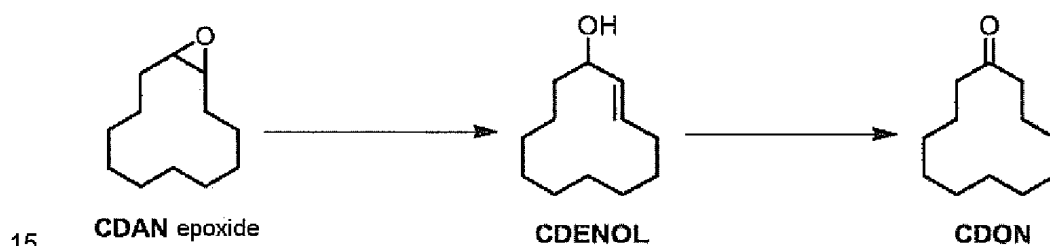


Process for preparing ketones from epoxides

The present invention relates to a process for preparing a ketone from an aliphatic or cycloaliphatic compound E containing at least one epoxy group,
 5 and to a process for synthesizing lactams.

The opening of oxirane rings with acidic or basic oxides is known (V.S. Joshi, N.P. Damodaran, S. Dev, *Tetrahedron* **1971**, 27, 459-474; K. Arata, K. Tanabe, *Bull. Chem. Soc. Jpn.* **1980**, 53, 299-303; K. Arata, H. Nakamura, Y. Nakamura, *Bull. Chem. Soc. Jpn.* **1994**, 67, 2351-2353). From a compound
 10 containing epoxy groups, such as monoepoxycyclododecane (CDAN epoxide), the allyl alcohol (3-cyclododecenol; CDENOL) is first obtained. This is followed by the conversion to the ketone (cyclododecanone; CDON).



The problem which occurs in this two-stage reaction is that, as well as the cyclic allyl alcohol, dehydrated dienes or dimers form as by-products.

20 A selective conversion of the epoxide to the ketone was reported by Chernyshkove and Mushenko (Chernyshkove, F.A.; Mushenko, D.V. *Neftekhimiya* **1976**, 16, 250-4). For this purpose, the epoxides were reacted in a hydrogen atmosphere over palladium and rhodium catalysts which were supported on alumina or carbon. With complete conversion of the reactant,
 25 the ketones were obtained with yields exceeding 80%.

EP-A-1090900 describes the reaction of CDAN epoxide to give a mixture of CDON and cyclododecanol (CDOL). For this purpose, platinum group metals, an inert support and a promoter are used. The reactions proceed in a

hydrogen atmosphere.

EP-A-1018498 discloses the reaction of cyclic epoxides with hydrogen and platinum group metals in a hydrogen atmosphere. This likewise gives a ketone/alcohol mixture. The hydrogen pressure is at least 1 bar. The document teaches that lower pressures would require an excessively long reaction time.

The problem thus addressed was that of adapting the production of ketones from epoxides such that a high proportion of ketone is obtained with a low alcohol content. In addition, by-products, especially unsaturated by-products, should form in a minimum concentration. Moreover, the reaction should be of lower technical complexity compared to the prior art. At the same time, the two-stage reaction to give the ketone should be possible without isolation of the allyl alcohol. The reaction times should correspond to the times in the prior art.

Accordingly, a process for preparing a ketone from a compound E containing at least one epoxy group using a mixture comprising at least one noble metal and at least one metal oxide as a catalyst system has been found, wherein the metal oxide comprises or consists of titanium dioxide, zirconium dioxide or mixtures of the two oxides. Zirconium dioxide is the preferred metal oxide.

In an aspect, there is provided a process for preparing a ketone, comprising: converting a compound E that comprises an epoxy group in the presence of a catalyst system to the ketone; wherein the catalyst system comprises a noble metal and a metal oxide, the metal oxide comprises at least one of titanium dioxide and zirconium dioxide, and a hydrogen pressure of the conversion is from 0 to 0.9 bar.

