



166166

27 MAR 2002

ELASTOMER COMPOSITE BLENDS AND METHODS FOR PRODUCING THEM



G00K002

Field of the Invention

5 The present invention is directed to novel methods for producing elastomer composite blends and to novel elastomer composite blends produced using such methods. More particularly, the invention is directed to methods for producing elastomer composite blends having particulate filler finely dispersed in elastomer, and to elastomer composite blends such as curative-free compositions, curative-bearing
10 compositions, and vulcanized rubber materials and products formed of such compositions.

Background

Numerous products of commercial significance are formed of elastomeric compositions wherein particulate filler is dispersed in any of various synthetic
15 elastomers, natural rubber or elastomer blends. Carbon black, for example, is widely used as a reinforcing agent in natural rubber and other elastomers. It is common to produce a masterbatch, that is, a premixture of filler, elastomer and various optional additives, such as extender oil, and then in some cases to blend such masterbatch with additional elastomer in a subsequent mixing step. Carbon black masterbatch is
20 prepared with different grades of commercially available carbon black which vary both in surface area per unit weight and in "structure." Numerous products of commercial significance are formed of such elastomeric compositions of carbon black particulate filler dispersed in natural rubber. Such products include, for example, vehicle tires

wherein different elastomeric compositions may be used for the tread portion, sidewalls, wire skim and carcass. Other products include, for example, engine mount bushings, conveyor belts, windshield wipers and the like. While a wide range of performance characteristics can be achieved employing currently available materials and manufacturing techniques, there has been a long standing need in the industry to develop elastomeric compositions having improved properties and to reduce the cost and complexity of current manufacturing techniques. In particular, it is known for example that macro-dispersion level, that is, the uniformity of dispersion of the carbon black or other filler within the elastomer, can significantly impact performance characteristics. For elastomeric compositions prepared by intensively mixing the carbon black or other filler with natural rubber or other elastomer (such as in a Banbury mixer or the like), any increase in macro-dispersion requires longer or more intensive mixing, with the consequent disadvantages of increased energy costs, manufacturing time, and similar concerns. For carbon black fillers of certain surface area and structure characteristics, dispersion beyond a certain degree has not been possible or commercially practicable using known mixing apparatus and techniques. In addition, such prolonged or more intensive mixing degrades the natural rubber by disruption of the polymeric chains of the natural rubber elastomer, and so reduces its molecular weight, rendering the finished elastomeric compound undesirable for certain applications. For use in tire tread, for example, reduced molecular weight is known to cause an undesirable increase in the so-called rolling resistance of the tire.

It is well known to employ carbon blacks having higher or lower structure and surface area to manipulate the performance characteristics of an elastomeric composition. Carbon blacks of higher surface area and lower structure are known to

improve crack growth resistance and cut-and-chip resistance as well as, generally, abrasion resistance, and other performance qualities. Commercially available mixing techniques have been unable to achieve excellent uniformity of dispersion of carbon blacks throughout the elastomer, however, without unacceptable degradation of the natural rubber. In fact, for typical carbon black loading levels in natural rubber, such as 45 phr to 75 phr, and oil loading from 0 phr to 10 phr, low structure carbon blacks, such as carbon blacks of DBPA less than 110cc/100g, particularly those having surface area above about $45\text{m}^2/\text{g}$ to $65\text{m}^2/\text{g}$ (CTAB), it has not been possible to achieve compounds having less than about 1% undispersed carbon black (measured as macro-dispersion, as described below) regardless of the duration and intensity level of mixing.

Furthermore, while theoretical analysis has indicated desirable improvements in certain performance characteristics of elastomeric compositions employing carbon blacks of higher surface area and lower structure, it has not been possible using known physical milling or other mastication processes to obtain such elastomeric compositions in which both the molecular weight of the natural rubber is well preserved and satisfactory macro-dispersion levels of the carbon black are achieved. Generally, it has been found, for example, that the elastomer reinforcing properties of a carbon black increase as the particle size of the carbon black decreases. However, with extremely fine carbon blacks an anomalous condition is known to be encountered, in which the expected improvement in properties is not achieved. This is understood to be due at least in part to the inability of conventional elastomer compounding methods to adequately disperse the carbon black in the natural rubber without undue breakdown of the elastomer polymer. There has been, therefore, consequent inability to take full

advantage of the natural affinity of the carbon black and the natural rubber for each other in the case of such carbon blacks.

Since good dispersion of carbon black in natural rubber compounds has been recognized for some time as one of the most important objectives for achieving good quality and consistent product performance, considerable effort has been devoted to the development of procedures for assessing dispersion quality in rubber. Methods developed include, e.g. the Cabot Dispersion Chart and various image analysis procedures. Dispersion quality can be defined as the state of mixing achieved. An ideal dispersion of carbon black is the state in which the carbon black agglomerates (or pellets) are broken down into aggregates (accomplished by dispersive mixing) uniformly separated from each other (accomplished by distributive mixing), with the surfaces of all the carbon black aggregates completely wetted by the rubber matrix (usually referred to as incorporation).

Common problems in the rubber industry which are often related to poor macro-dispersion can be classified into four major categories: product performance, surface defects, surface appearance and dispersion efficiency. The functional performance and durability of a carbon black-containing rubber formulation, such as tensile strength, fatigue life and wear resistance, are affected substantially by macro-dispersion quality. Undispersed carbon black can also cause surface defects on finished products, including visible defects. Eliminating the presence of surface defects is of critical importance in molded thin parts for functional reasons and in extruded profiles for both aesthetic and functional reasons.

A commercial image analyzer such as the IBAS Compact model image analyzer available from Kontron Elektronik GmbH (Munich, Germany) can be used to measure

macro-dispersion of carbon black or other filler. Typically, in quantitative macro-dispersion tests used in the rubber industry, the critical cut-off size is 10 microns. Defects larger than about 10 microns in size typically consist of undispersed black or other filler, as well as any grit or other contaminants, which can affect both visual and functional performance. Thus, measuring macro-dispersion involves measuring defects on a surface (generated by microtoming, extrusion or cutting) greater than 10 microns in size by total area of such defects per unit area examined using an image analysis procedure. Macro-dispersion D(%) is calculated as follows:

$$\% \text{ Undispersed area (\%)} = \frac{1}{A_m} \sum_{i=1}^m N_i \frac{\pi D_i^2}{4}$$

where A_m = Total sample surface area examined

N_i = Number of defects with size D_i

D_i = Diameter of circle having the same area as that of the defect (equivalent circle diameter).

m = number of images

Macro-dispersion of carbon black or other filler in uncured natural rubber or other suitable elastomer can be assessed using image analysis of cut surface samples. Typically, five to ten arbitrarily selected optical images are taken of the cut surface for image analysis. Knife marks and the like preferably are removed using a numerical filtering technique. Cut surface image analysis thus provides information regarding the carbon black dispersion quality inside a natural rubber compound. Specifically, percent undispersed area D(%) indicates carbon black macro-dispersion quality. As macro-dispersion quality is degraded, percent undispersed area increases. Dispersion

quality can be improved, therefore, by reducing the percent undispersed area. As noted above, the mixing operations have a direct impact on mixing efficiency and on macro-dispersion. In general, better carbon black macro-dispersion is achieved in the elastomer, for example in a natural rubber masterbatch, by longer mixing and by more intensive mixing. Unfortunately, however, achieving better macro-dispersion by longer, more intensive mixing, degrades the elastomer into which the carbon black is being dispersed. This is especially problematic in the case of natural rubber, which is highly susceptible to mechanical/thermal degradation. Longer and more intensive mixing, using known mixing techniques and apparatus, such as a Banbury mixer, reduces the molecular weight of the natural rubber masterbatch-composition. Thus, improved macro-dispersion of carbon black in natural rubber is known to be achieved with a corresponding, generally undesirable reduction in the molecular weight of the rubber.

In addition to dry mixing techniques, it is known to continuously feed latex and a carbon black slurry to an agitated coagulation tank. Such "wet" techniques are used commonly with synthetic elastomer, such as SBR. The coagulation tank contains a coagulant such as salt or an aqueous acid solution typically having a pH of about 2.5 to 4. The latex and carbon black slurry are mixed and coagulated in the coagulation tank into small beads (typically a few millimeters in diameter) referred to as wet crumb. The crumb and acid effluent are separated, typically by means of a vibrating shaker screen or the like. The crumb is then dumped into a second agitated tank where it is washed to achieve a neutral or near neutral pH. Thereafter the crumb is subjected to additional vibrating screen and drying steps and the like. (An early method of mixing rubber latex and foreign substance, such as carbon black, dispersed in a suitable liquid, is discussed in U.S. Patent No. 1,611,278 issued to Peterson on 21 December 1926. The mixture is said to be subjected to mechanical agitation with or without heating or superheating and optionally with soap, dilute glue or the like, to achieve coagulation.) Variations on this method have been suggested for the coagulation of natural and synthetic elastomers. In U.S.

patent 4,029,633 to Hagopian et al, which like the present invention is assigned to Cabot Corporation, a continuous process for the preparation of elastomer masterbatch is described. An aqueous slurry of carbon black is prepared and mixed with a natural or synthetic elastomer latex. This mixture undergoes a so-called creaming operation, optionally using any of various known creaming agents. Following the creaming of the carbon black/latex mixture, it is subjected to a coagulation step. Specifically, the creamed carbon black/latex mixture is introduced as a single coherent stream into the core of a stream of coagulating liquor. The solid stream of creamed carbon black/latex mixture is said to undergo shearing and atomizing by the stream of coagulating liquor prior to coagulation, being then passed to a suitable reaction zone for completion of the coagulation. Following such coagulation step, the remainder of the process is substantially conventional, involving separation of the crumb from the waste product "serum" and washing and drying of the crumb. A somewhat similar process is described in U.S. patent 3,048,559 to Heller et al. An aqueous slurry of carbon black is continuously blended with a stream of natural or synthetic elastomer or latex. The two streams are mixed under conditions described as involving violent hydraulic turbulence and impact. As in the case of the Hagopian et al patent mentioned above, the combined stream of carbon black slurry and elastomer latex is subsequently coagulated by the addition of an acid or salt coagulant solution.

There has long been a need in various industries for elastomeric compounds of particulate filler dispersed in suitable elastomer having improved macro-dispersion, especially, for example, carbon black dispersed in natural rubber blended with another elastomer. As discussed above, improved macro-dispersion can provide correspondingly improved aesthetic and functional characteristics. Especially desirable

are new elastomeric compounds of carbon black in a blend of natural rubber and synthetic elastomer, wherein improved macro-dispersion is achieved together with higher molecular weight of the natural rubber. It is an object of the present invention to meet some or all of these long felt needs.

5

Summary of the Invention

In accordance with a first aspect, a method for preparing elastomer composite blends comprises first preparing elastomer masterbatch by feeding simultaneously a particulate filler fluid and an elastomer latex fluid to a mixing zone of a coagulum reactor. Preferably, the coagulum reactor has an elongate coagulum zone extends from the mixing zone, most preferably having a progressively increasing cross-sectional area in the downstream direction toward a discharge end of the coagulum reactor. The elastomer latex may be either natural or synthetic and the particulate filler fluid comprises carbon black or other particulate filler effective to coagulate the latex. The particulate filler fluid is fed to the mixing zone preferably as a continuous, high velocity jet of injected fluid, while the latex fluid is fed at low velocity. The velocity, flow rate and particulate concentration of the particulate filler fluid are sufficient to cause mixture with high shear of the latex fluid and flow turbulence of the mixture within at least an upstream portion of the coagulum zone so as to substantially completely coagulate the elastomer latex with the particulate filler prior to the discharge end. Substantially complete coagulation can thus be achieved, in accordance with preferred embodiments, without the need of employing an acid or salt coagulation agent. The coagulated product of such wet mixing step then is dry mixed with additional elastomer to form an elastomer composite blend. Such additional elastomer

10

15

20

may be the same as, or different from, the elastomer used in the wet mixing step. Optionally, additional filler can be added during the dry mixing step. Such additional filler can be the same as, or different from, the particulate filler used in the wet mixing step.

5 In accordance with yet another aspect, elastomer composite blends are provided as a product of the process disclosed here. In accordance with preferred embodiments, novel elastomer composite blends are provided having macro-dispersion level of the particulate filler, molecular weight of the elastomer, particulate loading level, choice of particulate filler (including, for example, carbon black fillers of exceptionally high
10 surface area and low structure) and/or other characteristics not previously achieved. In that regard, preferred elastomer composite blends disclosed here have excellent macro-dispersion, even of certain fillers, such as carbon blacks having a structure to surface area ratio DBP:CTAB less than 1.2 and even less than 1, in elastomers such as natural rubber, etc. with little or no degradation of the molecular weight of the
15 elastomer. In accordance with yet other aspects of the invention, intermediate products are provided as well as final products which are formed of the elastomer composite blends produced by the method disclosed here. Macro-dispersion here means the macro-dispersion D(%) of the particulate filler measured as percent undispersed area for defects larger than 10 microns. In elastomer composite blends disclosed here
20 comprising natural rubber, the molecular weight of the natural rubber, that is, the MW_{sol} (weight average) of the sol portion, preferably is at least about 300,000, more preferably at least about 400,000, being in certain preferred embodiments between 400,000 and 900,000. The elastomer composite blends optionally comprise extender oil, such as about 0 to 20 phr, more preferably about 0 to 10 phr extender oil, and/or

other ingredients such as are well known for optional use in compounding natural rubber and/or other elastomers with carbon black and/or other fillers. As discussed further below in connection with certain preferred and exemplary embodiments, the novel elastomer composite blends disclosed here can provide highly desirable physical properties and performance characteristics. Accordingly, the invention presents a significant technological advance.

These and other aspects and advantages of various embodiments of the invention will be further understood in view of the following detailed discussion of certain preferred embodiments.

10

Brief Description of the Drawings

The following discussion of certain preferred embodiments will make reference to the appended drawings wherein:

Fig. 1 is a schematic flow chart illustration of the apparatus and method for preparing elastomer masterbatch in accordance with certain preferred embodiments;

15

Fig. 2 is an elevation view, partly schematic, of a preferred embodiment consistent with the schematic flow chart illustration of Fig. 1;

Fig. 3 is an elevation view, partially schematic, of an alternative preferred embodiment consistent with the schematic flow chart illustration of Fig. 1;

20

Fig. 4 is an elevation view, partially in section, of the mix head/coagulum reactor assembly of the embodiment of Fig. 3;

Fig. 5 is an elevation view, partially in section, corresponding to the view of Fig. 4, illustrating an alternative preferred embodiment;

Fig. 6 is a section view taken through line 6-6 of Fig. 5;

Fig. 7 is a section view of a mix head suitable for use in an alternative preferred embodiment;

Fig. 8 is a graph showing the surface area and structure properties (CTAB and DBPA) of carbon blacks employed in certain highly preferred masterbatch compositions in accordance with the present invention;

Figs. 9 - 25 are graphs showing the macro-dispersion, natural rubber molecular weight and/or other characteristics of novel elastomer composites in accordance with this invention comprising carbon blacks shown in Fig. 8, in some cases along with data relating to control samples for comparison, exemplifying the significant improvements in physical characteristics and performance properties achieved by the elastomer composites;

Figs. 26 - 29 are graphs showing morphological properties of carbon blacks, i.e., structure (DBPA) and surface area (CTAB), and identifying regions or zones of carbon blacks (by such morphological properties) which are suitable for specific product applications; and

Figs. 30 and 31 are graphs showing the macro-dispersion and natural rubber molecular weight of novel elastomer composites in accordance with this invention, along with control samples for comparison.

It should be understood that the appended drawings are not necessarily precisely to scale. Certain features may have been enlarged or reduced for convenience or clarity of illustration. Directional references used in the following discussion are based on the orientation of components illustrated in the drawings unless otherwise stated or otherwise clear from the context. In general, apparatus in accordance with different embodiments of the invention can be employed in various arrangements. It will be

within the ability of those skilled in the art, given the benefit of the present disclosure, to determine appropriate dimensions and orientations for apparatus of the invention employing routine technical skills and taking into account well-known factors particular to the intended application, such as desired production volumes, material selection, duty cycle, and the like. Reference numbers used in one drawing may be used in other drawings for the same feature or element.

Detailed Description of Certain Preferred Embodiments

By virtue of the method and apparatus disclosed here, elastomer composite blends are produced, comprising (i) elastomer masterbatch produced in a continuous flow process involving mixture of elastomer latex and particulate filler fluids at turbulence levels and flow control conditions sufficient to achieve coagulation even without use of traditional coagulating agents, and (ii) additional elastomer added to such elastomer masterbatch in a dry mixing step. In fact, it will be immediately recognized to be of great commercial benefit: (A) that elastomer masterbatch crumb is achieved, that is, coagulated latex is achieved in accordance with the "wet mixing" step of the present method, without the need for either intensive dry mastication of elastomer with filler or exposing a liquid latex/particulate composition to a stream or tank of coagulant, and (B) that elastomer composite blend is then achieved by the "dry mixing" step involving dry mixing such masterbatch with additional elastomer. Thus, in routine commercial implementation the cost and complexity of employing acid coagulation solutions can be avoided. Prior techniques involving premixing of latex and particulate, such as in the above-mentioned Heller et al patent and Hagopian et al patent do not even recognize the possibility of achieving coagulation without exposing

the latex/particulate mixture to the usual coagulant solution with its attendant cost and waste disposal disadvantages.

Advantageous flexibility is achieved by the wet/dry mixing method disclosed here for making elastomer composite blend. In particular, flexibility is provided as to the choice of elastomer(s) employed in the fluid or "wet mixing" step and in the choice of elastomer(s) used in the subsequent "dry mixing" step. The same elastomer (or mixture of elastomers) can be used in the wet and dry mixing steps or, alternatively, different elastomers can be used in any suitable relative weight proportion. Further flexibility is provided in that additional filler may optionally be added during the dry mix step. Such additional filler can be the same as or different from the particulate filler used in the wet mixing step. Advantageously, in preferred embodiments of the method disclosed here, the excellent macro-dispersion of particulate filler achieved in the elastomer masterbatch produced by the wet mixing step is maintained or even further improved in the subsequent dry mixing step. Without wishing to be bound by theory, it presently is understood that, at least in certain preferred embodiments, a multi-phase elastomer composite blend is produced by the wet/dry method disclosed here. That is, although difficult to identify or observe using techniques currently in general use in the elastomer industry, the elastomer composite blend is understood to comprise at least one elastomer phase produced during the wet mixing step and a subsequent elastomer phase produced during the dry mixing step. The degree of intermingling of the two phases and the degree to which boundary layers between the two phases are more or less distinct will depend on numerous factors including, for example, the mutual affinity of the elastomer of the wet mixing step and that of the dry mixing step, the level of particulate loading, the choice of particulate filler(s) and

whether additional filler was added during the dry mixing step, the relative weight proportion of the wet mixing step elastomer and the dry mixing step elastomer, etc.

The advantageous flexibility afforded by the present invention, and its use to better control distribution of filler between two different elastomer phases in an elastomer composite blend is seen in the example of an elastomer composite blend comprising natural rubber, butadiene rubber (referred in this discussion, in some instances, as "BR") and carbon black filler. For certain applications it is preferred to have the carbon black filler primarily in the natural rubber phase of the elastomer composite blend. In accordance with prior known dry/dry mixing techniques, the carbon black can be mixed with the natural rubber using a dry mixing technique, followed by the addition and further dry mixing of BR. A disadvantageously large portion of the carbon black will migrate into the BR phase, due to its affinity for the BR phase and the less than desirable macro-dispersion of the carbon black in the natural rubber phase. In comparison, improved performance properties of comparable elastomer composite blends prepared by the wet/dry mixing method disclosed here indicate that more of the carbon black is retained in the natural rubber phase when the carbon black is mixed with the natural rubber in the initial wet mixing step, followed by the addition of BR in a subsequent dry mixing step.

In accordance with the wet mixing step of the method disclosed here, feed rates of latex fluid and particulate filler fluid to the mixing zone of the coagulum reactor can be precisely metered to achieve high yield rates, with little free latex and little undispersed filler in the product crumb at the discharge end of the coagulum reactor. Without wishing to be bound by theory, it presently is understood that a quasi-mono-phase system is established in the mixing zone except that coagulum solids are being

formed there and/or downstream thereof in the coagulum zone. Extremely high feed velocity of the particulate filler fluid into the mixing zone of the coagulum reactor and velocity differential relative the latex fluid feed are believed to be significant in achieving sufficient turbulence, i.e., sufficiently energetic shear of the latex by the impact of the particulate filler fluid jet for thorough mixing and dispersion of the particulate into the latex fluid and coagulation. High mixing energies yield product masterbatch crumb with excellent dispersion, together with controlled product delivery. The coagulum is created and then formed into a desirable extrudate. The particulate filler fluid and elastomer latex are fed preferably continuously, meaning that an ongoing flow of coagulated masterbatch is established from the mixing zone to the discharged end of the coagulum reactor while an uninterrupted flow of the feed fluids is maintained. Typically, the uninterrupted flow of the feed fluids and simultaneous discharge of coagulated masterbatch are maintained for one or more hours, preferably, for example, more than 24 hours, and ever perhaps for a week or more.

Certain preferred embodiments are discussed below, of methods and apparatus for producing the novel elastomer composite blends disclosed here. While various preferred embodiments of the invention can employ a variety of different fillers and elastomers, certain portions of the following detailed description of method and apparatus aspects of the invention will, in some instances, for convenience, describe masterbatch comprising natural rubber and carbon black. It will be within the ability of those skilled in the art, given the benefit of this disclosure, to employ the method and apparatus disclosed here in accordance with the principles of operation discussed here to produce masterbatch and elastomer composite blends comprising a number of alternative or additional elastomers, fillers and other materials. In brief, preferred methods for

preparing elastomer masterbatch involve feeding simultaneously a slurry of carbon black or other filler and a natural rubber latex fluid or other suitable elastomer fluid to a mixing zone of a coagulum reactor. A coagulum zone extends from the mixing zone, preferably progressively increasing in cross-sectional area in the downstream direction from an entry end to a discharge end. The slurry is fed to the mixing zone preferably as a continuous, high velocity jet of injected fluid, while the natural rubber latex fluid is fed at relatively low velocity. The high velocity, flow rate and particulate concentration of the filler slurry are sufficient to cause mixture and high shear of the latex fluid, flow turbulence of the mixture within at least an upstream portion of the coagulum zone, and substantially completely coagulate the elastomer latex prior to the discharge end. Substantially complete coagulation can thus be achieved, in accordance with preferred embodiments, without the need of employing an acid or salt coagulation agent. The preferred continuous flow method of producing the elastomer composites comprises the continuous and simultaneous feeding of the latex fluid and filler slurry to the mixing zone of the coagulum reactor, establishing a continuous, semi-confined flow of a mixture of the latex and filler slurry in the coagulum zone. Elastomer composite crumb in the form of "worms" or globules are discharged from the discharge end of the coagulum reactor as a substantially constant flow concurrently with the on-going feeding of the latex and carbon black slurry streams into the mixing zone of the coagulum reactor. Notably, the plug-type flow and atmospheric or near atmospheric pressure conditions at the discharge end of the coagulum reactor are highly advantageous in facilitating control and collection of the elastomer composite product, such as for immediate or subsequent further processing steps. Feed rates of the natural rubber latex fluid and carbon black slurry to the mixing zone of the coagulum reactor

can be precisely metered to achieve high yield rates, with little free latex and little undispersed carbon black in the product crumb at the discharge end of the coagulum reactor. Without wishing to be bound by theory, it presently is understood that a quasi-mono-phase system is established in the mixing zone except that coagulum solids
5 are being formed there and/or downstream thereof in the coagulum zone. Extremely high feed velocity of the carbon black slurry into the mixing zone of the coagulum reactor and velocity differential relative the natural rubber latex fluid feed are believed to be significant in achieving sufficient turbulence, i.e., sufficiently energetic shear of the latex by the impact of the particulate filler fluid jet for thorough mixing and
10 dispersion of the particulate into the latex fluid and coagulation. High mixing energies yield the novel product with excellent macro-dispersion, together with controlled product delivery. The coagulum is created and then formed into a desirable extrudate.

The elastomer composite prepared by the above-described wet mixing technique and apparatus is formed into elastomer composite blends of the invention by subsequent
15 dry mixing with additional elastomer. Thus, the present invention can be described as involving a wet/dry method, whereas prior-known techniques employed a dry/dry method in which a masterbatch first is formed by dry mixing and additional elastomer is added by further dry mixing. The dry mixing step of the wet/dry mixing method of the present invention can be carried out with commercially available apparatus and
20 techniques including, for example, Banbury mixers and the like. The additional elastomer added during the dry mixing step of the wet/dry mixing method disclosed here can be one or more elastomers which are the same as or different from the elastomer(s) employed to form the masterbatch. Other ingredients also may be added along with the additional elastomer during the dry mix step including, for example,

extender oil, additional particulate filler, curatives, etc., in those embodiments wherein additional particulate filler is added during the dry mixing step such additional filler can be the same as or different from the filler(s) used in the masterbatch formed by the wet mixing step.

5 The aforesaid preferred apparatus and techniques for producing the elastomer composite blends disclosed here are discussed in conjunction with the appended drawings, wherein a continuous flow wet mixing step for producing elastomer masterbatch employs a continuous, semi-confined flow of elastomer latex, for example, natural rubber latex (field latex or concentrate) mixed with a filler slurry, for example,
10 an aqueous slurry of carbon black, in a coagulum reactor forming an elongate coagulum zone which extends, preferably with progressively increasing cross-sectional area, from an entry end to a discharge end. The term "semi-confined" flow refers to a highly advantageous feature. As used here the term is intended to mean that the flow path followed by the mixed latex fluid and filler slurry within the coagulum reactor is closed
15 or substantially closed upstream of the mixing zone and is open at the opposite, downstream end of the coagulum reactor, that is, at the discharge end of the coagulum reactor. Turbulence conditions in the upstream portion of the coagulum zone are maintained in on-going, at least quasi-steady state fashion concurrently with substantially plug flow-type conditions at the open discharge end of the coagulum
20 reactor. The discharge end is "open" at least in the sense that it permits discharge of coagulum, generally at or near atmospheric pressure and, typically, by simple gravity drop (optionally within a shrouded or screened flow path) into suitable collection means, such as the feed hopper of a de-watering extruder. Thus, the semi-confined flow results in a turbulence gradient extending axially or longitudinally within at least a portion of the

coagulum reactor. Without wishing to be bound by theory, it presently is understood that the coagulum zone is significant in permitting high turbulence mixing and coagulation in an upstream portion of the coagulum reactor, together with substantially plug-type discharge flow of a solid product at the discharge end. Injection of the carbon black or other filler slurry as a continuous jet into the mixing zone occurs in on-going fashion simultaneously, with ease of collection of the elastomer masterbatch crumb discharged under substantially plug-type flow conditions and generally ambient pressure at the discharge end of the coagulum reactor. Similarly, axial velocities of the slurry through the slurry nozzle into the mixing zone and, typically, at the upstream end of the coagulum zone are substantially higher than at the discharge end. Axial velocity of the slurry will typically be several hundred feet per second as it enters the mixing zone, preferably from a small bore, axially oriented feed tube in accordance with preferred embodiments discussed below. The axial velocity of the resultant flow at the entry end of a coagulum reactor with expanding cross-sectional area in a typical application may be, for example, 5 to 20 feet per second, and more usually 7 to 15 feet per second. At the discharge end, in contrast again, axial velocity of the masterbatch crumb product being discharged there will in a typical application be approximately 1 to 10 feet per second, and more generally 2 to 5 feet per second. Thus, the aforesaid semi-confined turbulent flow achieves the highly significant advantage that natural rubber or other elastomer latex is coagulated by mixture with carbon black or other filler even in the absence of subsequent treatment in a stream or tank of acid, salt or other coagulant solution, with controlled, preferably quasi-molded product delivery from the coagulum reactor for subsequent processing.

It should be understood in this regard that reference to the coagulum reactor as being "open" at the discharge end is not intended to mean that the discharge end is

necessarily exposed to view or easily accessed by hand. It may instead be permanently or releasably attached to a collection device or subsequent processing device, such as a diverter (discussed further below), dryer, etc. The discharge end of the coagulum reactor is open in the important sense that the turbulent flow within the coagulum zone of the coagulum reactor, which is under high pressure and sealed against any significant rearward (i.e., upstream) travel at the mixing zone, is permitted to establish the aforesaid pressure and/or velocity gradient as it travels toward and exits from the discharge end.

It should also be recognized in this regard that the turbulence of the flow lessens along the coagulum reactor toward the discharge end. Substantial plug flow of a solid product is achieved prior to the discharge end, dependent upon such factors as percent of capacity utilization, selection of materials and the like. Reference here to the flow being substantially plug flow at or before the discharge end of the coagulum reactor should be understood in light of the fact that the flow at the discharge end is composed primarily or entirely of masterbatch crumb, that is, globules or "worms" of coagulated elastomer masterbatch. The crumb is typically quasi-molded to the inside shape of the coagulum zone at the point along the coagulum zone at which flow became substantially plug flow. The ever-advancing mass of "worms" or globules advantageously have plug-type flow in the sense that they are traveling generally or primarily axially toward the discharge end and at any point in time in a given cross-section of the coagulum zone near the discharge end have a fairly uniform velocity, such that they are readily collected and controlled for further processing. Thus, the fluid phase mixing aspect disclosed here can advantageously be carried out at steady state or quasi-steady state conditions, resulting in high levels of product uniformity.

