

Field of the Invention

The present invention relates to a polyoxytetramethylene glycol (hereinafter, simply referred to as "PTMG") and a method for producing the same. More particularly, the present invention is concerned with a PTMG having not only a limited content of from 2 to 5 % by weight with respect to high molecular weight PTMG molecules, wherein the high molecular weight PTMG molecules are defined as PTMG molecules having molecular weights which are at least six times as large as the number average molecular weight of all PTMG molecules, but also a very limited heteropolyacid content of from 10 to 900 ppb by weight. The present invention is also concerned with a method for producing such PTMG. The PTMG of the present invention exhibits improved properties with respect to heat resistance and low viscosity. By virtue of these improved properties, the PTMG of the present invention can be advantageously used as a raw material for a polyester elastic fiber, a polyurethane elastic fiber and the like.



As described in Japanese Patent No. 2,525,155, in general, polyether type polymers, such as PTMG, are likely to suffer deterioration by oxidation, UV rays and heat. Thus, although PTMG exhibits excellent properties as raw materials for resins and lubricants, deterioration of such a polymer has been a problem. For example, a part of PTMG is decomposed by heat applied to the polymerization reaction or by heat generated during the polymerization reaction, and the resultant polymer product suffers discoloration and lowering of the elastic properties (such as strength and elongation), which are caused by the heat decomposition (heat deterioration) of a part of the PTMG. Therefore, there is a demand for a PTMG having excellent heat resistance.

Various stabilizers for PTMG are known in the art, but most of the stabilizers are antioxidants. In addition, it is noted that conventional stabilizers for preventing heat deterioration are unsatisfactory. Specifically, an aromatic stabilizer (Japanese Patent No. 2,525,155) is frequently used for preventing heat dete-



5 tively high, heating of the polymerization system is
necessary for producing PTMG by an economically and
commercially advantageous polymerization method which
employs no solvent or only a small amount of solvent.
When a PTMG is produced in the absence of a solvent,
10 heat deterioration of produced PTMG becomes a problem.
Accordingly, there is a demand for PTMG having both the
improved properties with respect to both heat resis-
tance and low viscosity.

 Further, the addition of the above-mentioned sta-
15 bilizer has a danger of causing discoloration and low-
ering of the elastic properties (such as strength and
elongation) of the polymer product. Therefore, there
has been a strong demand for a method of producing PTMG
having improved heat resistance, wherein the amount of
20 additives, such as a stabilizer, is suppressed to a
level as low as possible.

 Further, PTMG having high viscosity has the fol-
lowing problems. When PTMG is used in a polymerization
thereof with other compounds in the absence of a sol-
25 vent, it becomes necessary to employ high polymeriza-



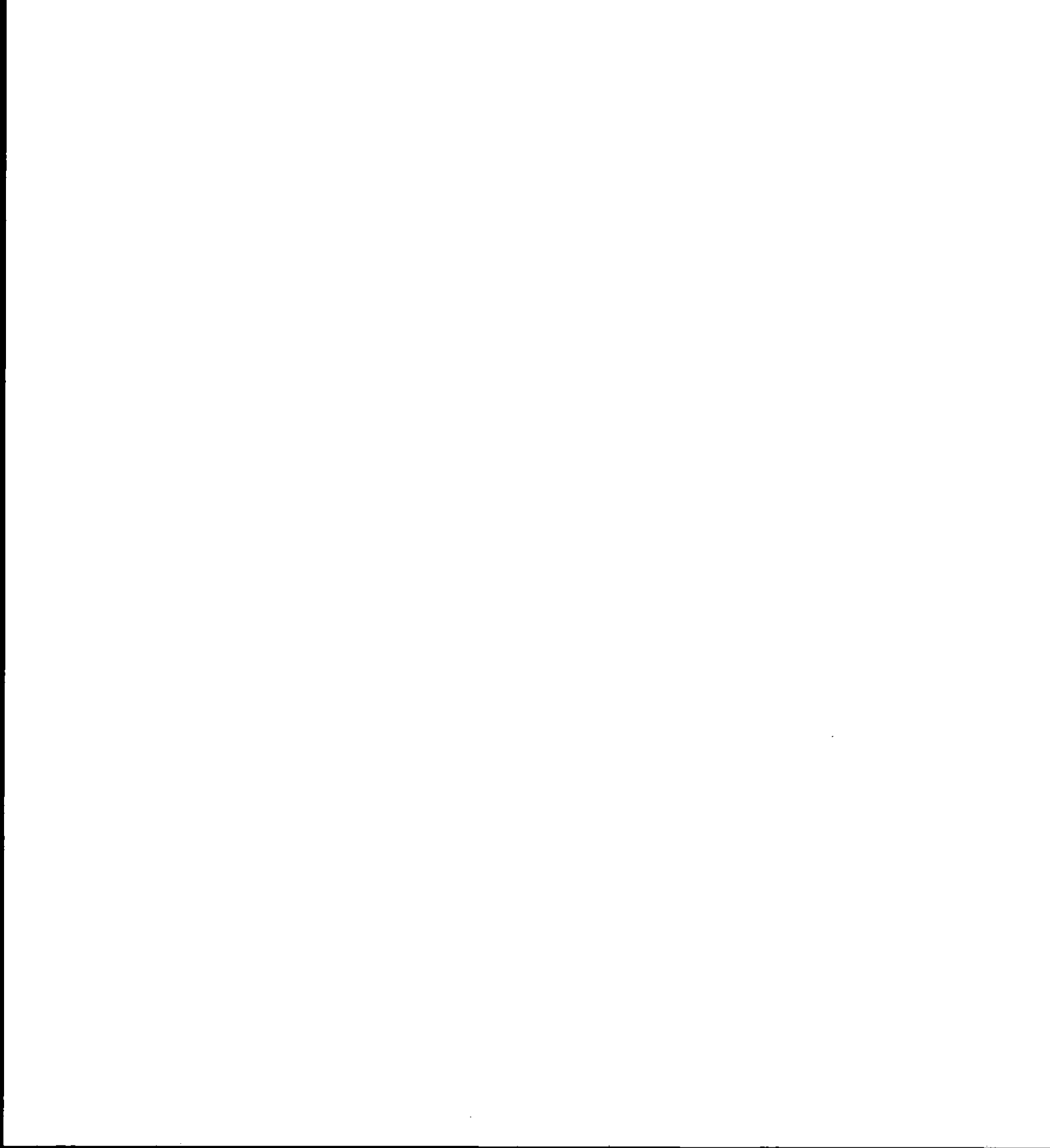
SUMMARY OF THE INVENTION

In this situation, the present inventors have made extensive and intensive studies with a view toward developing a PTMG having improved properties with respect to both heat resistance and low viscosity. As a result, it has unexpectedly been found that, when the PTMG has not only a molecular weight distribution as narrow as 1.8 or less so that the viscosity of the PTMG becomes low, but also a content of high molecular weight PTMG molecules within a specific range (2 to 5 % by weight), wherein the high molecular weight PTMG molecules are defined as being PTMG molecules having molecular weights which are at least six times as large as the number average molecular weight of all PTMG molecules, the crystalline, high molecular weight PTMG molecules contained in the PTMG do not suffer phase separation but interact with the low molecular weight PTMG molecules which are likely to suffer heat decomposition, thereby suppressing the heat decomposition of the PTMG. Such a PTMG, notwithstanding a low viscosity thereof,



5 within a specific range, a plurality of acid groups of
the heteropolyacid molecule interact with hydroxyl
groups of a plurality of PTMG molecules to thereby form
crosslinking sites, so that the heat resistance of the
PTMG is further improved without suffering promotion of
10 depolymerization of the PTMG.

 In addition, it has unexpectedly been found that
the above-mentioned PTMG having excellent properties
with respect to both heat resistance and low viscosity
can be effectively and efficiently obtained by a method
15 which comprises subjecting tetrahydrofuran (THF) to a
polymerization reaction in a continuous polymerization
reactor with a stirrer in the presence of a heteropoly-
acid catalyst, in which the polymerization reaction is
performed in the presence of water in an amount suffi-
20 cient to form a tetrahydrofuran organic phase and an
aqueous tetrahydrofuran/catalyst phase having a speci-
fic gravity of from 1.8 to 2.3, while maintaining the
retention time of tetrahydrofuran in the reactor within
a specific range (at 0.5 to 20 hours) and while main-
25 taining the motive power applied to the liquid in the



5 erage molecular weight of from 500 to 3,000 and a reaction-formed aqueous tetrahydrofuran/catalyst phase, separating the reaction-formed tetrahydrofuran organic phase containing the polyoxytetramethylene glycol from the polymerization reaction mixture, and adjusting the
10 heteropolyacid content of the polyoxytetramethylene glycol to a level of 10 to 900 ppb by weight.

 The present invention has been completed based on the above-mentioned findings.

 Accordingly, it is an object of the present invention to provide a polyoxytetramethylene glycol (PTMG)
15 having improved properties with respect to both heat resistance and low viscosity.

 It is another object of the present invention to provide a method for effectively and efficiently producing the above-mentioned PTMG having improved properties with respect to both heat resistance and low viscosity.
20

 The foregoing and other objects, features and advantages of the present invention will be apparent to
25 those skilled in the art from the following detailed



5 In the drawings:

Fig. 1 is a schematic diagram showing the production system used for the PTMG of the present invention; and

10 Fig. 2 is a chromatogram of the PTMG produced in Example 6 which shows the molecular weight distribution of the PTMG, wherein the abscissa shows the logarithm (log) of the molecular weight, the ordinate shows the weight % of component PTMG molecule, based on the total weight of all PTMG molecules, the intersection of the
15 vertical straight broken line and the abscissa shows the logarithm of the number average molecular weight, and the area of the hatched portion shows the amount of the PTMG molecules having molecular weights which are at least six times as large as the number average molecular weight of all PTMG molecules.
20

Description of Reference Numerals

- 1: stirrer
- 2: reactor
- 3: water feeding tank
- 25 4: first, phase-separation vessel

- 5 9: third, phase-separation vessel
10: vacuum distillation vessel

DETAILED DESCRIPTION OF THE INVENTION

In one aspect of the present invention, there is
10 provided a polyoxytetramethylene glycol (PTMG) having
the following characteristics:

(1) a number average molecular weight of from 500
to 3000;

(2) a molecular weight distribution of 1.8 or less
15 in terms of the Mw/Mn ratio, wherein Mw represents the
weight average molecular weight of PTMG and Mn repre-
sents the number average molecular weight of PTMG;

(3) a content of high molecular weight PTMG mo-
lecules of from 2 to 5 % by weight, based on the total
20 weight of all PTMG molecules, wherein the high molecu-
lar weight PTMG molecules are defined as PTMG molecules
having molecular weights which are at least six times
as large as the number average molecular weight of all
PTMG molecules; and