30

In another aspect, there is provided a method to convert a compound E which comprises an epoxy group to a ketone, comprising: conducting the conversion

in the presence of a catalyst system; the catalyst system comprising:
a noble metal and a metal oxide, wherein the catalyst system is selected from
the group of systems consisting of system I, system II and system III,
wherein the noble metal is at least one selected from the group consisting of
5 ruthenium, rhodium, palladium, osmium, iridium and platinum,
in system I the noble metal is unsupported and the metal oxide comprises at
least one of titanium dioxide and zirconium dioxide;
in system II the noble metal is supported, the noble metal support does not
comprise titanium dioxide or zirconium dioxide, and the system further
10 comprises at least one of titanium dioxide and zirconium dioxide; and
in system III the noble metal is supported on zirconium dioxide as the metal
oxide.

In another aspect, there is provided a process for synthesizing a lactam,
15 comprising: preparing a ketone as defined above; oximating the ketone to
obtain a ketoximine; and treating the ketoxime to effect a Beckmann
rearrangement and form the lactam.

The process according invention is a heterogeneous catalysis.

20

The compound E may be aliphatic or cycloaliphatic, preference being given to
cycloaliphatic compounds. Preferably 4 to 20 carbon atoms, more preferably 6
to 16 carbon atoms, especially preferably 8 to 14 carbon atoms, very
especially preferably 10 to 12 carbon atoms and especially 12 carbon atoms
25 are present.

The compound E may contain one or more epoxy groups, preference being

given to monoepoxy compounds.

In addition, the compound may be saturated or unsaturated. For example, one or two double bonds may be present.

5

Preferred compounds E are monoepoxycycloalkanes, monoepoxycycloalkanedienes and monoepoxycycloalkenes, particular preference being given to monoepoxycycloalkanes. A very particularly preferred compound E is monoepoxycyclododecane (CDAN epoxide).

10

It has been found that the formation of the corresponding alcohol as a by-product depends on the hydrogen pressure: with rising pressure, the alcohol content increases, and so the ketone selectivity decreases.

15 The process according to the invention can be executed at a hydrogen pressure of up to 8 bar, the hydrogen pressure being set preferably to 0 to 5 bar and more preferably to 0 to 2.5 bar. The hydrogen pressure is especially preferably 0 to 0.9 bar, very especially preferably 0 to 0.5 bar. The process according to the invention can be performed without hydrogen, but it is
20 preferable to initially charge at least a low hydrogen content to suppress unsaturated by-products. This may be 0.05 to 0.5 bar, preferably 0.1 to 0.4 bar.

A process without hydrogen or with a hydrogen pressure of not more than 0.9
25 bar is especially advantageous for catalyst systems comprising titanium dioxide.

The pressure figures given above are based on the partial pressure of hydrogen in the system. Typically, components of the reaction mixture,
30 including the solvent, air or inert gases such as nitrogen or argon, are further gaseous constituents of the system.

By virtue of the low hydrogen pressures, a much lower level of technical complexity is necessary compared to the prior art, especially in the suitable apparatus, for being able to work with hydrogen. The particular advantage of the invention is that the ketone can be obtained in high yields without the
5 presence of hydrogen.

The temperature during the reaction is preferably set to a range from 100 to 350°C, preferably 175 to 275°C and more preferably between 200 and 250°C. The reaction can be conducted with a compound E in the liquid or gaseous
10 state.

The noble metal in the catalyst system is preferably selected from ruthenium, rhodium, palladium, osmium, iridium and platinum, preference being given to ruthenium, palladium and platinum, and particular preference to palladium.
15 The noble metal may be in the form of powder (unsupported) or in supported form. Elemental noble metals or oxides thereof, for example, are suitable in powder form.

In addition, at least one metal oxide is present as a further constituent of the
20 catalyst system. The metal oxide in the catalyst system comprises titanium dioxide, zirconium dioxide or mixtures thereof, or consists of at least one of the aforementioned oxides. These also include titanium dioxide- or zirconium dioxide-doped or -coated substances such as alumina or silica.

25 The metal oxide in the catalyst system may function as a support for the noble metal in the catalyst system. The noble metal may optionally be applied to an alternative support selected, for example, from alumina, silica or activated carbon. Titanium dioxide or zirconium dioxide are preferred supports.

30 The metal oxides in the catalyst system and the alternative supports may be in the form of powders or shaped bodies. Suitable shaped bodies are spheres, extrudates, tablets, granules and pellets. It is preferable that the

supports of the noble metal are in the form of shaped bodies. It is likewise preferable that the metal oxide in the catalyst system, if it does not function as a support, is in the form of shaped bodies.