A preferred embodiment of the wet mixing step of the method and apparatus disclosed here is illustrated schematically in Fig. 1. Those skilled in the art will recognize that the various aspects of system configuration, component selection and the like will depend to some extent on the particular characteristics of the intended application. Thus, for example, such factors as maximum system through-put capacity and material selection flexibility will influence the size and layout of system components. In general, such considerations will be well within the ability of those skilled in the art given the benefit of the present disclosure. The system illustrated in Fig. 1 is seen to include means for feeding natural rubber latex or other elastomer latex fluid at low pressure and low velocity continuously to a mixing zone of a coagulum reactor. More particularly, a latex pressure tank 10 is shown, to hold the feed supply of latex under pressure. Alternatively, a latex storage tank can be used, equipped with a peristaltic pump or series of pumps or other suitable feed means adapted to hold elastomer latex fluid to be fed via feed line 12 to a mixing zone of a coagulum reactor 14. Latex fluid in tank 10 may be held under air or nitrogen pressure or the like, such that the latex fluid is fed to the mixing zone at a line pressure of preferably less than 10 psig, more preferably about 2 - 8 psig, and typically about 5 psig. The latex feed pressure and the flow lines, connections, etc., of the latex feed means should be arranged to cause shear in the flowing latex fluid as low as reasonably possible. Preferably all flow lines, for example, are smooth, with only large radius turns, if any, and smooth or faired line-to-line interconnections. The pressure is selected to yield the desired flow velocity into the mixing zone; an example of a useful flow velocity is no more than about 12 feet per second.

Suitable elastomer latex fluids include both natural and synthetic elastomer latices and latex blends. The latex must, of course, be suitable for coagulation by the selected particulate filler and must be suitable for the intended purpose or application of the final rubber product. It will be within the ability of those skilled in the art to select suitable elastomer latex or a suitable blend of elastomer latices for use in the methods and apparatus disclosed here, given the benefit of this disclosure. Exemplary elastomers include, but are not limited to, rubbers, polymers (e.g., homopolymers, copolymers and/or terpolymers) of 1,3-butadiene, styrene, isoprene, isobutylene, 2,3-dimethyl-1,3-butadiene, acrylonitrile, ethylene, and propylene and the like. The elastomer may have a glass transition temperature (T_g) as measured by differential scanning calorimetry (DSC) ranging from about -120°C to about 0°C . Examples include, but are not limited to, styrene-butadiene rubber (SBR), natural rubber and its derivatives such as chlorinated rubber, polybutadiene, polyisoprene, poly(styrene-co-butadiene) and the oil extended derivatives of any of them. Blends of any of the foregoing may also be used. The latex may be in an aqueous carrier liquid. Alternatively, the liquid carrier may be a hydrocarbon solvent. In any event, the elastomer latex fluid must be suitable for controlled continuous feed at appropriate velocity, pressure and concentration into the mixing zone. Particular suitable synthetic rubbers include: copolymers of from about 10 to about 70 percent by weight of styrene and from about 90 to about 30 percent by weight of butadiene such as copolymer of 19 parts styrene and 81 parts butadiene, a copolymer of 30 parts styrene and 70 parts butadiene, a copolymer of 43 parts styrene and 57 parts butadiene and a copolymer of 50 parts styrene and 50 parts butadiene; polymers and copolymers of conjugated dienes such as polybutadiene, polyisoprene, polychloroprene, and the like, and copolymers of such conjugated dienes with an

ethylenic group-containing monomer copolymerizable therewith such as styrene, methyl styrene, chlorostyrene, acrylonitrile, 2-vinyl-pyridine, 5-methyl-2-vinylpyridine, 5-ethyl-2-vinylpyridine, 2-methyl-5-vinylpyridine, alkyl-substituted acrylates, vinyl ketone, methyl isopropenyl ketone, methyl vinyl ether, aliphatic methylene carboxylic acids and the esters and amides thereof such as acrylic acid and dialkylacrylic acid amide. Also suitable for use herein are copolymers of ethylene and other high alpha olefins such as propylene, butene-1 and pentene-1.

The additional elastomer added during the dry mixing step of the wet/dry mixing method disclosed here can employ any elastomer or mixture of elastomers suitable to the intended use or application, including those listed above for use in the wet mixing step. In accordance with certain preferred embodiments, the elastomer latex employed in the wet mixing step is natural rubber latex and the additional elastomer employed in the dry mixing step is butadiene rubber (BR). In such preferred embodiments, the butadiene rubber preferably forms the minor phase or constituent of the elastomer composite blend, most preferably being from 10% to 50% by weight of total elastomer in the elastomer composite blend. In accordance with certain other preferred embodiments, the elastomer latex employed in the wet mixing step is natural rubber latex and the additional elastomer employed in the dry mixing step is styrene-butadiene rubber (SBR). In such preferred embodiments, the SBR preferably forms the major phase or constituent of the elastomer composite blend, most preferably being from 50% to 90% by weight of total elastomer in the elastomer composite blend. In accordance with certain other preferred embodiments, the additional elastomer is natural rubber. In accordance with certain other preferred embodiments, the elastomer latex employed in the wet mixing step is butadiene rubber latex and the additional elastomer employed in the dry mixing step is SBR. In

such preferred embodiments, the SBR preferably from 10% to 90% by weight of total elastomer in the elastomer composite blend. In accordance with certain other preferred embodiments, the elastomer latex employed in the wet mixing step is butadiene rubber latex and the additional elastomer employed in the dry mixing step is natural rubber. In

5 such preferred embodiments, the natural rubber preferably is the minor constituent or phase of the elastomer composite blend, most preferably being from 10% to 50% by weight of total elastomer in the elastomer composite blend. In accordance with certain other preferred embodiments employing butadiene rubber latex in the wet mixing step, the additional elastomer is additional butadiene rubber. In accordance with certain other

10 preferred embodiments, the elastomer latex employed in the wet mixing step is SBR and the additional elastomer is butadiene rubber. In such preferred embodiments, the butadiene rubber preferably is from 10% to 90% by weight of total elastomer in the elastomer composite blend. In accordance with certain other preferred embodiments, the elastomer latex employed in the wet mixing step is SBR and the additional elastomer is

15 natural rubber. In such preferred embodiments, the natural rubber preferably is the major constituent or phase, most preferably being from 50% to 90% by weight of total elastomer in the elastomer composite blend. Certain other preferred embodiments SBR is employed in both the wet mixing and dry mixing steps, thus being essentially 100% of the elastomer in the elastomer composite blend.

20 As noted further below, the rubber compositions of the present invention can contain, in addition to the elastomer and filler, curing agents, a coupling agent, and optionally, various processing aids, oil extenders and antidegradents. In that regard, it should be understood that the elastomer composite blends disclosed here include vulcanized compositions (VR), thermoplastic vulcanizates (TPV), thermoplastic

elastomers (TPE) and thermoplastic polyolefins (TPO). TPV, TPE, and TPO materials are further classified by their ability to be extruded and molded several times without substantial loss of performance characteristics. Thus, in making the elastomer composite blends one or more curing agents such as, for example, sulfur, sulfur donors, activators, accelerators, peroxides, and other systems used to effect vulcanization of the elastomer composition may be used.

Where the elastomer latex employed in the wet mixing step comprises natural rubber latex, the natural rubber latex can comprise field latex or latex concentrate (produced, for example, by evaporation, centrifugation or creaming). The natural rubber latex must, of course, be suitable for coagulation by the carbon black. The latex is provided typically in an aqueous carrier liquid. Alternatively, the liquid carrier may be a hydrocarbon solvent. In any event, the natural rubber latex fluid must be suitable for controlled continuous feed at appropriate velocity, pressure and concentration into the mixing zone. The well known instability of natural rubber latex is advantageously accommodated, in that it is subjected to relatively low pressure and low shear throughout the system until it is entrained into the aforesaid semi-confined turbulent flow upon encountering the extraordinarily high velocity and kinetic energy of the carbon black slurry in the mixing zone. In certain preferred embodiments, for example, the natural rubber is fed to the mixing zone at a pressure of about 5 psig, at a feed velocity in the range of about 3 - 12 ft. per second, more preferably about 4 - 6 ft. per second. Selection of a suitable latex or blend of latices will be well within the ability of those skilled in the art given the benefit of the present disclosure and the knowledge of selection criteria generally well recognized in the industry.

The particulate filler fluid, for example, carbon black slurry, is fed to the mixing zone at the entry end of coagulum reactor 14 via feed line 16. The slurry may comprise any suitable filler in a suitable carrier fluid. Selection of the carrier fluid will depend largely upon the choice of particulate filler and upon system parameters. Both aqueous and non-aqueous liquids may be used, with water being preferred in many embodiments in view of its cost, availability and suitability of use in the production of carbon black and certain other filler slurries.

When a carbon black filler is used, selection of the carbon black will depend largely upon the intended use of the elastomer composite blend. Optionally, the carbon black filler can include also any material which can be slurried and fed to the mixing zone in accordance with the principles disclosed here. Suitable additional particulate fillers include, for example, conductive fillers, reinforcing fillers, fillers comprising short fibers (typically having an L/D aspect ratio less than 40), flakes, etc. Thus, exemplary particulate fillers which can be employed in producing elastomer masterbatch in accordance with the methods and apparatus disclosed here, are carbon black, fumed silica, precipitated silica, coated carbon black, chemically functionalized carbon blacks, such as those having attached organic groups, and silicon-treated carbon black, either alone or in combination with each other. Suitable chemically functionalized carbon blacks include those disclosed in International Application No. PCT/US95/16194 (WO9618688), the disclosure of which is hereby incorporated by reference. In silicon-treated carbon black, a silicon containing species such as an oxide or carbide of silicon, is distributed through at least a portion of the carbon black aggregate as an intrinsic part of the carbon black. Conventional carbon blacks exist in the form of aggregates, with each aggregate consisting of a single phase, which is

carbon. This phase may exist in the form of a graphitic crystallite and/or amorphous carbon, and is usually a mixture of the two forms. As discussed elsewhere herein, carbon black aggregates may be modified by depositing silicon-containing species, such as silica, on at least a portion of the surface of the carbon black aggregates. The result
5 may be described as silicon-coated carbon blacks. The materials described herein as silicon-treated carbon blacks are not carbon black aggregates which have been coated or otherwise modified, but actually represent a different kind of aggregate. In the silicon-treated carbon blacks, the aggregates contain two phases. One phase is carbon, which will still be present as graphitic crystallite and/or amorphous carbon, while the
10 second phase is silica (and possibly other silicon-containing species). Thus, the silicon-containing species phase of the silicon-treated carbon black is an intrinsic part of the aggregate; it is distributed throughout at least a portion of the aggregate. It will be appreciated that the multiphase aggregates are quite different from the silica-coated carbon blacks mentioned above, which consist of pre-formed, single phase carbon
15 black aggregates having silicon-containing species deposited on their surface. Such carbon blacks may be surface-treated in order to place a silica functionality on the surface of the carbon black aggregate. In this process, an existing aggregate is treated so as to deposit or coat silica (as well as possibly other silicon-containing species) on at least a portion of the surface of the aggregate. For example, an aqueous sodium
20 silicate solution may be used to deposit amorphous silica on the surface of carbon black aggregates in an aqueous slurry at high pH, such as 6 or higher, as discussed in Japanese Unexamined Laid-Open (Kokai) Publication No. 63-63755. More specifically, carbon black may be dispersed in water to obtain an aqueous slurry consisting, for example, of about 5% by weight carbon black and 95% by weight

water. The slurry is heated to above about 70°C, such as to 85-95°C, and the pH adjusted to above 6, such as to a range of 10-11, with an alkali solution. A separate preparation is made of sodium silicate solution, containing the amount of silica which is desired to be deposited on the carbon black, and an acid solution to bring the sodium silicate solution to a neutral pH. The sodium silicate and acid solutions are added dropwise to the slurry, which is maintained at its starting pH value with acid or alkali solution as appropriate. The temperature of the solution is also maintained. A suggested rate for addition of the sodium silicate solution is to calibrate the dropwise addition to add about 3 weight percent silicic acid, with respect to the total amount of carbon black, per hour. The slurry should be stirred during the addition, and after its completion for from several minutes (such as 30) to a few hours (i.e., 2-3). In contrast, silicon-treated carbon blacks may be obtained by manufacturing carbon black in the presence of volatilizable silicon-containing compounds. Such carbon blacks are preferably produced in a modular or "staged" furnace carbon black reactor having a combustion zone followed by a zone of converging diameter, a feed stock injection zone with restricted diameter, and a reaction zone. A quench zone is located downstream of the reaction zone. Typically, a quenching fluid, generally water, is sprayed into the stream of newly formed carbon black particles flowing from the reaction zone. In producing silicon-treated carbon black, the aforesaid volatilizable silicon-containing compound is introduced into the carbon black reactor at a point upstream of the quench zone. Useful compounds are volatilizable compounds at carbon black reactor temperatures. Examples include, but are not limited to, silicates such as tetraethoxy orthosilicate (TEDS) and tetramethoxy orthosilicate, silanes such as, tetrachloro silane, and trichloro methylsilane; and volatile silicone polymers such as

octamethylcyclotetrasiloxane (OMTS). The flow rate of the volatilizable compound will determine the weight percent of silicon in the treated carbon black. The weight percent of silicon in the treated carbon black typically ranges from about 0.1 percent to 25 percent, preferably about 0.5 percent to about 10 percent, and more preferably about 2 percent to about 6 percent. The volatilizable compound may be pre-mixed with the carbon black-forming feed stock and introduced with the feed stock into the reaction zone. Alternatively, the volatilizable compound may be introduced to the reaction zone separately, either upstream or downstream from the feed stock injection point.

As noted above, additives may be used, and in this regard coupling agents useful for coupling silica or carbon black should be expected to be useful with the silicon-treated carbon blacks. Carbon blacks and numerous additional suitable particulate fillers are commercially available and are known to those skilled in the art.

Selection of the particulate filler or mixture of particulate fillers will depend largely upon the intended use of the elastomer composite blends. As used here, particulate filler can include any material which can be slurried and fed to the mixing zone in accordance with the principles disclosed here. Suitable particulate fillers include, for example, conductive fillers, reinforcing fillers, fillers comprising short fibers (typically having an L/D aspect ratio less than 40), flakes, etc. In addition to the carbon black and silica-type fillers mentioned above, fillers can be formed of clay, glass, polymer, such as aramid fiber, etc. It will be within the ability of those skilled in the art to select suitable particulate fillers for use in the method and apparatus disclosed here given the benefit of the present disclosure, and it is expected that any filler suitable for use in elastomer compositions may be incorporated into the elastomer

composites using the teachings of the present disclosure. Of course, blends of the various particulate fillers discussed herein may also be used.

Preferred embodiments of the invention consistent with Fig. 1 are especially well adapted to preparation of particulate filler fluid comprising aqueous slurries of carbon black. In accordance with known principles, it will be understood that carbon blacks having lower surface area per unit weight must be used in higher concentration in the particulate slurry to achieve the same coagulation efficacy as lower concentrations of carbon black having higher surface area per unit weight. Agitated mixing tank 18 receives water and carbon black, e.g., optionally pelletized carbon black, to prepare an initial mixture fluid. Such mixture fluid passes through discharge port 20 into fluid line 22 equipped with pumping means 24, such as a diaphragm pump or the like. Line 28 passes the mixture fluid to colloid mill 32, or alternatively a pipeline grinder or the like, through intake port 30. The carbon black is dispersed in the aqueous carrier liquid to form a dispersion fluid which is passed through outlet port 31 and fluid line 33 to a homogenizer 34. Pumping means 36, preferably comprising a progressing cavity pump or the like is provided in line 33. Homogenizer 34 more finely disperses the carbon black in the carrier liquid to form the carbon black slurry which is fed to the mixing zone of the coagulum reactor 14. It has an inlet port 37 in fluid communication with line 33 from the colloid mill 32. The homogenizer 34 may preferably comprise, for example, a Microfluidizer[®] system commercially available from Microfluidics International Corporation (Newton, Massachusetts, USA). Also suitable are homogenizers such as models MS18, MS45 and MC120 Series homogenizers available from the APV Homogenizer Division of APV Gaulin, Inc. (Wilmington, Massachusetts, USA). Other suitable homogenizers are commercially

available and will be apparent to those skilled in the art given the benefit of the present disclosure. Typically, carbon black in water prepared in accordance with the above described system will have at least about 90% agglomerates less than about 30 microns, more preferably at least about 90% agglomerates less than about 20 microns in size. Preferably, the carbon black is broken down to an average size of 5 - 15 microns, e.g., about 9 microns. Exit port 38 passes the carbon black slurry from the homogenizer to the mixing zone through feed line 16. The slurry may reach 10,000 to 15,000 psi in the homogenizer step and exit the homogenizer at about 600 psi or more. Preferably, a high carbon black content is used to reduce the task of removing excess water or other carrier. Typically, about 10 to 30 weight percent carbon black is preferred. Those skilled in the art will recognize, given the benefit of this disclosure, that the carbon black content (in weight percent) of the slurry and the slurry flow rate to the mixing zone should be coordinated with the natural rubber latex flow rate to the mixing zone to achieve a desired carbon black content (in phr) in the masterbatch. The carbon black content will be selected in accordance with known principles to achieve material characteristics and performance properties suited to the intended application of the product. Typically, for example, carbon blacks of CTAB value 10 or more are used in sufficient amount to achieve carbon black content in the masterbatch of at least about 30 phr.

The slurry preferably is used in masterbatch production immediately upon being prepared. Fluid conduits carrying the slurry and any optional holding tanks and the like, should establish or maintain conditions which substantially preserve the dispersion of the carbon black in the slurry. That is, substantial reagglomeration or settling out of the particulate filler in the slurry should be prevented or reduced to the extent

reasonably practical. Preferably all flow lines, for example, are smooth, with smooth line-to-line interconnections. Optionally, an accumulator is used between the homogenizer and the mixing zone to reduce fluctuations in pressure or velocity of the slurry at the slurry nozzle tip in the mixing zone.

5 Natural rubber latex fluid or other elastomer latex fluid passed to the mixing zone via feed line 12 and carbon black slurry fed to the mixing zone via feed line 16 under proper process parameters as discussed above, can produce a novel elastomer composite, specifically, elastomer masterbatch crumb. Means may also be provided for incorporating various additives into the elastomer masterbatch. An additive fluid
10 comprising one or more additives may be fed to the mixing zone as a separate feed stream. One or more additives also may be pre-mixed, if suitable, with the carbon black slurry or, more typically, with the elastomer latex fluid. Additives also can be mixed into the masterbatch subsequently, i.e., during the dry mixing step. Numerous additives are well known to those skilled in the art and include, for example,
15 antioxidants, antiozonants, plasticizers, processing aids (e.g., liquid polymers, oils and the like), resins, flame-retardants, extender oils, lubricants, and a mixture of any of them. The general use and selection of such additives is well known to those skilled in the art. Their use in the system disclosed here will be readily understood with the benefit of the present disclosure. In accordance with certain alternative embodiments,
20 curative also can be incorporated in like manner, to produce a curable elastomer composite which may be referred to as a curable base compound.

 The elastomer masterbatch crumb is passed from the discharge end of coagulum reactor 14 to suitable drying apparatus. In the preferred embodiment of Fig. 1 the masterbatch crumb undergoes multi-stage drying. It is passed first to a de-watering

extruder 40 and then via conveyor or simple gravity drop or other suitable means 41 to a drying extruder 42. In routine preferred embodiments consistent with that illustrated in Fig. 1 producing natural rubber masterbatch with carbon black filler, the de-watering/drying operation will typically reduce water content to about 0 to 1 weight percent, more preferably .0 to .5 weight percent. Suitable dryers are well known and commercially available, including for example, extruder dryers, fluid bed dryers, hot air or other oven dryers, and the like, such as French Mills available from the French Oil Machinery Co., (Piqua, Ohio, USA).

Dried masterbatch crumb from drying extruder 42 is carried by a cooling conveyor 44 to a baler 46. The baler is an optional, advantageous feature of the apparatus of Fig. 1, wherein the dried masterbatch crumb is compressed within a chamber into form-stable compressed blocks or the like. Typically, 25 to 75 pound quantities of the elastomer masterbatch are compressed into blocks or bales for transport, further processing, etc. Alternatively, the product is provided as pellets, for example, by chopping the crumb.

The dimensions and particular design features of the coagulum reactor 14, including the mixing zone/coagulum zone assembly, suitable for an embodiment in accordance with Fig. 1, will depend in part on such design factors as the desired throughput capacity, the selection of materials to be processed, etc. One preferred embodiment is illustrated in Fig. 2 wherein a coagulum reactor 48 has a mix head 50 attached to a coagulum zone 52 with a fluid-tight seal at joint 54. Fig. 2 schematically illustrates a first subsystem 56 for feeding elastomer latex to the mixing zone, subsystem 57 for feeding carbon black slurry or other particulate filler fluid to the mixing zone, and subsystem 58 for feeding an optional additive fluid, pressurized air,

etc. to the mixing zone. The mix head 50 is seen to have three feed channels 60, 61, 62. Feed channel 60 is provided for the natural rubber latex fluid and feed channel 62 is provided for direct feed of gas and/or additive fluid. In connection with preferred embodiments employing direct injection of additives, significant advantage is achieved in connection with hydrocarbon additives or, more generally, non-water miscible additives. While it is well known to employ emulsion intermediates to create additive emulsions suitable for pre-blending with an elastomer latex, preferred embodiments in accordance with the present disclosure employing direct injection of additives can eliminate not only the need for emulsion intermediates, but also the equipment such as tanks, dispersing equipment, etc. previously used in forming the emulsions. Reductions in manufacturing cost and complexity can, therefore, be achieved. As discussed further below, the feed channel 61 through which slurry is fed to the mixing zone is preferably coaxial with the mixing zone and the coagulum zone of the coagulum reactor. While only a single feed channel is shown to receive the elastomer latex fluid, any suitable number of feed channels may be arranged around the central feed channel through which the slurry is fed to the mixing zone. Thus, for example, in the embodiment of Fig. 2 a fourth feed channel could be provided through which ambient air or high pressure air or other gas is fed to the mixing zone. Pressurized air may be injected likewise with the slurry through the central axial feed channel 61. Auxiliary feed channels can be temporarily or permanently sealed when not in use.

The coagulum zone 52 of the coagulum reactor 48 is seen to have a first portion 64 having an axial length which may be selected depending upon design objectives for the particular application intended. Optionally, the coagulum zone may have a constant cross-sectional area over all or substantially all of its axial length. Thus, for example,

the coagulum reactor may define a simple, straight tubular flow channel from the mixing zone to the discharge end. Preferably, however, for reasons discussed above, and as seen in the preferred embodiment illustrated in the drawings, the cross-sectional area of the coagulum zone 52 increases progressively from the entry end 66 to discharge end 68. More specifically, the cross-sectional area increases in the longitudinal direction from the entry end to the discharge end. In the embodiment of Fig. 2, the coagulum zone increases in cross-sectional area progressively in the sense that it increases continuously following constant cross-sectional portion 64. References to the diameter and cross-sectional area of the coagulum reactor (or, more properly, the coagulum zone defined within the coagulum reactor) and other components, unless stated otherwise, are intended to mean the cross-sectional area of the open flow passageway and the inside diameter of such flow passageway.

Elastomer composite, specifically, coagulated elastomer latex in the form of masterbatch crumb 72, is seen being discharged from the coagulum reactor 48 through a diverter 70. Diverter 70 is an adjustable conduit attached to the coagulum reactor at discharge end 68. It is adjustable so as to selectively pass the elastomer masterbatch crumb 72 to any of various different receiving sites. This feature advantageously facilitates removal of masterbatch crumb from the product stream, for example, for testing or at the beginning of a production run when initial process instability may result temporarily in inferior product. In addition, the diverter provides design flexibility to direct product from the coagulum reactor to different post-processing paths. In accordance with the preferred embodiment of Fig. 1, the masterbatch crumb 72 being discharged from coagulum reactor 48 through diverter 70 is seen to be received by a drier 40.

The cross-sectional dimension of coagulum reactor 48 is seen to increase at an overall angle α between entry end 66 and discharge end 68. Angle α is greater than 0° and in preferred embodiments is less than 45° , more preferably less than 15° , most preferably from 0.5° to 5° . The angle α is seen to be a half angle, in that it is measured from the central longitudinal axis of the coagulum zone to a point A at the outer circumference of the coagulum zone at the end of the coagulum reactor. In this regard, it should be understood that the cross-sectional area of the upstream portion of the coagulum reactor, that is, the portion near the entry end 66, preferably increases sufficiently slowly to achieve quasi-molding of the coagulum in accordance with the principles discussed above. Too large an angle of expansion of the coagulum zone may result in the elastomer masterbatch not being produced in desirable crumb form of globules or worms and simply spraying through the coagulum reactor. Increasing the bore of the coagulum reactor too slowly can result, in certain embodiments, in backup or clogging of the feeds and reaction product into the mix head. In a downstream portion of the coagulum zone, wherein the latex has been substantially coagulated and flow has become essentially plug flow, the coagulum zone may extend either with or without increase in cross-sectional area. Thus, reference here to the coagulum zone in preferred embodiments having a progressively increasing cross-sectional area should be understood to refer primarily to that portion of the coagulum zone wherein flow is not substantially plug flow.

The cross-sectional area of the coagulum zone (that is, at least the upstream portion thereof, as discussed immediately above) may increase in step-wise fashion, rather than in the continuous fashion illustrated in the embodiment of Fig. 2. In the embodiment illustrated in Fig. 3, a continuous flow system for production of elastomer

masterbatch in accordance with the method and apparatus disclosed here, is seen to include a mix head/coagulum zone assembly wherein the cross-sectional area of the coagulum zone increases in step-wise fashion. Preferably, the individual sections of the coagulum zone in such a step-wise embodiment have a faired connection to adjacent sections. That is, they combine to form a smooth and generally continuous coagulum zone surface, as opposed, for example, to a sharp or instantaneous increase in diameter from one section to the next. The coagulum zone of Fig. 3 increases in three steps, such that there are four different sections or sub-zones 74 - 77. Consistent with the design principles discussed immediately above, the cross-sectional area of coagulum zone 53 increases from the entry end 66 to point A at the discharge end 68 at an overall angle which achieves the necessary flow control in the upstream portion of the coagulum reactor. The first section 74 can be taken as including (a) the constant diameter portion of the mix head 50 immediately downstream of the mixing zone, and (b) the same or similar diameter portion connected thereto at joint 54 at the entry end 66. This first section has a constant cross-sectional diameter D_1 and an axial dimension or length L_1 . In this first section 74 the length L_1 should be greater than three times the diameter D_1 , more preferably greater than five times D_1 , and most preferably from about 12 to 18 times D_1 . Typically, this section will have a length of about fifteen times D_1 . Each subsequent section preferably has a constant cross-sectional dimension and cross-sectional area approximately double that of the preceding (i.e., upstream) section. Thus, for example, section 75 has a constant cross-sectional dimension and a cross-sectional area which is twice that of section 74. Similarly, the cross-sectional area of section 76 is double that of section 75, and the cross-sectional area of section 77 is double that of section 76. In each of sections 75 - 77, the length

is preferably greater than three times its diameter, more preferably about three to seven times its diameter and generally about five times its diameter. Thus, for example, in section 76 longitudinal dimension L_3 is preferably about five times its diameter D_3

A mix head and coagulum zone assembly corresponding to the embodiment of Fig. 3 is shown in Fig. 4 partially in section view. Mix head 50 is integral with coagulum zone extender 53 via joint 54. It defines a mixing zone wherein multiple feed channels 60, 61, 62 form a junction, with an elongate, substantially cylindrical channel 80 substantially coaxial with the coagulum zone portion within extender 53. It will be recognized that it is not essential to the operability of the method and apparatus disclosed here, to precisely define the boundaries of the mixing zone and/or coagulum zone. Numerous variations are possible in the design of the flow channels junction area, as will be apparent to those skilled in the art given the benefit of the present disclosure. In that regard, as a generally preferred guideline, in embodiments of the type illustrated in Fig. 4, for example, the slurry tip 67 generally is upstream of the beginning of cylindrical portion 80, being approximately centered longitudinally in the junction of the feed channels. In such embodiments, preferably, the minimum cross-sectional area defined by the imaginary cone from the slurry tip 67 to the circumferential perimeter at the beginning of the cylindrical portion 80 is advantageously greater than, or at least equal to, the cross-sectional area of the latex feed channel 60. Preferably, both channel 80 and at least the upstream portion of the coagulum zone wherein flow turbulence exists prior to substantially complete coagulation of the elastomer latex, have a circular cross-section.

The means for feeding carbon black slurry or other particulate filler fluid is seen to comprise a feed tube 82 extending substantially coaxially with the mixing chamber to

an opening or slurry nozzle tip 67 which is open toward the coagulum zone. This is a highly advantageous feature of the preferred embodiments discussed here. The carbon black slurry, as noted above, is fed to the mixing zone at very high velocity relative the feed velocity of the latex, and the axial arrangement of narrow bore feed tube 82 results in excellent development of flow turbulence. The diameter D_m of the channel 80 (which, as noted above, is preferably substantially equal to the diameter D_1 of immediately following portion of section 74 of the coagulum zone) preferably is at least twice the inside diameter of slurry feed tube 82, more preferably about four to eight times the diameter of feed tube 82, typically about seven to eight times that diameter. Feed tube 82 is seen to form a fluid-tight seal with the entry port 83 at the upstream end of feed channel 61 of mix head 50. The diameter of the axial feed tube 82 is determined largely by the required volumetric flow rate and axial velocity of the slurry as it passes through the slurry nozzle tip 67 into the mixing chamber. The correct or required volume and velocity can be readily determined by those skilled in the art given the benefit of this disclosure, and will be a function, in part, of the concentration and choice of materials. Embodiments such as that illustrated and disclosed here, wherein the feed tube for the carbon black slurry is removable, provide desirable flexibility in manufacturing different masterbatch compositions at different times. The feed tube used in one production run can be removed and replaced by a larger or smaller bore tube appropriate to a subsequent production. In view of the pressure and velocity at which the slurry exits the feed tube, it may be referred to as a spray or jet into the mixing zone. This should be understood to mean in at least certain embodiments, high speed injection of the slurry into an area already substantially filled with fluid. Thus, it is a spray in the sense of its immediate

distribution as it passes through the slurry nozzle tip , and not necessarily in the sense of free-flying material droplets in a simple spreading trajectory.