25 (4) a heteropolyacid content of from 10 to 900 ppb



polyoxytetramethylene glycol (PME), which comprises

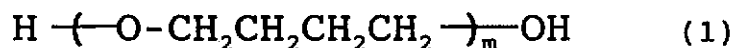
5 subjecting tetrahydrofuran to a polymerization reaction
in a continuous polymerization reactor with a stirrer
in the presence of a heteropolyacid catalyst, while
feeding tetrahydrofuran to the continuous polymeriza-
tion reactor,

10 the polymerization reaction being continuously
performed in the presence of water, wherein the water
is present in an amount sufficient to form a tetra-
hydrofuran organic phase and an aqueous tetrahydro-
furan/catalyst phase which comprises a solution of the
15 heteropolyacid catalyst in a tetrahydrofuran/water mix-
ture and which has a specific gravity of from 1.8 to
2.3,
while maintaining a V/F value at 0.5 to 20 hours where-
in V represents the volume (m^3) of the liquid in the
20 reactor and F represents the rate (m^3 /hour) of feeding
tetrahydrofuran to the reactor so that the V/F value
represents the retention time (hour or hours) of tetra-
hydrofuran in the reactor and while maintaining a P/V
value at 1.3 kW or more wherein P represents the motive
25 power (kW) applied to the liquid in the reactor and V

5 comprising a reaction-formed tetrahydrofuran organic
phase containing a polyoxytetramethylene glycol having
a number average molecular weight of from 500 to 3,000
and a reaction-formed aqueous tetrahydrofuran/catalyst
phase,
10 separating the reaction-formed tetrahydrofuran or-
ganic phase containing the polyoxytetramethylene glycol
from the polymerization reaction mixture, and
adjusting the heteropolyacid content of the poly-
oxytetramethylene glycol to a level of 10 to 900 ppb by
15 weight.

Hereinbelow, the present invention will be de-
scribed in more detail.

The polyoxytetramethylene glycol (PTMG) of the
20 present invention is a mixture of polymer chains each
independently represented by the following formula (1):



wherein, m is independently an integer of
from 2 to 4000, preferably from 2 to 2100.

PTMG of the present invention is within the range of from 500 to 3000. A preferred range of Mn is 650 to 3000. The improvement in the heat resistance becomes most significant when Mn is within the range of from 700 to 2300, preferably from 800 to 2200.

The molecular weight distribution (Mw/Mn ratio) (Mw is a weight average molecular weight) of the PTMG of the present invention is 1.8 or less, preferably 1.7 or less, and more preferably 1.66 or less. A PTMG having an excellent low viscosity characteristic is obtained when the Mw/Mn ratio is 1.8 or less.

The above-mentioned Mn and Mw values are determined by gel permeation chromatography (GPC). The conditions (apparatus, types of columns, temperature, type and flow rate of carrier (eluent), molecular weight standards and the like) for the GPC analysis are shown below.

Apparatus: Shodex GPC system-11 (manufactured and sold by Showa Denko K. K., Japan);

Columns: Shodex OH pak SB806M (two columns) and



Detector: Differential Refractometer;

5 Temperature: 60 °C;

Carrier: 0.02 mol/liter solution of LiBr in
dimethylacetamide;

Flow rate of the carrier: 1.0 ml/min;

Sample: 100 µl of 0.8% PTMG solution in the
10 carrier; and

Molecular weight standards: PTMG, $M_n = 547,000$

($M_w/M_n = 1.35$), $M_n = 283,000$ ($M_w/M_n = 1.08$), $M_n =$

99,000 ($M_w/M_n = 1.08$), $M_n = 67,000$ ($M_w/M_n = 1.04$),

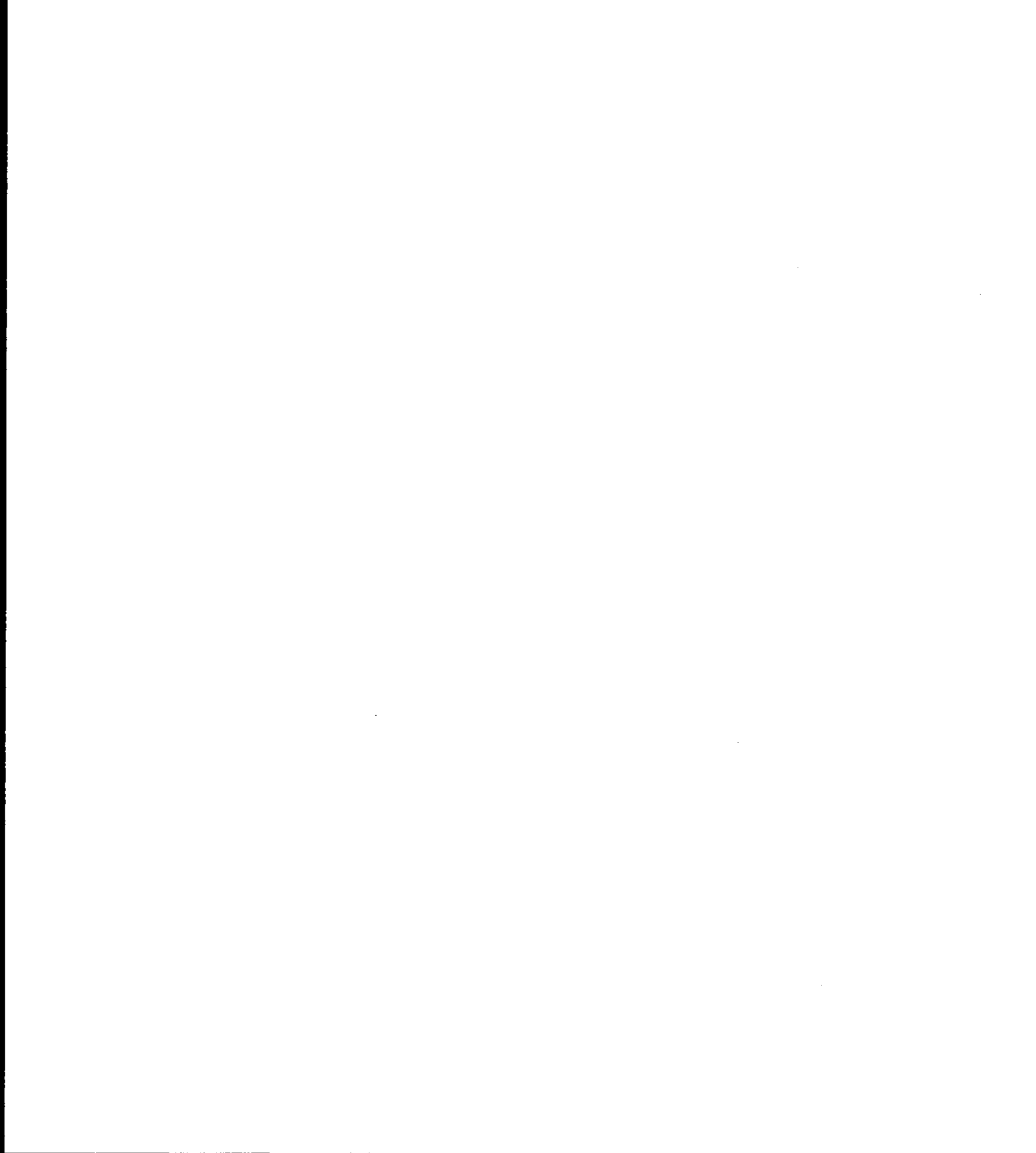
$M_n = 35,500$ ($M_w/M_n = 1.06$), $M_n = 15,000$ ($M_w/M_n =$

15 1.09), $M_n = 6,700$ ($M_w/M_n = 1.13$), $M_n = 2,170$ (M_w/M_n

$= 1.12$), $M_n = 1,300$ ($M_w/M_n = 1.12$), $M_n = 650$ (M_w/M_n

$= 1.18$), and THF monomer.

In the present invention, for improving the heat
resistance of PTMG, it is necessary that the content of
20 high molecular weight PTMG molecules (namely, PTMG mo-
lecules having molecular weights which are at least six
times as large as the number average molecular weight
of all PTMG molecules) be within the range of from 2 to
5 % by weight, based on the total weight of all PTMG
25 molecules. It is more preferred that the content of



5 sidered to have low heat resistance, and the high molecular weight PTMG molecules defined in the present invention suppress heat decomposition of PTMG through an interaction thereof with the low molecular weight PTMG molecules which are likely to suffer heat decomposition. However, when the content of the high molecular weight PTMG molecules is more than 5 % by weight, the PTMG is likely to separate into two phases, namely a solid phase consisting essentially of high molecular weight PTMG molecules and a liquid phase consisting essentially of low molecular weight PTMG molecules. Thus, the high molecular weight PTMG molecules are not uniformly dispersed in the PTMG. In such a PTMG, the improvement in the heat resistance is not large. On the other hand, when the content of the high molecular weight PTMG molecules is less than 2 % by weight, the high molecular weight PTMG molecules tend to be uniformly dispersed in the PTMG; however, the improvement in the heat resistance becomes small because only a small amount of high molecular weight PTMG molecules is contained in the PTMG.



5 have molecular weights of at least six times as large as the Mn are given as follows.

(1) Mn is represented by the following formula:

$$M_n = \sum (N_i M_i) / \sum N_i .$$

10 In the above formula, N_i represents the number of molecules i , and M_i represents the molecular weight of molecule i .

(2) The weight average molecular weight (M_w) which is used in the formula M_n/M_w is represented by the following formula:

15
$$M_w = \sum (N_i M_i^2) / \sum (N_i M_i) .$$

In the above formula, N_i and M_i are as defined above. M_n in the formula M_n/M_w is defined in item (1) above.

(3) The content of PTMG molecules having molecular weights which are at least six times as large as the number average molecular weight (high molecular weight PTMG molecules), based on the total weight of all PTMG molecules, is determined from the area of a chromatogram obtained by GPC (see Fig. 2).

20

In the present invention, a heteropolyacid is an acid obtained by the condensation of an oxide of at

25



5 boron (B), titanium (Ti), cerium (Ce), cobalt (Co) and
niobium (Nb). The atomic ratio of the metal species
(any one or more of metals selected from the group con-
sisting of Mo, W and V) contained in the heteropolyacid
to other elements in the heteropolyacid is 2.5 to 12.