- 5 Irrespective of whether or not the noble metal is supported and which support is used, it is essential to the invention that at least one metal oxide is present in the catalyst system.

The catalyst system may consequently independently be present as one of
10 the following system forms:

- I) The noble metal is unsupported; the metal oxide present in the catalyst system is at least titanium dioxide or zirconium dioxide;
- 15 II) the noble metal is supported, where the support does not comprise or consist of titanium dioxide and/or zirconium dioxide. The system additionally comprises at least one metal oxide selected from titanium dioxide and zirconium dioxide.
- III) The noble metal is supported on a metal oxide selected from titanium dioxide and zirconium dioxide.

- 20 System forms II and III are preferred, system form III being particularly preferred.

Suitable titanium dioxide as a metal oxide in the catalyst system can be obtained by the sulphate process, the chloride process, or by flame hydrolysis
25 (pyrogenic process) of titanium tetrachloride. All the processes are known to those skilled in the art. Suitable polymorphs are rutile and anatase, and the titanium dioxide used may comprise mixtures of the polymorphs mentioned.

The titanium dioxide prepared by the sulphate or chloride process may give
30 an acidic reaction in water, the compounds typically having a pH of 3 or less (acidic titanium dioxide). Acidic titanium dioxide likewise usually contains more than 5% by weight, based on the total weight of the titanium dioxide

support, of substances such as titanyl sulphate or titanyl hydroxide. A titanium dioxide based on an acidic titanium dioxide is commercially available as Aerolyst 7750 (Evonik, Germany). Acidic titanium oxide is less preferred for the present process. In other words, it is preferable not to use acidic titanium dioxide. Suitable nonacidic titanium dioxide, which is preferred, exhibits a pH of 5 or more in water.

Particularly preferred titanium dioxide is obtained by means of flame pyrolysis, as described, for example, in DE-A-830786.

10

Suitable titanium dioxide is obtainable under the Aeroxide P25 titanium dioxide (powder) or Aerolyst 7711 (shaped bodies) name from Evonik, Germany, and Hombikat M234 (shaped bodies) from Sachtleben, Germany.

15 Zirconium dioxide (zirconium(IV) oxide) is obtainable, for example, from zirconium hydroxide, by calcining it at more than 200°C, for example at 350°C. The zirconium dioxide may be doped, for example, with yttrium oxide.

Suitable zirconium dioxide is monoclinic or tetragonal. Mixtures of these polymorphs are possible.

20

The metal oxide in the catalyst system may have an average bulk density of 0.5 to 2 g/cm³.

25 The metal oxide in the catalyst system may have a BET surface area of at least 5 m²/g.

The proportion of noble metal, based on the total weight of noble metal and support, may be 0.01 to 5% by weight, preferably 0.05 to 1.2% by weight and more preferably 0.1 to 0.6% by weight.

30

The noble metal may be distributed on or within the support.

The molar proportion of noble metal, based on the molar amount of the compound E, may be 0.00001 to 0.1, preferably 0.0001 to 0.01.

- 5 The molar proportion of metal oxide in the catalyst system, based on the molar amount of the compound E, may be 0.01 to 100, preferably 0.01 to 10.

The process according to the invention can be conducted in organic solvents, though it is preferable to work without solvents and hence not to use any
 10 organic solvent. Suitable solvents are, for example, alkanes such as n-hexane, n-heptane, n-tetradecane and cyclohexane; ethers such as tetrahydrofuran and dioxane; alkanols such as methanol, ethanol and t-butanol; esters such as ethyl acetate and butyl acetate. The solvents themselves may be used alone or in mixtures. The solvent is preferably used
 15 in an amount of 20 times or less, preferably 10 times or less, the weight of the compound E.

The process according to the invention can be executed continuously or batchwise.

20

The ketone can be purified by distillation, crystallization or recrystallization.