The additional feed channels 60 and 62 are seen to form a junction 84, 85, respectively, with feed channel 60 and downstream channel 80 at an angle β . The angle β may in many embodiments have a value from greater than 0° to less than 180° . Typically, β may be, for example, from 30° - 90° . It is desirable to avoid a negative pressure, that is, cavitation of the latex fluid as it is entrained by the high velocity slurry exiting at slurry nozzle tip 67, since this may disadvantageously cause inconsistent mixing leading to inconsistent masterbatch product. Air or other gas can be injected or otherwise fed to the mixing zone to assist in breaking any such vacuum. In addition, an expanded feed line for the natural rubber latex leading to the entry port 86 of feed channel 60 is desirable to act as a latex fluid reservoir. In the preferred embodiment of Fig. 4, latex feed channel 60 intersects the mixing zone adjacent slurry nozzle tip 67. Alternatively, however, the latex feed channel can intersect the mixing channel upstream or downstream of the slurry nozzle tip 67.

The carbon black slurry or other particulate filler fluid typically is supplied to feed tube 82 at a pressure above about 300 psig, such as about 500 to 5000 psig, e.g. about 1000 psig. Preferably the liquid slurry is fed into the mixing zone through the slurry nozzle tip 67 at a velocity above 100 ft. per second, preferably about 100 to about 800 ft. per second, more preferably about 200 to 500 ft. per second, for example, about 350 feet per second. Arrows 51 in Fig. 4 represent the general direction of flow of the elastomer latex and auxiliary feed materials through feed channels 60 and 62 into the channel 80 below slurry nozzle tip 67. Thus, the slurry and latex fluids are fed to the mixing zones at greatly different feed stream velocities, in accordance with the numbers

set forth above. While not wishing to be bound by theory, it presently is understood that the differential feed achieves latex shear conditions in the mixing zone leading to good macro-dispersion and coagulation.

5 An alternative preferred embodiment is illustrated in Figs. 5 and 6 wherein the single axial feed tube 82 in the embodiment of Fig. 4 is replaced by multiple axially extending feed tubes 90 - 92. Even greater numbers of feed tubes may be employed, for example, up to about 6 or 8 axially-extending feed tubes. Advantageously, production flexibility is achieved by using different feed tubes of different diameter for production of different formulations. Also, multiple feed tubes can be used simultaneously to
10 achieve good flow turbulence within the mixing zone and coagulum zone of the coagulum reactor.

An alternative embodiment of the mix head is illustrated in Fig. 7. Mix head 150 is seen to define a mixing zone 179. An axial feed channel 161 receives a feed tube 182 adapted to feed carbon black slurry or other particulate filler fluid at high velocity into
15 the mixing chamber 179. It can be seen that the central bore in feed tube 182 terminates at slurry nozzle tip 167. A constant diameter nozzle land 168 is immediately upstream of slurry nozzle tip 167, leading to a larger bore area 169. Preferably the axial dimension of land 168 is about 2 to 6, e.g. about 5, times its diameter. A second feed channel 160 forms a junction 184 with the mixing zone 179 at a 90° angle for feeding
20 elastomer latex fluid to the mixing zone. The cross-sectional diameter of the latex fluid feed channel 160 is substantially larger than the cross-sectional diameter of the slurry nozzle tip 167 and land 168. Without wishing to be bound by theory, the axial elongation of nozzle land 168, coupled with the expanded diameter bore section upstream of the nozzle land, is believed to provide advantageous stability in the flow of slurry

through feed tube 182 into the mixing zone 179. The bore of feed tube 182 is found to function well with a 20° chamfer, that is, conical area 169 which expands in the upstream direction at about a 20° angle. Downstream of mixing zone 179 is an elongate coagulum zone. Consistent with the principles discussed above, such coagulum zone need be only marginally elongate. That is, its axial dimension need be only marginally longer than its diameter. Preferably, however, a progressively enlarged coagulum zone is used.

As discussed above, coagulation of the elastomer masterbatch is substantially complete at or before the end of the coagulum reactor. That is, coagulation occurs without the necessity of adding a stream of coagulant solution or the like. Coagulation may occur in the mixing zone. The mixing zone may be considered all or portion of the coagulum zone for this purpose. Also, reference to substantially complete coagulation prior to the elastomer masterbatch exiting the coagulum reactor is not meant to exclude the possibility of subsequent processing and follow-on treatment steps, for any of various purposes appropriate to the intended use of the final product. In that regard, substantially complete coagulation in preferred embodiments of the novel method disclosed here employing natural rubber latex means that at least about 95 weight percent of the rubber hydrocarbon of the latex is coagulated, more preferably at least about 97 weight percent, and most preferably at least about 99 weight percent is coagulated.

The masterbatch (or other elastomer composite) produced by the wet mixing step optionally undergoes any suitable further processing prior to addition of additional elastomer in the dry mixing step of the wet/dry method disclosed here. Suitable apparatus for the dry mixing step is commercially available and will be apparent to those skilled in the art given the benefit of this disclosure. Suitable dry mixing apparatus

include, for example, Banbury mixers, mills, roller mixers, etc. The coagulum from the wet mixing step, with or without any further intermediate processing, is introduced into the Banbury mixer or other mixing device along with the additional elastomer in any suitable order and relative proportion suitable to the intended use or application. It will be within the ability of those skilled in the art, given the benefit of this disclosure to determine suitable order of addition and relative proportion for the wet mixing product and the additional elastomer. Likewise, it will be within the ability of those skilled in the art given the benefit of this disclosure to select suitable additional ingredients for addition during the dry mixing step suitable to the intended use or application. for example, extender oil, curatives, and other additives known for use in elastomer composites and elastomer composite blends of the general type disclosed here.

The method and apparatus disclosed and described here produce elastomer composite blends having excellent physical properties and performance characteristics. Novel elastomer composite blends of the present invention include masterbatch compositions produced by the above-disclosed method and apparatus, as well as intermediate compounds and finished products made from such masterbatch compositions. Notably, elastomer masterbatch can be produced using natural rubber latex (latex concentrate or field latex), along with various grades of carbon black filler, having excellent physical properties and performance characteristics. Carbon blacks presently in broad commercial use for such application as tire tread have been used successfully, as well as carbon blacks heretofore considered unsuitable for commercial use in known production apparatus and methods. Those unsuitable because their high surface area and low structure rendered them impractical to achieve acceptable levels of macro-dispersion at routine commercial loading levels for the carbon black and/or to

preserve the molecular weight of the elastomer are highly preferred for certain applications of the novel elastomer composite blends disclosed here. Such elastomer composite blend are found to have excellent dispersion of the carbon black in the elastomer. Moreover, these advantageous results were achieved without the need for a
5 coagulation step involving a treatment tank or stream of acid solution or other coagulant. Thus, not only can the cost and complexity of such coagulant treatments be avoided, so too the need to handle effluent streams from such operations also is avoidable also is avoided.

Prior known dry mastication techniques could not achieve equal dispersion of
10 fillers in elastomer composite blends without significant molecular weight degradation and, therefore, could not produce the novel natural rubber compositions made in accordance with certain preferred embodiments of the present invention. In that regard, novel elastomer composite blends are disclosed here having excellent macro-dispersion of carbon black in natural rubber, even of carbon blacks having a structure
15 to surface area ratio DBPA:CTAB less than 1.2 and even less than 1.0, with high molecular weight of the natural rubber. Known mixing techniques in the past did not achieve such excellent macro-dispersion of carbon black without significant molecular weight degradation of the natural rubber and, therefore, did not produce the novel masterbatch compositions and other elastomer composites of the present invention.
20 Preferred novel elastomer composite blends in accordance with this disclosure, having carbon black macro-distribution levels not heretofore achieved, can be used in place of prior known elastomer materials having poorer macro-dispersion. Thus, elastomer composite blends disclosed here can be used as cured compounds in accordance with known techniques. Such novel cured compounds are found in preferred embodiments

to have physical characteristics and performance properties generally comparable to, and in some instances significantly better than, those of otherwise comparable cured compounds comprising masterbatch of poorer macro-dispersion. Elastomer composite blends can be produced in accordance with the present invention, with reduced mixing
5 time, reduced energy input, and/or other cost savings.

As used here, the carbon black structure can be measured as the dibutyl phthalate adsorption (DBPA) value, expressed as cubic centimeters of DBPA per 100 grams carbon black, according to the procedure set forth in ASTM D2414. The carbon black surface area can be measured as CTAB expressed as square meters per gram of carbon black,
10 according to the procedure set forth in ASTM D3765-85. It will be recognized that other factors affecting the level of dispersion achievable using the method and apparatus disclosed here, include the concentration of the carbon black in the slurry, total energy input into the slurry and energy input during mixing of the fluid streams, etc.

The macro-dispersion quality of carbon black in natural rubber masterbatch
15 disclosed here is significantly better than that in previously known masterbatch of approximately equal MW_{sol} (weight average). In some preferred embodiments excellent carbon black distribution is achieved with MW_{sol} approximately equal to that of natural rubber in the field latex state, (e.g., approximately 1,000,000) a condition not previously achieved. The dispersion quality advantage is especially significant in the above
20 mentioned preferred embodiments using carbon black with low structure and high surface area, e.g., DBPA less than 110cc/100g, CTAB greater than 45 to 65 m²/g, and DBPA:CTAB less than 1.2 and preferably less than 1.0.

EXAMPLES

Blends-CIP

45

Test Procedures

The following test procedures were used in the examples and comparisons presented below.

1. **Bound Rubber:** A sample weighing .5 g. $\pm$.025 g. is weighed and placed in
5 100 ml. toluene in a sealed flask and stored at ambient temperature for approximately
24 hours. The toluene is then replaced with 100 ml. fresh toluene and the flask is
stored for 4 days. The sample is then removed from the solvent and air-dried under
a hood at ambient temperature for 24 hours. The sample is then further dried in a
vacuum oven at ambient temperature for 24 hours. The sample is then weighed and
10 the bound rubber is calculated from the weight loss data.

2. **MW_{sol}:** As used in this disclosure and in the claims, MW_{sol} refer to weight
average molecular weight of the sol portion of the natural rubber. Standard GPC
techniques for molecular weight measurement were followed in accordance with the
following:
 - 15 2.1 Two 10 μ m 10⁶ Å columns, a 10 μ m 500Å column and a 10 μ m mixed
bed column from Polymer Laboratories, UK.
 - 2.2 UV detection at 215nm.
 - 2.3 Solvent: Tetra hydro furan (THF)
 - 2.4 Concentration, nominally 2mg/ml in THF.
 - 20 2.5 Samples are left to dissolve in THF for 3 days, stabilized with BHT.
 - 2.6 Solutions are centrifuged to separate any gel and the supernatant is
injected onto the column.
 - 2.7 Sample Preparations Sample preparation is designed to prepare sol
concentrations in the range of 0.5 to 0.05 percent by weight to provide
25 a good detector response for accurate measurement of the molecular

weight distribution. Depending on the filler loading, sample weight is adjusted according to the following formula:

$$\text{sample wt.} = (100 + \text{filler loading (phr)}) * 20/100 \text{ mg} \pm 2 \text{ mg}$$

5 Samples are placed in UV protected vials and dissolved in 4 mL of stabilized tetrahydrofuran (THF) containing 0.02% butylated-hydroxytoluene (BHT) for three days. The supernatant from the dissolution step, containing mostly the sol portion, is transferred to Teflon centrifuge tubes and centrifuged in an Avanti 30 (Beckman) centrifuge for 60 minutes at 26,000 revolutions per minute (corresponding to a maximum field strength of 57,500 g). At this field strength, a majority of the gel phase sediments allowing a gel-free supernatant. This gel-free solution is diluted at 1:5, again using stabilized THF. At this point, the samples are transferred to GPC vials and placed inside a Waters 717 Auto-Sampler (Water Corporation, 10 Milford, Massachusetts, USA) in preparation for the GPC testing. 15

Molecular Weight Determination The weight average molecular weight of the sol portion MW_{so} is then determined. Using Millenium software (available from Waters Corporation, Milford, Massachusetts, USA) a baseline is defined using a valley-to-valley mode within the time increments of 15 and 35 minutes. This time increment is appropriate for the column set described above in paragraph 2.1 with the mobile phase flow rate set at 0.75 mL/min. Once a reasonable baseline is established the distribution can be determined. The elution time is converted to molecular weight. Polystyrene solutions made from commercially available standards (EasiCal : Polymer Laboratories, U.K.) are prepared containing a series of molecular weights with very narrow distributions. The conversion of polystyrene molecular weight to polyisoprene molecular weight equivalents is based on the universal calibration method of Benoit and coworkers. The hydrodynamic radius is proportional to the product of the molecular weight times the intrinsic viscosity. After converting the polystyrene molecular weights to polyisoprene equivalents, the calibration curve relates absolute molecular weight to elution time. The standards are run under conditions identical to the samples, and the standards are integrated to assign the appropriate molecular weight for a given elution time, based on a best fit to the standards data. Once the time based distribution is properly converted to molecular weight, the appropriate molecular weight averages are calculated by the Waters' Millenium software. 20 25 30 35

3. **Mooney Viscosity:** Standard procedures were followed for ML 40 (1+4)@100°C. 4. **Test Sample Cure Conditions:** Test pieces were cured to 150°C for the time periods indicated below:

Blends-CIP

47

SUBSTITUTE SHEET (RULE 26)

- 4.1 Tensile Sheet: 20 min.
 - 4.2 Resilience: 23 min.
 - 4.3 Hardness: 23 min.
 - 4.4 Heat Build-Up: 25 min.
5. **Dispersion:** The Cabot Dispersion Chart method is used with subjective evaluation of 50x optical micrographs. (ASTM D2663 Method).
6. **Stress-Strain:** Tested to BS903:A2 and ISO 37.
7. **Hardness:** Tested to ISO 48 (1994), temperature 23°C.
8. **Resilience:** Tested to BS903:A8 (1990), Method A, temperature 23°C (8 mm molded disc test piece).
9. **Heat Buildup:** Tested to ASTM D623, Method A.
- 9.1 Start temperature: 23°C
 - 9.2 Static load: 24 lbs.
 - 9.3 Stroke: 0.225 inches.
 - 9.4 Frequency: 30 Hz.
 - 9.5 Run for 30 minutes.
10. **Tan δ :** Measured on Rheometrics® model RDS II. Reported values are maximums from strain sweeps. Strain sweeps at 0°, 30°, and 60°C, 1 Hz, and 0.1% to 60% strain.
11. **Crack Growth Resistance:** Measured in accordance with ASTM D3629-94

Example A

Elastomer masterbatch was produced in accordance with the present invention. Specifically, an elastomer masterbatch was produced comprising standard natural rubber field latex from Malaysia with 52.5 phr filler consisting of carbon black of

commercial grade N234 available from Cabot Corporation. The properties of the natural rubber field latex are provided in Table 1 below.

Table 1 Natural Rubber Latex Properties

Additives	% Dry Rubber	% Total Solids	% Ash	Nitrogen ppm	Volatile Fatty Acid	ML(1+4) @100 C
0.15% HNS ^a 0.3% NH ₃ , ZnO, TMTD ^b	28.4	34.2	0.38	0.366	0.052	68

- a. HNS: hydroxylamine neutral sulfate, Mooney viscosity stabilizer.
b. ZnO/TMTD: used for biological preservation, typically 0.025% of 1:1 mixture.

The full compound formulation is set forth in Table 2 below, and is representative of a commercial truck tire tread known to have excellent resistance to reversion during cure.

Table 2 Masterbatch Formulation

<u>Ingredient</u>	<u>Parts by Wt.</u>
Rubber	100
Carbon Black	52.5
ZnO	4.0
Stearic acid	2.0
6PPD (antioxidant)	2.0
Sunproof Improved (wax)	2.0
Ennerflex 74 (aromatic oil)	3.0
Total	165.5

The elastomer masterbatch production apparatus was substantially identical to the apparatus described above with reference to Figs. 1 and 7 of the drawings. The slurry nozzle tip (see reference No. 167 in Fig. 7) was .039 inch diameter with a land (see reference No. 168 in Fig. 7) having an axial length of 0.2 inch. The coagulum zone was 0.188 inch diameter and had .985 inch axial length of constant diameter between

the mixing zone and its discharge end. Preparation of the masterbatch is described in further detail immediately below.

1. Carbon Black Slurry Preparation. Bags of carbon black were mixed with deionized water in a carbon black slurry tank equipped with an agitator. The agitator broke the pellets into fragments and a crude slurry was formed with 12.5 wt. % carbon black. During operation, this slurry was continually pumped by an air diaphragm pump to a colloid mill for initial dispersion. The slurry was then fed by a progressing cavity pump to a homogenizer, specifically, a model M3 homogenizer from APV Gaulin, Inc. The homogenizer produced a finely ground slurry. The slurry flow rate from the homogenizer to the mixing zone was set by the homogenizer speed, the homogenizer acting as a high-pressure positive displacement pump. Slurry flow rate was monitored with a Micromotion® mass flow meter. The carbon black slurry was fed to the homogenizer at a pressure ranging from 50 to 100 psig and the homogenization pressure was set at 4000 psig, such that the slurry was introduced as a jet into the mixing zone at a flow rate of 4.1 to 4.4 lb/min and at a velocity of about 130 ft/sec.
2. Latex Delivery. The latex was charged to a 100 gallon pressurized feed tank. Antioxidant emulsion was added to the latex prior to charging. Antioxidants were added consisting of 0.3 phr tris nonyl phenyl phosphite (TNPP) and 0.4 phr Santoflex® 134 (alkyl-aryl p-phenylene diamine mixture). Each of the antioxidants was prepared as a 15 wt. % emulsion using 3 parts potassium oleate

per 100 parts antioxidant along with potassium hydroxide to adjust the emulsion to a pH of approximately 10. Also, 3 phr extender oil was added. Air pressure (51 psig) was used to move the latex from the feed tank to the mixing zone of the coagulum reactor. The latex flow rate was 3.2 to 3.4 lbs/min and about 3.8 feet per second, and was automatically metered and controlled with a Micromotion® mass flow meter and a rubber tube pinch valve. The desired carbon black loading of a 52.5 phr was obtained by maintaining proper ratio of the latex feed rate to the carbon black slurry feed rate.

3. Carbon Black and Latex Mixing. The carbon black slurry and latex were mixed by entraining the latex into the carbon black slurry. During entrainment, the carbon black was intimately mixed into the latex and the mixture coagulated. Soft, wet spongy "worms" of coagulum exited the coagulum reactor.
4. Dewatering. The wet crumb discharged from the coagulum reactor was about 79% water. The wet crumb was dewatered to about 5 to 10% moisture with a dewatering extruder (The French Oil Mill Machinery Company; 3½ in. diameter). In the extruder, the wet crumb was compressed and water squeezed from the crumb and through a slotted barrel of the extruder.
5. Drying & Cooling. The dewatered crumb dropped into a second extruder where it was again compressed and heated. Water was flashed off upon expulsion of the crumb through the dieplate of the extruder. Product exit

temperature was approximately 300°F and moisture content was about 0.5 to 1 wt.%. The hot, dry crumb was rapidly cooled (approximately 20 seconds) to about 100°F by a forced air vibrating conveyor. The resulting dry crumb had about 66. wt.% rubber solids and about 33. wt.% carbon black.

5 **Example B**

A control masterbatch was prepared by dry mastication. The control employed the same formulation as Example A (see Table 2 above), except that the natural rubber was SMR 10 rather than latex. It was prepared by premastication of the rubber in a OOC Banbury mixer (approximately 3 kg) at 50 rpm using 10 phr carbon black. The
10 premastication was performed for approximately 3 min. to a total of 800 MJ/m³.

Comparisons of Example A and Example B

The masterbatch of Example A and the control masterbatch of Example B were compounded in a two-stage mixing operation in a OOC Banbury mixer (approximately 3 kg). Table 3 below sets forth the mixing schedule for the first stage. It can be seen
15 that the Example A masterbatch followed a modified mixing schedule.

Table 3 Stage 1 Mixing Schedules

Time (min)	Example A	Example B Dry Mix Control
0.0	All ingredients	Pre-Masticated Rubber
0.5		Carbon Black and Oil
1.0	Sweep	
1.5		Remaining Ingredients

2.0			
2.5		Sweep	
3.0			
X	dump at approx. 700 MJ/m ³	dump at approx. 1,000 MJ/m ³	

5 In the second stage, curatives listed in Table 4 below were added with a further mixing cycle of 500 MJ/m³.

Table 4 Final Stage Curative Addition

	<u>Ingredient</u>	<u>Parts by Wt.</u>
10	Stage 1 compound	165.5
	Goodyear Winstay 100 (antioxidant)	1.0
	TBBS (sulfur accelerator)	1.8
	Sulfur	1.0
	Total	169.3

15 Thus, Banbury mixing energy for the compounding of Example A masterbatch was about 53% of the Banbury mixing energy required for the premastication and compounding of the control material of Example B. Despite the reduced energy input, the Example A material was found to have very good macro-dispersion, and the molecular weight (weight average) of its sol portion MW_{sol} was substantially higher

20 than that of the control. These data are summarized in Table 5 below.

Table 5 Compounding and Curing Data

Sample	Mix Energy (MJ/m ³)				ML (1+4, 100C)		MW
	Pre-Masticate	Stage 1	Final	Total	Stage 1	Final	wt. av.

Example A	0	694	500	1,194	102	72	444,900
Example B	800	965	500	2,265	92	67	327,000

Additional testing results for the cured (unaged) Example A and control material are set forth in Table 6 below.

Table 6 Additional Test Data

Sample	Hardness	100% Modulus (MPa)	300% Modulus (MPa)	Tensile (MPa)		
Example A	71	2.82	16.1	28.7		
Example B	72	3.12	16.2	28.5		
Sample	Elongation at Break (%)	Resilience (%)	Heat Build-Up (°C)	Max Tan Delta		
				60°C	30°C	0°C
Example A	526	56.5	70.5	0.203	0.240	0.290
Example B	511	57.6	76.5	0.206	0.236	0.286

Example C

Elastomer masterbatch was produced in accordance with the present invention. Specifically, an elastomer masterbatch was produced comprising standard natural rubber field latex from Malaysia with 55 phr filler consisting of carbon black of commercial grade Regal ® 660 available from Cabot Corporation. The compound formulation (excluding minor ordinary latex additives) is set forth in Table 7 below.

Table 7 Masterbatch Formulation

Ingredient	Parts by Wt.
Rubber	100
Carbon Black	55.
Santoflex 134 (antioxidant)	0.4
TNPP (antioxidant)	0.3
Total	155.7

The elastomer masterbatch production apparatus was substantially identical to the apparatus described above with reference to Figs. 1, 3 and 7 of the drawings. The slurry nozzle tip (see reference No. 167 in Fig. 7) was .025 inch diameter with a land (see reference No. 168 in Fig. 7) having an axial length of 0.2 inch. The coagulum zone (see No. 53 in Fig. 3) included a first portion of .188 inch diameter and approximately .985 inch axial length (being partly within the mix-head and partly within the extender sealed thereto); a second portion of .266 inch diameter and 1.6 inch axial length; a third portion of .376 inch diameter and 2.256 axial length; and a fourth portion of .532 inch diameter and 3.190 inch axial length. In addition, there are axially short, faired interconnections between the aforesaid portions. Preparation of the masterbatch is described in further detail immediately below.

1. Carbon Black Slurry Preparation. Bags of carbon black were mixed with deionized water in a carbon black slurry tank equipped with an agitator. The agitator broke the pellets into fragments and a crude slurry was formed with 14.9 wt. % carbon black. The crude slurry was recirculated using a pipeline grinder. During operation, this slurry was continually pumped by an air diaphragm pump to a colloid mill for initial dispersion. The slurry was then fed by a progressing cavity pump to a homogenizer, specifically, Microfluidizer Model M210 from Microfluidics International Corporation for pressurizing and shear, to produce a finely ground slurry. The slurry flow rate from the microfluidizer to the mixing zone was set by the microfluidizer speed, the microfluidizer acting as a high-pressure positive displacement pump. Slurry flow rate was monitored with a Micromotion® mass flow meter. The carbon

black slurry was fed to the microfluidizer at a pressure of about 130 psig and the output pressure was set at 3000 psig to an accumulator set at 450 psig output pressure, such that the slurry was introduced as a jet into the mixing zone at a flow rate of about 3.9 lb/min and at a velocity of about 300 ft/sec.

- 5 2. Latex Delivery. The latex was charged to a tank, specifically, a 55 gallon feed drum. Antioxidant emulsion was added to the latex prior to charging. Antioxidants were added consisting of 0.3 phr tris nonyl phenyl phosphite (TNPP) and 0.4 phr Santoplex® 134 (alkyl-aryl p-phenylene diamine mixture). Each of the antioxidants was prepared as a 40 wt.% emulsion using 4 parts
10 potassium oleate per 100 parts antioxidant along with potassium hydroxide to adjust the emulsion to a pH of approximately 10. A peristaltic pump was used to move the latex from the feed tank to the mixing zone of the coagulum reactor. The latex flow rate was 3.2 to 3.3 lbs/min and about 3.9 feet per second, and was metered with a Endress + Hauser (Greenwood, Indiana, USA)
15 mass flow meter. The desired carbon black loading of a 55 phr was obtained by maintaining proper ratio of the latex feed rate to the carbon black slurry feed rate.
- 20 3. Carbon Black and Latex Mixing. The carbon black slurry and latex were mixed by entraining the latex into the carbon black slurry. During entrainment, the carbon black was intimately mixed into the latex and the mixture coagulated. Soft, wet spongy "worms" of coagulum exited the coagulum reactor.

4. Dewatering. The wet crumb discharged from the coagulum reactor was about 78% water. The wet crumb was dewatered to about 12 to 13% moisture with a dewatering extruder (The French Oil Mill Machinery Company; 3½ in. diameter). In the extruder, the wet crumb was compressed and water squeezed from the crumb and through a slotted barrel of the extruder.
5. Drying & Cooling. The dewatered crumb dropped into a second extruder where it was again compressed and heated. Water was flashed off upon expulsion of the crumb through the dieplate of the extruder. Product exit temperature was approximately 280°F to 370°F and moisture content was about 0.3 to .4 wt.%. The hot, dry crumb was rapidly cooled (approximately 20 seconds) to about 100°F by a forced air vibrating conveyor.

Examples D and E

Two dry mix control masterbatches were prepared by dry mastication. The controls employed the same formulation as Example C (see Table 7 above), except that in Example D the rubber was RSS1 NR rather than latex. In Example E the rubber was SMR 10 NR. Each was prepared by premastication of the rubber in a BR Banbury mixer. The rubber of Example D was masticated at 118 rpm for 10 minutes. The rubber of Example E was masticated at 77 rpm for 4 minutes.

Comparison of Examples C, D and E

The masterbatch of Example C and the two control masterbatches of Example D and E were compounded in a BR Banbury mixer. Table 8 below sets forth the compounding schedules.

5

Table 8 Compounding Schedules

Masterbatch	Pre-Mastication	Stage I Mixing	Stage II (Final) Mixing
Example C	No	No	BR Banbury 77 rpm, 4.5 min.
Example D	BR Banbury mixer 118 rpm, 10 min.	BR Banbury mixer 77 rpm, 3 min.	BR Banbury 77 rpm, 4.5 min.
Example E	BR Banbury mixer 77 rpm, 4 min.	BR Banbury mixer 77 rpm, 8 min.	BR Banbury 77 rpm, 4.5 min.

10

The compounding formulation is given in Table 9 below.

Table 9 Stage II Curative Addition

	<u>Ingredient</u>	<u>Parts by Wt.</u>
15	Example 4 Masterbatch or Example 5 or 6 Stage 1 Dry Mix	155
	Azo 66 (zinc oxide)	4.0
	Hystrene 5016 (stearic acid)	2.0
	Santoflex 13 (antioxidant)	2.0
	Sunproof Improved (wax)	2.0
20	Wingstay 100 (antioxidant)	1.0
	Santocure NS (sulfur accelerator)	1.8
	<u>Sulfur</u>	<u>1.0</u>
	Total:	168.8

All three compounds exhibited well-behaved cure with minimal reversion. Despite the reduced energy input, the Example C material was found to have significantly better

25

macro-dispersion than the dry mix controls, and the molecular weight (weight average) of its sol portion MW_{sol} was substantially higher than that of the controls. These data are summarized in Table 10 below.