10 The heteropolyacid contained in the PTMG may be in
the form of a salt. Specific examples of heteropoly-
acids include phosphomolybdic acid, phosphotungstic
acid, phosphomolybdotungstic acid, phosphomolybdo-
vanadic acid, phosphomolybdotungstovanadic acid,
15 phosphotungstovanadic acid, phosphomolybdoniobic acid,
silicotungstic acid, silicomolybdic acid, silicomoly-
bdotungstic acid, silicomolybdotungstovanadic acid,
germanotungstic acid, borotungstic acid, boromolybdic
acid, boromolybdotungstic acid, boromolybdovanadic acid,
20 boromolybdotungstovanadic acid, cobaltmolybdic acid,
cobalttungstic acid, arsenomolybdic acid, arsenotung-
stic acid, titanomolybdic acid and ceromolybdic acid,
and metal salts thereof. A preferred heteropolyacid is
an oxyacid obtained by the condensation of an oxide of
25 at least one metal species selected from the group con-



5 sten and vanadium in the heteropolyacid, relative to
the weight of the PTMG. When the amount of heteropoly-
acid contained in the PTMG is 10 to 900 ppb, the heat
resistance of the PTMG is improved. It is preferred
that the heteropolyacid content is 30 to 800 ppb by
10 weight, more preferably 50 to 600 ppb by weight.

It is considered that individual heteropolyacid
molecules influence the hydroxyl terminal of the PTMG
molecule which has high mobility. In general, the hy-
droxyl terminals of a low molecular weight PTMG molecu-
15 le have high mobility, and such hydroxyl terminals are
considered to be likely to suffer heat decomposition.
Since a heteropolyacid is a polyvalent acid, a plural-
ity of acid groups in one heteropolyacid molecule in-
teract with the hydroxyl groups in a plurality of PTMG
20 molecules to form crosslinking sites. As a result, a
PTMG-heteropolyacid complex having a low mobility is
composed and the heat resistance of the PTMG is im-
proved.

When the heteropolyacid content of a PTMG is more
25 than 900 ppb, not only does an occurrence of discolora-



the PTMG. On the other hand, when the heteropolyacid
5 content of a PTMG is less than 10 ppb, almost no PTMG
-heteropolyacid complex is formed and, thus, the
heteropolyacid is incapable of improving the heat re-
sistance.

The contents of molybdenum, tungsten and vanadium
10 in the PTMG are determined mainly by ICP-Mass spectrometry.

The PTMG of the present invention which has high
heat resistance and low viscosity may contain compo-
nents other than PTMG as long as the components cause
15 no adverse effects on the ultimate products, such as an
elastic fiber. Examples of other components include
tetrahydrofuran (hereinafter, frequently referred to as
"THF") used as a raw material, a cyclic PTMG by-
produced during the polymerization reaction, and satu-
20 rated hydrocarbons having 5 to 10 carbon atoms and ac-
tivated carbons, both of which are used in the below
-mentioned operations for adjusting the heteropolyacid
content of a PTMG. When for example, less than 1 % by
weight of THF, 3 % by weight or less of a cyclic PTMG,
25 1 % by weight or less of a saturated hydrocarbon having

5 on the properties of an ultimate elastic fiber. Especially, when a PTMG contains a cyclic PTMG in an amount of 0.003 to 0.03 % by weight, the viscosity of the PTMG is advantageously lowered without causing a lowering of the heat resistance.

10 The details about how an improvement in the heat resistance of a PTMG is achieved in the present invention is still unknown. However, it is considered to be as follows. In the PTMG of the present invention, the molecular weight distribution is 1.8 or less. By virtue of this, 2 to 5 % by weight of the high molecular weight PTMG molecules can be stably dispersed in the PTMG, so that the heat resistance of the PTMG as a whole is improved. In addition, the heteropolyacid contained in the PTMG is considered to cause strong interactions with the terminal hydroxyl groups of the PTMG to thereby suppress the motion of the PTMG molecules which motion is likely to be caused by the heat added to the PTMG, so that the heat resistance of the PTMG is improved.

25

5

properties with respect to both of high heat resistance
and low viscosity.

10

The method of the present invention comprises subjecting tetrahydrofuran to a polymerization reaction in a continuous polymerization reactor with a stirrer in the presence of a heteropolyacid catalyst, while feeding tetrahydrofuran to the continuous polymerization reactor,

15

the polymerization reaction being continuously performed in the presence of water, wherein the water is present in an amount sufficient to form a tetrahydrofuran organic phase and an aqueous tetrahydrofuran/catalyst phase which comprises a solution of the heteropolyacid catalyst in a tetrahydrofuran/water mixture and which has a specific gravity of from 1.8 to 2.3,

20

while maintaining a V/F value at 0.5 to 20 hours wherein V represents the volume (m^3) of the liquid in the reactor and F represents the rate (m^3 /hour) of feeding tetrahydrofuran to the reactor so that the V/F value represents a retention time (hour or hours) of tetrahydrofuran in the reactor and while maintaining a P/V

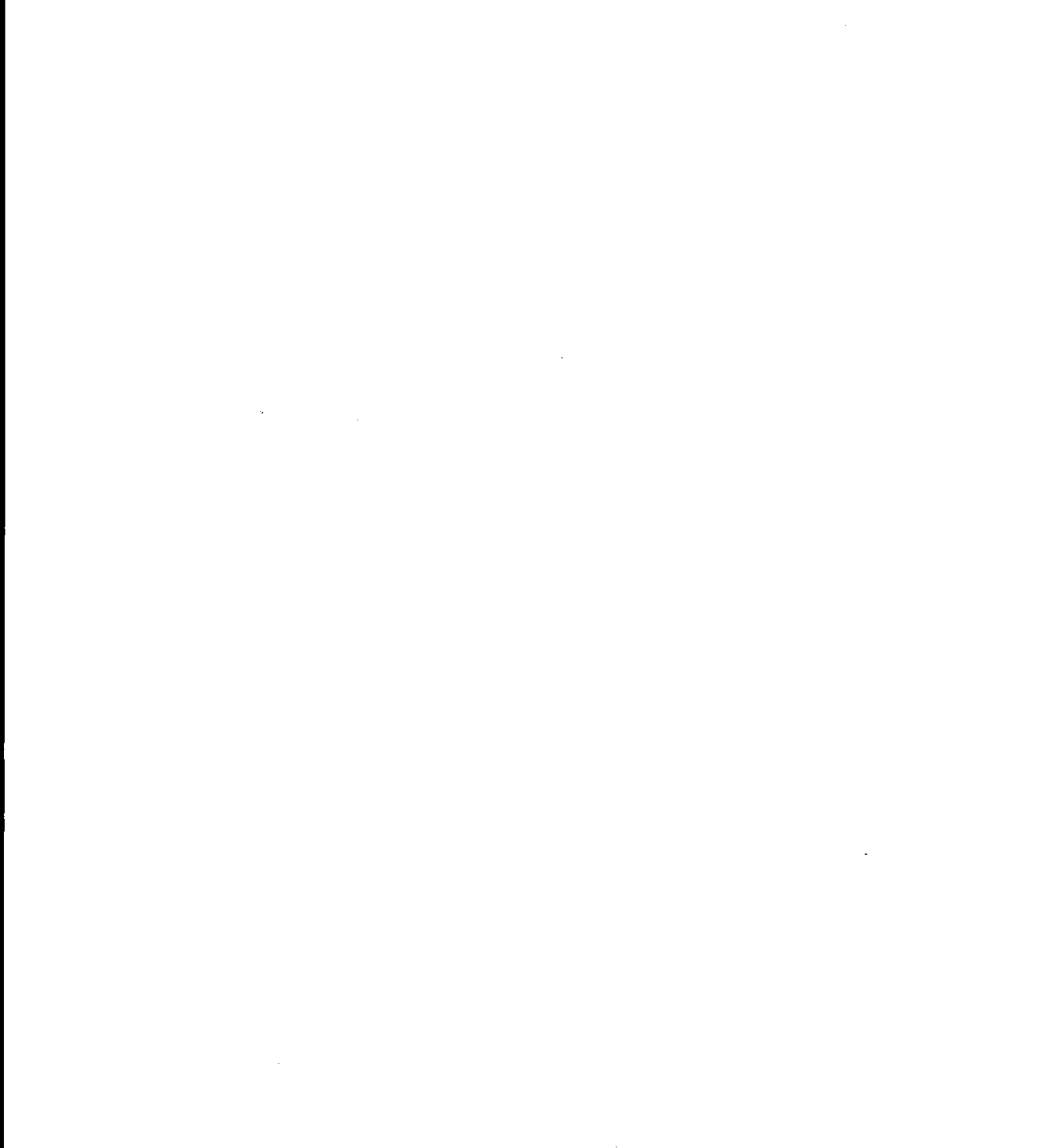
25

the motive power (KW/m²) applied to the liquid per unit
5 volume thereof,
to thereby obtain a polymerization reaction mixture
comprising a reaction-formed tetrahydrofuran organic
phase containing a polyoxytetramethylene glycol having
a number average molecular weight of from 500 to 3,000
10 and a reaction-formed aqueous tetrahydrofuran/catalyst
phase,

separating the reaction-formed tetrahydrofuran or-
ganic phase containing the polyoxytetramethylene glycol
from the polymerization reaction mixture, and

15 adjusting the heteropolyacid content of the poly-
oxytetramethylene glycol to a level of 10 to 900 ppb by
weight.

The reaction system used in the method of the pre-
sent invention comprises a tetrahydrofuran (THF) or-
20 ganic phase and an aqueous THF/catalyst phase which
comprises a solution of the heteropolyacid catalyst in
a THF/water mixture and which has a specific gravity of
from 1.8 to 2.3. A heteropolyacid is sparingly soluble
in an anhydrous THF, but well soluble in a mixed sol-
25 vent prepared by adding a small amount of water to THF.



5 that the specific gravity of the resultant heteropoly-
acid solution falls within the above-mentioned range.
When the thus prepared heteropolyacid solution is added
to THF, the resultant reaction system separates into
two phases, namely a THF organic phase and an aqueous
10 THF/catalyst phase (hereinafter, frequently referred to
as "aqueous THF/catalyst phase" or simply as "catalyst
phase"). The reason why such a reaction system is ob-
tained is not fully elucidated, but it is considered
that a small amount of water is coordinated to the
15 heteropolyacid.

 Hereinbelow, an explanation is made on the repre-
sentative example of a method for producing the PTMG of
the present invention.