It is preferable that the process according to the invention is performed without a promoter component. The promoter component may be a member
 25 which is selected from the elements of group VIII, of group Ib, of group IIb, of group IIIb, of group IVb, of group Vb, of group VIb and of group VIIb, lanthanide elements, and compounds of the aforementioned elements. Corresponding promoter components are described in EP-A-1090900. The aforementioned metal oxides in the catalyst system or alternative supports are
 30 not regarded as promoter components.

In a preferred embodiment of the invention, CDAN epoxide is converted to

CDON without solvent at temperatures of 200 to 250°C, the catalyst used being a palladium-zirconium dioxide having a palladium content of 0.1 to 0.6% by weight, based on the total weight of the catalyst. In the reaction, a maximum of 0.9 bar of hydrogen, most preferably a maximum of 0.5 bar, is used.

The invention further comprises a catalyst system comprising noble metal and metal oxide, wherein

- I) the noble metal is unsupported; the metal oxide present in the catalyst system is at least titanium dioxide or zirconium dioxide;
- II) the noble metal is supported, and wherein the support does not comprise or consist of titanium dioxide and/or zirconium dioxide; the system additionally comprises at least one metal oxide selected from titanium dioxide and zirconium dioxide;
- III) the noble metal is supported on a metal oxide selected from titanium dioxide and zirconium dioxide.

In catalyst system III, zirconium dioxide is preferred.

The invention further provides for the use of at least one inventive catalyst system for catalysis of a reaction in which at least one compound E is converted to the corresponding ketone derivative.

The invention further provides a process for synthesizing lactams (inventive lactam process), in which the aforementioned process according to the invention for preparing ketones is employed. The compound E is preferably selected from aliphatic monoepoxycycloalkanes, aliphatic monoepoxycycloalkane-dienes and aliphatic monoepoxycycloalkenes, preference being given to monoepoxycycloalkanes.

If the ketone is in a mixture with the corresponding alcohol derivative, the alcohol can be dehydrogenated to the ketone. Subsequently, the ketone can be oximated. In the next step, the Beckmann rearrangement to give the

lactam can be effected, in which case the rearrangement can be effected by means of sulphuric acid or cyanuric chloride. The lactams can be processed further by polycondensation to give polyamides.

- 5 The dehydrogenation, the oximation, the Beckmann rearrangement and the condensation reaction are known to those skilled in the art.

In a preferred embodiment of the inventive lactam process, laurolactam is prepared from monoepoxycyclododecane (i.e. cyclododecane epoxide or 1,2-
10 cyclododecane epoxide).

In the context of the preferred lactam process, cyclododecane epoxide can be obtained by the following reaction steps: 1,3-butadiene is converted by cyclotrimerization to cyclododecatriene. This is followed by hydrogenation to
15 give the cyclododecene. Subsequent epoxidation gives the cyclododecane epoxide. The person skilled in the art in the field of synthesis of organic compounds can prepare other aliphatic and cycloaliphatic compounds E in analogy to the synthesis of cyclododecane epoxide.

20 Even without any further details, it is assumed that a person skilled in the art can utilize the above description to the broadest extent. The preferred embodiments and examples should therefore be regarded merely as descriptive disclosure which is not limiting in any way whatsoever.

25 The present invention is illustrated in detail hereinafter by examples. Alternative embodiments of the present invention are obtainable in an analogous manner.

Examples

The percentage figure in the case of catalysts indicates the proportion by weight of the noble metal based on the total weight of the catalyst including noble metal and support. The abbreviation "calc." stands for "calcined". The abbreviations for the substances are: CDAN: cyclododecane; CDEN: cyclododecene; ECD: epoxycyclododecane; CDON: cyclododecanone; CDOL: cyclododecanol; CDENOL: cyclododecen-3-ol.

Example 1: Alumina support (prior art)

The reaction was conducted in a mechanically stirred 500 ml round-bottom flask. The reactor was heated with an electrical aluminium heating block and the internal temperature was monitored with a temperature sensor. The flask was charged with 50 ml of 1,2-cyclododecane epoxide and 10 g of catalyst, supported on alumina in the form of shaped bodies. The catalyst bed lay on the base of the flask and the liquid reaction mixture was stirred over the bed. The flask was subsequently inertized with nitrogen and heated to internal temperature 215°C. The temperature was maintained over 5 hours.

