the catalyst is dried at 50°C and normal pressure until constant weight is reached.

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Yield of dry, powdered catalyst: 3.08 g

Elemental analysis:

20 cobalt = 13.6 %, zinc = 27.4 %, tert.-butanol = 14.2 %

Preparation of polyether polyols**General procedure**

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50 g of polypropylene glycol starter (molecular weight = 1000 g/mol) and from 3 to 5 mg of catalyst (from 15 to 25 ppm, based on the amount of polyether polyol to be prepared) are placed under a protective gas (argon) in a 500 ml pressurised reactor and heated to 105°C, with stirring. Propylene oxide (approximately 5 g) is then metered in in a single batch until the total pressure has risen to 2.5 bar. No further propylene oxide is then metered in until an accelerated pressure drop in the reactor is observed. That accelerated pressure drop indicates that the catalyst is activated. The

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remaining propylene oxide (145 g) is then metered in continuously at a constant total pressure of 2.5 bar. When metering in of the propylene oxide is complete and after a subsequent reaction time of 2 hours at 105°C, volatile portions are distilled off at 90°C (1 mbar) and then cooled to room temperature.

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The resulting polyether polyols were characterised by determination of the OH numbers, the double bond contents and the viscosities.

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The progress of the reaction was monitored by means of time-conversion curves (propylene oxide consumption [g] vs. reaction time [min]). The induction time was determined from the point of intersection of the tangent at the steepest point of the time-conversion curve with the extended base line of the curve. The propoxylation times, which are of decisive importance for the catalyst activity, correspond to the period of time between activation of the catalyst (end of the induction time) and the end of propylene oxide metering. The total reaction time is the sum of the induction time and the propoxylation time.

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Example 1

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Preparation of polyether polyol using catalyst A (15 ppm)

induction time:	280 min
propoxylation time:	500 min
total reaction time:	780 min
polyether polyol:	OH number (mg of KOH/g): 31.6
	double bond content (mmol/kg): 9
	viscosity 25°C (mPas): 864

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Without removal of the catalyst, the metal content in the polyol is: Zn = 4 ppm, Co = 2 ppm.

Example 2

Preparation of polyether polyol using catalyst B (15 ppm)

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induction time:	375 min
propoxylation time:	385 min
total reaction time:	760 min
polyether polyol:	OH number (mg of KOH/g): 29.9
	double bond content (mmol/kg): 8
	viscosity 25°C (mPas): 1005

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Example 3

15 Preparation of polyether polyol using catalyst C (25 ppm)

induction time:	265 min
propoxylation time:	175 min
total reaction time:	440 min
20 polyether polyol:	OH number (mg of KOH/g): 30.2
	double bond content (mmol/kg): 8
	viscosity 25°C (mPas): 926

Example 4

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Catalyst D (15 ppm) exhibits no activity under the reaction conditions described above.

30 Examples 1 to 3 show that, on account of their markedly increased activity in the preparation of polyether polyols, the novel DMC catalysts according to the invention

can be used in such low concentrations that it is possible to dispense with separation of the catalyst from the polyol.

**Patent claims**

1. Double metal cyanide (DMC) catalyst containing
 - 5 a) one or more double metal cyanide compounds,
 - b) one or more organic complex ligands other than c), and
 - c) one or more polyalkylene glycol sorbitan esters.
- 10 2. DMC catalyst according to claim 1, additionally comprising d) water and/or
e) water-soluble metal salt.
- 15 3. DMC catalyst according to claim 1 or 2, wherein the double metal cyanide
compound is zinc hexacyanocobaltate(III).
4. DMC catalyst according to any one of claims 1 to 3, wherein the organic
complex ligand is tert.-butanol.
- 20 5. DMC catalyst according to any one of claims 1 to 4, wherein the catalyst
comprises from 1 to 80 wt.%, preferably from 1 to 40 wt.%, of a
polyalkylene glycol sorbitan ester.
- 25 6. DMC catalyst according to any one of claims 1 to 5, wherein the
polyalkylene glycol sorbitan ester is a polyethylene glycol sorbitan ester.
7. Process for the preparation of a DMC catalyst according to any one of
claims 1 to 6, comprising the steps:
 - 30 i) reacting in aqueous solution
 - α) metal salts with metal cyanide salts,

- β) organic complex ligands other than polyalkylene glycol sorbitan esters, and
- γ) polyalkylene glycol sorbitan esters,
- ii) isolating, washing and drying the catalyst obtained in step i).

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8. Process for the preparation of polyether polyols by polyaddition of alkylene oxides to starter compounds containing active hydrogen atoms, in the presence of one or more DMC catalysts according to any one of claims 1 to 6.

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9. Polyether polyol as prepared by the process according to claim 8.

10. Use of one or more DMC catalysts according to any one of claims 1 to 6 for the preparation of polyether polyols by polyaddition of alkylene oxides to starter compounds containing active hydrogen atoms.

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