 In general, PTMG is produced by a cationic poly-
20 merization of THF in the presence of an acid catalyst.
However, with the conventional polymerization method,
it is very difficult to produce a PTMG of the present
invention which has specific molecular weight distribu-
tion properties, that is, a PTMG having a molecular
25 weight distribution of 1.8 or less and having a limited

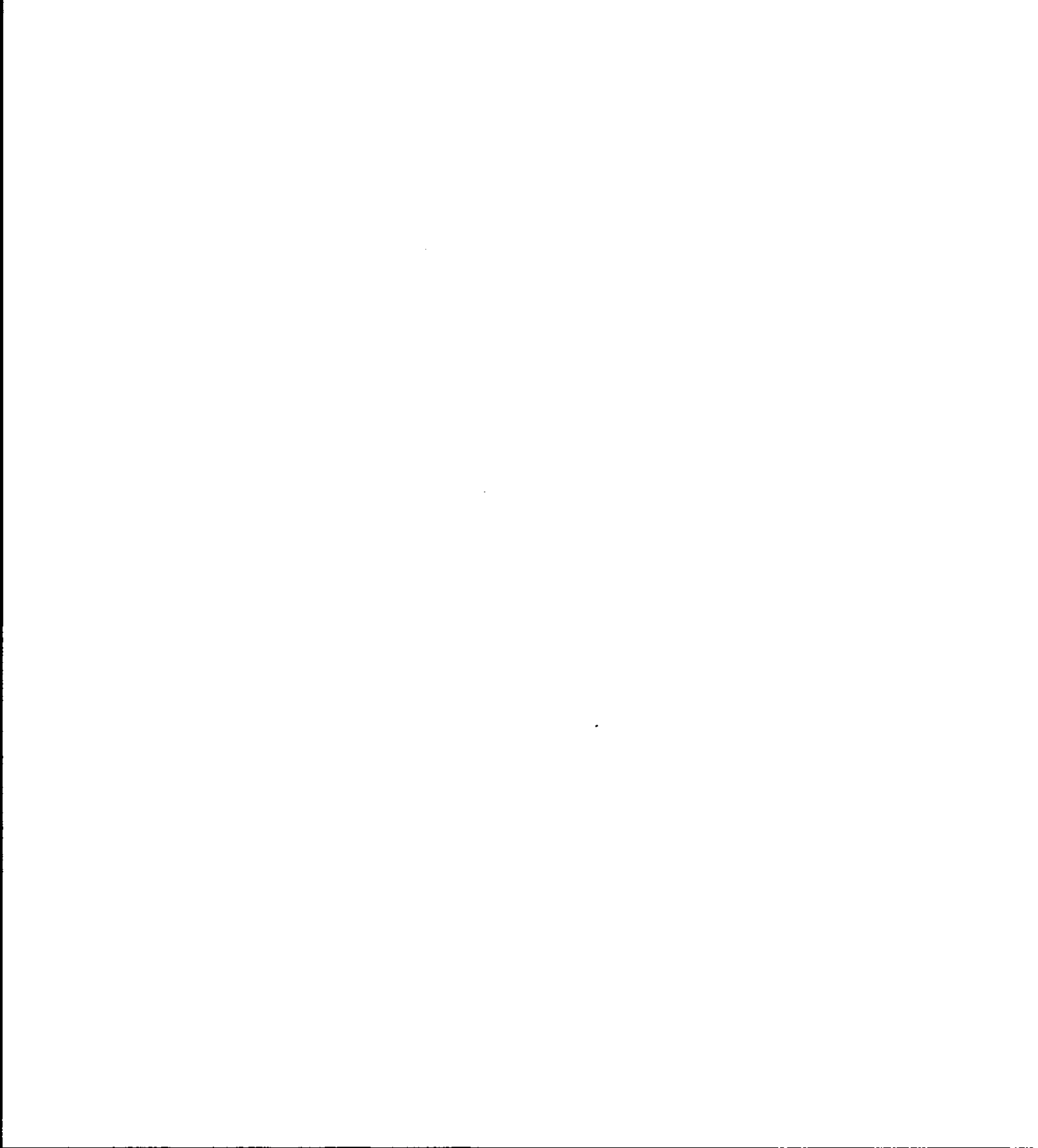


5 molecular weight of all PTMG molecules. Specifically,
the reaction conditions need to be controlled precisely
for producing such a PTMG.

10 Illustratively stated, in the method of the pre-
sent invention, use is made of a continuous polymeriza-
tion reactor with a stirrer, wherein THF can be fed
continuously to the reactor and the produced PTMG can
be withdrawn continuously from the reactor. The above-
mentioned heteropolyacid is used as a polymerization
catalyst, and the polymerization reaction is continu-
15 ously performed in the presence of water in an amount
sufficient to form a THF organic phase (THF phase) and
an aqueous THF/catalyst phase, while controlling the
retention time (V/F) of THF in the reactor {wherein V
represents the volume (m^3) of the liquid in the reactor
20 and F represents the rate (m^3/hour) of feeding THF to
the reactor} and while controlling the motive power
(P/V) applied to the liquid per unit volume thereof
{wherein P represents the motive power (kW) applied to
the liquid in the reactor and V represents the volume
25 (m^3) of the liquid in the reactor}. In addition, as

5 sily formed by measuring and adjusting the specific
gravity of the aqueous THF/catalyst phase to 1.8 to 2.3
so as to control the amount of water coordinated to the
heteropolyacid. The molecular weight distribution
properties of the obtained PTMG can be controlled by
10 controlling the specific gravity of the catalyst phase,
the retention time (V/F) of THF in the reactor and the
motive power (P/V) applied to the liquid per unit volu-
me of the reactor.

It should be noted that Unexamined Japanese Patent
15 Application Laid-Open Specification No. 63-30932 (cor-
responding to U.S. Patent No. 4,568,775) describes that
the amount of water coordinated to a heteropolyacid
catalyst influences the catalytic activity of the cata-
lyst, and that there is a correlation between the
20 amount of water coordinated to a heteropolyacid cata-
lyst and the number average molecular weight of a PTMG
obtained by polymerizing THF in the presence of the
heteropolyacid catalyst. However, although this patent
document describes that the molecular weight distribu-
25 tion of the obtained PTMG is narrow, it contains no de-



conditions for stably producing the PTMG of the present

5 invention which has a specific molecular weight distribution properties, the present inventors have found that the molecular weight distribution properties of a PTMG can be controlled precisely without changing the number average molecular weight thereof by controlling
10 the retention time of the monomer (THF) which reacts in the catalyst phase while feeding THF in a constant amount, relative to the volume of the aqueous THF/catalyst phase in the reactor, to the reactor. It is considered that the substantial time of reaction can be
15 made constant by controlling both the amount of and the specific gravity of the aqueous THF/catalyst phase in the reactor. As a result, it becomes possible to control the molecular weight distribution properties of the produced PTMG, while maintaining the number average
20 molecular weight of the PTMG at a constant value.

In the above-mentioned polymerization method, a part of the polymerization product (PTMG) is sampled during the polymerization reaction so as to determine the molecular weight distribution properties thereof.
25 Based on the results of the determination, the molecu-

5 reaction-formed THF organic phase containing a polymer
and a reaction-formed aqueous THF/catalyst phase are
mutually dispersed in each other both in the form of
globules. The polymerization reaction is considered to
take place in the aqueous THF/catalyst phase. In ac-
10 cordance with the progress of the polymerization reac-
tion, the PTMG dissolved in the aqueous THF/catalyst
phase is partitioned between the aqueous THF/catalyst
phase and the THF organic phase, and the state of par-
tition reaches an equilibrium under specific reaction
15 conditions and becomes stationary.

Therefore, in order to obtain a PTMG having a
specific average number molecular weight, the retention
time of raw material THF in the aqueous THF/catalyst
phase is controlled, so that the molecular weight dis-
20 tribution properties of the thus produced PTMG can be
controlled. With respect to the PTMG produced in the
aqueous THF/catalyst phase, the polymerization reaction
proceeds as an equilibrium reaction, but the polymeri-
zation degree is considered to vary in accordance with
25 the retention time of THF (monomer) in the aqueous

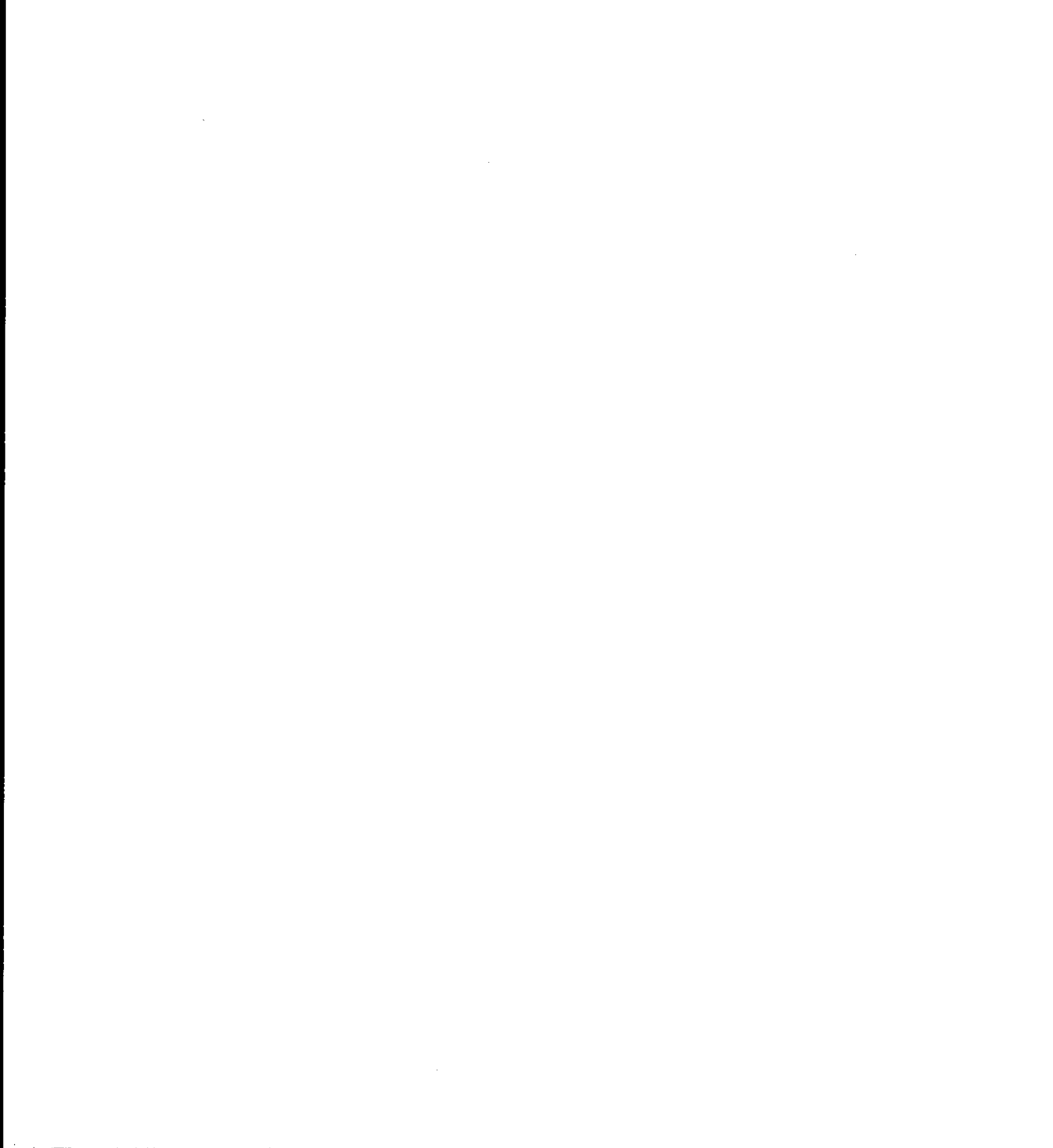


5 the final PTMG reflect the molecular weight distribution properties of the PTMG in the aqueous THF/catalyst phase.