Table 1. Composition (area%, GC) of the reaction mixture (5 h)

Catalyst	Support	Conversion (%)	Selectivity (%)				
			CDAN	CDEN	CDON	CDOL	CDENOL
Ru/Al ₂ O ₃ 1.5%	γ -Al ₂ O ₃	99	0.2	5	71	7	1.3
Pd/Al ₂ O ₃ 0.5%	γ -Al ₂ O ₃	100	1	4	75	6	0

Example 2: Various metals and supports (inventive)

The reaction was conducted in a mechanically stirred 500 ml round-bottom flask. The reactor was heated with an electrical aluminium heating block and the internal temperature was monitored with a temperature sensor. The flask was charged with 50 ml of 1,2-cyclododecane epoxide and 10 g of catalyst system III (noble metal supported on titanium dioxide or zirconium dioxide, each in the form of shaped bodies). The catalyst bed lay on the base of the flask and the liquid reaction mixture was stirred over the bed. The flask was

subsequently inertized with nitrogen and heated to internal temperature 215°C. The temperature was maintained over 5 hours.

Table 2. Composition (area%, GC) of the reaction mixture (5 h)

Catalyst	Support	Conversion (%)	Selectivity (%)				
			CDAN	CDEN	CDON	CDOL	CDENOL
Ru/TiO ₂ 1.0%	Aerolyst® 7711	89	0	3	86	4	0.6
Pd/TiO ₂ 0.5%	Aerolyst® 7711	93	0.4	1	90	3	0
Pd/ZrO ₂ 0.5%	from Zr(OH) ₄ 350°C calc.	90	0	0	96	3	0
Pd/ZrO ₂ 0.5%	<i>t</i> -ZrO ₂ , 8% Y ₂ O ₃	94 ^(a)	0.2	0	94	3	0.3

5 (a) 30 g of catalyst and T = 235°C

Example 3: Mixture of catalysts (inventive)

The reaction was conducted in a mechanically stirred 500 ml round-bottom flask. The reactor was heated with an electrical aluminium heating block and the internal temperature was monitored with a temperature sensor. The flask was charged with 50 ml of 1,2-cyclododecane epoxide, 10 g of supported noble metal (0.5% by weight of palladium on silica in the form of shaped bodies) and 10 or 20 g of metal oxide of the catalyst system (shaped bodies) (catalyst system II). The catalyst bed lay on the base of the flask and the liquid reaction mixture was stirred over the bed. The flask was subsequently inertized with nitrogen and heated to internal temperature 215°C. The temperature was maintained over 5 hours.

Table 3. Composition (area%, GC) of the reaction mixture (5 h)

Catalyst (10 g)	Oxide	Conversion (%)	Selectivity (%)				
			CDAN	CDEN	CDON	CDOL	CDENOL
Pd/SiO ₂ 0.5%	---	7	0	0	97	0	0
	10 g TiO ₂ <i>Aerolyst®</i> 7711	>99	0.3	2	90	2	0
	10 g TiO ₂ <i>Hombikat</i> M234	>99	0.6	12	77	0.7	0
	20 g m-ZrO ₂ <i>m-ZrO₂</i>	68	<0.1	0	98	1	0
	20 g ZrO ₂ <i>from</i> <i>Zr(OH)₄</i> <i>350°C calc.</i>	>99	0	0	95	3	0

* not in accordance with the invention

Example 4: Reaction with full conversion (inventive)

- 5 The reaction was conducted in a mechanically stirred 500 ml round-bottom flask. The reactor was heated with an electrical aluminium heating block and the internal temperature was monitored with a temperature sensor. The flask was charged with 50 ml of 1,2-cyclododecane epoxide and catalyst (palladium on titanium dioxide in the form of shaped bodies or on zirconium dioxide in the
- 10 form of shaped bodies; catalyst system III). The catalyst bed lay on the base of the flask and the liquid reaction mixture was stirred over the bed. The flask was subsequently inertized with nitrogen and heated to the desired internal temperature. The temperature was maintained over the given time until a full conversion of the epoxide was attained.