Table 10 Masterbatch and Compound Properties

	Example C	Example D	Example E
5	Masterbatch Properties		
	Mooney Viscosity ML(1+4)@100C	125	124
	Bound Rubber (%)	50	32
10	MW sol ($\times 10^{-6}$)	0.678	.466
	Percent Undispersed Area (D%)	.12	1.48
	Compound Properties		
15	Hardness	62	65
	100% Modulus (psi)	239	315
	300% Modulus (psi)	1087	1262
20	Tensile strength (psi)	4462	4099
	Elongation, %	675	591
25	Max. Tan Delta @ 60 C (Strain Sweep)	0.189	.237
	Crack Growth Rate (cm/per million cycles)	0.8	5.0
			5.8

30 **Additional Examples and Comparisons**

Highly preferred elastomer composites in accordance with the present invention were produced in accordance with the method and apparatus disclosed above. In

particular, novel masterbatch compositions were formed of natural rubber latex and carbon black filler, having significantly better macro-dispersion levels and/or natural rubber molecular weight than heretofore found in known compositions formed of the same or similar starting materials. Fig. 8 shows the surface area and structure of various carbon black fillers used in these preferred masterbatch compositions, specifically, the CTAB surface area expressed as square meters per gram of carbon black per ASTM D3765-85 and dibutyl phthalate absorption (DBPA) value expressed as cubic centimeters of DBP per hundred grams carbon black per ASTM D2414 are shown. Fig. 8 is seen to be divided into three different regions of carbon blacks. Region I contains carbon blacks having lower structure and higher surface area, being those most difficult to disperse in natural rubber and other elastomers using traditional dry mixing techniques. Hence, carbon blacks of Region I are not used commercially as widely as other carbon blacks. Masterbatch and cured elastomeric compositions made with Region I carbon blacks using traditional dry mixing techniques have poorer macro-dispersion and typically lower MW_{sol} . The carbon blacks of Region II have higher structure than those of Region I. Typically, they achieve reasonably good dispersion in natural rubber for vehicle tire products and the like if subjected to such extended dry mixing that the MW_{sol} of the natural rubber is significantly degraded. The carbon blacks of Region III of Fig. 8 have lower surface area relative their structure. Accordingly they have been used with acceptable dispersion in natural rubber via dry mixing, but again, with undesirable degradation of MW_{sol} . The dispersion of carbon blacks of all three regions of Fig. 8, specifically, macro-dispersion, is significantly improved in the elastomer composites disclosed here, and

can be achieved with significantly higher MW_{sol} of the natural rubber in accordance with preferred embodiments.

Control Samples 1 - 443

Control samples of masterbatch were prepared by dry mixing in accordance with the following procedures, for purposes of comparison to elastomer composites of the present invention.

1. Mastication of Natural Rubber

In order to produce dry masterbatches with a wide range of molecular weight, commercial natural rubber (RSS1, SMR CV, and SMR 10) bales were pre-masticated in a BR banbury mixer using the following conditions (fill factor: 0.75):

Table 11 Natural Rubber Mastication Conditions

Sample Code	Mastication	Rotor Speed (rpm)	Cooling Water	Mastication time (min.)
M1	No			
M2	Yes	77	On	4
M3	Yes	118	On	6
M4	Yes	118	On	10

2. Mixing Carbon Black with Pre-Masticated Natural Rubber

In order to prepare natural rubber dry masterbatches with different levels of macro-dispersion quality, the following mixing procedures were used in a BR Banbury mixer. The fill factor was 0.70. The masterbatch ingredients and mixing procedures are described as follows in Table 12.

Table 12 Natural Rubber Dry Masterbatch Formulation

Ingredient	phr (Parts per hundred parts of rubber by weight)
Natural Rubber	100
Carbon Black	See Tables Below
Oil	See Tables Below
Santofex (antioxidant)	0.4
TNPP (antioxidant)	0.3
Mixing Procedures: 0 minute: Add pre-masticated natural rubber (77 rpm, 45 C) 1 minute: Add black, oil and antioxidants	

Different levels of macro-dispersion were produced by dry mixing samples of M1 through M4 pre-masticated natural rubber for different mixing times, as shown in Table 13, below. For example, sample code M2D1 in Table 13 indicates a control sample of premasticated natural rubber M2 (see Table 11, above) mixed for 10 minutes in accordance with the formulation of Table 12.

Table 13 Mixing Times

Dry NR Masterbatch Sample Code	Pre-Masticated NR	Mixing Time
M1D4	M1	4
M1D3	M1	6
M1D2	M1	8
M1D1	M1	10
M2D4	M2	4
M2D3	M2	6
M2D2	M2	8
M2D1	M2	10

M3D4	M3	4
M3D3	M3	6
M3D2	M3	8
M3D1	M3	10
M4D4	M4	4
M4D3	M4	6
M4D2	M4	8
M4D1	M4	10

3. Final mixing of Natural Rubber Masterbatch Control Samples

To evaluate compound performance, additional ingredients were added to the dry masticated natural rubber masterbatch control samples of Table 13 in accordance with the formulation shown in Table 14.

Table 14 Additional Ingredients for Final Mixing

Ingredient	Amount (phr)
Azo 66 (zinc oxide)	4.0
Hystere 5016 (stearic acid)	2.0
Santoflex 13 (antioxidant)	2.0
Sunproof Improved (wax)	2.0
Wingstay 100 (antioxidant)	1.0
Santocure NS (sulfur accelerator)	1.8
Sulfur	1.0

The compounds were cured in accordance with standard cure techniques at 150°C until at least substantially completely cured, typically between 10 and 30 minutes. In that regard, the same or substantially the same final mixing procedures, including the

formulation given above in Table 14, were used for all control samples, as well as all samples of elastomer composites of the invention prepared in the manner described below (see "Preferred Embodiments Examples) which were cured and tested for compound properties and performance characteristics.

5 The following tables 15 - 23 set forth the sol molecular weight MW_{sol} and macro-dispersion $D(\%)$ of control samples 1 through 443. The samples are grouped in the tables according to choice of carbon black. Within a given table, the samples are grouped by choice of natural rubber and by carbon black loading and oil loading. The table headings show this information in accordance with standard nomenclature. Thus, for example, the
10 heading for Table 15 "N330/55phr/0" indicates 55phr N330 carbon black with no oil. The table sub-headings show the choice of natural rubber. Specifically, control samples 1 through 450 are seen to be made from standard grade natural rubber RSS1, SMRCV and SMR10. Technical description of these natural rubbers is widely available, such as
15 in Rubber World Magazine's Blue Book published by Lippincott and Peto, Inc. (Akron, Ohio, USA). The molecular weight MW_{sol} of the natural rubber prior to any premastication (M1) and after the various amounts of premastication (M2-M4) also are shown below in Tables 15 - 23.

Table 15

Code	N330/55phr/0					
	RSS1			SMRCV		
	Sample No.	Mw _{mol} (K)	D (%)	Sample No.	Mw _{mol} (K)	D (%)
M1		1300			971	
M2		932			725	
M3		664			596	
M4		485			482	
M1D1	1	465	4.24	17	426	4.35
M1D2	2	571	3.70	18	467	3.89
M1D3	3	706	4.79	19	486	4.86
M1D4	4	770	4.52	20	535	4.78
M2D1	5	445	3.66	21	380	2.44
M2D2	6	490	2.68	22	398	3.71
M2D3	7	512	3.68	23	433	4.30
M2D4	8	581	3.93	24	498	5.81
M3D1	9	373	1.33	25	342	3.79
M3D2	10	402	2.50	26	358	4.35
M3D3	11	407	2.98	27	371	5.55
M3D4	12	452	3.35	28	408	5.01
M4D1	13	311	3.63	29	311	3.66
M4D2	14	337	3.40	30	325	5.31
M4D3	15	362	5.03	31	344	5.91
M4D4	16	382	5.23	32	369	5.67

Table 16

Code	Black Pearl 800/55phr/0					
	RSS1			SMRCV		
	Sample No.	Mw _{mol} (K)	D (%)	Sample No.	Mw _{mol} (K)	D (%)
M1		1041			869	
M2		786			662	
M3		663			491	
M4		527			420	
M1D1	113	507	12.20	129	418	5.15
M1D2	114	551	15.10	130	482	4.94
M1D3	115	700	10.20	131	515	6.93
M1D4	116	786	5.72	132	583	8.74
M2D1	117	420	5.65	133	403	2.60
M2D2	118	441	6.50	134	438	2.74
M2D3	119	549	7.70	135	434	2.83
M2D4	120	606	5.88	136	530	3.88
M3D1	121	387	3.26	137	366	2.38
M3D2	122	409	2.98	138	378	2.83
M3D3	123	456	3.61	139	399	3.04
M3D4	124	483	4.61	140	431	2.39
M4D1	125	339	2.13	141	311	2.22
M4D2	126	367	2.23	142	332	2.27
M4D3	127	360	2.60	143	344	2.27
M4D4	128	403	1.96	144	390	2.73

Table 17

Code	N351/33phr/20phr		
	RSS1		
	Sample No.	Mw _{mol} (K)	D (%)
M1		1300	
M2		803	
M3		601	
M1D1	401	854	2.08
M1D2	402	969	3.41
M1D3	403	1040	3.68
M1D4	404	1130	4.91
M2D1	405	648	1.15
M2D2	406	668	2.16
M2D3	407	675	2.98
M2D4	408	721	4.70
M3D1	409	532	1.10
M3D2	410	537	2.17
M3D3	411	535	2.45
M3D4	412	558	4.06

Blends-CIP

66

SUBSTITUTE SHEET (RULE 26)

Table 18A

Code	Regal 250/55phr/t					
	RSS1			SMRCV		
	Sample No.	Mw _{mol} (K)	D (%)	Sample No.	Mw _{mol} (K)	D (%)
M1		1332			1023	
M2		896			748	
M3		603			581	
M4		408			504	
M1D1	33	585	6.95	49	609	1.93
M1D2	34	669	8.03	50	634	3.29
M1D3	35	759	10.5	51	681	2.21
M1D4	36	896	14.1	52	702	4.09
M2D1	37	580	2.71	53	539	2.14
M2D2	38	602	2.61	54	569	2.72
M2D3	39	631	3.61	55	587	4.75
M2D4	40	667	5.43	56	595	6.25
M3D1	41	457	1.53	57	466	2.88
M3D2	42	476	2.09	58	449	3.19
M3D3	43	493	2.32	59	464	4.53
M3D4	44	495	3.54	60	500	5.89
M4D1	45	372	1.53	61	423	2.89
M4D2	46	382	2.09	62	433	3.42
M4D3	47	381	2.32	63	437	4.39
M4D4	48	403	3.54	64	447	4.73

Table 18B

Code	Regal 250/65/0			Regal 250/75/0			Regal 250/65/10		
	RSS1			RSS1			RSS1		
	Sample No.	Mw _{mol} (K)	D (%)	Sample No.	Mw _{mol} (K)	D (%)	Sample No.	Mw _{mol} (K)	D (%)
M1		1138			1138			1138	
M2		901			901			901	
M3		660			660			660	
M4		483			483			483	
M1D1	65	570	1.50	81	539	2.87	97	661	1.89
M1D2	66	622	3.25	82	624	4.50	98	702	2.69
M1D3	67	707	7.50	83	685	4.17	99	741	3.14
M1D4	68	788	4.77	84	763	14.35	100	822	5.24
M2D1	69	534	1.62	85	484	4.32	101	593	0.91
M2D2	70	548	4.19	86	512	2.96	102	572	3.48
M2D3	71	585	4.31	87	557	4.71	103	642	4.23
M2D4	72	621	6.21	88	605	4.85	104	664	5.35
M3D1	73	459	3.64	89	429	2.27	105	507	2.65
M3D2	74	469	5.79	90	446	2.68	106	544	2.96
M3D3	75	511	5.30	91	466	3.46	107	535	3.69
M3D4	76	541	9.13	92	491	6.22	108	524	3.27
M4D1	77	380	2.34	93	368	2.11	109	416	1.85
M4D2	78	392	2.86	94	372	3.13	110	413	3.18
M4D3	79	399	4.59	95	375	2.92	111	418	6.96
M4D4	80	395	4.57	96	388	2.92	112	441	6.46

Blends-CIP

67

SUBSTITUTE SHEET (RULE 26)

Table 19

Code	N326/55phr/0					
	RSS1			SMRCV		
	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)
M1		1200			1060	
M2		1030			934	
M3		724			777	
M4		635			644	
M1D1	145	550	3.49	161	644	1.15
M1D2	146	636	3.54	162	661	1.32
M1D3	147	650	5.89	163	697	1.35
M1D4	148	724	4.79	164	732	2.01
M2D1	149	517	3.16	165	590	1.50
M2D2	150	572	2.41	166	621	1.56
M2D3	151	613	3.11	167	641	2.22
M2D4	152	696	4.37	168	676	2.31
M3D1	153	489	2.78	169	551	1.22
M3D2	154	521	1.93	170	550	1.62
M3D3	155	504	3.14	171	563	2.06
M3D4	156	538	2.81	172	578	2.68
M4D1	157	415	1.74	173	487	1.96
M4D2	158	447	2.17	174	495	2.22
M4D3	159	466	3.13	175	505	2.99
M4D4	160	469	2.93	176	526	3.37

Table 21(A)

Code	S6740/55phr/0			
	RSS1			
	Sample No.	Mw _{sol} (K)	D (%)	
M1		1080		
M2		837		
M3		724		
M4		532		
M1D1	412	515	1.24	
M1D2	413	556	1.32	
M1D3	414	633	1.41	
M1D4	415	732	1.43	
M2D1	416	433	0.86	
M2D2	417	451	0.90	
M2D3	418	495	1.53	
M2D4	419	542	2.15	
M3D1	420	405	0.25	
M3D2	421	418	0.50	
M3D3	422	447	0.75	
M3D4	423	469	0.73	
M4D1	424	371	0.21	
M4D2	425	387	0.42	
M4D3	426	382	0.30	
M4D4	427	396	0.56	

Table 20

Code	N110/55phr/0					
	RSS1			SMRCV		
	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)
M1		937			730	
M2		764			653	
M3		569			541	
M4		449			463	
M1D1	369	360	1.24	385	334	1.28
M1D2	370	426	2.50	386	339	1.60
M1D3	371	490	2.69	387	372	1.42
M1D4	372	618	4.68	388	413	2.80
M2D1	373	340	0.69	389	309	0.72
M2D2	374	356	0.85	390	314	1.17
M2D3	375	395	0.90	391	342	1.27
M2D4	376	433	1.17	392	380	2.94
M3D1	377	295	0.81	393	271	0.94
M3D2	378	313	1.27	394	292	0.93
M3D3	379	333	1.20	395	314	1.43
M3D4	380	353	1.35	396	351	1.77
M4D1	381	255	1.12	397	260	0.74
M4D2	382	269	1.14	398	267	0.93
M4D3	383	287	1.30	399	284	1.49
M4D4	384	316	1.67	400	297	1.83

Table 21(B)

Code	S6740/55phr/0			
	SMRCV			
	Sample No.	Mw _{sol} (K)	D (%)	
M1		876		
M2		754		
M3		574		
M4		444		
M1D1	428	433	0.25	
M1D2	429	441	0.36	
M1D3	430	467	0.34	
M1D4	431	540	0.84	
M2D1	432	399	0.35	
M2D2	433	399	0.41	
M2D3	434	422	0.62	
M2D4	435	469	0.44	
M3D1	436	340	0.44	
M3D2	437	363	0.81	
M3D3	438	377	0.89	
M3D4	439	403	0.86	
M4D1	440	363	0.65	
M4D2	441	328	1.05	
M4D3	442	342	1.52	
M4D4	443	360	1.99	

Blends-CIP

68

SUBSTITUTE SHEET (RULE 26)

Table 22(A)

Code	Regal 660/55phr/0								
	RSS1			SMRCV			SMR10		
	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)
M1		1110			836			746	
M2		844			709			632	
M3		609			584			492	
M4		522			513			416	
M1D1	177	674	8.35	193	564	1.87	209	501	9.54
M1D2	178	792	7.89	194	611	2.50	210	572	6.68
M1D3	179	891	8.53	195	708	3.08	211	681	7.37
M1D4	180	676	7.46	196	671	2.31	212	594	7.18
M2D1	181	598	8.56	197	520	5.28	213	463	2.82
M2D2	182	602	3.89	198	558	4.85	214	483	4.57
M2D3	183	697	6.40	199	603	2.88	215	565	3.92
M2D4	184	659	5.71	200	541	4.25	216	550	5.68
M3D1	185	473	2.03	201	486	2.79	217	395	2.13
M3D2	186	506	1.66	202	482	2.76	218	393	1.98
M3D3	187	562	1.94	203	504	3.54	219	443	2.49
M3D4	188	559	4.33	204	526	2.41	220	449	1.90
M4D1	189	401	2.18	205	415	3.16	221	335	1.49
M4D2	190	426	1.72	206	418	2.92	222	345	1.71
M4D3	191	466	1.48	207	446	2.80	223	363	1.78
M4D4	192	449	3.57	208	465	3.13	224	374	2.35

Table 22(B)

Code	Regal 660/45/0			Regal 660/65/0			Regal 660/65/10		
	RSS1			RSS1			RSS1		
	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)
M1		1245			1245			1245	
M2		876			876			876	
M3		625			625			625	
M4		482			482			482	
M1D1	225	646	3.45	241	563	14.55	257	639	1.63
M1D2	226	697	3.04	242	638	14.09	258	699	3.55
M1D3	227	762	7.70	243	691	13.64	259	814	5.44
M1D4	228	830	6.75	244	790	11.26	260	764	11.25
M2D1	229	574	4.79	245	469	5.88	261	572	2.77
M2D2	230	589	3.02	246	507	7.31	262	580	4.39
M2D3	231	636	6.41	247	558	9.72	263	610	5.51
M2D4	232	675	6.55	248	543	10.59	264	638	7.29
M3D1	233	471	2.66	249	420	5.48	265	474	4.10
M3D2	234	481	5.17	250	426	6.97	266	485	5.72
M3D3	235	510	7.78	251	468	8.81	267	502	6.24
M3D4	236	518	7.89	252	471	9.55	268	495	7.13
M4D1	237	388	3.20	253	335	5.19	269	390	5.02
M4D2	238	392	5.65	254	344	6.06	270	365	5.88
M4D3	239	397	5.14	255	344	5.59	271	410	7.45
M4D4	240	403	7.54	256	361	8.54	272	388	7.59

Table 23(A)

Code	N234/55phr70								
	RSS1			SMRCV			SMR10		
	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)
M1		1060			845			743	
M2		811			712			621	
M3		595			577			445	
M4		466			477			388	
M1D1	273	350	1.88	289	312	0.61	305	325	0.78
M1D2	274	476	3.40	290	317	0.64	306	363	1.66
M1D3	275	459	2.70	291	361	1.03	307	400	1.89
M1D4	276	665	2.70	292	419	1.56	308	459	1.73
M2D1	277	323	0.40	293	304	0.76	309	294	0.54
M2D2	278	371	0.73	294	306	0.72	310	321	1.24
M2D3	279	398	0.74	295	318	0.74	311	354	1.28
M2D4	280	464	1.42	296	357	1.30	312	363	1.39
M3D1	281	278	0.47	297	260	0.53	313	260	0.69
M3D2	282	304	0.83	298	272	0.65	314	268	0.48
M3D3	283	323	0.82	299	295	0.58	315	289	1.38
M3D4	284	360	1.06	300	302	1.14	315	303	0.78
M4D1	285	251	0.61	301	244	0.53	317	236	1.00
M4D2	286	266	0.51	302	253	0.81	318	239	0.77
M4D3	287	273	0.64	303	266	0.62	319	257	0.72
M4D4	288	282	0.53	304	296	0.88	320	268	1.30

Table 23(B)

Code	N234/45/0			N234/65/0			N234/65/10		
	RSS1			RSS1			RSS1		
	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)	Sample No.	Mw _{sol} (K)	D (%)
M1		1185			1185			1185	
M2		828			828			828	
M3		623			623			623	
M4		462			462			462	
M1D1	321	507	7.33	337	336	3.44	353	395	5.51
M1D2	322	598	8.15	338	458	5.09	354	478	7.68
M1D3	323	731	8.97	339	479	8.17	355	555	9.46
M1D4	324	772	12.02	340	706	9.90	356	637	8.39
M2D1	325	486	3.48	341	255	3.22	357	295	0.58
M2D2	326	479	5.44	342	288	3.34	358	352	1.23
M2D3	327	527	5.51	343	295	4.65	359	394	1.35
M2D4	328	566	7.70	344	393	5.45	360	449	2.37
M3D1	329	419	0.88	345	237	1.50	361	292	0.86
M3D2	330	423	1.24	346	252	1.78	362	286	1.14
M3D3	331	431	2.55	347	270	2.88	363	313	2.19
M3D4	332	458	4.03	348	304	3.92	364	340	2.51
M4D1	333	341	0.62	349	226	1.18	365	265	0.83
M4D2	334	338	1.13	350	214	1.81	366	273	0.99
M4D3	335	319	1.37	351	233	2.97	367	291	1.39
M4D4	336	354	2.06	352	258	3.83	368	307	2.41

Preferred Embodiment Examples

Additional samples of elastomer composites in accordance with the present invention were prepared. Specifically, a series of natural rubber elastomer composites no. 1 - 32 in accordance with the present invention was produced using apparatus and procedures generally in accordance with those of Example A above. The elastomer composites comprised natural rubber field latex from Malaysia with the properties shown in Table 24 below. The elastomer composites each further comprised carbon black with morphological properties (structure and surface area) of Regions I, II or III in Fig. 8. Specifically, the following carbon blacks were used: Regal ® 660, N234, N326, N110, Regal ® 250, N330, Black Pearl ® 800, Sterling ® 6740 and N351. The carbon black loadings ranged from 30 to 75 phr. and extender oil loadings were in an amount from 0 to 20 phr. The production details for elastomer composite sample nos. 1 - 32 are shown below in Table 25.

As noted above, the apparatus and procedures used to prepare elastomer composites no. 1 - 32 were generally in accordance with those of Example A, including the masterbatch formulation additives shown in Table 2. A more detailed description of the apparatus and procedures used for elastomer composites no. 1 - 32 is set forth below.

1. Apparatus

Invention samples no. 1 - 32 were prepared using masterbatch production apparatus substantially in accordance with the invention apparatus described above with reference to Figs. 1, 4 and 7. The diameter of the slurry nozzle tip (see item 167 in Fig. 7) and the length of the land (see item 168 in Fig. 7) are given in Table 25 for each of samples no. 1 - 32. The coagulum zone of the apparatus had four zones of progressively

larger diameter from the mixing zone to the discharge end. The diameter and axial length of each of the four zones (the first zone being partly within the mix-head and partly within the extender sealed thereto) are set forth in Table 25. There were axially short, faired interconnections between the zones.

5 **2. Carbon Black Slurry Preparation**

Bags of carbon black were mixed with deionized water in a carbon black slurry tank equipped with an agitator. The agitator broke the pellets into fragments to form a crude carbon black slurry. The carbon black concentration (as weight percent) in the carbon black slurry for each of the sample is given in Table 25. During operation, this
10 slurry was continually pumped by an air diaphragm pump to a grinder for initial dispersion. The slurry was then fed via an air diaphragm pump to a colloid mill which then fed into a progressing cavity pump to a homogenizer, specifically, Microfluidizer Model M210 from Microfluidics International Corporation. The microfluidizer produced a finely ground slurry. The slurry flow rate from the microfluidizer to the mixing zone
15 was set by the microfluidizer pressure, the microfluidizer acting as a high-pressure positive displacement pump. Slurry flow rate was monitored with a Micromotion® mass flow meter. The pressure at which the carbon black slurry was fed to the homogenizer and the homogenizer output pressure (all pressures are psig) are set forth for each sample in Table 25. From the homogenizer the carbon black slurry was fed to an accumulator
20 to reduce any fluctuation in slurry pressure at the slurry nozzle tip in the mixing zone. The slurry nozzle tip pressure and flow rate at which the slurry was fed to the mixing zone for each sample are given in Table 25.

3. Latex Delivery

The latex was charged to a 55 gallon feed drum. Antioxidant emulsion was then added to the latex and mixed in prior to charging. Antioxidants were added consisting of tris nonyl phenyl phosphite (TNPP) and Santoflex® 134 (alkylaryl p-phenylene diamine mixture) in the amounts shown in Table 25. Each of the antioxidants was prepared as a 40 wt.% emulsion using 4 parts potassium oleate per 100 parts antioxidant along with potassium hydroxide to adjust the emulsion to a pH of approximately 10. Extender oil, if any, was added in the amount shown in Table 25. A peristaltic pump was used to move the latex from the feed drum to the mixing zone of the coagulum reactor. The latex flow rate and velocity are shown in Table 25. Latex flow was automatically metered with a Endress + Hauser mass flow meter. The desired carbon black loading was obtained by maintaining proper ratio of the latex feed rate to the carbon black slurry feed rate.

4. Carbon Black and Latex Mixing

The carbon black slurry and latex were mixed by entraining the latex into the carbon black slurry. During entrainment, the carbon black was intimately mixed into the latex and the mixture coagulated. Soft, wet spongy "worms" of coagulum exited the coagulum reactor.

5. Dewatering

The water content of the wet crumb discharged from the coagulum reactor is shown in Table 25. The wet crumb was dewatered with a dewatering extruder (The French Oil Mill Machinery Company; 3½ in. diameter). In the extruder, the wet crumb

was compressed and water squeezed from the crumb and through a slotted barrel of the extruder. The final crumb moisture content is shown in Table 25 for each of the invention samples.

5. Drying and Cooling

5 The dewatered crumb dropped into a second extruder where it was again compressed and heated. Water was flashed off upon expulsion of the crumb through the die plate of the extruder. Product exit temperature and moisture content are shown in Table 25. The hot, dry crumb was rapidly cooled (approximately 20 seconds) to about 100°F by a forced air vibrating conveyor.

10

Table 24 Natural Rubber Latex Properties

Latex Type	Source	Additives	% Dry Rubber	% Total Solids	% Ash	Nitrogen ppm	Volatile Fatty Acid
Concentrate	TITI Latex SDN BHD	0.35% NH ₃ ZnO, TMTD 0.1% HHS	60	62.0	0.15	0.29	0.022
Field Latex	RRIM ^a , 9/94	0.15% HNS ^c 0.3% NH ₃ ZnO, TMTD ^b	28.4	34.2	0.38	0.366	0.052

15

- a. RRIM is the Rubber Research Institute of Malaysia
- b. ZnO/TMTD: used for biological preservation, typical 0.025% of 1:1 mixture
- c. HNS: hydroxylamine neutral sulfate. Mooney viscosity stabilizer

Table 25 Invention Sample Production Details

Invention Sample No.	Cabot Elastomer Composite				Slurry Nozzle Tip		MicroFluidizer	
	Latex type	Type	Carbon Black	Oil loading (phr)	Dia. (in)	Land length (in)	Inlet pressure (psi)	Outlet pressure (psi)
1	field latex	N330	55	0	0.025	0.5	180	3000
2	field latex	N330	55	0	0.039	1	300	0
3	field latex	N330	55	0	0.039	1	300	0
4	field latex	REGAL 250	55	0	0.025	0.5	180	3500
5	field latex	REGAL 250	65	0	0.025	0.5	300	10000
6	field latex	REGAL 250	75	0	0.025	0.5	200	13000
7	field latex	REGAL 250	65	10	0.025	0.5	250	12000
8	field latex	BLACK PEARL 800	55	0	0.025	0.5	200	4000
9	field latex	N326	55	0	0.025	1	250	3000
10	field latex	REGAL 680	55	0	0.025	1	-	-
11	field latex	REGAL 680	45	0	0.025	0.5	200	12500
12	field latex	REGAL 680	65	0	0.025	0.5	260	15000
13	field latex	REGAL 680	65	10	0.025	0.5	200	12000
14	field latex	N234	55	0	0.025	1	180	5500
15	field latex	N234	55	0	0.025	0.5	-	14500
16	field latex	N234	55	0	0.025	0.5	-	14500
17	field latex	N234	55	0	0.025	0.5	-	14500
18	field latex	N234	45	0	0.025	0.5	200	13000
19	field latex	N234	65	0	0.025	0.5	220	13000
20	field latex	N234	65	10	0.025	0.5	300	14500
21	field latex	N110	55	0	0.025	1	120	4500
22	latex concentrate	N351	33	20	0.025	0.5	250	12500
23	field latex	STERLING 6740	55	0	0.025	0.5	250	12000
24	field latex	N234	48	5	0.023	0.5	250	11000
25	field latex	N234	53	5	0.023	0.5	250	11000
26	field latex	N234	58	5	0.023	0.5	250	11000
27	field latex	N234	63	5	0.023	0.5	250	11000
28	field latex	N234	68	5	0.023	0.5	250	11000
29	latex concentrate	N234	49	5	0.023	0.5	-	-
30	latex concentrate	N234	54	5	0.023	0.5	-	11000
31	latex concentrate	N234	63	5	0.023	0.5	-	11000
32	latex concentrate	N234	65	5	0.023	0.5	-	11000

Table 26 (Continued)

Invention Sample No.	Coagulum Zone										CB Slurry CB conc. (%wt)
	1st portion		2nd portion		3rd portion		4th portion				
	Dia. (in)	Length (in)	Dia. (in)	Length (in)	Dia. (in)	Length (in)	Dia. (in)	Length (in)			
1	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	15.2		
2	0.19	1.1	0.27	1.6	0.38	2.3	0.53	3.2	14.9		
3	0.19	1.1	0.27	1.6	0.38	2.3	0.53	3.2	14.9		
4	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	19.0		
5	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	21.0		
6	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	21.0		
7	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	21.0		
8	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	15.0		
9	0.19	1.1	0.27	1.6	0.38	2.3	0.53	3.2	14.8		
10	0.19	1.1	0.27	1.6	0.38	2.3	0.53	3.2	14.9		
11	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	15.2		
12	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	15.2		
13	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	15.2		
14	0.19	1.1	0.27	1.6	0.38	2.3	0.53	3.2	14.8		
15	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	13.7		
16	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	13.7		
17	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	13.7		
18	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	14.6		
19	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	14.6		
20	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	14.6		
21	0.19	1.1	0.27	1.6	0.38	2.3	0.53	3.2	11.8		
22	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	15.0		
23	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	14.7		
24	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	13.5		
25	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	13.5		
26	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	13.5		
27	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	13.5		
28	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	13.5		
29	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	12.8		
30	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	12.8		
31	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	12.8		
32	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	12.8		

Table 25 (Continued)

Invention Sample No.	Slurry Nozzle Tip Pressure (psi)	Mixing Zone					
		Slurry flow rate (lb/min)	Slurry velocity (ft/sec)	Antioxidant		Latex flow rate (lbs/min)	Latex velocity (ft/sec)
				TNPP (phr)	Santoflex(phr)		
1	1400	4.6	336	0.3	0.4	4.7	6.8
2	425	8.2	247	0.3	0.4	8.9	13.2
3	425	8.2	247	0.3	0.4	8.9	13.2
4	1500	4.8	344	0.3	0.4	6.7	9.7
5	1500	5.2	370	0.3	0.4	6.6	9.6
6	1575	5.2	370	0.3	0.4	5.9	8.5
7	1550	5.2	370	0.3	0.4	6.9	10.0
8	1800	5.2	380	0.3	0.4	4.9	7.1
9	600	4.2	308	0.3	0.4	4.0	5.6
10	-	4.0	293	0.3	0.4	3.6	5.2
11	1500	5.1	373	0.3	0.4	7.0	10.1
12	1300	4.8	351	0.3	0.4	4.6	6.7
13	1375	4.9	358	0.3	0.4	4.8	6.9
14	900	5.3	388	0.3	0.4	4.8	6.9
15	1400	5.7	420	0.3	0.4	5.4	7.6
16	1400	5.7	420	0.3	0.4	5.4	7.6
17	1400	5.7	420	0.3	0.4	5.4	7.6
18	1600	5.2	381	0.3	0.4	6.5	9.4
19	1650	5.3	388	0.3	0.4	4.5	6.5
20	1625	5.3	388	0.3	0.4	4.6	6.7
21	900	5.3	394	0.3	0.4	4.1	5.9
22	1550	5.1	373	0.3	0.4	5.1	7.6
23	1550	5.2	381	0.3	0.4	5.7	8.3
24	2270	5.1	444	0.3	0.4	6.1	8.6
25	2250	5.1	444	0.3	0.4	5.5	7.9
26	2270	5.1	444	0.3	0.4	5.0	7.2
27	2280	5.1	444	0.3	0.4	4.6	6.6
28	-	5.1	444	0.3	0.4	4.2	6.1
29	2350	5.3	463	0.3	0.4	2.6	3.8
30	2360	5.3	463	0.3	0.4	2.3	3.4
31	2350	5.3	463	0.3	0.4	2.1	3.1
32	2420	5.3	463	0.3	0.4	2.0	3.0

Blends-CIP

77

SUBSTITUTE SHEET (RULE 26)

Table 25 (Continued)

Invention Sample No.	Dewatering		Drying and Cooling	
	Initial crumb moisture (%)	Final crumb moisture (%)	Product temperature (°F)	Product moisture (%)
1	77.6	6.5	312	0.3
2	78.7	-	450	0.2
3	76.7	7.8	400	0.2
4	74.9	-	350	0.3
5	76.2	7.9	310	0.2
6	76.4	11.4	-	0.2
7	75.6	8.8	335	0.3
8	77.7	6.5	310	0.2
9	77.9	8.8	345	0.2
10	77.8	-	-	0.4
11	78.7	9.7	285	0.5
12	79.7	-	335	0.2
13	79.1	-	-	0.9
14	77.9	8.4	330	0.1
15	79.2	-	oven dried	-
16	79.2	10.3	oven dried	-
17	79.2	11.2	oven dried	-
18	79.0	15.0	370	0.4
19	80.0	3.6	325	0.3
20	79.5	9.4	345	0.5
21	80.5	9.5	350	0.2
22	65.1	9.1	280	0.3
23	78.1	6	330	0.6
24	77.4	-	380	0.3
25	77.6	-	380	0.4
26	78.1	-	400	0.7
27	78.4	-	410	0.4
28	78.7	-	420	1.1
29	71.2	-	400	0.6
30	72.3	-	420	0.4
31	73.3	-	400-450	0.9
32	74.1	-	400-450	0.2

It should be noted that samples 2 and 3 were produced with approximately no outlet pressure at the Microfluidizer outlet, etc.. to determine macro-dispersion under adverse process conditions.