10 For broadening the molecular weight distribution of a PTMG, the retention time distribution of the monomer (THF) in the aqueous THF/catalyst phase needs to be broadened, whereas, for narrowing the molecular weight distribution of a PTMG, the retention time distribution of the monomer in the aqueous THF/catalyst phase needs to be narrowed. The retention time of the monomer in the aqueous THF/catalyst phase can be controlled, for
15 example, by controlling the area of and the time of contact between the aqueous THF/catalyst phase and the THF organic phase.

20 The following methods (1) and (2) are the preferred methods for controlling the retention time distribution of the monomer in the catalyst phase.

(1) The retention time distribution of the monomer in the aqueous THF/catalyst phase is controlled by varying the retention time (V/F) of the monomer in the reactor. Specifically, V/F value is increased
25 for broadening the molecular weight distribution of



5 retention time distribution of the monomer in the
aqueous THF/catalyst phase is controlled by varying
the motive power (P/V) applied to the liquid (per
unit volume thereof) in the reactor. Specifically,
P/V value is decreased for broadening the molecular
10 weight distribution of the polymer, and the P/V
value is increased for narrowing the molecular
weight distribution of the polymer.

In the above methods (1) and (2), V represents the
volume (m^3) of the liquid in the reactor, F represents
15 the rate (m^3 /hour) of feeding THF to the reactor, and P
represents the motive power (kW) applied to the liquid
in the reactor.

The mechanism in the control of the molecular
weight distribution of a PTMG in method (1) above by
20 varying the V/F value is explained below.

During the continuous polymerization reaction, the
variation in the V/F value of the monomer leads to a
variation in the average retention time of the monomer
in the reactor. When the average retention time is
25 long, the retention time distribution of the monomer in



the monomer in the aqueous THF/catalyst phase becomes narrow. This means that, when the V/F value is increased, the retention time distribution of the monomer in the aqueous THF/catalyst phase becomes large, and the molecular weight distribution of the produced PTMG becomes broader. Contrary to the above, when the V/F value is decreased, the retention time distribution of the monomer in the aqueous THF/catalyst phase becomes small, and the molecular weight distribution of the produced PTMG becomes narrower.

In accordance with the above-mentioned mechanism, the molecular weight distribution of the PTMG can be controlled by varying the V/F value of the monomer used in the continuous reaction for producing the PTMG.

The molecular weight distribution of a PTMG can also be controlled as in method (2) above, that is, by varying the P/V value. When the value of P/V applied to the liquid in the reactor is varied, the average particle diameters of globules of the aqueous THF/catalyst phase and THF organic phase become varied. This variation in the average particle diameters of the globules results in the variation in the area of con-

mentioned globules (hereinbelow, this frequency is referred to as the "coalescence-redivision frequency of the globules"). It is conceivable that these variations cause the variations in the amounts of substances which are moving from one of the two phases to the other phase. It is apparent that the retention time distribution of the monomer in the aqueous THF/catalyst phase can be controlled by varying the value of P/V applied to the liquid in the reactor and, therefore, it is also possible to control the molecular weight distribution of a PTMG by varying the P/V value.

Specifically, when the P/V value is increased, the average particle diameters of the globules of the aqueous THF/catalyst phase and the globules of the THF organic phase become small, thereby increasing both the area of contact between the two phases and the coalescence-redivision frequency of the globules. As a consequence, the amounts of substances which are moving between the catalyst phase and the organic phase become increased, and this increase causes the retention time of the monomer molecules in the catalyst phase to become uniform and the retention time distribution of the

5 between the two phases and the coalescence-redivision
frequency of the globules to become decreased, and the
retention time distribution of the monomer in the cata-
lyst phase to become broad. As a result, a PTMG having
a broad molecular weight distribution is produced.

10 In accordance with the above-mentioned mechanism,
using a reactor with a stirrer, the value of P/V ap-
plied to the liquid in the reactor can be varied to
control the molecular weight distribution of a PTMG
without varying the number average molecular weight
15 thereof.

Specifically, in order to produce a PTMG having a
broader molecular weight distribution and having a
higher content of the high molecular weight PTMG mo-
lecules whose molecular weights are at least six times
20 as large as the number average molecular weight, the
 $1/(P/V)$ value (i.e., a reciprocal of the motive power
applied to the liquid per unit volume of the reactor)
and the V/F value (i.e., the retention time of the
monomer) are increased simultaneously or successively.
25 On the other hand, in order to produce a PTMG having a



5

By using the above-mentioned methods (1) and (2) for controlling the molecular weight distribution properties of the PTMG, it becomes possible to stably produce the PTMG of the present invention which has the specific molecular weight distribution properties.

10

Hereinbelow, the preferred method for polymerizing THF is explained in detail.

15

First, operation conditions for producing a PTMG having a specific number average molecular weight are determined by conducting a test operation. Specifically, a PTMG is produced by subjecting THF to a ring-opening polymerization reaction in a continuous polymerization reactor with stirrer in the presence of a heteropolyacid catalyst, wherein the ring-opening polymerization reaction is continuously performed in

20

the presence of water, so that the water is present in an amount sufficient to form the following two phases in the reactor: a THF organic phase and an aqueous THF/catalyst phase comprising a solution of the heteropolyacid catalyst in a THF/water mixture and having a

25

specific gravity of from 1.8 to 2.3.



curves under the reaction conditions for producing a
5 PTMG having a desired number average molecular weight:
a calibration curve showing the relationship between
the motive power (P/V) applied to the liquid per unit
volume of the reactor and the molecular weight dis-
tribution properties of the PTMG, and a calibration
10 curve showing the relationship between the retention
time (V/F) of THF and the molecular weight distribution
properties of the PTMG;
(b): a step comprising sub-steps of sampling a portion
of the reaction mixture being produced in the polymeri-
15 zation reactor, determining the number average molecu-
lar weight of the produced PTMG contained in the sam-
pled reaction mixture, and modifying the reaction con-
ditions when the number average molecular weight of the
produced PTMG is different from the desired value so as
20 to produce a PTMG having a desired number average mo-
lecular weight;
(c): a step of determining the molecular weight dis-
tribution properties of the produced PTMG when the PTMG
has the desired number average molecular weight; and
25 (d): a step of finally adjusting the reaction condi-



5 calibration curves obtained in step (a) based on the
molecular weight distribution properties determined
above and adjusting the motive power (P/V) and reten-
tion time (V/F) in accordance with the corrected cali-
bration curves, so as to enable a PTMG having desired
molecular weight distribution properties to be produced.

10 In general, a highly pure THF (containing impuri-
ties in an amount of less than 500 ppm by weight) is
used as a raw material for preparing the calibration
curves in step (a). Whereas, in step (b), THF is recy-
cled to the reaction system during the stable operation
15 of the reactor and the recycled THF is used as a raw
material. Since the recycled THF contains some impuri-
ties, there is a slight difference in some reaction
conditions (such as reaction rate) between the reaction
using pure THF and the reaction using recycled THF.
20 That is, it is difficult to directly apply the calibra-
tion curves prepared with respect to PTMG produced
within a short operation time to a production of a PTMG
by a stationary, stable operation of the reactor be-
cause the composition of the recycled THF varies to
25 some extent, depending on the operation conditions of

(c) to thereby obtain the calibration curves for use
5 commercial scale PTMG production. In step (d), the reaction conditions for producing PTMG are determined in accordance with the corrected calibration curves.

Hereinbelow, a further explanation is made with respect to the above-mentioned steps (a) to (d).

10 Step (a): The relationships among the molecular weight distribution of a PTMG having a predetermined number average molecular weight, the P/V value and the V/F value are obtained in the form of empirical formulae. The tolerance in the number average molecular
15 weight (i.e., the difference between the desired number average molecular weight and the actual number average molecular weight of the produced PTMG) varies depending on the use of the PTMG. For example, when the PTMG is used as a raw material for an elastic fiber, it is
20 preferred that the tolerance in the number average molecular weight is ± 100 , more advantageously ± 50 . When the PTMG is used as a starting material for a reaction, it is more preferred that the tolerance in the number average molecular weight is ± 30 .

25 For example, when a PTMG having a number average



$$M_w/M_n = K(V/F)^\alpha \quad (2), \text{ and}$$

$$M_w/M_n = K'(P/V)^\beta \quad (3)$$

wherein K , α , K' and β are constants which can be experimentally determined.

Step (b): Under conditions determined so as to
10 obtain a PTMG having a desired number average molecular weight, a polymerization reaction of THF is performed in the presence of water, wherein the water is present in an amount sufficient to form a THF organic phase and an aqueous THF/catalyst phase which has a specific
15 gravity of from 1.8 to 2.3, while maintaining the specific gravity of the aqueous THF/catalyst phase. Subsequently, the number average molecular weight of the produced PTMG is determined. When the determined value of number average molecular weight of the pro-
20 duced PTMG is different from the desired value, the polymerization reaction conditions (such as the amount of water coordinated to the heteropolyacid, the reaction temperature and the like) are regulated by conventional methods so as to obtain a PTMG having a desired



5

Step (d): When the molecular weight distribution properties of the PTMG which have been determined in step (c) above are different from the desired values, the P/V value and the V/F value are regulated in accordance with the calibration curves (formulae) obtained in step (a) above so as to control the molecular weight distribution properties of the PTMG.

10

If desired, steps (b) to (d) are repeated until a PTMG having both the desired number average molecular weight and the desired molecular weight distribution properties is obtained.

15

In order to control the molecular weight distribution properties of a PTMG so that the content of the high molecular weight PTMG molecules becomes 2 to 5 % by weight, the retention time (V/F) of THF must be in the range of from 0.5 to 20 hours, preferably from 2 to 15 hours. In the production of a PTMG having a desired number average molecular weight, when the V/F value is small, the conversion and efficiency of the reaction become lowered. On the other hand, when the V/F value is large, the reaction time becomes long. Therefore,

20

25



tion, that is, a PTMG having a molecular weight distribution of 1.8 or less and a content of high molecular weight PTMG molecules of from 2 to 5 % by weight, the following three factors should be considered for determining the polymerization conditions: the specific gravity of the aqueous THF/catalyst phase, the V/F value and the motive power (P/V) of the reactor. For this reason, it is difficult to univocally determine the specific numerical value range of the motive power. In general, when the V/F value and the volume of the aqueous THF/catalyst phase are fixed, the higher the specific gravity of the aqueous THF/catalyst phase, the higher the number average molecular weight of produced PTMG. When the specific gravity and volume of the aqueous THF/catalyst phase are fixed, the longer the V/F, the higher the number average molecular weight of the produced PTMG. In the present invention, when the specific gravity of the aqueous THF/catalyst phase is in the range of from 1.8 to 2.3 and the V/F value is from 0.5 to 20 hours, the P/V value should be maintained at 1.3 kW/m³ or more. In view of the fluctuation of the operation conditions during the production

distribution of 1.8 or less and a content of high molecular weight PTMG molecules of 2 to 5 % by weight.