Table 4. Composition (area%, GC) of the reaction mixture (5 h)

Catalyst	Support	Temp. (°C)	Time (h)	Yield (%)				CDON + CDOL
				CDAN	CDEN	CDON	CDOL	
20 g Pd/TiO ₂ 0.5%	Aerolyst® 7711	215	5	0.7	1.7	92.1	2.1	94.2
10 g Pd/TiO ₂ 0.5%	Aerolyst® 7711	215	10*	1.8	0	95.7	2.5	98.2
30 g Pd/ZrO ₂ 0.5%	<i>t</i> -ZrO ₂ with 8% by weight Y ₂ O ₃	235	10	0.2	0	96.2	3.4	99.6
30 g Pd/ZrO ₂ 0.5%	from Zr(OH) ₄ 350°C calc.	235	5	0.5	0.5	93.5	5.5	99
10 g Pd/ZrO ₂ 0.5%	from Zr(OH) ₄ 350°C calc.	235	10	0.3	0.1	95.3	2.9	98.2

* H₂/N₂ mixture (1 bar with 90% by volume of H₂ and 10% by volume of N₂) was fed in during the last hour of the reaction.

5 Example 5: Reaction with various hydrogen pressures (inventive)

The reaction was conducted in a 100 ml autoclave with a magnetic stirrer. The reactor was heated with a 200°C oil bath. The autoclave was charged with 20 ml of 1,2-cyclododecane epoxide and 4 g of catalyst system III (palladium, supported on titanium dioxide powder (mortar-ground Aerolyst® 7711 support)). It was inertized with nitrogen, heated to the desired internal temperature and then pressurized with hydrogen up to the desired pressure. The oil temperature was maintained over 24 h.

Table 5. Composition (area%, GC) of the reaction mixture (5 h)

Catalyst (4 g)	H ₂ pressure (bar)	Conversion (%)	Selectivity (%)				
			CDAN	CDEN	CDON	CDOL	CDENOL
Pd/TiO ₂ 0.5%	0	83	0.4	0	97	2	0
	3	91	0.8	0	87	12	0
	5	94	1.6	0	67	31	0
	7	89	1.1	0	59	39	0

Example 6: Mixture of Pd powder and TiO₂ (inventive)

The reaction was conducted in a mechanically stirred 500 ml round-bottom flask. The reactor was heated with an electrical aluminium heating block and the internal temperature was monitored with a temperature sensor. The flask was charged with 50 ml of 1,2-cyclododecane epoxide, 10 g of TiO₂ powder and palladium(II) oxide powder as noble metal (catalyst system I). The catalyst bed lay on the base of the flask and the liquid reaction mixture was stirred over the bed. The flask was subsequently inertized with nitrogen and heated to internal temperature 215°C. The temperature was maintained over 5 hours.

Table 6. Composition (area%, GC) of the reaction mixture (5 h)

Metal oxide	Noble metal	Conversion (%)	Selectivity (%)				
			CDAN	CDEN	CDON	CDOL	CDENOL
---*	0.12 g PdO (powder)	no conversion					
10 g TiO ₂ Aerolyst® 7711	none	90	0	6	3	0	84
10 g TiO ₂ Aerolyst® 7711	0.12 g PdO powder	79	0	5	46	0	22
10 g TiO ₂ Aerolyst® 7711	0.76 g PdO powder	91	0	9	68	3	1

* not in accordance with the invention

Example 7: Reaction with ZrO₂ powder (inventive)

The reaction was conducted in a mechanically stirred 500 ml round-bottom flask. The reactor was heated with an electrical aluminium heating block and the internal temperature was monitored with a temperature sensor. The flask was charged with 50 ml of 1,2-cyclododecane epoxide and the catalyst system. The Pd/SiO₂ catalyst bed lay – where present – on the base of the flask. The liquid reaction mixture comprising ZrO₂ powder or Pd supported on ZrO₂ (powder) was stirred over the bed. The flask was subsequently inertized with nitrogen and heated to internal temperature 215°C. The temperature was maintained over 5 hours.