5 The excellent carbon black dispersion in the resultant masterbatches is demonstrated by their macro-dispersion quality and molecular weight of the sol portion MW_{sol} . Table 26 below shows the MW_{sol} and macro-dispersion values for invention samples 1 - 32, along with the carbon black and oil (if any) used in each of the samples. The carbon black loading and oil loading are shown as phr values in Table 26.

Table 26 Sol Molecular Weight and Undispersed Area of Invention Samples

Invention Sample No.	CB/Loading/Oil	Mw _{sol} (K)	D (%)
1	N330/55/0	305	0.26
2	N330/55/0	726	0.54
3	N330/55/0	544	0.40
4	R250/55/0	876	0.08
5	R250/65/0	670	0.16
6	R250/75/0	655	0.03
7	R250/65/10	519	0.02
8	BP800/55/0	394	0.14
9	N326/55/0	666	0.20
10	R660/55/0	678	0.12
11	R660/45/0	733	0.05
12	R660/65/0	568	0.04
13	R660/65/10	607	0.02
14	N234/55/0	433	0.15
15	N234/55/0	1000	0.10
16	N234/55/0	500	0.15
17	N234/55/0	550	0.10
18	N234/45/0	485	0.17
19	N234/65/0	359	0.20
20	N234/65/10	350	0.11
21	N110/55/0	612	0.17
22	N351/33/20	800	0.10
23	S6740/55/0	630	0.10
24	N234/48/5	569	0.05
25	N234/53/5	485	0.12
26	N234/58/5	447	0.12
27	N234/63/5	403	0.13
28	N234/58/5	378	0.16
29	N234/49/5	618	0.12
30	N234/54/5	482	0.16
31	N234/63/5	390	0.17
32	N234/65/5	325	0.20

The results for all invention samples having carbon black loading of 55 phr are shown in the semi-log plot of Fig. 9 along with macro-dispersion and MW_{sol} values for a corresponding series of the above described natural rubber control samples produced by dry mixing techniques. At least one data point for an invention sample comprising 55 phr loading of each carbon black is shown in Fig. 9, along with all of the control samples having carbon black loading of 55 phr. (Control samples 401 to 412, also shown in Fig. 9, used 33 phr N351 carbon black and 20 parts extender oil.) It can be seen in Table 26 and in Fig. 9 that the invention samples have excellent macro-dispersion. Specifically, the invention samples have $D(\%)$ values generally below 0.2%, even at MW_{sol} values above $.85 \times 10^6$ whereas the control samples never achieve such excellent macro-dispersion at any MW_{sol} . Thus, the data shown in Fig. 9 clearly reveals that the macro-dispersion quality of the novel elastomer composites over a wide range of MW_{sol} values is significantly superior to that achievable using comparable ingredients in prior-known dry mixing methods. The symbols used for the various data points shown in Fig. 9 and those used in subsequently discussed Figs. 10 - 25 are explained in the legends below.

Figure Captions**Figure 9 Dispersion Quality and MW Sol of NR Masterbatches**

x control samples 177 to 224
 ▲ control samples 273 to 320
 # control samples 145 to 176
 Δ control samples 369 to 400
 ○ control samples 33 to 64
 x control samples 1 to 32
 ● control samples 113 to 144
 ◇ control samples 412 to 443
 ◆ control samples 401 to 412
 ■ invention samples

Figure 10 Dispersion Quality and MW Sol of NR Masterbatches (Region I)

x control samples 177 to 224
 ○ invention sample 10
 # control samples 145 to 176
 :: invention sample 9
 ○ control samples 33 to 64
 □ invention sample 4
 x control samples 1 to 32
 ○ invention sample 1
 ● control samples 113 to 144
 ■ invention sample 8

Figure 11 Dispersion Quality and MW Sol of NR Masterbatches (Region II)

▲ control samples 273 to 320
 ■ invention sample 14
 Δ control samples 369 to 400
 □ invention sample 21

Figure 12 Dispersion Quality and MW Sol of NR Masterbatches (Region III)

◆ control samples 401 to 412
 ■ invention sample 22
 ◇ control samples 412 to 443
 □ invention sample 23

Figure 13 Dispersion Quality and MW Sol of NR Masterbatches (N330 Carbon Black, 55 phr)

● control samples 1 to 32
 ■ invention samples 1 to 3

Figure 14 Dispersion (Quality and MW Sol of NR Masterbatches
(REGAL 250 Carbon Black)

- control samples 33 to 64
- invention sample 4
- control sample 65 to 80
- invention sample 5
- ◇ control samples 81 to 96
- △ invention sample 6
- ◆ control samples 97 to 112
- ▲ invention sample 7

Figure 15 Dispersion Quality and MW Sol of NR Masterbatches
(BLACK PEARL 800 Carbon Black, 55 phr)

- control samples 113 to 144
- invention sample 8

Figure 16 Dispersion Quality and MW Sol of NR Masterbatches
(N326 Carbon Black, 55 phr)

- control samples 145 to 176
- invention sample 9

Figure 17 Dispersion Quality and MW sol of NR Masterbatches
(REGAL 660 Carbon Black)

- control samples 177 to 224
- invention sample 10
- control samples 225 to 240
- invention sample 11
- ◇ control samples 241 to 256
- △ invention sample 12
- ◆ control samples 257 to 272
- ▲ invention sample 13

Figure 18 Dispersion Quality and MW sol of NR Masterbatches
(N234 Carbon Black)

- control samples 273 to 320
- invention samples 14 to 17
- control samples 337 to 352
- invention sample 19
- ◇ control samples 321 to 336
- △ invention sample 18
- ◆ control samples 353 to 368
- ▲ invention sample 20

Figure 19 Dispersion Quality and MW Sol of NR Masterbatches
(N110 Carbon Black, 55 phr)

● control samples 369 to 400
■ invention sample 21

Figure 20 Dispersion Quality and MWsol of NR Masterbatch
(N351 Carbon Black, 33 phr)

● control samples 401 to 412
■ invention sample 22

Figure 21 Dispersion Quality and MW Sol of NR Masterbatches
(STERLING 6740 Carbon Black, 55 phr)

● control samples 412 to 443
■ invention sample 23

Figure 22 MW sol Effect on Crack Growth Rate
(NR Compounds Containing N234 Carbon Black @ 55 phr Loading)

● control samples 273 to 288
■ invention sample 16

Figure 23 MW sol Effect on Crack Growth Rate
(NR Compounds Containing N326 Carbon Black @ 55 phr Loading)

● control samples 145 to 160
○ invention sample 9

Figure 24 MW sol Effect on Crack Growth Rate
(NR Compounds Containing REGAL 660 Carbon Black @ 55 phr Loading)

● control samples 177 to 192
■ invention sample 10

Figure 25 Max. Tan δ (Strain Sweep @60 C) of NR Compounds Containing N234 Black
at Different Loadings

● invention samples 24 to 28
○ invention samples 29 to 32
■ control sample 444 to 450

Figure Captions

**Figure 30 Macro-dispersion Quality and MW of Sol Portion of NR Masterbatch
Containing Dual Phase (Carbon Black/Silica) Aggregates**

- control samples 451 to 458
- invention sample 33
- control samples 459 to 466
- invention sample 34

**Figure 31 Macro-dispersion Quality and MW of Sol Portion of NR Masterbatch
Containing Blend of Carbon Black and Silica**

- control samples 491 to 498
- invention sample 38
- control samples 483 to 490
- invention sample 37
- control samples 475 to 482
- invention sample 36
- control samples 467 to 474
- invention sample 35

The macro-dispersion values for the elastomer composites of the invention shown in Fig. 9 are described by the following equations:

$$D(\%) < 0.2\% \quad (1)$$

when MW_{sol} is less than 0.45×10^6 ; and

5
$$\log(D) < \log(0.2) + 2.0 \times [MW_{sol} - (0.45 \times 10^6)] \times 10^{-6} \quad (2)$$

when $0.45 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

It will be recognized from the discussion above, that macro-dispersion $D(\%)$ in the above equation (1) is the percent undispersed area measured for defects greater than 10 microns. It can be seen in Fig. 9 that $D(\%)$ equal to 0.2% is the threshold macro-dispersion quality for all carbon blacks in Regions I, II and III for natural rubber dry masterbatches. That is, none of the dry masticated masterbatches achieved macro-dispersion quality of 0.2% at any MW_{sol} , even after mixing sufficiently to degrade MW_{sol} below 0.45×10^6 , as described by equation (1) above. When the MW_{sol} of the dry masterbatch control samples shown in Fig. 9 is between 0.45×10^6 and 1.1×10^6 , 10 the dispersion quality is even poorer while, in contrast, the dispersion quality of the invention samples having MW_{sol} in that range remains excellent. None of the preferred embodiments shown in Fig. 9 having MW_{sol} between 0.45×10^6 and 1.1×10^6 exceeds the preferred macro-dispersion limit of 0.2%. In that regard, it should be understood that the data points for preferred embodiments which are seen in Fig. 9 15 (and in other Figures discussed below) to lie on the X axis (i.e., at $D(\%)$ value of

20

0.1%) may have macro-dispersion quality of 0.1% or an even better (i.e., lower) D(%) value.

Region I Carbon Black Samples

Invention samples comprising carbon blacks having morphological properties (i.e., structures and surface area) of Region I in Fig. 8, and corresponding control samples described above made with such Region I carbon blacks, are compared in the semi-log plot of Fig. 10. Specifically, Fig. 10 shows the macro-dispersion values and MW_{sol} values of the invention samples and corresponding control samples comprising the carbon blacks Regal® 660, N326, Regal® 250, N330, and Black Pearl® 800, at carbon black loading ranging from 30 phr to 75 phr and extender oil loading ranging from 0 phr to 20 phr. Excellent carbon black dispersion is seen in Fig. 10 for all of the invention samples, representing preferred embodiments of elastomer composites in accordance with the present disclosure. All of the invention samples advantageously are below line 101 in Fig. 10, whereas all of the control samples have poorer dispersion, being above line 101. In fact, the preferred embodiments shown in Fig. 10, even through comprising carbon blacks from Region I, the most difficult to disperse, all fall below a D(%) value of .3%. The most preferred embodiments all have a D(%) value not exceeding .2% even at an MW_{sol} value advantageously exceeding $.7 \times 10^6$. The data shown in Fig. 10 clearly reveals that the macro-dispersion quality of the novel elastomer composites disclosed here comprising Region I carbon blacks, over a wide range of MW_{sol} values, is significantly superior to that achievable using comparable ingredients by prior dry mastication mixing methods. The macro-dispersion values for the elastomer composites of the invention shown in Fig. 10 are described by the following equations:

Blends-CIP

87

$$D(\%) < 1.0\% \quad (3)$$

when MW_{sol} is less than 0.7×10^6 ; and

$$\log D < \log (1.0) + 2.5 \times [MW_{sol} - (0.7 \times 10^6)] \times 10^{-6} \quad (4)$$

when $0.7 \times 10^6 < MW_{sol} < 1.1 \times 10^6$

5 It will be recognized that D (%) is the percent undispersed area measured for defects greater than 10 microns and 1% is the threshold macro-dispersion quality for all carbon blacks in Region I for natural rubber masterbatches in accordance with the present invention. That is, none of the dry masticated masterbatches achieved macro-dispersion quality of 1.0% or better at any MW_{sol} , even after dry mixing sufficiently
10 to degrade MW_{sol} below $.7 \times 10^6$, as described by Equation (3) above. When the MW_{sol} of the dry masterbatch control samples shown in Fig. 10 is between 0.7×10^6 and 1.1×10^6 , the dispersion quality is even poorer. In contrast, the dispersion quality of the invention samples having MW_{sol} in that range remains excellent. The preferred embodiment shown in Fig. 10 having MW_{sol} between $.7 \times 10^6$ and 1.1×10^6 falls well
15 below the preferred macro-dispersion limit of .2%. It can be seen that the elastomer composites of the invention comprising carbon blacks from Region I provide heretofore unachieved balance between macro-dispersion quality and MW_{sol} .

Region II Carbon Black Samples

Invention samples comprising carbon blacks having morphological properties
20 (i.e., structure and surface area) of Region II in Fig. 8, and corresponding control samples described above made with such Region II carbon blacks are compared in the semi-log plot of Fig. 11. Specifically, Fig. 11 shows the macro-dispersion values and MW_{sol}

Blends-CIP

88

values of the invention samples and corresponding control samples comprising the carbon blacks N234 and N110 at carbon black loading ranging from 40 phr to 70 phr and extender oil loading ranging from 0 phr to 10 phr. Excellent carbon black dispersion is seen in Fig. 11 for all of the invention samples, representing preferred embodiments of elastomer composites in accordance with the present disclosure. The invention samples advantageously are below line 111 in Fig. 11, whereas all of the control samples have poorer dispersion, being above line 111. In fact, the preferred embodiments shown in Fig. 11 comprising carbon blacks from Region II fall below a D(%) value of .3%. Most preferred embodiments have a D(%) value not exceeding .2% at any MW_{sol} value. The data shown in Fig. 11 clearly reveal that the macro-dispersion quality of the novel elastomer composites disclosed here comprising Region II carbon blacks, over a wide range of MW_{sol} values, is significantly superior to that achievable using comparable ingredients in prior dry mixing methods. The macro-dispersion values for the elastomer composites of the invention shown in Fig. 11 are described by the following equations:

$$D(\%) < 0.3\% \quad (5)$$

when MW_{sol} is less than 0.35×10^6 ; and

$$\log D < \log (0.3) + 2.8 \times [MW_{sol} - (.35 \times 10^6)] \times 10^{-6} \quad (6)$$

when $0.35 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

It will be recognized that D (%) of .30% is the threshold macro-dispersion quality for all carbon blacks in Region II for natural rubber masterbatches in accordance with the present invention, and 0.35×10^6 is the threshold MW_{sol} value. That is, none of the dry masterbatches achieved macro-dispersion quality of 0.30% or better at any MW_{sol} even

after dry mixing sufficiently to degrade MW_{sol} below $.35 \times 10^6$, as described by Equation (5) above. When the MW_{sol} of the dry masterbatch control samples shown in Fig. 11 is between 0.35×10^6 and 1.1×10^6 , the dispersion quality is even poorer. In contrast, the dispersion quality of the invention samples having MW_{sol} in that range remains excellent. The preferred embodiments shown in Fig. 11 having MW_{sol} between $.35 \times 10^6$ and 1.1×10^6 fall well below the preferred macro-dispersion limit of .2%. It can be seen that the elastomer composites of the invention comprising carbon blacks from Region II provide heretofore unachieved balance between macro-dispersion quality and MW_{sol} .

10 **Region III Carbon Black Samples**

Invention samples comprising carbon blacks having morphological properties (i.e., structures and surface area) of Region III in Fig. 8, and corresponding control samples described above made with such Region III carbon blacks are compared in the semi-log plot of Fig. 12. Specifically, Fig. 12 shows the macro-dispersion values and MW_{sol} values of the invention samples and corresponding control samples comprising the carbon blacks N351 and Sterling 6740, at carbon black loading ranging from 30 phr to 70 phr and extender oil loading ranging from 0phr to 20 phr. Excellent carbon black dispersion is seen in Fig. 12 for all of the invention samples, representing preferred embodiments of elastomer composites in accordance with the present disclosure. All of the invention samples advantageously are below line 121 in Fig. 12, whereas all of the control samples have poorer dispersion, being above line 121. In fact, the preferred embodiments shown in Fig. 12, comprising carbon blacks from Region III, fall at or below a D(%) value of .1%, even at an MW_{sol} value advantageously exceeding $.3 \times 10^6$ and even $.7 \times 10^6$. The data shown in Fig. 12 clearly reveals that the macro-dispersion

quality of the novel elastomer composites disclosed here comprising Region III carbon black, over a wide range of MW_{sol} values, is significantly superior to that achievable using comparable ingredients in prior dry mixing methods. The macro-dispersion values for the elastomer composites of the invention shown in Fig. 12 are described by the following equations:

$$D(\%) < 0.1\% \quad (7)$$

when MW_{sol} is less than 0.35×10^6 ; and

$$\log D < \log (0.1) + 2.0 \times [MW_{sol} - (0.30 \times 10^6) \times 10^{-6}] \quad (8)$$

when $0.30 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

It will be recognized that D (%) of 0.1% is the threshold macro-dispersion quality for all carbon blacks in Region III for natural rubber masterbatches in accordance with the present invention, and 0.3×10^6 is the threshold MW_{sol} value. That is, none of the dry masterbatches achieved macro-dispersion quality of .1% at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below $.35 \times 10^6$, as described by Equation (7) above. When the MW_{sol} of the dry masterbatch control samples shown in Fig. 12 is between 0.30×10^6 and 1.1×10^6 , the dispersion quality is even poorer. In contrast, the dispersion quality of the invention samples having MW_{sol} in that range remains excellent. The preferred embodiments shown in Fig. 12 having MW_{sol} between $.30 \times 10^6$ and 1.1×10^6 fall well below the preferred macro-dispersion limit of .2%, and, in fact, are at or below D(%) value of 0.1%. It can be seen that the elastomer composites of the present invention comprising carbon blacks from Region III provide heretofore unachieved balance between macro-dispersion quality and MW_{sol} .

Additional Sample Comparisons

The macro-dispersion values for the invention samples are shown graphically in the semi-long plots of Figs. 13 through 21, as a function of their MW_{sol} values, as in Figs. 8 through 12 discussed above. More specifically, in Figs. 13 through 21 all invention samples described above comprising a particular carbon black (being limited to those of a specific carbon black loading when so indicated) are shown together in a single semi-log plot together with the corresponding control samples. (See the legends above giving the reference numbers of the invention samples and control samples included in each figure.) Thus, Fig. 13 shows the dispersion quality and MW_{sol} of invention and control samples described above comprising 55 phr N330 carbon black. The data shown in Fig. 13 clearly reveals that the macro-dispersion quality of the novel elastomer composites of the invention, comprising N330 carbon black, over a wide range of MW_{sol} values, is significantly superior to that of the control samples. Macro-dispersion for elastomer composites of the invention comprising N330 carbon black, as shown in Fig. 13 is described by the following equations:

$$D(\%) < 1\% \quad (9)$$

when $MW_{sol} < 0.6 \times 10^6$; and

$$\log(D) < \log(1) + 2.5 \times [MW_{sol} - (0.6 \times 10^6)] \times 10^{-6} \quad (10)$$

when $0.6 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

None of the dry masticated masterbatches achieved macro-dispersion quality of 1.0% at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below 0.6×10^6 (see Equation 9, above). In control samples comprising 55 phr N330 carbon black in which the MW_{sol} was maintained between 0.6×10^6 and 1.1×10^6 , the D(%) value is even higher, such as more than 4% undispersed area.

Fig. 14 shows the dispersion quality and MW_{sol} of the invention and control samples described above comprising REGAL® 250 carbon black. Selected invention and control samples shown in Fig. 14 comprised oil, as set forth above. The data shown in Fig. 14 clearly reveals that the macro-dispersion quality of the novel elastomer composites of the invention comprising REGAL® 250 carbon black, over a wide range of MW_{sol} values, is significantly superior to that of the control samples. The macro-dispersion values for the elastomer composites of the invention comprising REGAL® 250 carbon black, as shown in Fig. 14 are described by the following equations:

$$D(\%) < 1\% \quad (9)$$

when $MW_{sol} < 0.6 \times 10^6$; and

$$\log(D) < \log(1) + 2.5 \times [MW_{sol} - (0.6 \times 10^6)] \times 10^{-6} \quad (10)$$

when $0.6 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

None of the control samples achieved macro-dispersion quality of 1.0% or better at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below 0.6×10^6 . In contrast, elastomer composites of the invention comprising Regal® 250 carbon black and having MW_{sol} above 0.6×10^6 have excellent macro-dispersion, such as D(%) less than 0.2%. Compound properties and performance characteristics for the invention and control samples shown in Fig. 14, comprising REGAL® 250 carbon black, are set forth in Table

27 below. It can be seen that invention sample No. 4 has exceptionally good resistance to crack growth, as indicated by its very low crack growth rate value of only 0.92 cm/million cycles. In fact, the invention sample is far superior to the corresponding control samples. This is believed to be due largely to the better MW_{sol} and macro-

5 dispersion of carbon black in the invention sample, as discussed above.

**Table 27 Compound Properties of NR Compounds
Containing REGAL 250 Carbon Black at 55 phr Loading**

Sample No.	Mooney ML(1+4)@100C	Hardness	E100 (psi)	E300 (psi)	Tensile (psi)	EB (%)
control 33	60.63	55.35	181.26	999.82	4090.24	675.0
control 34	73.58	57.80	235.14	1293.88	3978.24	595.0
control 35	81.49	58.65	243.66	1265.26	4103.41	613.0
control 36	84.04	59.95	244.23	1215.87	3960.32	614.0
control 37	57.35	56.75	218.70	1259.99	4119.85	502.0
control 38	60.10	57.05	216.75	1206.60	4023.65	620.0
control 39	68.28	57.25	225.44	1256.23	4134.06	621.0
control 40	77.40	59.10	255.15	1330.87	4059.01	597.0
control 41	44.40	56.25	216.00	1214.78	4038.68	618.0
control 42	47.96	56.50	214.53	1202.93	3944.05	613.0
control 43	49.84	57.05	221.26	1229.07	4018.24	611.0
control 44	50.10	56.60	210.50	1140.90	4058.33	638.0
control 45	36.82	52.90	177.47	982.86	3790.56	533.0
control 46	38.23	54.50	198.63	1111.04	3860.56	629.0
control 47	35.35	54.60	199.03	1110.00	3871.49	505.0
control 48	40.58	55.50	204.52	1139.94	3961.06	632.0
invention 4	71.97	57.00	218.18	1230.30	4036.30	611.0

Sample No.	Rebound	Crack Growth Rate (cm/million cycles)	Abrasion loss (g)	Tan δ @ 0°C	Tan δ @ 60°C
control 33	64.50	2.00	0.191	0.167	0.091
control 34	64.55	1.83	0.182	0.155	0.083
control 35	63.75	2.38	0.192	0.150	0.091
control 36	63.30	1.42	0.180	0.162	0.091
control 37	64.65	3.00	0.168	0.176	0.100
control 38	63.45	2.99	0.163	0.184	0.099
control 39	63.90	2.17	0.186	0.170	0.092
control 40	62.30	1.69	0.182	0.175	0.093
control 41	64.20	2.84	0.190	0.189	0.102
control 42	64.20	3.24	0.182	0.168	0.103
control 43	64.50	3.52	0.177	0.183	0.101
control 44	63.90	3.50	0.179	0.185	0.104
control 45	63.80	3.86	0.199	0.197	0.104
control 46	64.30	3.94	0.191	0.184	0.107
control 47	64.35	3.81	0.192		0.106
control 48	63.65	3.46	0.180	0.182	0.110
invention 4	64.70	0.92	0.190	0.148	0.096

Fig. 15 shows the dispersion quality and MW_{sol} of the invention and control samples described above comprising BLACK PEARL® 800 carbon black at 55 phr loading. The data shown in Fig. 15 clearly reveals that the macro-dispersion quality of the novel elastomer composites of the invention comprising Black Pearl® 800 carbon black, is significantly superior to that of the control samples. The macro-dispersion values for elastomer composites of the invention comprising Black Pearl® 800 carbon black, as shown in Fig. 15, are described by the following equations:

$$D(\%) < 1.5\% \quad (11)$$

when $MW_{sol} < 0.65 \times 10^6$; and

$$\log(D) < \log(1.5) + 2.5 \times [MW_{sol} - (0.65 \times 10^6)] \times 10^{-6} \quad (12)$$

when $0.65 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

None of the control samples achieved macro-dispersion quality of 1.0% or better at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below 0.65×10^6 . In contrast, elastomer composites of the invention comprising Black Pearl® 800 carbon black and having MW_{sol} above 0.65×10^6 have excellent macro-dispersion, such as $D(\%)$ less than 0.2%. Compound properties and performance characteristics for the invention and control samples shown in Fig. 15, comprising Black Pearl® 800 carbon black, are set forth in Table 28 below. It can be seen that invention sample No. 8 has exceptionally good resistance to crack growth, as indicated by its very low crack growth rate value of only 0.27 cm/million cycles. In fact, the invention samples are far superior to the corresponding control samples. This is believed to be due largely to the better MW_{sol} and macro-dispersion of carbon black in the invention sample, as discussed above.