Hereinbelow, an explanation is made with respect to the continuous polymerization reactor with a stirrer, which is used for producing the PTMG of the present invention.

The polymerization reactor may be or may not be equipped with a baffle on the inner wall of the reactor. It is preferred that the polymerization reactor is equipped with a baffle.

With respect to the liquid contents in the polymerization reactor, the L/D value (wherein L represents the depth of the liquid contents in the polymerization reactor and D represents the diameter of the polymerization reactor) is from 0.5 to 10, preferably from 1 to 3.

There is no particular limitation with respect to the morphology of the impeller. For example, the impeller is selected from an anchor impeller, a turbine, a propeller, a plane blade puddle, a curved blade puddle, a Pfaudler type impeller, and a Bulmarzin type impeller, preferably from an anchor impeller, a turbine,

5 number of the blades attached to the shaft of the impeller is generally from 1 to 10, usually from 1 to 3. However, an impeller having more than ten blades and an impeller having only one blade can be used without causing any problem.

10 With respect to the size of the impeller, it is preferred that the value d/D (wherein d represents the diameter of the blade of the impeller, which is twice as long as the length of the blade of the impeller; and D represents the diameter of the polymerization reactor) is from 0.1 to 0.95, preferably from 0.3 to 0.8.

15 The preferred range of the revolution speed of the stirrer greatly varies depending on the structure of the impeller. Therefore, the revolution speed of the stirrer is controlled in accordance with the structures of the reactor and impeller so as to give a motive power (P) within the desired range. Basically, it is preferred that the impeller has a structure such that a large motive power is obtained by a slow revolution speed.

25 Hereinbelow, brief explanation is made with re-



5 fluence and effects thereof.

The motive power (P) not only determines the molecular weight distribution (Mw/Mn) and the content of high molecular weight PTMG molecules (whose molecular weights are at least six times as large as the number
10 average molecular weight of all PTMG molecules), but also influences the degree of polymerization (in other words, the number average molecular weight of a PTMG). Especially when the motive power is lower than 1.1 kW/m³, the influence of the motive power on the number
15 average molecular weight is extremely large.

Until now, many patent documents disclosed the production of a PTMG from THF and water in the presence of a heteropolyacid catalyst. However, none of these patent documents describe the motive power used for
20 producing the PTMG. The fact that the variation in the motive power applied to the liquid in the reactor causes the variation in the number average molecular weight of a PTMG has been found for the first time by the present inventors.

25 The present inventors have chosen the above-



5 uses a phosphomolybdic acid (the number of water coordinated thereto = 6.0) as a catalyst. Specifically, the present inventors conducted the reworking of Example 1 while varying only the motive power. As a result, the relationship among the motive power, the number average molecular weight of a PTMG and the content of high molecular weight PTMG molecules has become clear. 10 The results are shown in Table 1 below.

Table 1

Motive power (kW/m ³)	0.004	0.4	2.6	17.9
Mn	950	1050	1100	1150
Content of high molecular weight PTMG molecules (% by weight)	5.6	5.4	4.9	4.5

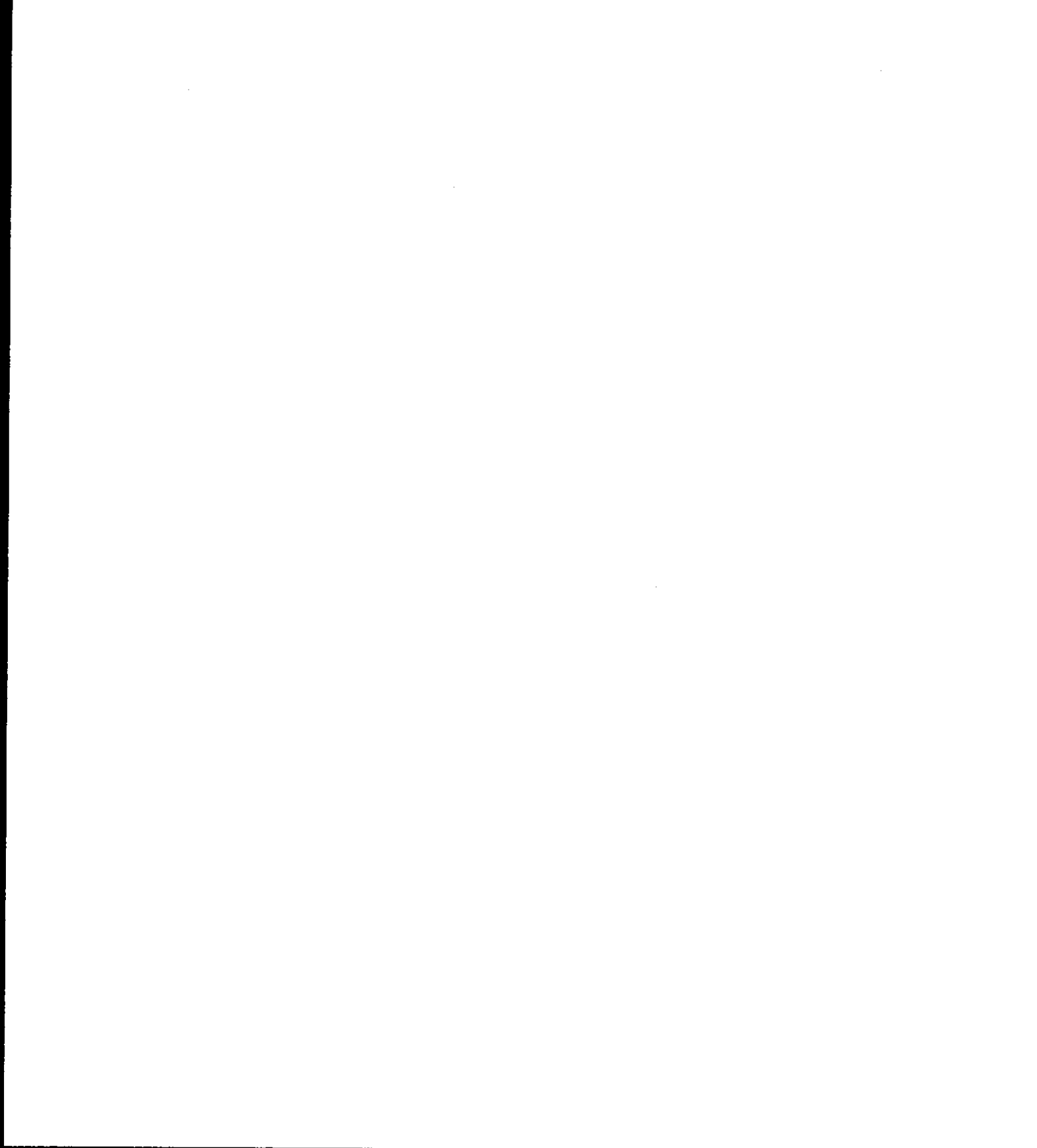
15 Table 1 above clearly shows that the increase in the motive power causes an increase in the number average molecular weight of a PTMG. It should be noted that Example 1 of Examined Japanese Patent Application



5 contained in a reaction system is consumed in accordance with the progress of the polymerization reaction, and the specific gravity of the aqueous THF/catalyst phase is gradually increased.) From Table 1 above, it is easily estimated that the motive power applied in
10 Example 1 is smaller than 0.4 kW/m^3 . Further, the estimated content of high molecular weight PTMG molecules is more than 5.4 % by weight.

The results of the above-mentioned reworking show that the motive power employed in the conventional
15 batchwise polymerization reaction of THF was approximately 0.4 kW/m^3 , and that, therefore, the motive power required in the present invention (i.e., 1.3 kW/m^3 or more) is a peculiar value in this technical field.

There is no particular limitation with respect to
20 the amount of the heteropolyacid used in the present invention for polymerizing THF. However, when the amount of the heteropolyacid in the reaction system is too small, the polymerization rate is lowered. Therefore, it is preferred that the weight ratio of the heteropolyacid to the monomer (THF) is from 0.05 to 10,
25



5 desired, predetermined value of number average molecular weight, the specific gravity of the aqueous THF/catalyst phase is maintained within the range of from 1.8 to 2.3. The water in the reactor is consumed during the continuous polymerization reaction, so water
10 must be fed into the reaction system to maintain the specific gravity of the aqueous THF/catalyst phase within the above-mentioned range.

 When the polymerization temperature is too high, depolymerization of a polymer is likely to occur,
15 thereby lowering the polymerization degree of the polymer. Therefore, in the present invention, the polymerization temperature is maintained at 0 to 100 °C, preferably 30 to 80 °C.

 The polymerization reaction proceeds by the mixing
20 of the monomer (THF) with the heteropolyacid. That is, no solvent is necessary for this polymerization reaction. However, if desired, the reaction system may contain an inert solvent. For example, a saturated hydrocarbon having 5 to 10 carbon atoms (which is used in
25 the below-mentioned operation for adjusting the hetero-

weight or less.

5 The desired PTMG of the present invention can be
obtained by obtaining a reaction mixture of a ring-
opening polymerization reaction of THF and adjusting
the heteropolyacid content of the obtained reaction
mixture to 10 to 900 ppb by weight. The heteropolyacid
10 content can be adjusted by conventional methods, such
as a method disclosed in Unexamined Japanese Patent Ap-
plication Laid-Open Specification Nos. 61-118420, 61-
115934 and 61-123629 (each corresponding to U.S. Patent
No. 4,677,231). However, it is preferred that the
15 heteropolyacid content is adjusted by a method which
comprises the following steps (i) to (vi):

 (i) separating the polymerization reaction mix-
ture into a reaction-formed aqueous THF/catalyst phase
and a reaction-formed THF organic phase containing a
20 PTMG, and obtaining the THF organic phase containing
PTMG;

 (ii) distilling off a portion of THF in the ob-
tained THF organic phase, to thereby obtain a PTMG con-
centrate;

25 (iii) adding at least one saturated hydrocarbon

in the PTMG concentrate) and an organic phase (composed
5 mainly of the above-mentioned saturated hydrocarbon and
PTMG) are formed, and subsequently removing the cata-
lyst phase;

(iv) after removal of the catalyst phase, sub-
jecting the organic phase to a treatment with an acti-
10 vated carbon so that the heteropolyacid dissolved in
the organic phase is adsorbed on the activated carbon
and removed from the organic phase;

(v) distilling off THF remaining in the organic
phase so that a saturated hydrocarbon phase and a PTMG
15 phase are formed, and subsequently removing the satu-
rated hydrocarbon phase; and

(vi) after removal of the saturated hydrocarbon
phase, distilling off the low boiling point substances
contained in the remaining PTMG phase under reduced
20 pressure, so as to obtain a PTMG in which the hetero-
polyacid content is adjusted to 10 to 900 ppb by weight.