Table 7. Composition (area%, GC) of the reaction mixture (5 h)

Catalyst system	Conversion (%)	Selectivity (%)				
		CDAN	CDEN	CDON	CDOL	CDENOL
10 g Pd/SiO ₂ 0.5% (extrudate) + 20 g ZrO ₂ (powder, 300°C calcined) (system II)	> 99	0	0	95	3	0
10 g Pd/SiO ₂ 0.5% (extrudate) + 10 g ZrO ₂ (powder, 300°C calcined) (system II)	75	0	0	92	2	0
10 g Pd/ZrO ₂ 0.5% (powder, 300°C calcined) (system III)	75	0	0	96	2	0

Example 8: Continuous process (inventive)

- 5 The reaction was conducted in a continuously operated plant. The plant consisted of a fixed bed reactor (catalyst bed approx. 100 ml) and a steel reservoir vessel (1 l) with level measurement. The fixed bed reactor was charged with 100 g of Pd/ZrO₂ (0.5%; system III), and the vessel with 950 g of CDAN epoxide. The liquid was pumped in circulation from the reservoir
- 10 through the catalyst bed and back into the reservoir vessel by means of a circulation pump (21 l/h). The reactor was heated to the desired internal temperature in the reaction mixture with an electrical heater. Once a conversion of 80% had been attained, fresh feed (CDAN epoxide) was metered into the plant. The product was discharged continuously from the
- 15 plant, such that the fill level in the reservoir vessel remained constant. The reaction mixture was passed through the fixed bed and the vessel with nitrogen. The reaction was conducted without hydrogen (Table 8, line 1) and with hydrogen (partial pressure 0.25 bar; Table 8, line 2).

Table 8. Composition (area%, GC) of the reaction mixture

Pressure	Temp (°C)	Feed (g/h)	Conver- sion (%)	Selectivity (%)				
				CDAN + CDEN	CDON	CDOL	CDEN- ON	CDEN- OL
1.1 bar N ₂ 0 bar H ₂	215	12	80.4	3.2	89	1.7	3.2	2.1
1.4 bar N ₂ 0.25 bar H ₂	205	34	84.7	9.2	84	5.1	0	0.1

Claims

1. A process for preparing a ketone, comprising:
converting a compound E that comprises an epoxy group in the presence of a
5 catalyst system to the ketone; wherein the catalyst system comprises a noble
metal and a metal oxide,
the metal oxide comprises at least one of titanium dioxide and zirconium dioxide, and
a hydrogen pressure of the conversion is from 0 to 0.9 bar.
- 10 2. The process according to claim 1, wherein the compound E is a cycloaliphatic
compound.
3. The process according to claim 1, wherein the noble metal is selected from the
group consisting of ruthenium, palladium and platinum.
- 15 4. The process according to claim 1, wherein the compound E comprises four to
twenty carbon atoms.
5. The process according to claim 1, wherein the hydrogen pressure is from 0 to 0.5
20 bar.
6. The process according to claim 1, wherein the catalyst system is selected from the
group of systems consisting of system I, system II and system III,
wherein
25 in system I the noble metal is unsupported and the metal oxide comprises at least
one of titanium dioxide and zirconium dioxide;
in system II the noble metal is supported, the noble metal support does not comprise
titanium dioxide or zirconium dioxide, and the system further comprises at least one
of titanium dioxide and zirconium dioxide; and
30 in system III the noble metal is supported on zirconium dioxide as the metal oxide.
7. The process according to claim 1, wherein the process is conducted without
hydrogen.

8. A method to convert a compound E which comprises an epoxy group to a ketone, comprising:

conducting the conversion in the presence of a catalyst system;

the catalyst system comprising:

5 a noble metal and

a metal oxide, wherein the catalyst system is selected from the group of systems consisting of system I, system II and system III,

wherein

the noble metal is at least one selected from the group consisting of ruthenium,

10 rhodium, palladium, osmium, iridium and platinum,

in system I the noble metal is unsupported and the metal oxide comprises at least one of titanium dioxide and zirconium dioxide;

in system II the noble metal is supported, the noble metal support does not comprise titanium dioxide or zirconium dioxide, and the system further comprises at least one

15 of titanium dioxide and zirconium dioxide; and

in system III the noble metal is supported on zirconium dioxide as the metal oxide.

9. A process for synthesizing a lactam, comprising:

preparing a ketone according to the process of claim 1;

20 oximating the ketone to obtain a ketoximine; and

treating the ketoxime to effect a Beckmann rearrangement and form the lactam.

10. The process according to claim 9, wherein the compound E is 1,2-cyclododecane epoxide.

25