**Table 28 Compound Properties of NR Compounds
Containing BLACK PEARL 800 Carbon Black at 55 phr Loading**

Sample No.	Mooney ML(1+4)@100C	Hardness	E100 (psi)	E300 (psi)	Tensile (psi)	EB (%)
control 113	110.5	66.4	345.0	1333.0	3878.0	598
control 114	109.0	67.3	367.0	1427.0	4033.0	606
control 115	106.4	67.2	363.0	1311.0	3896.0	610
control 116	105.7	69.0	322.0	1202.0	3856.0	626
control 117	110.6	67.1	316.0	1400.0	4180.0	616
control 118	118.9	67.1	310.0	1395.0	3967.0	607
control 119	111.9	67.7	309.0	1323.0	4149.0	634
control 120	110.6	67.6	373.0	1188.0	4199.0	653
control 121	114.7	66.3	287.0	1262.0	4329.0	667
control 122	110.6	65.8	288.0	1223.0	4217.0	659
control 123	115.0	67.5	280.0	1282.0	4071.0	624
control 124	116.5	66.5	309.0	1388.0	4166.0	623
control 125	113.4	65.4	281.0	1274.0	3978.0	631
control 126	101.4	66.8	280.0	1222.0	4206.0	656
control 127	105.5	66.4	262.0	1150.0	4167.0	670
control 128	110.7	66.8	292.0	1301.0	4209.0	643
invention 8	131.3	62.5	227.0	1291.0	3418.0	532

Sample No.	Rebound	Crack Growth Rate (cm/million cycles)	Abrasion loss (g)	Tan δ @ 0°C	Tan δ @ 60°C
control 113	44.7	3.14	0.148	0.281	0.184
control 114	45.0	2.72	0.125	0.274	0.185
control 115	47.0	2.54	0.163	0.233	0.171
control 116	46.6	2.41	0.194	0.244	0.163
control 117	40.9	4.56	0.086	0.327	0.214
control 118	41.8	2.80	0.112	0.335	0.225
control 119	41.7	4.33	0.091	0.321	0.216
control 120	42.1	3.89	0.095	0.301	0.207
control 121	39.2	3.38	0.075	0.312	0.256
control 122	38.7	4.58	0.108	0.344	0.236
control 123	40.2	4.79	0.103	0.329	0.232
control 124	41.7	3.78	0.102	0.321	0.209
control 125	38.9	3.40	0.076	0.352	0.248
control 126	38.1	5.57	0.070	0.355	0.241
control 127	38.2	4.79	0.073	0.346	0.254
control 128	39.4	3.40	0.113	0.357	0.23
invention 8	44.8	0.27	0.130	0.297	0.199

Fig. 16 shows the dispersion quality and MW_{sol} of the invention and control samples described above comprising N326 carbon black at 55 phr loading. The data shown in Fig. 16 clearly reveals that the macro-dispersion quality of the novel elastomer composites of the invention comprising N326 carbon black is significantly superior to that of the control samples. The macro-dispersion values for the elastomer composites of the invention comprising N326 carbon black, as shown in Fig. 16, are described by the following equations:

$$D(\%) < 1\% \quad (13)$$

when $MW_{sol} < 0.7 \times 10^6$; and

$$\log(D) < \log(1) + 2.5 \times [MW_{sol} - (0.7 \times 10^6)] \times 10^{-6} \quad (14)$$

when $0.7 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

None of the control samples achieved macro-dispersion quality of 1.0% or better at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below 0.7×10^6 . In contrast, elastomer composites of the invention comprising N326 carbon black and having MW_{sol} above 0.7×10^6 have excellent macro-dispersion, such as $D(\%)$ not greater than 0.2%. Compound properties and performance characteristics for the invention and control samples shown in Fig. 16, comprising N326 carbon black are set forth in Table 29 below. It can be seen that invention sample No. 9 has exceptionally good resistance to crack growth, as indicated by its very low crack growth rate value of only 0.77 cm/million cycles. In fact, the invention sample is far superior to the corresponding control samples. This is believed to be due largely to the better MW_{sol} and macro-dispersion of carbon black in the invention sample, as discussed above.

**Table 29 Compound Properties of NR Compounds
Containing N326 Carbon Black at 55 phr Loading**

Sample No.	Mooney ML(1+4)@100°C	Hardness	E100 (psi)	E300 (psi)	Tensile (psi)	EB (%)
control 145	64.6	60.5	289	1713	3921	548
control 146	88.2	62.4	340	1802	4094	553
control 147	91.7	63.3	391	1917	3991	528
control 148	96.8	64.3	326	1664	4045	572
control 149	62.4	61.5	310	1763	4029	552
control 150	67.7	62.6	326	1855	4055	551
control 151	76.5	60.6	287	1641	4015	575
control 152	79.4	63.6	329	1720	3980	559
control 153	57.2	60.1	282	1623	3968	579
control 154	57.2	62.8	354	1889	3879	525
control 155	57.3	62.2	323	1763	3975	556
control 156	60.1	61.9	310	1667	3918	564
control 157	45.1	61.2	328	1748	3768	533
control 158	50.1	60.6	315	1740	3817	546
control 159	53.2	61.3	306	1675	3886	563
control 160	50.5	62.6	331	1752	3884	549
invention 9	77.8	60.9	277	1563	4167	593
Sample No.	Rebound	Crack Growth Rate (cm/million cycles)	Abrasion loss (g)	Tan δ @ 0°C	Tan δ @ 60°C	
control 145	57.8	2.84	0.0952	0.225	0.129	
control 146	58.1	2.52	0.0887	0.217	0.126	
control 147	57.6	2.03	0.0946	0.205	0.123	
control 148	56.3	1.63	0.0927	0.221	0.129	
control 149	57.2	3.39	0.0827	0.234	0.142	
control 150	56.8	2.77	0.0866	0.234	0.150	
control 151	55.6	2.61	0.0933	0.241	0.149	
control 152	54.5	2.79	0.0857	0.249	0.155	
control 153	55.4	3.12	0.0911	0.258	0.170	
control 154	56.0	3.35	0.0858	0.241	0.147	
control 155	55.4	3.63	0.0811	0.254	0.152	
control 156	54.9	3.55	0.0906	0.261	0.153	
control 157	55.5	3.02	0.0931	0.254	0.149	
control 158	55.4	3.81	0.0914	0.249	0.150	
control 159	54.9	3.23	0.0933	0.240	0.158	
control 160	55.2	3.19	0.0942	0.246	0.163	
invention 9	58.4	0.77	0.0939	0.225	0.136	

Fig. 17 shows the dispersion quality and MW_{sol} of the invention and control samples described above comprising REGAL (trademark) 660 carbon black. Selected invention and control samples shown in Fig. 17 comprised oil, as set forth above. The data shown in Fig. 17 clearly reveals that the macro-dispersion quality of the novel elastomer composites of the invention comprising REGAL ® 660 carbon black, over a wide range of MW_{sol} values, is significantly superior to that of the control samples. The macro-dispersion values for the elastomer composites of the invention comprising REGAL ® 660 carbon black, as shown in Fig. 17 are described by the following equations:

$$D(\%) < 1\% \quad (15)$$

when $MW_{sol} < 0.6 \times 10^6$; and

$$\log(D) < \log(1) + 2.5 \times [MW_{sol} - (0.6 \times 10^6)] \times 10^{-6} \quad (16)$$

when $0.6 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

None of the control samples achieved macro-dispersion quality of 1.0% or better at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below 0.6×10^6 . In contrast, elastomer composites of the invention comprising Regal® 660 carbon black and having MW_{sol} above 0.6×10^6 have excellent macro-dispersion, such as $D(\%)$ less than 0.2%. Compound properties and performance characteristics for the invention sample No. 10 and various control samples shown in Fig. 17, comprising Regal® 660 carbon black, are set forth in Table 30 below. It can be seen that invention sample No. 10 has exceptionally good resistance to crack growth, as indicated by its very low crack growth rate value of only 0.69 cm/million cycles. In fact, the invention samples are far superior to the corresponding control samples. This is believed to be due largely to the better MW_{sol} and macro-dispersion of carbon black in the invention sample, as discussed above.

**Table 30 Compound Properties of NR Compounds
Containing REGAL 660 Carbon Black at 55 phr Loading**

Sample No.	Mooney ML(1+4)@100°C	Hardness	E100 (psi)	E300 (psi)	Tensile (psi)	EB (%)
control 177		61.0	213	942		702
control 178	87.6	63.2	232	943	4002	694
control 179	87.1	64.9	285	1134	4016	644
control 180	85.6	64.0	271	1198	4058	618
control 181	80.1	61.0	206	945	4098	661
control 182	93.4	59.0	192	835	3924	733
control 183	89.0	61.0	215	920	4134	698
control 184	83.4	62.4	223	996	4236	694
control 185	70.1	60.0	178	794	3768	717
control 186	69.8	60.3	196	920	4051	666
control 187	76.7	63.5	166	866	4157	720
control 188	72.1	62.0	191	883	4182	704
control 189	54.3	61.2	222	1079	4240	674
control 190	55.7	61.1	193	942	4125	692
control 191		65.0				
control 192	61.1	60.4	191	902	4189	710
invention 10	88.1	62.9	249	1202	4292	634

Sample No.	Rebound	Crack Growth Rate (cm/million cycles)	Abrasion loss (g)	Tan δ @ 0°C	Tan δ @ 60°C
control 177	54.6				0.131
control 178	55.6	2.34	0.1649	0.194	0.129
control 179	53.7	2.78	0.1620	0.200	0.140
control 180	52.9	2.98	0.1385	0.220	0.153
control 181	51.0	3.41	0.1189	0.267	0.185
control 182	49.9	3.11	0.1076	0.270	0.194
control 183	50.1	3.15	0.1086	0.264	0.192
control 184	48.0	3.11	0.1085	0.284	0.208
control 185	47.5	4.59	0.0937	0.306	0.209
control 186	48.5	4.06	0.1008	0.295	0.211
control 187	47.7	3.53	0.1041	0.297	0.198
control 188	47.8	3.79	0.0985	0.285	0.207
control 189	47.5	3.71	0.0957	0.306	0.203
control 190	46.8	4.14	0.0962	0.300	0.200
control 191	47.4				0.226
control 192	46.5	4.78	0.0897	0.301	0.226
invention 10	48.2	0.69	0.0942	0.271	0.178

Fig. 18 shows the dispersion quality and MW_{sol} of the invention and control samples described above comprising N234 carbon black. Selected invention and control samples shown in Fig. 18 comprised oil, as set forth above. The data shown in Fig. 18 clearly reveals that the macro-dispersion quality of the novel elastomer composites of the invention comprising N234 carbon black, over a wide range of MW_{sol} values, is significantly superior to that of the control samples. The macro-dispersion values for the elastomer composites of the invention comprising N234 carbon black, as shown in Fig. 18 are described by the following equations:

$$D(\%) < 0.3\% \quad (17)$$

when $MW_{sol} < 0.35 \times 10^6$; and

$$\log(D) < \log(0.3) + 2.8 \times [MW_{sol} - (0.35 \times 10^6)] \times 10^{-6} \quad (18)$$

when $0.35 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

None of the control samples achieved macro-dispersion quality of 0.3% or better at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below 0.35×10^6 . In contrast, elastomer composites of the invention comprising N234 carbon black and having MW_{sol} greater than 0.35×10^6 have excellent macro-dispersion, such as $D(\%)$ not more than 0.3% or even 0.2%. Compound properties and performance characteristics for invention sample No. 14 and various control samples shown in Fig. 18, comprising N234 carbon black, are set forth in Table 31 below. It can be seen that invention sample No. 14 has good resistance to crack growth, as indicated by its crack growth rate value of only 2.08 cm/million cycles.

**Table 31 Compound Properties of NR Compounds
Containing N234 Carbon Black at 55 phr Loading**

Sample No.	Mooney ML(1+4)@100°C	Hardness	E100 (psi)	E300 (psi)	Tensile (psi)	EB (%)
control 273	94.5	68.0	386	2077	3718	511
control 274	121.6	69.6	464	2299	3925	501
control 275	121.4	72.5	564	2545	3994	472
control 276	132.2	71.9	511	2259	3964	520
control 277	79.6	68.5	468	2453	3857	469
control 278	96.3	70.0	531	2499	3874	469
control 279	108.6	69.0	406	2131	3863	532
control 280	120.3	71.5	476	2273	3852	502
control 281	76.4	69.7	556	2723	4027	451
control 282	89.8	69.8	553	2574	3896	465
control 283	93.6	69.6	506	2416	3867	475
control 284	106.7	71.8	526	2384	3788	484
control 285	73.3	69.3	529	2586	3831	444
control 286	79.2	69.5	531	2574	3856	456
control 287	77.8	70.7	544	2486	3834	461
control 288	82.8	71.2	485	2295	3799	499
invention 14	82.6	71.5	500	2440	3883	531
Sample No.	Rebound	Crack Growth Rate (cm/million cycles)	Abrasion loss (g)	Tan δ @ 0°C	Tan δ @ 60°C	
control 273	45.9	2.14	0.0563	0.285	0.183	
control 274	47.2	1.84	0.0583	0.274	0.173	
control 275	46.1	1.70	0.0538	0.284	0.172	
control 276	46.9	1.21	0.0620	0.270	0.173	
control 277	47.1	2.22	0.0628	0.305	0.173	
control 278	45.8	2.40	0.0634	0.299	0.196	
control 279	45.4	2.00	0.0680	0.306	0.198	
control 280	44.2	1.81	0.0646	0.298	0.198	
control 281	46.3	3.10	0.0598	0.293	0.174	
control 282	46.5	2.33	0.0537	0.307	0.182	
control 283	46.4	2.41	0.0594	0.309	0.186	
control 284	44.2	1.99	0.0579	0.304	0.190	
control 285	47.0	2.99	0.0554	0.295	0.178	
control 286	45.6	2.85	0.0551	0.294	0.172	
control 287	45.4	2.93	0.0569	0.305	0.187	
control 288	44.0	2.39	0.0647	0.316	0.198	
invention 14	45.1	2.08	0.0698	0.310	0.198	

Fig. 19 shows the dispersion quality and MW_{sol} of the invention and control samples described above comprising N110 carbon black at 55 phr loading. The data shown in Fig. 19 clearly reveals that the macro-dispersion quality of the novel elastomer composites of the invention comprising N110 carbon black, over a wide range of MW_{sol} values, is significantly superior to that of the control samples. The macro-dispersion values for the elastomer composites of the invention comprising N110 carbon black, as shown in Fig. 19, are described by the following equations:

$$D(\%) < 0.5\% \quad (19)$$

when $MW_{sol} < 0.35 \times 10^6$; and

$$\log(D) < \log(0.5) + 2.5 \times [MW_{sol} - (0.6 \times 10^6)] \times 10^{-6} \quad (20)$$

when $0.35 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

None of the control samples achieved macro-dispersion quality of 0.5% at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below 0.35×10^6 . In contrast, elastomer composites of the invention comprising N110 carbon black and having MW_{sol} above 0.35×10^6 have excellent macro-dispersion, such as $D(\%)$ less than 0.2%.

Fig. 20 shows the dispersion quality and MW_{sol} of invention sample 22 and the control samples described above comprising N351 carbon black at 33 phr loading. The data shown in Fig. 20 clearly reveals that the macro-dispersion quality of the novel elastomer composites of the invention comprising N351 carbon black, over a wide range of MW_{sol} values, is significantly superior to that of the control samples. The macro-dispersion values for the elastomer composites of the invention comprising N351 carbon black, as shown in Fig. 20, are described by the following equations:

$$D(\%) < 0.3\% \quad (21)$$

when $MW_{sol} < 0.55 \times 10^6$; and

$$\log(D) < \log(0.3) + 2.0 \times [MW_{sol} - (0.55 \times 10^6)] \times 10^{-6} \quad (22)$$

when $0.55 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

5 None of the control samples achieved macro-dispersion quality of 1.0% at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below 0.35×10^6 . In contrast, elastomer composites of the invention comprising N351 carbon black and having MW_{sol} above 0.35×10^6 have excellent macro-dispersion, such as $D(\%)$ less than 0.2%.

Fig. 21 shows the dispersion quality and MW_{sol} of the invention sample No. 23
10 and control samples described above comprising STERLING® 6740 carbon black at 55 phr loading. The data shown in Fig. 21 clearly reveals that the macro-dispersion quality of the novel elastomer composites of the invention comprising STERLING® 6740 carbon black, over a wide range of MW_{sol} values, is significantly superior to that of the control samples. The macro-dispersion values for the elastomer composites of the
15 invention comprising STERLING® 6740 carbon black, as shown in Fig. 21 are described by the following equations:

$$D(\%) < 0.1\% \quad (23)$$

when $MW_{sol} < 0.3 \times 10^6$; and

$$\log(D) < \log(0.1) + 2.0 \times [MW_{sol} - (0.3 \times 10^6)] \times 10^{-6} \quad (24)$$

20 when $0.3 \times 10^6 < MW_{sol} < 1.1 \times 10^6$.

None of the control samples achieved macro-dispersion quality of 0.1% or even 0.2% at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below 0.3×10^6 . In

contrast, elastomer composites of the invention comprising STERLING ® 6740 carbon black and having MW_{sol} above 0.3×10^6 have excellent macro-dispersion, such as D(%) less than 0.2% and even less than 0.1%. Compound properties and performance characteristics for invention sample No. 23 and the control samples shown in Fig. 21, comprising STERLING ® 6740 carbon black, are set forth in Table 32 below. It can be seen that invention sample No. 23 has good resistance to crack growth, as indicated by its crack growth rate value of only 0.91 cm/million cycles. In fact, the invention sample is far superior to the corresponding control samples. This is believed to be due largely to the better MW_{sol} and macro-dispersion of carbon black in the invention sample, as discussed above.

**Table 32 Compounds Properties of NR Compounds
Containing STERLING 6740 Carbon Black at 55 phr Loading**

Sample No.	Mooney ML(1+4)@100°C	Hardness	E100 (psi)	E300 (psi)	Tensile (psi)	EB (%)
control 412	75.50	65.1	467.0	2308.0	3519	451
control 413	85.70	65.7	469.0	2314.0	3655	479
control 414	92.70	67.7	462.0	2243.0	3613	472
control 415	99.60	66.9	492.0	2260.0	3572	477
control 416	74.50	65.8	521.0	2468.0	3584	445
control 417	78.20	67.1	502.0	2372.0	3445	436
control 418	82.00	66.0	534.0	2418.0	3604	453
control 419	86.10	67.8	540.0	2330.0	3620	475
control 420	66.70	66.0	515.0	2382.0	3468	444
control 421	76.30	67.8	488.0	2310.0	3375	440
control 422	78.30	65.8	548.6	2440.0	3549	442
control 423	82.10	66.5	487.0	2219.0	3452	466
control 424	64.80	66.5	541.0	2448.0	3397	425
control 425	67.50	66.5	524.0	2374.0	3474	445
control 426	70.30	66.9	546.0	2351.0	3428	446
control 427	71.00	68.1	554.0	2340.0	3322	435
invention 23	110.50	64.8	453.6	2241.0	3324	443
Sample No.	Rebound	Crack Growth Rate (cm/million cycles)	Abrasion loss (g)	Tan δ @ 0°C	Tan δ @ 60°C	
control 412	59.8	5.04	0.127	0.202	0.107	
control 413	60.0	3.63	0.128	0.203	0.108	
control 414	59.3	3.96	0.126	0.208	0.114	
control 415	58.8	4.56	0.12	0.217	0.118	
control 416	60.3	5.67	0.117	0.188	0.094	
control 417	60.0	4.67	0.112	0.202	0.104	
control 418	59.3	4.23	0.125	0.204	0.105	
control 419	57.5	3.22	0.122	0.218	0.117	
control 420	60.0	4.23	0.131	0.204	0.099	
control 421	58.8	3.84	0.127	0.206	0.105	
control 422	59.8	3.98	0.126	0.210	0.106	
control 423	56.8	3.85	0.12	0.213	0.117	
control 424	58.3	4.54	0.131	0.200	0.104	
control 425	58.8	3.65	0.129	0.207	0.100	
control 426	58.0	3.07	0.134	0.211	0.110	
control 427	56.9	3.25	0.126	0.217	0.115	
invention 23	57.3	0.91	0.1642	0.204	0.124	

Addition Examples: Cured Samples

A number of the masterbatch samples described above, including both selected invention samples and corresponding control samples, were cured and tested. Specifically, samples were mixed accordingly to Stage II in Table 8, above, using the formulation of Table 9, to produce a final compound. The final compound in each case was then cured in a mold using standard techniques at about 150°C until substantially complete cure was achieved. Performance characteristics of the cured samples were determined by measuring their respective crack growth rates in accordance with the measurement technique set forth above, i.e., using a rotating flexing machine per ASTM D3629-94. The rotating type flexing machine used to measure crack growth is commercially available and well known. It is discussed, for example, in the Proceedings of the International Rubber Conference, 1995 (Kobe, Japan), Paper No. 27A - 6 (p. 472 - 475). The compounds were tested at 100°C and at a 45° flexing angle. It is generally accepted by those skilled in the art that crack growth rate in such compounds is affected by the molecular weight of the natural rubber and the dispersion quality of the carbon black i.e., by the MW_{sol} and $D(\%)$ values of the compounds. Higher MW_{sol} and lower $D(\%)$ correlate well with reduced crack growth rate. The crack growth rate and other information for invention samples nos. 9, 10 and 16 are set forth in Table 33 below. The corresponding test results for corresponding control samples is set forth in Table 34 below, grouped by choice of carbon black. Also, $\tan \delta_{max}$ @ 60°C was measured for invention samples nos. 24 - 32 and for corresponding control samples. The $\tan \delta_{max}$ @ 60°C values for the invention samples are set forth in Table 35 below. The corresponding test results for control samples is set forth in Table 36 below.

Control samples No. 444 - 450 shown in Table 36 were made in accordance with the procedures described above for control sample code M2D1 using RSS1 natural rubber. All used carbon black N234 at the loading level (phr) shown in Table 36, along with 5 phr extender oil.

Table 33 Crack Growth Rate of Invention Samples

<i>Invention Sample No.</i>	<i>CB/Loading/Oil</i>	<i>Mw_{oil} (K)</i>	<i>CGR (cm/million cycles)</i>
9	N326/55/0	666	0.77
10	R660/55/0	678	0.69
16	N234/55/0	500	0.88

Table 34 Crack Growth Rate of Control Samples

Code	N234/55phr/0			Code	N326/55phr/0		
	RSS1				RSS1		
	Sample No.	Mw _{oil} (K)	CGR (cm/million cycles)		Sample No.	Mw _{oil} (K)	CGR (cm/million cycles)
M1D1	273	585	2.14	M1D1	145	550	2.84
M1D2	274	669	1.84	M1D2	146	636	2.52
M1D3	275	759	1.70	M1D3	147	650	2.03
M1D4	276	896	1.21	M1D4	148	724	1.63
M2D1	277	580	2.22	M2D1	149	517	3.39
M2D2	278	602	2.40	M2D2	150	572	2.77
M2D3	279	631	2.00	M2D3	151	613	2.61
M2D4	280	667	1.81	M2D4	152	696	2.79
M3D1	281	457	3.10	M3D1	153	489	3.12
M3D2	282	476	2.33	M3D2	154	521	3.35
M3D3	283	493	2.41	M3D3	155	504	3.63
M3D4	384	495	1.99	M3D4	156	538	3.55
M4D1	285	372	2.99	M4D1	157	415	3.02
M4D2	286	382	2.85	M4D2	158	447	3.81
M4D3	287	381	2.93	M4D3	159	466	3.23
M4D4	288	403	2.39	M4D4	160	469	3.19
Code	Regal 660/55phr/0			Code	Regal 660/55phr/0		
	RSS1				RSS1		
	Sample No.	Mw _{oil} (K)	CGR (cm/million cycles)		Sample No.	Mw _{oil} (K)	CGR (cm/million cycles)
M1D1	177	674		M3D1	185	473	4.59
M1D2	178	792	2.34	M3D2	186	506	4.06
M1D3	179	891	2.78	M3D3	187	562	3.53
M1D4	180	676	2.98	M3D4	188	559	3.79
M2D1	181	598	3.41	M4D1	189	401	3.71
M2D2	182	602	3.11	M4D2	190	426	4.14
M2D3	183	697	3.15	M4D3	191	466	
M2D4	184	659	3.11	M4D4	192	449	4.78

Table 35 Tan δ at 60°C for Invention Samples

<i>Invention Sample No.</i>	<i>N234 Loading/Oil (phr)</i>	<i>MW_{ave} (K)</i>	<i>Max. Tan δ @ 60°C</i>
24	48/5	569	0.169
25	53/5	485	0.176
26	58/5	447	0.191
27	63/5	403	0.219
28	68/5	378	0.227
29	49/5	618	0.159
30	54/5	482	0.171
31	63/5	390	0.228
32	65/5	325	0.224

Table 36 Tan δ at 60°C for Control Samples

<i>Sample No.</i>	<i>MW (K)</i>	<i>D (%)</i>	<i>N234 Loading/Oil (phr)</i>	<i>Max. Tan D (@60 C)</i>
444	428	0.25	37/5	0.154
445	409	0.37	42/5	0.170
446	379	0.42	46/5	0.179
447	361	0.58	51/5	0.195
448	366	0.27	53/5	0.212
449	290	0.39	58/5	0.215
450	296	0.64	63/5	0.245

It can be seen from a comparison of Table 33 and 34 that advantageously lower crack growth rate is achieved by the invention samples, compared to the control samples. Lower crack growth rate correlates with good durability and related characteristics for numerous applications, including tire applications and the like. In addition, it can be seen from a comparison of Tables 35 and 36 that better $\tan \delta_{\max}$ values are achieved by the invention samples, that is, values which are lower than the values of the control sample. Accordingly, improved performance is achieved by the invention samples for numerous product applications including, for example, tire applications and the like requiring low hysteresis for correspondingly low rolling resistance.

The advantageous performance characteristics of the elastomer composites of the invention are exemplified by the crack growth rate of invention sample no. 16 comprising N234 carbon black and corresponding test results for control samples nos. 273 to 288 shown graphically in Fig. 22. Specifically, Fig. 22 clearly demonstrates a correlation between MW_{sol} and crack growth rate for the control samples, as well as the advantageous impact of excellent macro-dispersion in the elastomer composites of the present invention. It should be understood that the MW_{sol} values shown in Figs. 22 - 24 and in Tables 33 - 36 are for the masterbatch materials prior to cure. The molecular weight of the cured material is understood to correlate well to the MW_{sol} value of the uncured masterbatch. The crack growth rate of the control samples over an MW_{sol} range of about $.25 \times 10^6$ to $.6 \times 10^6$ is seen to fit well along a straight line correlation to MW_{sol} . In contrast, the invention sample no. 16 at MW_{sol} 0.5×10^6 has significantly better (i.e., lower) crack growth rate than any of the corresponding control samples, due to the better macro-dispersion D(%) of the invention sample. This is further established by the similar showing in Fig. 23, wherein the crack growth rate of invention sample no. 9 comprising

N326 carbon black is seen to be significantly lower than that of any of the corresponding control samples nos. 145 to 160, and is well below the correlation line. Likewise in Fig. 24 the excellent macro-dispersion of invention sample no. 10 is seen to result again in a crack growth value which lies far below the correlation line between crack growth rate and MW_{sol} established by the corresponding control samples nos. 177 to 192. In Fig. 25, the max $\tan \delta$ at 60°C is shown graphically to be better, i.e., lower, for invention samples nos. 24 to 28 and invention samples nos. 29 to 32 than for corresponding control samples nos. 444 to 450.

The superior crack growth results discussed above for elastomer composites of the present invention not only demonstrates advantageous fatigue properties, but also indicates advantageous fracture properties, such as excellent tear and cut-and-chip resistance. The superior hysteresis results discussed above for the elastomer composites of this invention not only demonstrate advantageously low rolling resistance (and correspondingly higher fuel economy) for motor vehicle tire applications, but also indicates advantageous improvement in related performance properties, such as reduced heat build-up. One or more of these superior properties, fatigue and fracture resistance, low hysteresis, low heat build-up, etc., render elastomer composites of the present invention well suited for use in commercial applications such as tire applications and in industrial rubber products. Regarding tire applications, various preferred embodiments of the invention are particularly well-suited for use as: tire tread, especially in tread for radial and bias truck tires, off-the-road ("OTR") tires, airplane tires and the like; sub-tread; wire skim; sidewalls; cushion gum for retread tires; and similar tire applications. The superior performance characteristics achieved by various preferred embodiments of the invention can provide improved tire durability, tread life and casing life, better fuel

economy for the motor vehicle and other advantages. Regarding industrial rubber products, various preferred embodiments of the invention are particularly well-suited for use as: engine mounts, hydro-mounts, bridge bearings and seismic isolators, tank tracks or tread, mining belts and similar products applications. The superior performance characteristics achieved by various preferred embodiments of the invention can provide improved fatigue life, durability and other advantages for such product applications.

Figs. 26 - 29 are graphical representations of carbon black morphology, structure (DBPA) and surface area (CTAB), corresponding generally to Fig. 8. Carbon black morphology region 261 in Fig. 26 includes carbon blacks currently in commercial use for OTR tire tread applications. Arrow 262 indicates the direction in which region 261 can be advantageously extended in accordance with the present invention. Performance characteristics such as cut-and-chip resistance, crack growth resistance and tear resistance are understood to improve generally in the direction of trend arrow 262 subject, however, in the past, to offsetting degradation of these and other characteristics due to reduced molecular weight of the natural rubber and/or poorer macro-dispersion resulting from the use of such higher surface area, lower structure carbon blacks. Elastomer composites of the present invention can employ such lower structure, higher surface area carbon black indicated by trend arrow 262 to achieve significantly improved OTR trend materials, in view of their excellent macro-dispersion and MW_{sol} .

Similarly, carbon black morphology region 271 in Fig. 27 includes carbon blacks currently in commercial use for truck and bus (T/B) tire tread applications. Arrow 272 indicates the direction in which region 271 can be advantageously extended in accordance with the present invention. Performance characteristics, such as wear resistance, are understood to improve generally in the direction of trend arrow 272 subject, however, in

the past, to offsetting degradation of these and other characteristics due to reduced molecular weight of the rubber and/or poorer macro-dispersion resulting from use of such higher surface area carbon blacks. Elastomer composites of the present invention can employ such higher surface area carbon blacks indicated by trend arrow 272 to achieve improved T/B tread materials, in view of their excellent macro-dispersion and MW_{sol} .