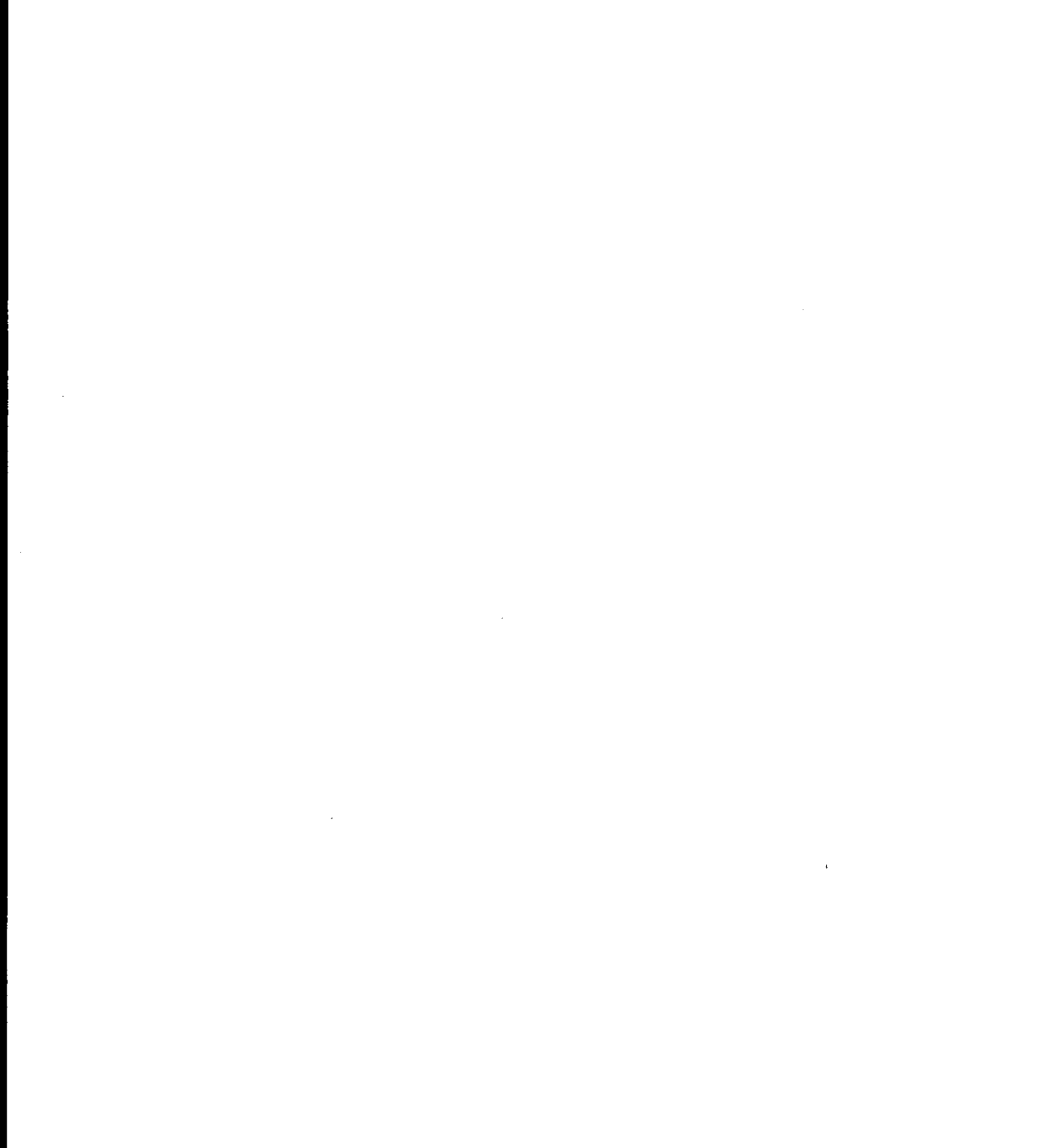
Hereinbelow, the above-mentioned steps (i) to (vi)
for adjusting the heteropolyacid content of a PTMG are
explained in more detail.

5 from the reaction system at the same rate as the rate
of the feeding of the monomer (THF) and introduced into
a phase-separation vessel (such as a decanter), to
thereby separate the reaction mixture into a reaction-
formed THF organic phase (composed mainly of THF and
10 the PTMG) and a reaction-formed aqueous THF/catalyst
phase. The THF organic phase is withdrawn from the
phase-separation vessel and subjected to the next-step
treatment. The separated aqueous THF/catalyst phase is
recycled to the reaction system.

15 The THF organic phase contains 4 to 30 % by weight
of the PTMG, and the higher the degree of polymeriza-
tion of the PTMG, the higher the PTMG content of the
THF organic phase. For example, when a PTMG having an
Mn of approximately 1800 is produced, the PTMG content
20 of the THF organic phase is approximately 23 to 25 % by
weight.

Step (ii) Removal of a portion of THF in the THF or-
ganic phase by distillation:

25 A portion of unreacted THF in the THF organic



from 0.5 to 1.5. When the weight ratio of the remaining THF is less than 0.1, the efficiency of phase-separation of the catalyst phase (which occurs in Step (iii) described below by the addition of a saturated hydrocarbon to the PTMG concentrate) becomes low. In other words, the amount of the heteropolyacid (dissolved in the THF organic phase) which is removed by the phase-separation becomes small. This lowering of the efficiency of the phase-separation can be explained as follows. Since the solubility of a PTMG in a saturated hydrocarbon is low, when the weight ratio of THF remaining in the PTMG concentrate to the PTMG is low, the mixture of the saturated hydrocarbon and PTMG concentrate is readily separated into a PTMG phase and a hydrocarbon phase. This phase separation results in a lowering of the efficiency of phase-separation of the catalyst dissolved in the PTMG. On the other hand, when the weight ratio of the remaining THF is more than 3, the remaining THF functions as a good solvent for the heteropolyacid and lowers the efficiency of phase-separation of the catalyst phase.



phase:

5 Examples of saturated hydrocarbons to be added to
the PTMG concentrate include C₅-C₁₀ saturated hydrocar-
bons, such as cyclopentane, cyclohexane, cycloheptane,
cyclooctane, cyclononane, cyclodecane, methylcyclopent-
tane, methylcyclohexane, 2-ethylhexane, pentane, hexane,
10 heptane, octane, nonane and decane. These saturated
hydrocarbons can be used individually or in combination.

 The amount of the saturated hydrocarbon used is
from 10 to 90 % by weight, preferably from 30 to 80 %
by weight, more preferably from 50 to 70 % by weight,
15 based on the total weight of a liquid mixture obtained
by adding the saturated hydrocarbon to the PTMG concen-
trate.

 In this step (iii), two liquid phases, namely a
catalyst phase containing a portion of the heteropoly-
acid contained in the PTMG concentrate and an organic
20 phase composed mainly of the saturated hydrocarbon and
PTMG, are formed. The catalyst phase is separated and
removed from the organic phase, and the organic phase
is subjected to a treatment with an activated carbon in
25 the subsequent step (iv).

In general, the heteropolyacid content of the organic phase (which is subjected to step (iv)) is 1 to 100 ppm.

When the organic phase is applied at a rate of 100 kg/hour to a column packed with an activated carbon, the activated carbon is used in an amount such that the absolute value of γ represented by the following formula (4) is in the range of from 5 to 100:

$$\gamma = \alpha / \beta \quad (4)$$

wherein α is the amount (kg) of the activated carbon, and β is the heteropolyacid content (ppm) of the organic phase.

In the step for removing the heteropolyacid using an activated carbon, when the temperature of the column packed with an activated carbon is maintained within the range of from 15 to 60 °C and the time of contact between the heteropolyacid and the activated carbon is controlled within the range of from 5 to 60 minutes, it becomes possible to easily adjust the heteropolyacid content of the final PTMG to 10 to 900 ppb without being influenced by the variation in the initial hetero-

adsorption vessel is used in place of a column, and the

5 activated carbon having adsorbed thereon the hetero-
polyacid is removed from the treated organic phase by
filtration with a filter.

By the above-described treatment with an activated
carbon, almost all of the heteropolyacid contained in
10 the organic phase is adsorbed on the activated carbon.
However, with respect to the heteropolyacid molecules
which are interacting with the terminal hydroxyl groups
of the PTMG molecules, the adsorption of such hetero-
polyacid molecules on the activated carbon is in a
15 specific equilibrium state. Therefore, it is possible
to preserve the heteropolyacid molecules which are in-
teracting with the terminal hydroxyl groups of the PTMG
molecules, in the organic phase with high selectivity.

With respect to the heteropolyacid molecules which
20 are interacting with the terminal hydroxyl groups of
the PTMG molecules, their heat stabilization action re-
sulting from the suppression of the thermal motion of
the terminal hydroxyl groups of the PTMG molecules is
strongly exhibited than their depolymerizing action
25 which is conventionally considered in this technical



acid in a specific amount.

5 That is, by the above-described treatment with an
activated carbon, the amount of heteropolyacid con-
tained in the saturated hydrocarbon is rendered ex-
tremely low, and the variation in the amount of the
heteropolyacid remaining in the PTMG is kept to a mini-
10 mum so that the amount of the heteropolyacid molecules
interacting with the terminal hydroxyl groups of the
PTMG molecules is controlled within the predetermined
range.

15 Step (v) Removal of a saturated hydrocarbon phase from
the organic phase by phase-separation:

 In this step, THF remaining in the organic phase
(after the activated carbon treatment) is distilled off
so that the saturated hydrocarbon in the organic phase
20 can be removed by phase-separation, namely the separa-
tion into a saturated hydrocarbon phase and a PTMG
phase. The THF concentration in the still residue af-
ter removal of THF is 0.1 % or less, preferably 100 ppm
or less, and more preferably 50 ppm or less. By lower-
25 ing the THF concentration as much as possible, it be-

carbon content of the PTMG phase and the PTMG content
5 of the saturated hydrocarbon phase. As a result, the
yield of the polymerization product is improved by the
lowering of the amount of the PTMG dissolved in the
saturated hydrocarbon phase. Further, the load of the
distillation conducted in the subsequent step (vi) for
10 removing the saturated hydrocarbon is reduced.