Similarly, carbon black morphology regions 281 and 283 in Fig. 28 show carbon blacks currently in commercial use for tread base and passenger car (PC) tire tread, respectively. Trend arrows 282 and 284 indicate the direction in which region 281 and 283, respectively, can be advantageously extended in accordance with the present invention. Performance characteristics such as heat build-up (HBU) and rolling resistance are understood to improve for tread base in the direction of trend arrow 282 subject, however, in the past, to offsetting degradation of these and other characteristics due to reduced molecular weight of the rubber and/or poorer macro-dispersion resulting from use of such higher surface area, lower structure carbon blacks. Likewise, performance characteristics such as rolling resistance are understood to improve for PC tread in the direction of trend arrow 284 subject, however, in the past, to offsetting degradation of these and other characteristics due to reduced molecular weight of the rubber and/or poorer macro-dispersion resulting from use of such higher surface area, lower structure carbon blacks. Elastomer composites of the present invention can employ higher surface area, lower structure carbon blacks indicated by arrows 282 and 284 to achieve improved tread base and PC tread, respectively, in view of the excellent macro-dispersion and the optional preservation of high molecular weight in such elastomer composites.

Similarly, carbon black morphology regions 291, 293 and 294 in Fig. 29 show carbon blacks currently in commercial use for sidewall, apex and steel belt tire applications, respectively. Trend arrows 292 and 295 indicate the direction in which region 291 and 294, respectively, can be advantageously extended in accordance with the present invention. Performance characteristics such as heat build-up (HBU) and fatigue life are understood to improve for sidewall in the direction of trend arrow 292 subject, however, in the past, the offsetting degradation of these and other characteristics due to reduced molecular weight of the rubber and/or poorer macro-dispersion resulting from use of such lower structure carbon blacks. Likewise, performance characteristics such as heat buildup, processing and wire adhesion are understood to improve for steel belt elastomeric materials in the direction of trend arrow 295 subject, however, in the past, to offsetting degradation of these and other characteristics due to reduced molecular weight of the rubber and/or poorer macro-dispersion resulting from use of such higher surface area, lower structure carbon blacks. Elastomer composites of the present invention can employ higher surface area and/or lower structure carbon blacks as indicated by arrows 292 and 295 to achieve improved sidewall and steel belt rubber materials, respectively, in view of the excellent macro-dispersion and the optional preservation of high molecular weight in such elastomer composites.

Additional Examples: Preferred Embodiment and Control Samples Comprising Other Fillers

Additional samples of elastomer composites in accordance with certain preferred embodiments of the present invention, and corresponding control samples, were prepared.

A first group of these employed a multiphase aggregate filler of the type referred to above as a silicon-treated carbon black.

Specifically, invention samples nos. 33 - 34 employed ECOBLACK® silicon-treated carbon black commercially available from Cabot Corporation (Billerica, Massachusetts). Such ECOBLACK® filler has morphological properties, i.e., structure and surface area, similar to that of carbon black N234. Sample no. 33 employed 45 phr ECOBLACK® filler and no extender oil. Sample no. 34 employed 68 phr ECOBLACK® filler and no extender oil. Typical filler and extender oil usage for various product applications are shown in Table 37, for elastomer composites of the invention comprising natural rubber and a blend of carbon black and silica filler. It should be understood that the use of silica filler in the compositions shown in Table 37 would typically replace a like amount of the carbon black filler.

Table 37 Typical NR Formulations for Tire Applications

Application	Carbon Black Type	Carbon Black Loading	Oil Loading	Silica Loading
Truck/Bus Tread	N110,N115,N121,N134,N220,N299	40 - 60 phr	0 - 20 phr	0 - 10 phr
OTR Tread	N110,N115,N220,N231	45 - 55 phr	5 - 10 phr	5 - 20 phr
Steel Belt	N326	50 - 75 phr	0 - 5 phr	0 - 20 phr
Truck/Bus Tread Base	N330,N550	40 - 60 phr	0 - 20 phr	
Carcass Ply	N326,N330,N550	40 - 60 phr	5 - 30 phr	
Sidewall	N330,N351,N550	30 - 60 phr	5 - 30 phr	
Apex	N326,N330,N351	50 - 90 phr	0 - 20 phr	
LRR PC Tread	N234,N299,N339,N343,N347,N351	40 - 60 phr	0 - 30phr	

A second group of samples employed a blend or mixture of silica and carbon black. In embodiments of the present invention employing a blend of carbon black and silica fillers, it is generally preferred that they be used in weight ratio of at least about 60:40. That is, the carbon black preferably comprises at least about 60 weight percent of the filler to achieve good coagulation of the elastomer and to reduce or eliminate reagglomeration of the silica in the masterbatch. In particular, in examples nos. 35 - 38, as shown in Table 40, carbon black is used together with particulate SiO₂ filler HiSil ® 233 available from PPG Industries (Pittsburgh, Pennsylvania, USA), having surface area BET of 150 m²/g, surface area DBPA of 190 mls/100g, pH of 7 and a primary particulate size of 19 nanometers.

All of the invention samples, i.e., additional invention samples nos. 33 - 38, were prepared in accordance with the procedures and apparatus used for invention samples 1 - 32, as described above. Process and apparatus details for each of invention samples nos. 33 - 38 is given in Table 38, below. The field latex or concentrate employed in samples nos. 33 - 38, as the case may be, is the same as described above with reference to Table 24. It will be appreciated that the data in Table 38 parallels that provided in Table 25, above, for invention samples nos. 1-32. The carbon black filler "CRX2000" listed in Table 38 is the ECOBLACK® silicon-treated carbon black described above.

Table 38 Invention Sample Production Details

Table 30 Invention Sample 1 Production Data									
Invention Sample No.	Cabot Elastomer Composite					Slurry Nozzle Tip		CB Slurry CB conc. (%wt)	
	Latex type	Carbon Black		HISil 233 Loading (phr)	Oil loading (phr)	Dia. (in)	Land length (in)		
		Type	Loading (phr)						
33	field latex	CRX2000	46	0	0.020	0.5	14.5		
34	field latex	CRX2000	58	0	0.020	0.5	14.5		
35	field latex	N220	43	10	0.025	0.5	13.9		
36	field latex	N234	41	9	0.020	0.5	13.5		
37	field latex	N234	31	20	0.020	0.5	14.0		
38	latex concentrate	STERLING 6740	29	20	0.020	0.5	15.5		
Coagulum Zone									
Invention Sample No.	1st portion		2nd portion		3rd portion		4th portion		
	Dia. (in)	Length (in)	Dia. (in)	Length (in)	Dia. (in)	Length (in)	Dia. (in)	Length (in)	
	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	
	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	
	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	
	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	
	0.19	3.0	0.27	1.6	0.38	2.3	0.53	3.2	
Mixing Zone									
Invention Sample No.	Slurry flow rate (lb/min)	Slurry velocity (ft/sec)	Antioxidant		Latex flow rate (lbs/min)	Latex velocity (ft/sec)	Inlet pressure (psi)	Outlet pressure (psi)	
			TNPP (phr)	Santoflex(phr)					
	6.2	710	0.3	0.4	Field	7.4	10.7	17000	
	6.2	710	0.3	0.4	Field	5.8	8.3	17000	
	5.2	380	0.3	0.4	Field	4.9	7.1	14500	
	5.0	576	0.3	0.4	Field	4.3	6.2	10000	
	4.8	550	0.3	0.4	Field	4.1	5.9	9500	
38	5.1	580	0.3	0.4	Conc	2.2	3.2	9000	
Invention Sample No.	Slurry Nozzle Tip Pressure (psi)	Dewatering		Drying and Cooling		Mixer Type	Production Rate (lb/hr)	Invention Sample No.	
		Initial crumb moisture (%)	Final crumb moisture (%)	Product temp. (°F)	Product moisture (%)				
	-	77.5	>8.0	435	0.2	T-block	68	33	
	-	78.0	1.6	470	0.3	T-block	52	34	
	1650	77.9	>4.0	360	0.4	T-block	54	35	
	3000	79.2	1.0	475	0.5	T-block	39	36	
	2930	78.9	12.3	435	0.4	T-block	34	37	
38	2600	69.7	4.2	455	0.2	T-block	48	38	

The control samples 451-498 were prepared in accordance with the procedures and apparatus described above for control samples nos. 1-450. The processing code (see Table 13 above), filler loading, rubber, MW_{sol} and macro-dispersion for masterbatches 451-466 are set forth below in Table 39. The processing code, filler loading, rubber, 5 MW_{sol} and macro-dispersion values of the invention samples nos. 33-38 (along with the filler and oil loadings for convenient reference) are shown in Table 40. It will be seen from Table 39 that control samples 451-466 correspond in composition to invention samples nos. 33 and 34. Similarly, control samples nos. 467-498 correspond to invention samples nos. 35-38.

Table 39

Code	CRX 2000/44/0			CRX 2000/58/0		
	RSS1			RSS1		
	Sample No.	Mw _{nom} (K)	D (%)	Sample No.	Mw _{nom} (K)	D (%)
M2		909			909	
M3		590			590	
M2D1	451	461	3.48	459	333	8.61
M2D2	452	474	3.68	460	392	5.71
M2D3	453	489	7.17	461	388	9.48
M2D4	454	515	6.28	462	394	8.05
M3D1	455	393	2.89	463	280	2.23
M3D2	456	422	2.87	464	298	2.13
M3D3	457	435	4.15	465	350	4.05
M3D4	458	449	3.23	466	379	7.22

Table 40 Sol Molecular Weight and Undispersed Area of Invention Samples

Invention Sample No.	CB>Loading/Oil	Mw _{nom} (K)	D (%)
33	CRX 2000/44/0	380	0.18
34	CRX 2000/58/0	448	0.10
35	N220/Hilsil 233/43/10/5	500	0.14
36	N234/Hilsil 233/40/10/0	490	0.36
37	N234/Hilsil 233/30/20/0	399	0.23
38	STERLING 6740/Hilsil 233/30/20/0	354	0.39

Table 41

Code	N220/Hilsil 233/43/10/5			N234/Hilsil 233/40/10/0		
	RSS1			RSS1		
	Sample No.	Mw _{mol} (K)	D (%)	Sample No.	Mw _{mol} (K)	D (%)
M2		803			909	
M3		601			590	
M2D1	467	493	1.51	475	443	8.74
M2D2	468	537	2.61	476	517	10.9
M2D3	469	523	2.82	477	569	12.5
M2D4	470	615	2.95	478	592	8.25
M3D1	471	417	0.95	479	358	6.65
M3D2	472	438	1.40	480	420	13.8
M3D3	473	433	2.15	481	516	13.9
M3D4	474	485	2.22	482	447	7.25
Code	N234/Hilsil 233/30/20/0			STERLING 6740/Hilsil 233/30/20/0		
	RSS1			RSS1		
	Sample No.	Mw _{mol} (K)	D (%)	Sample No.	Mw _{mol} (K)	D (%)
M2		909			909	
M3		590			590	
M2D1	483	394	4.37	491	430	3.77
M2D2	484	507	5.66	492	488	4.39
M2D3	485	526	4.7	493	517	5.37
M2D4	486	568	5.94	494	563	4.66
M3D1	487	377	8.39	495	375	3.5
M3D2	488	363	4.49	496	380	2.73
M3D3	489	376	5.07	497	419	2.72
M3D4	490	432	5.26	498	448	3.29

The excellent carbon black dispersion in the masterbatches of invention samples 33-38 is demonstrated by comparison of the macro-dispersion quality and MW_{sol} values shown in Tables 39-41. The invention samples nos. 33-34 made with ECOBLACK® silicon-treated carbon black, and the corresponding control samples are compared in the semi-log plot of Fig. 30. Excellent carbon black dispersion is seen in Fig. 30 for the invention samples, representing preferred embodiments of elastomer composites in accordance with the present disclosure. The invention samples advantageously are below line 301 in Fig. 30, whereas all of the control samples have poorer dispersion, being above line 301. In fact, the preferred embodiments shown in Fig. 30 fall below a $D(\%)$ value of .2% even at an MW_{sol} value advantageously exceeding $.4 \times 10^6$. The data shown in Fig. 30 clearly reveals that the macro-dispersion quality of the novel elastomer composites, disclosed here, comprising silicon-treated carbon black is significantly superior to that achievable using comparable ingredients in prior dry mixing methods. The macro-dispersion values for the elastomer composites of the invention shown in Fig. 30 are described by the following equations:

$$D(\%) < 1.0\% \quad (25)$$

when MW_{sol} is less than 0.4×10^6 ; and

$$\log(D) < \log(1.0) + 2.0 \times [MW_{sol} - (0.4 \times 10^6)] \times 10^{-6} \quad (26)$$

when $0.4 \times 10^6 < MW_{sol} < 1.1 \times 10^6$

It will be recognized that $D(\%)$ is the percent undispersed area measured for defects greater than 10 microns and 1% is the threshold macro-dispersion quality for the masterbatches in accordance with these preferred embodiments of the present invention. That is, none of the dry masticated masterbatches achieved macro-dispersion quality of

1.0% or better at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below $.4 \times 10^6$. The preferred embodiments shown in Fig. 30 fall well below the threshold. It can be seen that the elastomer composites of the invention comprising silicon-treated carbon black provide heretofore unachieved balance between macro-dispersion quality and MW_{sol} .

Invention samples nos. 35-38 comprising carbon black blended with silica filler and corresponding control samples are compared in the semi-log plot of Fig. 31. Specifically, Fig. 31 shows the macro-dispersion values and MW_{sol} values of the invention samples nos. 35 - 38 and corresponding control samples nos. 467 - 498. Excellent carbon black dispersion is seen in Fig. 31 for the invention samples, representing preferred embodiment of elastomer composites in accordance with the present disclosure. The invention samples advantageously are below line 311 in Fig. 31, whereas all of the control samples have poorer dispersion, being above line 311. In fact, all of the preferred embodiments shown in Fig. 31 fall below a $D(\%)$ value of .4%. The data shown in Fig. 31 clearly reveals that the macro-dispersion quality of the novel elastomer composites, disclosed here, comprising carbon black/silica blends over a range of MW_{sol} values, is significantly superior to that achievable using comparable ingredients in prior dry mastication mixing methods. The macro-dispersion values for the elastomer composites of the invention shown in Fig. 31 are described by the following equations:

$$D(\%) < 0.8\% \quad (27)$$

when MW_{sol} is less than 0.5×10^6 ; and

$$\log(D) < \log(0.8) + 2.2 \times [MW_{sol} - (0.5 \times 10^6)] \times 10^{-6} \quad (28)$$

when $0.5 \times 10^6 < MW_{sol} < 1.1 \times 10^6$

Blends-CIP
125

It will be recognized that D(%) is the percent undispersed area measured for defects greater than 10 microns and .8% is the threshold macro-dispersion quality for masterbatches in accordance with these preferred embodiments of the present invention. That is, none of the dry masticated masterbatches achieved macro-dispersion quality of 0.8% or better at any MW_{sol} , even after dry mixing sufficiently to degrade MW_{sol} below $.4 \times 10^6$. The preferred embodiments shown in Fig. 31 fall well below the threshold macro-dispersion value of .8%, and even below .4%. It can be seen that the elastomer composites of the invention comprising carbon black/silica blend filler provide heretofore unachieved balance between macro-dispersion quality and MW_{sol} .

10

ADDITIONAL EXAMPLES

Elastomer composite blends were prepared in accordance with the present invention and compared to corresponding blends made using prior known dry/dry mixing techniques, as now described. The elastomer composite blends were prepared with elastomer composite samples referred to below as "CEC" or "CEC masterbatch."

15

CEC masterbatches were made using field latex natural rubber and Vulcan 7H carbon black (ASTM N234 carbon black) as follows:

20

Preparing Elastomer Composite (wet mixing step) Elastomer masterbatch was produced in accordance with the present invention. Specifically, an elastomer masterbatch was produced comprising standard natural rubber field latex from Malaysia with 71 phr filler consisting of carbon black of commercial grade N234 available from Cabot Corporation. The compound formulation (excluding minor ordinary latex additives) is set forth in Table 7 below.

Table 7A Masterbatch Formulation

	<u>Ingredient</u>	<u>Parts by Wt.</u>
5	Rubber	100
	Carbon Black	71.
	Santoflex 134 (antioxidant)	0.4
	<u>TNPP (antioxidant)</u>	<u>0.3</u>
	Total	171.7

10 The elastomer masterbatch production apparatus was substantially identical to the
 apparatus described above with reference to Figs. 1, 3 and 7 of the drawings. The
 slurry nozzle tip (see reference No. 167 in Fig. 7) was .018 inch diameter with a land
 (see reference No. 168 in Fig. 7) having an axial length of 0.2 inch. The coagulum
 zone (see No. 53 in Fig. 3) included a first portion of .188 inch diameter and
 approximately .985 inch axial length (being partly within the mix-head and partly within
 15 the extender sealed thereto); a second portion of .266 inch diameter and 1.6 inch axial
 length; a third portion of .376 inch diameter and 2.256 axial length; and a fourth
 portion of .532 inch diameter and 3.190 inch axial length. In addition, there are
 axially short, faired interconnections between the aforesaid portions. Preparation of
 the masterbatch is described in further detail immediately below.

- 20 1. Carbon Black Slurry Preparation. Bags of carbon black were mixed with
 deionized water in a carbon black slurry tank equipped with an agitator. The
 agitator broke the pellets into fragments and a crude slurry was formed with
 15.1 wt. % carbon black. The crude slurry was recirculated using a pipeline
 grinder. During operation, this slurry was continually pumped by an air
 25 diaphragm pump to a colloid mill for initial dispersion. The slurry was then
 fed by a progressing cavity pump to a homogenizer, specifically, Microfluidizer

Model M210 from Microfluidics International Corporation for pressurizing and shear, to produce a finely ground slurry. The slurry flow rate from the microfluidizer to the mixing zone was set by the microfluidizer speed, the microfluidizer acting as a high-pressure positive displacement pump. Slurry flow rate was monitored with a Micromotion® mass flow meter. The carbon black slurry was fed to the microfluidizer at a pressure of about 250 psig and the output pressure was set at 7500 psig to an accumulator set at about 1200 psig output pressure, such that the slurry was introduced as a jet into the mixing zone at a flow rate of about 3.6 lb/min and at a velocity of about 500 ft/sec.

2. Latex Delivery. The latex was charged to a tank, specifically, a 55 gallon feed drum. Antioxidant emulsion was added to the latex prior to charging. Antioxidants were added consisting of 0.3 phr tris nonyl phenyl phosphite (TNPP) and 0.4 phr Santoplex® 134 (alkyl-aryl p-phenylene diamine mixture). Each of the antioxidants was prepared as a 40 wt.% emulsion using 4 parts potassium oleate per 100 parts antioxidant along with potassium hydroxide to adjust the emulsion to a pH of approximately 10. A peristaltic pump was used to move the latex from the feed tank to the mixing zone of the coagulum reactor. The latex flow rate was 3.2 to 3.3 lbs/min and about 4.8 feet per second, and was metered with a Endress + Hauser (Greenwood, Indiana, USA) mass flow meter. The desired carbon black loading of a 71 phr was obtained by maintaining proper ratio of the latex feed rate to the carbon black slurry feed rate.

3. Carbon Black and Latex Mixing. The carbon black slurry and latex were mixed by entraining the latex into the carbon black slurry. During entrainment, the carbon black was intimately mixed into the latex and the mixture coagulated. Soft, wet spongy "worms" of coagulum exited the coagulum reactor.

4. Dewatering. The wet crumb discharged from the coagulum reactor was about 80% water. The wet crumb was dewatered to about 11 to 13% moisture with a dewatering extruder (The French Oil Mill Machinery Company; 3½ in. diameter). In the extruder, the wet crumb was compressed and water squeezed from the crumb and through a slotted barrel of the extruder.

5. Drying & Cooling. The dewatered crumb dropped into a second extruder where it was again compressed and heated. Water was flashed off upon expulsion of the crumb through the dieplate of the extruder. Product exit temperature was approximately 280°F to 310°F and moisture content was about 3.0 to 4.0 wt.%. The hot, dry crumb was rapidly cooled (approximately 20 seconds) to about 100°F by a forced air vibrating conveyor. Partially wet crumb was completely dried to less than 0.5 wt.% in a forced air convector oven (Aeroglide, Raleigh, North Carolina) at a temperature of 200°F - 240°F.

Dry Mixing Step In the following examples both of the two "dry mixing" steps of the dry/dry method used below for comparison and control purposes, and the

“dry mixing” step of the wet/dry method of the present invention were carried out in a Farrell BR Banbury mixer.

Reference in the following procedures and the following examples to “natural rubber masterbatch” refers to the product of the first dry mixing stage. The term masticated natural rubber refers to the product of the “natural rubber mastication condition” set forth below. The term NR refers to natural rubber. The term CB refers to carbon black. In all cases, carbon black is N234 carbon black. The full formulations for the wet and dry mixing steps is provided in the formulation table immediately below.

It can be seen from the foregoing examples that excellent properties are achieved in the elastomer composite blends of the present invention.

Formulation

Ingredients		phr
Rubbers	(masticated RSS1 + Taktene 220 or, CEC NR + Taktene 220 or, CEC NR + masticated RSS1 or, masticated RSS1)	100.0
Carbon Black	(V7H)	50.0
Oil	(Sundex 790)	5.0
Antioxidant 1	(Santoflex 134)	0.4
Antioxidant 2	(TNPP)	0.3
Zinc Oxide	(Azo 66)	4.0
Stearic Acid	(Hystrene 5016)	2.0
Accelerator	(Santocure NS)	1.8
Sulfur		1.0
Total		164.5

Mixing Procedures of CEC NR/BR Blends and Dry NR/BR Blends

Mixing Method

1. Blend natural rubber masterbatch, in which all carbon black was loaded, with butadiene rubber and oil. The ratios of natural rubber to butadiene rubber were 90/10, 80/20 and 70/30;
2. Blend natural rubber masterbatch, in which all carbon black and oil were loaded, with butadiene rubber. The ratios of natural rubber to butadiene rubber were 80/20 and 70/30;
3. Blend natural rubber masterbatch, in which 50 phr of carbon black was loaded, with butadiene masterbatch, in which 50 phr of carbon black was loaded, and oil. The ratios of natural rubber to butadiene rubber were 80/20, 70/30, 60/40 and 50/50;
4. Blend natural rubber masterbatch, in which 50 phr of carbon black and all oil were loaded, with butadiene masterbatch, in which 50 phr of carbon black was loaded. The ratios of natural rubber to butadiene rubber were 80/20, 70/30, 60/40 and 50/50;
5. Blend CEC masterbatch, in which all carbon black was loaded, with butadiene rubber and oil. The ratios of natural rubber to butadiene rubber were 90/10, 80/20 and 70/30;
6. Blend CEC masterbatch, in which all carbon black and oil were loaded, with butadiene rubber. The ratios of natural rubber to butadiene rubber were 80/20 and 70/30;
7. Blend CEC masterbatch, in which 50 phr of carbon black was loaded, with butadiene masterbatch, in which 50 phr of carbon black was loaded, and oil. The ratios of natural rubber to butadiene rubber were 80/20, 70/30, 60/40 and 50/50;
8. Blend CEC masterbatch, in which 50 phr of carbon black and all oil were loaded, with butadiene masterbatch, in which 50 phr of carbon black was loaded. The ratios of natural rubber to butadiene rubber were 80/20, 70/30, 60/40 and 50/50.

Mixing Procedures

A three stage Banbury mix was used for dry mix blends and two stage Banbury mix for CEC blends. Natural rubber was masticated before first stage mix for dry mix blends. Butadiene rubber was used without mastication.

Natural rubber mastication condition:

Fill factor:	0.75
Rotor speed:	100 rpm
Banbury Temperature:	30°C
Total batch energy:	950 Watt-Hours

Banbury mixing procedures:

Mixing method 1:

Stage 1:

Fill factor:	varied
Rotor speed:	70 rpm
Banbury temperature:	30°C

<i>Time</i>	<i>Operation</i>
0"	add masticated NR
30"	add 40phr of CB
1'00"	add ½ remaining CB
1'30"	add remaining CB
8' to 13'	dump according to power curve

Sample No.	Fill factor	Mixing time	Dump temp. (°C)	Energy input (KWH)
1-1 (stage 1)	0.67	8'	140.8	1.45
1-2 (stage 1)	0.65	8'	148.6	1.59
1-3 (stage 1)	0.63	10'	167.3	1.89

Stage 2:

Fill factor: 0.70
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

<i>Time</i>	<i>Operation</i>
0"	add NR masterbatch, BR bale, chemicals and oil
3'00"	dump

Sample No.	Dump Temperature (°C)	Energy Input (KWH)
1-1 (stage 2)	113.5	0.42
1-2 (stage 2)	118.2	0.46
1-3 (stage 2)	116.4	0.44

Stage 3:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

<i>Time</i>	<i>Operation</i>
0"	add stage 2 compound and curatives
3'00"	dump

Sample No.	Dump Temperature (°C)	Energy Input (KWH)
1-1	99.5	0.42
1-2	99.8	0.43
1-3	103.9	0.45

Mixing method 2:**Stage 1:**

Fill factor: 0.65
 Rotor speed: 70 rpm (50rpm when temp. reached 160°C)
 Banbury temperature: 30°C

<i>Time</i>	<i>Operation</i>
0"	add masticated NR
30"	add 40phr of CB
1'00"	add ½ remaining CB
1'30"	add remaining CB
2'00"	add oil
9' to 13'	dump according to power curve

Sample No	Mixing time	Dump temp. (°C)	Energy input (KWH)
2-1(stage 1)	9'	148	1.60
2-2(stage 1)	9.5'	145	1.84

Stage 2:

Fill factor: 0.70
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add NR masterbatch, BR bale, chemicals
3'00"	dump

Sample No	Dump Temperature (°C)	Energy input (KWH)
2-1 (stage 2)	127	0.48
2-2 (stage 2)	126	0.51

Stage 3:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add stage 2 compound and curatives
3'00"	dump

Sample ID	Dump Temperature (°C)	Energy Input (KWH)
2-1	99	0.42
2-2	107	0.44

Mixing method 3:**Stage 1:**

• NR masterbatch:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add masticated NR
30"	add 40phr of CB
1'00"	add remaining CB
9'00"	dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
3-1 to 3-4 (stage 1)	142	1.51
3-1 to 3-4 (stage 1)	143	1.48
3-1 to 3-4 (stage 1)	148	1.52

• BR masterbatch:

Fill factor: 0.75
 Rotor speed: 85 rpm (60rpm when temp. reached 160°C)
 Banbury temperature: 30°C

Time	Operation
0'	add BR bale
30"	add 30 phr carbon black

1'00" add 1/2 of rest of carbon black
 1'30" add remaining carbon black
 7'00" dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
3-1 to 3-4 (stage 1)	159	1.38
3-1 to 3-4 (stage 1)	158	1.35
3-1 to 3-4 (stage 1)	157	1.33

Stage 2:

Fill factor: 0.70
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time *Operation*
 0" add stage 1 masterbatches and chemicals and oil
 3'00" dump

Sample No.	Dump Temperature (°C)	Energy Input (KWH)
3-1 (stage 2)	115	0.36
3-2 (stage 2)	123	0.40
3-3 (stage 2)	120	0.40
3-4 (stage 2)	118	0.37

Stage 3:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time *Operation*
 0" add stage 2 compound and curatives
 3'00" dump

Sample ID	Dump Temperature (°C)	Energy Input (KWH)
3-1	103	0.44
3-2	107	0.45
3-3	109	0.47
3-4	97	0.38

Mixing method 4:**Stage 1:**

• NR masterbatches

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time *Operation*
 0" add masticated NR
 30" add 40phr of CB
 1'00" add remaining CB
 2'00" add oil
 9'00" dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
4-1 to 4-4 (stage 1)	140	1.49
4-1 to 4-4 (stage 1)	136	1.49
4-1 to 4-4 (stage 1)	137	1.40

• BR masterbatch

Fill factor: 0.75
 Rotor speed: 85 rpm (60rpm when temp. reached 160°C)
 Banbury temperature: 30°C

Time	Operation
0'	add BR bale
30"	add 30 phr carbon black
1'00"	add ½ of rest of carbon black
1'30"	add remaining carbon black
7'00"	dump

Sample No.	Dump Temperature (°C)	Energy input (KWH)
4-1 to 4-4 (stage 1)	159	1.38
4-1 to 4-4 (stage 1)	158	1.35
4-1 to 4-4 (stage 1)	157	1.33

Stage 2.

Fill factor: 0.70
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add stage 1 masterbatches and chemicals
3'00"	dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
4-1 (stage 2)	133	0.52
4-2 (stage 2)	133	0.56
4-3 (stage 2)	133	0.55
4-4 (stage 2)	132	0.53

Stage 3:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add stage 2 compound and curatives
3'00"	dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
4-1	107	0.48
4-2	108	0.48
4-3	109	0.47
4-4	111	0.46

Mixing method 5:

Stage 1:

Fill factor: 0.75
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add CEC masterbatch
4'	add BR bale
7'	add powders and oil
9'	dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
5-1 (stage 1)	104.2	1.78
5-2 (stage 1)	107.1	1.72
5-3 (stage 1)	103.9	1.79

Stage 2:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add stage 1 compound and curatives
3'00"	dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
5-1	76.7	0.46
5-2	81.0	0.46
5-3	83.3	0.46

Mixing method 6:

Stage 1:

Fill factor: 0.75
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add CEC masterbatch
4'	add BR bale
7'	add powders
9'	dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
6-1 (stage 1)	114.8	1.67
6-2 (stage 1)	115.6	1.72

Stage 2:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add stage 1 compound and curatives
3'00"	dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
6-1	81.6	0.47
6-2	81.4	0.47

Mixing method 7:

Stage 1:

Fill factor: 0.75
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add CEC masterbatch
2'	add BR masterbatch
5'	add powders and oil
7'	dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
7-1 (stage1)	117.4	1.33
7-2 (stage1)	112.6	1.21
7-3 (stage1)	106.0	1.14
7-4 (stage1)	105.7	1.24

Stage 2:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add stage 1 compound and curatives
3'00"	dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
7-1	83.6	0.48
7-2	83.0	0.46
7-3	83.6	0.46
7-4	83.4	0.46

Mixing method 8:

Stage 1:

Fill factor: 0.75
 Rotor speed: 70 rpm
 Banbury temperature: 30°C

Time	Operation
0"	add CEC masterbatch
2'	add BR masterbatch
5'	add powders
7'	dump

Sample ID	Dump Temperature (°C)	Energy Input (KWH)
8-1 (stage 1)	108.4	1.25
8-2 (stage 1)	112.4	1.27
8-3 (stage 1)	103.1	1.13
8-4 (stage 1)	111.3	1.20

Stage 2:

Fill factor: 0.65

Rotor speed: 70 rpm

Banbury temperature: 30°C

Time Operation

0" add stage 1 compound and curatives

3'00" dump

Sample ID	Dump Temperature (°C)	Energy Input (KWH)
8-1	78.8	0.48
8-2	81.0	0.45
8-3	76.4	0.44
8-4	78.5	0.44

Table 1 Sample Description and Code for NRBR Blends

Mixing Method No.	Description	Sample No.	Ratio of NR/BR	Black loading in natural rubber	Black loading in butadiene rubber	Oil loaded to
1	blend natural rubber masterbatch, in which all carbon black was loaded, with butadiene rubber and oil.	1-1	80/10	55.5 phr	0 phr	blend
		1-2	80/20	82.5 phr	0 phr	blend
		1-3	70/30	71.4 phr	0 phr	blend
2	blend natural rubber masterbatch, in which all carbon black and oil were loaded, with butadiene rubber.	2-1	80/20	82.5 phr	0 phr	natural rubber
		2-2	70/30	71.4 phr	0 phr	natural rubber
3	blend natural rubber masterbatch, in which 50 phr of carbon black was loaded, with butadiene rubber masterbatch, in which 50 phr of carbon black was loaded, and oil.	3-1	80/20	50 phr	50 phr	blend
		3-2	70/30	50 phr	50 phr	blend
		3-3	60/40	50 phr	50 phr	blend
		3-4	50/50	50 phr	50 phr	blend
4	blend natural rubber masterbatch, in which 50 phr of carbon black and all oil were loaded, with butadiene rubber masterbatch, in which 50 phr of carbon black was loaded.	4-1	80/20	50 phr	50 phr	natural rubber
		4-2	70/30	50 phr	50 phr	natural rubber
		4-3	60/40	50 phr	50 phr	natural rubber
		4-4	50/50	50 phr	50 phr	natural rubber
5	blend CEC masterbatch, in which all carbon black was loaded, with butadiene rubber and oil.	5-1	90/10	55.5 phr	0 phr	blend
		5-2	80/20	82.5 phr	0 phr	blend
		5-3	70/30	71.4 phr	0 phr	blend
6	blend CEC masterbatch, in which all carbon black and oil were loaded, with butadiene rubber.	6-1	80/20	82.5 phr	0 phr	CEC
		6-2	70/30	71.4 phr	0 phr	CEC
7	blend CEC masterbatch, in which 50 phr of carbon black was loaded, with butadiene rubber masterbatch, in which 50 phr of carbon black was loaded, and oil.	7-1	80/20	50 phr	50 phr	blend
		7-2	70/30	50 phr	50 phr	blend
		7-3	60/40	50 phr	50 phr	blend
		7-4	50/50	50 phr	50 phr	blend
8	blend CEC masterbatch, in which 50 phr of carbon black and all oil were loaded, with butadiene rubber masterbatch, in which 50 phr of carbon black was loaded.	8-1	80/20	50 phr	50 phr	CEC
		8-2	70/30	50 phr	50 phr	CEC
		8-3	60/40	50 phr	50 phr	CEC
		8-4	50/50	50 phr	50 phr	CEC

Table 2 Compound Characterization of NR/BR Blends

Mixing Method No.	Sample No.	Mooney Viscosity ML(1+4)@100°C	Undispersed Area %	Sol Molecular Weight K	Bound Rubber %
1	1-1	58	1.15	295	40
	1-2	60	1.00	277	42
	1-3	64	2.84	243	43
2	2-1	63	1.26	276	41
	2-2	62	1.28	245	41
3	3-1	62	0.86	337	37
	3-2	61	0.58	336	36
	3-3	64	0.65	336	38
	3-4	64	0.84	333	34
4	4-1	70	0.68	359	37
	4-2	70	0.62	361	37
	4-3	68	0.68	342	37
	4-4	66	0.54	324	35
5	5-1	58		334	43
	5-2	59		319	43
	5-3	58		296	41
6	6-1	60	0.32	430	36
	6-2	59	0.40	347	37
7	7-1	65	0.51	422	43
	7-2	65	0.46	434	42
	7-3	62	0.54	428	40
	7-4	64	0.47	404	41
8	8-1	62	0.52	401	40
	8-2	64	0.52	434	40
	8-3	58	0.65	407	34
	8-4	63	0.51	359	41

Table 3. Physical Properties of NR/BR Blends

Sample No.	Hardness	E100 MPa	E300 MPa	Tensile MPa	Elongation %	Rebound 60°C, %	Rebound 0°C, %	Rebound r.t., %
1-1	65	2.9	16	29	500	62	38	62
1-2	64	3.1	17	28	462	65	43	55
1-3	65	3.2	18	25	404	65	46	56
2-1	69	2.9	16	26	459	60	39	50
2-2	69	2.9	16	24	434	60	41	51
3-1	65	2.4	13	26	510	63	43	53
3-2	66	2.4	13	26	514	63	45	54
3-3	66	2.5	13	25	486	62	46	54
3-4	67	2.5	13	23	468	62	49	57
4-1	68	2.6	14	27	502	61	42	52
4-2	69	2.6	14	25	472	61	43	53
4-3	68	2.6	14	24	467	60	44	53
4-4	68	2.7	14	24	459	60	46	53
5-1	65	2.9	17	28	452	65	41	64
5-2	64	2.8	16	27	452	66	43	66
5-3	64	2.9	16	25	432	65	45	56
6-1	66	2.5	14	27	505	62	42	54
6-2	65	2.9	15	26	462	63	45	55
7-1	68	3.0	17	29	472	64	45	55
7-2	68	3.0	17	28	459	64	46	57
7-3	67	2.9	16	25	429	64	48	58
7-4	67	3.0	16	23	397	65	51	59
8-1	67	2.8	15	28	480	64	46	56
8-2	67	2.8	15	27	476	64	47	56
8-3	66	2.6	14	25	465	62	47	55
8-4	65	2.8	15	23	400	67	54	60

Table 4 Fracture Properties and Dynamic Property of NR/BR Blends

Sample No.	Crack Growth Rate $\times 10^{-6}$, cm/million cycle	Tear Strength Die C, N/mm	Abrasion Rating	Max. Tan δ @ 60°C
1-1	4.32	128	81	0.176
1-2	3.11	88	83	0.147
1-3	1.34	54	88	0.132
2-1	4.37	55	100	0.178
2-2	2.39	50	95	0.164
3-1	4.30	107	74	0.165
3-2	3.86	97	80	0.161
3-3	3.54	80	85	0.153
3-4	2.23	73	100	0.158
4-1	4.47	108	85	0.188
4-2	4.64	104	96	0.173
4-3	3.82	70	113	0.175
4-4	3.73	63	150	0.174
5-1	4.03	78	114	0.176
5-2	3.72	85	113	0.156
5-3	1.99	62	88	0.152
6-1	1.64	75	101	0.186
6-2	0.61	81	107	0.166
7-1	4.59	70	117	0.178
7-2	4.30	75	132	0.168
7-3	4.81	58	144	0.151
7-4	3.43	52	146	0.132
8-1	5.08	66	112	0.186
8-2	4.60	66	134	0.181
8-3	5.19	58	140	0.165
8-4	4.43	64	138	0.140

Abrasion Rating = (weight loss of reference sample/weight loss of sample) $\times$ 100
(reference sample was sample no. 2-1)

Mixing Procedures of CEC/RSS1 Blends and Dry Mix RSS1 Compound

Mixing Method

Dry: Masticated RSS1 was mixed with other ingredients;

CEC: Blend CEC masterbatch, in which all carbon black was loaded, with masticated RSS1 and oil. The ratios of CEC natural rubber to RSS1 natural rubber were 100/0, 90/10, 80/20 and 70/30.

Mixing Procedures

A three stage Banbury mix was used for dry mix compound and two stage Banbury mix for CEC/RSS1 blends. RSS1 natural rubber was masticated before first stage mix for dry mix compound and CEC/RSS1 blends.

RSS1 mastication condition:

Fill factor: 0.75
Rotor speed: 100 rpm
Banbury Temperature: 30°C
Total batch energy: 950 Watt-Hours

Banbury mixing procedures:

Dry:

Stage 1:

Fill factor: 0.65
Rotor speed: 70 rpm
Banbury temperature: 30°C

Time	Operation
0"	add masticated RSS1
30"	add 30 phr of CB
1'00"	add ½ remaining CB
1'30"	add remaining CB
10'	dump according to power curve

Sample Code	Mixing time	Dump temp. (°C)	Energy input (KWH)
Dry (stage 1)	10'	130	1.7

Stage 2:

Fill factor: 0.70
Rotor speed: 70 rpm
Banbury temperature: 30°C

Time	Operation
0"	add stage 1 masterbatch, oil and all chemicals except curatives
3'00"	dump

Sample Code	Dump Temperature (°C)	Energy Input (KWH)
Dry (stage 2)	124	0.42

Stage 3:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C
Time Operation
 0" add stage 2 compound and curatives
 3'00" dump

Sample Code	Dump Temperature (°C)	Energy Input (KWH)
1-1	91	0.36

CEC:

Stage 1:

Fill factor: 0.75
 Rotor speed: 70 rpm
 Banbury temperature: 30°C
Time Operation
 0" add CEC masterbatch
 4' add masticated RSS1
 7' add powders and oil
 6'-9' dump

Sample Code	Dump Temperature (°C)	Energy Input (KWH)	Mixing Time
CEC-1 (stage 1)	113.9	1.28	6'
CEC-2 (stage 1)	104.2	1.78	9'
CEC-3 (stage 1)	107.1	1.72	9'
CEC-4 (stage 1)	103.9	1.79	9'

Stage 2:

Fill factor: 0.65
 Rotor speed: 70 rpm
 Banbury temperature: 30°C
Time Operation
 0" add stage 1 compound and curatives
 3'00" dump

Sample No	Dump Temperature (°C)	Energy Input (KWH)
CEC-1	81.3	0.53
CEC-2	76.7	0.46
CEC-3	81.0	0.46
CEC-4	83.3	0.46

Table 1 Sample Description and Code for CEC/RSS1 Blends

Mixing Method	Description	Sample Code	Ratio of CEC/RSS1	Black loading in CEC	Black loading in RSS1	Oil loaded to
Dry	natural rubber (RSS1) was mixed with ingredients	Dry	/	/	50 phr	dry
CEC	blend CEC masterbatch, in which all carbon black was loaded, with maslilated RSS1 and oil.	CEC-1	100/0	50 phr	/	CEC
		CEC-2	90/10	55.5 phr	0 phr	blend
		CEC-3	80/20	62.5 phr	0 phr	blend
		CEC-4	70/30	71.4 phr	0 phr	blend

Table 2 Compound Characteristics of CEC/RSS1 Blends

Sample Code	Mooney Viscosity ML(1+4)@100°C	Sol Molecular Weight K	Bound Rubber %
<i>Dry</i>	61	304	38
CEC-1	63	378	41
CEC-2	61	362	40
CEC-3	61	363	40
CEC-4	60	377	45

Table 3. Physical Properties of CEC/RSS1 Blends

Sample Code	Hardness	E100 MPa	E300 MPa	Tensile MPa	Elongation %	Rebound 60°C, %	Rebound 0°C, %	Rebound r.t., %
Dry	69	2.8	15	27	472	59	35	48
CEC-1	69	2.7	16	30	533	62	36	50
CEC-2	68	3.0	17	30	483	63	39	52
CEC-3	63	2.8	17	30	497	64	38	53
CEC-4	65	2.8	16	31	506	65	38	54

Table 4 Fracture Properties and Dynamic Property of CEC/RSS1 Blends

Sample Code	Crack Growth Rate $\times 10^{-3}$, cm/million cycle	Tear Strength Die C, N/mm	Abrasion Rating	Max. Tan δ @ 60°C
Dry	4.83	122	80	0.178
CEC-1	3.43	91	120	0.179
CEC-2	4.31	94	110	0.174
CEC-3	3.85	97	108	0.174
CEC-4	4.11	106	98	0.188

Abrasion Rating = (weight loss of reference sample/weight loss of sample) $\times 100$
(reference sample was the sample no. 2-1 in CEC in NR/BR blends application)

In view of the foregoing disclosure, it will be apparent to those skilled in the art that various additions, modifications, etc. can be made without departing from the true scope and spirit of the invention. All such additions and modifications are intended to be covered by the following claims.

27 MAR 2002

We claim:

1. A method for producing elastomer composite blend comprising elastomer, particulate filler and optionally other ingredients, characterized by:

5 feeding a continuous flow of first fluid comprising elastomer latex to a mixing zone of a coagulum reactor;

feeding a continuous flow of second fluid comprising particulate filler under pressure to the mixing zone of the coagulum reactor to form a mixture with the elastomer latex, the particulate filler being effective to coagulate the elastomer latex and the mixing
10 of the first fluid and the second fluid within the mixing zone being sufficiently energetic to substantially completely coagulate the elastomer latex with the particulate filler in the coagulum reactor;

discharging a substantially continuous flow of elastomer composite from the coagulum reactor; and

15 dry mixing the elastomer composite with additional elastomer to form elastomer composite blend.

2. The method of producing elastomer composite blend in accordance with claim 1 further characterized in that:

20 the elastomer latex and the additional elastomer each is independently selected from natural rubber, chlorinated natural rubber, homopolymer, copolymer terpolymers of 1,3-butadiene, styrene, isoprene, isobutylene, 2,3-dimethyl-1,3-butadiene, acrylonitrile, ethylene, and propylene, the oil extended derivatives of any of them, and mixtures of any of them; and

25 the particulate filler is selected from carbon black, fumed silica, precipitated silica, coated carbon blacks, chemically functionalized carbon blacks, silicon-treated carbon black, and mixtures of any of them.

3. The method of producing elastomer composite blend in accordance with claims 1 or 2 further characterized in that additional particulate filler is added during the dry mixing of the elastomer composite with additional elastomer.
- 5 4. The method of producing elastomer composite blend in accordance with claim 3 further characterized in that the additional particulate filler is mixed with the additional elastomer prior to the dry mixing of the elastomer composite with additional elastomer.
- 10 5. The method of producing elastomer composite blend in accordance with any of claim 1 to 4, further characterized by feeding additive to the mixing zone of the coagulum reactor, selected from antiozonants, antioxidants, plasticizers, processing aids, resins, flame retardants, extender oils, lubricants, and mixtures of any of them.
- 15 6. The method of producing elastomer composite blend in accordance with any of claims 1 to 5 further characterized in that:
the elastomer latex and the additional elastomer is each independently selected from natural rubber latex, SBR rubber latex and butadiene rubber latex;
the additional elastomer is present in an amount equal to 50% to 90% by weight of total elastomer in the elastomer composite blend; and
20 the elastomer composite blend has 30 to 85 phr carbon black.
- 25 7. The method of producing elastomer composite blend in accordance with any of claims 1 to 5, further characterized in that the coagulum reactor defines an elongate coagulum zone extending with progressively increasing cross-sectional area from the mixing zone to a discharge end.
8. Elastomer composite blend comprising particulate filler finely dispersed in elastomer, characterized in that the elastomer composite blend is formed by a method

27 MAR 2002

comprising the steps of:

feeding a continuous flow of first fluid comprising elastomer latex to a mixing zone of a coagulum reactor;

5 feeding a continuous flow of second fluid comprising particulate filler under pressure to the mixing zone of the coagulum reactor to form a mixture with the elastomer latex, the mixing of the first fluid and the second fluid within the mixing zone being sufficiently energetic to substantially completely coagulate the elastomer latex in the coagulum reactor;

10 discharging a substantially continuous flow of elastomer composite from the coagulum reactor; and

dry mixing the elastomer composite with additional elastomer to form elastomer composite blend.

9. The elastomer composite blend of claim 8 further characterized by macro-
15 dispersion D(%) of the particulate filler being less than 0.2% undispersed area in a first elastomer phase of the elastomer composite blend, said first elastomer phase comprising essentially only elastomer from the elastomer latex.

10. Vulcanizate comprising elastomer composite in accordance with claim 8 or 9,
20 characterized by having a crack growth rate no more than 1.20 cm/million cycles, measured in accordance with ASTM D3629-94.

11. An elastomer composite blend comprising at least 30 phr particulate filler
25 dispersed in a multi-phase elastomer, the particulate filler being selected from carbon black, silicon coated carbon black, silicon treated carbon black, fumed silica, precipitated silica or a mixture of any of them, and each phase of the multi-phase elastomer being independently selected from natural rubber, a chlorinated derivative of natural rubber, homopolymer, copolymer or terpolymer of butadiene, styrene, isoprene, isobutylene, 3.3-

27 MAR 2002

dialkyl-1,3-butadiene where the alkyl group is C1 to C3 alkyl, acrylonitrile, ethylene and propylene, an oil extend derivative of any of them and a mixture of any of them wherein macro-dispersion D(%) of the particulate filler in the elastomer composite blend is less than 0.2% undispersed area.

12. A method of producing elastomer composite blend, comprising:

feeding a continuous flow of first fluid comprising elastomer latex to a mixing zone of a coagulum reactor;

feeding a continuous flow of second fluid comprising particulate filler under pressure to the mixing zone of the coagulum reactor to form a mixture with the elastomer latex, the particulate filler being effective to coagulate the elastomer latex and the feeding of the second fluid against the first fluid within the mixing zone being sufficiently energetic to substantially completely coagulate the elastomer latex with the particulate filler in the coagulum reactor;

discharging a substantially continuous flow of elastomer composite from the coagulum reactor; and

dry mixing the elastomer composite with additional elastomer to form elastomer composite blend.

13. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex comprises elastomer selected from natural rubber, chlorinated natural rubber, homopolymer, copolymer terpolymers of 1,3-butadiene, styrene, isoprene, isobutylene, 2,3-dimethyl-1,3-butadiene, acrylonitrile, ethylene, and propylene, the oil extended derivatives of any of them, and mixtures of any of them.

14. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex comprises elastomer selected from natural rubber, BR, SBR, and mixtures of any of them.

15. The method of producing elastomer composite blend in accordance with claim 1 wherein the additional latex is natural rubber, chlorinated natural rubber, homopolymer,

copolymer or terpolymer of 1,3-butadiene, styrene, isoprene, isobutylene, 2,3-dimethyl-1,3-butadiene, acrylonitrile, ethylene, and propylene, the oil extended derivative of any of them, or a mixture of any of them.

16. The method of producing elastomer composite blend in accordance with claim 1 wherein the additional latex is natural rubber, BR, SBR or a mixture of any of them.

17. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex comprises a first elastomer, and the additional elastomer is the same as the first elastomer.

18. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer, latex comprises a first elastomer, and the additional elastomer comprises a second elastomer different from the first elastomer.

19. The method of producing elastomer composite blend in accordance with claim 1 wherein the particulate filler is selected from carbon black, fumed silica, precipitated silica, coated carbon blacks, chemically functionalized carbon blacks, silicon-treated carbon black, and mixtures of any of them.

20. The method of producing elastomer composite blend in accordance with claim 1 wherein the particulate filler is carbon black.

21. A method of producing elastomer composite blend, comprising:

feeding a continuous flow of first fluid comprising elastomer latex to a mixing zone of a coagulum reactor;

feeding a continuous flow of second fluid comprising silica particulate filler under pressure to the mixing zone of the coagulum reactor to form a mixture with the elastomer latex, the particulate filler being effective to coagulate the elastomer latex and the mixing of the first fluid and the second fluid within the

mixing zone being sufficiently energetic to substantially completely coagulate the elastomer latex with the particulate filler in the coagulum reactor;

discharging a substantially continuous flow of elastomer composite from the coagulum reactor; and

dry mixing the elastomer composite with additional elastomer to form elastomer composite blend.

22. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer composite blend has 30 to 85 phr of the particulate filler.

23. The method of producing elastomer composite blend in accordance with claim 1 wherein additional particulate filler is added during the dry mixing of the elastomer composite with additional elastomer.

24. The method of producing elastomer composite blend in accordance with claim 12 wherein the additional particulate filler is the same as the particulate filler of the second fluid.

25. The method of producing elastomer composite blend in accordance with claim 12 wherein the additional particulate filler is carbon black, fumed silica, precipitated silica, coated carbon blacks, chemically functionalized carbon blacks, silicon-treated carbon black, and any mixture of them.

26. The method of producing elastomer composite blend in accordance with claim 11 wherein the additional particulate filler is carbon black.

27. The method of producing elastomer composite blend in accordance with claim 11 wherein the additional particulate filler is silica.

28. The method of producing elastomer composite blend in accordance with claim 12 wherein the particulate filler the elastomer composite blend has the particulate filler of 30 to 85 phr.

29. A method of producing elastomer composite blend, comprising:

feeding a continuous flow of first fluid comprising elastomer latex to a mixing zone of a coagulum reactor;

feeding a continuous flow of second fluid comprising particulate filler under pressure to the mixing zone of the coagulum reactor to form a mixture with the elastomer latex, the particulate filler being effective to coagulate the elastomer latex and the mixing of the first fluid and the second fluid within the mixing zone being sufficiently energetic to substantially completely coagulate the elastomer latex with the particulate filler in the coagulum reactor;

feeding additive to the mixing zone of the coagulum reactor;

discharging a substantially continuous flow of elastomer composite from the coagulum reactor; and

dry mixing the elastomer composite with additional elastomer to form elastomer composite blend.

30. The method of producing elastomer composite blend in accordance with claim 18 wherein the additive is selected from antiozonants, antioxidants, plasticizers, processing aids, resins, flame retardants, extender oils, lubricants, and mixtures of any of them.

31. The method of producing elastomer composite blend in accordance with claim 1 further comprising adding additive during dry mixing of the elastomer composite with additional elastomer.

32. The method of producing elastomer composite blend in accordance with claim 20 wherein the additive is selected from antiozonants, antioxidants, plasticizers, processing aids, resins, flame retardants, extender oils, lubricants, and mixtures of any of them.

33. The method of producing elastomer composite blend in accordance with claim 1 wherein the weight ratio in the elastomer composite blend of elastomer in the elastomer composite blend from the elastomer latex to the additional elastomer is from 95:5 to 5:95.

34. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex is natural rubber latex and the additional elastomer is butadiene rubber, and butadiene rubber is from 10% to 50% by weight of total elastomer in the elastomer composite blend.

35. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex is natural rubber latex and the additional elastomer is SBR, and SBR is from 50% to 90% by weight of total elastomer in the elastomer composite blend.

36. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex is natural rubber latex and the additional elastomer is natural rubber.

37. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex is butadiene rubber latex and the additional elastomer is SBR, and SBR is from 10% to 90% by weight of total elastomer in the elastomer composite blend.

38. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex is butadiene rubber latex and the additional elastomer is butadiene rubber.

39. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex is butadiene rubber latex and the additional elastomer is natural rubber, and natural rubber is from 10% to 50% by weight of total elastomer in the elastomer composite blend.

40. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex is SBR latex and the additional elastomer is butadiene rubber, and butadiene rubber is from 10% to 90% by weight of total elastomer in the elastomer composite blend.

41. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex is latex SBR and the additional elastomer is SBR.

42. The method of producing elastomer composite blend in accordance with claim 1 wherein the elastomer latex is SBR and the additional elastomer is natural rubber, and natural rubber is from 50% to 90% by weight of total elastomer in the elastomer composite blend.

43. The method in accordance with any of claims 23 to 31 wherein the elastomer composite blend has 30 to 85 phr carbon black.

44. The method of producing elastomer composite blend in accordance with claim 1 wherein the coagulum reactor defines an elongate coagulum zone extending from the mixing zone to a discharge end.

45. Elastomer composite blend comprising particulate filler finely dispersed in elastomer, formed by a method comprising the steps of:

A) establishing a continuous, semi-confined flow of mixed elastomer latex and particulate filler under pressure in a coagulum reactor forming an elongate

coagulum zone extending with progressively increasing cross-sectional area from an entry end to a discharge end, by simultaneously

- (i) feeding elastomer latex fluid continuously to a mixing zone at the entry end of the coagulum reactor, and
- (ii) entraining the elastomer latex fluid into particulate filler fluid by feeding the particulate filler fluid as a continuous jet into the mixing zone;

B) discharging from the discharge end of the coagulum reactor a substantially constant flow of elastomer masterbatch globules concurrently with feeding of the fluid streams in accordance with steps A(i) and A(ii), wherein macro-dispersion (D %) of the particulate filler in the elastomer masterbatch is less than 0.2% undispersed area; and

C) dry mixing the elastomer composite with additional elastomer to form elastomer composite blend.

46. Elastomer composite blend formed by:

feeding a continuous flow of first fluid comprising elastomer latex to a mixing zone of a coagulum reactor;

feeding a continuous flow of second fluid comprising particulate filler under pressure to the mixing zone of the coagulum reactor to form a mixture with the elastomer latex, the particulate filler being effective to coagulate the elastomer latex, the particulate filler being effective to coagulate the elastomer latex and the mixing of the first fluid and the second fluid within the mixing zone being sufficiently energetic to substantially completely coagulate the elastomer latex with the particulate filler in the coagulum reactor;

discharging a substantially continuous flow of elastomer composite from the coagulum reactor wherein macro-dispersion (D %) of the particulate filler in the elastomer composite is less than 0.2% undispersed area; and

dry mixing the elastomer composite with additional elastomer to form elastomer composite blend.

47. The elastomer composite blend of claim 34 or 35 wherein macro-dispersion D(%) of the particulate filler in a first elastomer phase of the elastomer composite blend comprising essentially elastomer from the elastomer latex is less than 0.2% undispersed area.

48. The elastomer composite blend of claim 34 or 35 wherein macro-dispersion D(%) of the particulate filler throughout the elastomer composite blend is less than 0.2% undispersed area.

49. The elastomer composite blend of claim 35 wherein the particulate filler is carbon black, silicon coated carbon black, silicon treated carbon black, fumed silica, precipitated silica or a mixture of any of them.

50. The elastomer composite blend of claim 35 wherein the elastomer of the elastomer latex is selected from natural rubber, a chlorinated derivative of natural rubber, a homopolymer, copolymer or terpolymer of butadiene, styrene, isoprene, isobutylene, 3,3-dimethyl-1,3-butadiene, acrylonitrile, ethylene propylene, an oil extended derivative of any of them and a mixture of any of them.

51. An elastomer composite blend comprising at least 30 phr particulate filler dispersed in a multi-phase elastomer, the particulate filler being selected from carbon black, silicon coated carbon black, silicon treated carbon black, fumed silica, precipitated silica or a mixture of any of them, and each phase of the multiphase elastomer being independently selected from natural rubber, a chlorinated derivative of natural rubber, homopolymer, copolymer or terpolymer of butadiene, styrene, isoprene, isobutylene, 3,3-dialkyl-1,3-butadiene where the alkyl group is C1 to C3 alkyl, acrylonitrile, ethylene and propylene, an oil extended derivative of any of them and a mixture of any of them wherein macro-

dispersion D(%) of the particulate filler in the elastomer composite blend is less than 0.2% undispersed area.

52. Vulcanizate comprising the vulcanization product of elastomer composite blend in accordance with any of claims 34, 35 or 40.

53. Tire tread comprising vulcanizate in accordance with claim 41.

54. Tire sub-tread comprising vulcanizate in accordance with claim 41.

55. Wire-skim for a tire comprising vulcanizate in accordance with claim 41.

56. Tire sidewall comprising vulcanizate in accordance with claim 41.

57. Cushion gum for a re-tread tire, comprising vulcanizate in accordance with claim 41.

58. A rubber component of an engine mount, comprising vulcanizate in accordance with claim 41.

59. Tank track comprising vulcanizate in accordance with claim 41.

60. Mining belt, comprising vulcanizate in accordance with claim 41.

61. A rubber component of a hydro-mount comprising vulcanizate in accordance with claim 41.

62. A bridge bearing comprising vulcanizate in accordance with claim 41.

63. A seismic isolator comprising vulcanizate in accordance with claim 41.

64. Vulcanizate in accordance with any of claims 41 having a crack growth rate no more than 1.20 cm/million cycles, measured in accordance with ASTM D3629-94.

65. A method of producing elastomer composite blend, comprising:
feeding a continuous flow of first fluid comprising elastomer latex to a mixing zone;
feeding a continuous flow of second fluid comprising particulate filler under pressure to the mixing zone to form a mixture with the elastomer latex, the feeding of the second fluid against the first fluid within the mixing zone being sufficiently energetic to substantially completely coagulate the elastomer latex with the particulate filler;
discharging a substantially continuous flow of elastomer composite from the coagulum reactor; and
dry mixing the elastomer composite with additional elastomer to form elastomer composite blend.

66. The method of producing elastomer composite blend in accordance with claim 54, wherein the additional latex is dry mixed with the elastomer composite to form elastomer composite blend.

67. The method of producing elastomer composite blend in accordance with claim 54, wherein the second fluid is an aqueous fluid having 10 to 30 wt% carbon black.