Step (vi) Removal of low-boiling point substances from
the PTMG phase:

Low-boiling point substances contained in the PTMG
15 phase (which has been separated from the saturated hydrocarbon phase) are removed by distillation under reduced pressure. In this distillation, the degree of vacuum is generally 5 Torr or less, preferably 0.5 Torr or less, more preferably 0.005 Torr or less. By conducting the distillation under the degree of vacuum as
20 high as possible, not only can the distillation temperature be lowered, but also the time in which the PTMG is exposed to a high temperature is shortened. As a result, a thermal decomposition of the PTMG during
25 the distillation is suppressed. Therefore, it is

from 60 to 160 °C, preferably in the range of from 70
5 to 130 °C.

PTMG having the heteropolyacid content of from 100
ppb to 900 ppb is obtained by conducting the above-
mentioned steps (i) to (vi).

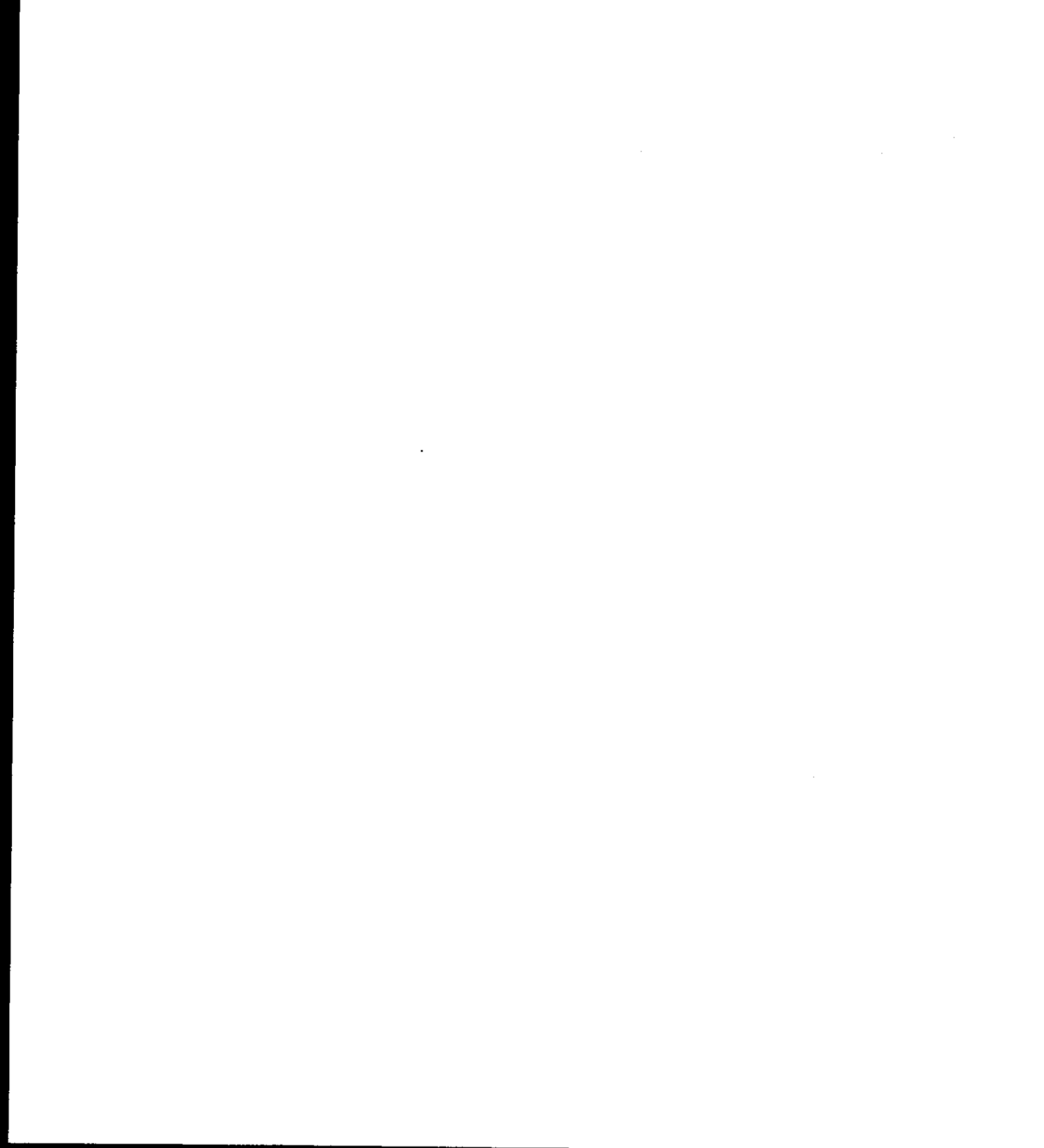
10 As described above, the PTMG of the present inven-
tion can be produced by a method which comprises:

subjecting THF to a ring opening-polymerization
reaction in a continuous polymerization reactor with
stirrer in the presence of a heteropolyacid catalyst,
15 to thereby obtain a PTMG having a specific molecular
weight distribution properties; and

adjusting the heteropolyacid content of the PTMG
by removing a portion of the catalyst (heteropolyacid)
from the polymerization reaction mixture.

20 Hereinbelow, an explanation is made with respect
to the method for producing the PTMG of the present in-
vention, with reference to Fig. 1 which shows a typical
production system for PTMG.

In the production system of Fig. 1, THF (monomer)
25 and an aqueous THF solution of a heteropolyacid (cata-



the resultant reaction system in reactor 2 is stirred vigorously. The specific gravity of the catalyst solution (CS), the retention time (V/F) of THF and the motive power (P/V) applied to the liquid per unit volume of the reactor correlate to each other. Therefore, for producing a PTMG having a specific molecular weight distribution properties, the polymerization of THF is performed under conditions wherein the specific gravity of the catalyst solution (CS), the V/F value and the P/V value are appropriately selected from the above-mentioned ranges. During the polymerization reaction, THF is continuously fed to reactor 2 and water from water feeding tank 3 is fed to reactor 2 so as to maintain the amount of water coordinated to the catalyst (in other words, so as to maintain the amount of water in reactor 2) at a desired, predetermined level. The polymerization reaction mixture is continuously withdrawn from reactor 2 and transferred to first, phase-separation vessel 4 so as to be separated into a reaction-formed THF phase (upper phase) and a reaction-formed aqueous THF/catalyst phase (CP) (lower phase). The aqueous THF/catalyst phase (CP) is recycled to re-

of the feeding of THF.

5 The THF phase withdrawn from phase-separation vessel 4 is introduced to distillation vessel 5. A portion of THF in the THF phase is distilled off to thereby obtain a PTMG concentrate. The PTMG concentrate is a solution of PTMG in which the PTMG concentration has
10 been increased in distillation vessel 5. The PTMG concentrate is introduced to second, phase-separation vessel 6. An organic solvent (S) (such as a C₅-C₁₀ saturated hydrocarbon) is added to the PTMG concentrate in second, phase-separation vessel 6, and after mixing the
15 solvent and the PTMG concentrate by stirring, the resultant mixture is separated into two liquid phases. By this phase-separation, a catalyst phase (CP) containing a portion of the catalyst dissolved in the polymerization reaction mixture (PTMG concentrate)
20 (lower phase) and an organic phase composed mainly of the organic solvent (S) and PTMG (upper phase) are formed. Subsequently, the catalyst phase (CP) is removed. The remaining organic phase is subjected to an adsorption treatment with an activated carbon (AC) by,
25 for example, introducing the organic phase into column

but a portion of the catalyst which is considered to be
5 interacting with the terminal hydroxyl groups of the
PTMG molecules remains in the organic phase. The or-
ganic phase which passed through column 7 packed with
an activated carbon is introduced to distillation col-
umn 8 to distill off THF from the organic phase. THF
10 is distilled off from the organic phase in an amount
sufficient to cause phase-separation of the organic
phase into an organic solvent (S) phase and a PTMG
phase. That is, it is not necessary to remove all of
THF in the organic phase.

15 After removing THF, the resultant organic phase is
introduced into third, separation vessel 9 so as to
separate the organic phase into two liquid phases,
namely, an organic solvent phase and a PTMG phase. Next,
the organic solvent phase is removed from separation
20 vessel 9 and the remaining PTMG phase is introduced into
vacuum distillation vessel 10 (such as thin film distil-
lation apparatus). In distillation vessel 10, low-
boiling point substances (LBPS) (such as remaining THF,
the organic solvent and THF oligomers) are distilled off,
25 thereby obtaining the PTMG of the present invention.

5 content of heteropolyacid and specific molecular weight distribution properties.

The PTMG of the present invention can be used in the form of a PTMG copolymer, i.e., a copolymer of THF with a monomer of another ether type polymer. Examples of the comonomer to be copolymerized with THF include 10 3-methyl-tetrahydrofuran, 1,2-propylene oxide, 3-methyl-oxetane and the like. In such a PTMG copolymer, the content of the comonomer units is 20 % by weight or less, preferably 10 % by weight or less, based on the weight of the PTMG copolymer.

15 The PTMG of the present invention exhibits improved properties with respect to heat resistance and low viscosity. By virtue of these excellent properties, not only can decomposition of the PTMG during the storage be suppressed, but also the amount of a stabilizer 20 can be decreased. Further, thermal decomposition of PTMG being formed during the polymerization process is suppressed. Therefore, the PTMG of the present invention can be advantageously used for producing high performance elastic fibers, such as a polyester elastic 25 fiber and a polyurethane elastic fiber.

Examples, Comparative Examples and Test Examples, but
5 they should not be construed as limiting the scope of
the present invention.

In the following Examples, various properties were
measured using the following instruments and by the
following methods.

10
(1) GPC

1) Instruments

GPC apparatus: Shodex GPC system-11 (manufactured
and sold by Showa Denko K.K.,
15 Japan)

Column: Shodex OH pack (manufactured and sold by
Showa Denko K. K., Japan):

SB 806 M (2 columns)

SB 802.5 (1 column)

20 ii) Conditions used for analysis

Detector: Differential refractometer

Column temperature: 60 °C

Carrier (eluent): 0.02 mol/liter LiBr solution of
dimethylacetamide

25 Flow rate of carrier: 1.0 ml/min

5 (2) Viscosity

1) Instruments

Apparatuses: E-type viscometer, Controller E2 and
Circulating constant-temperature
bath VCH-4 (each manufactured and
sold by TOKIMEC, Japan)

10

ii) Conditions used for measuring viscosity

Temperature: 40 °C (39 to 41 °C)

Revolution of rotor: 20 rpm

15 (3) TGA (Thermogravimetric analysis)

1) Instrument

Apparatus: TA 2950 (manufactured and sold by TA
Instrument, U.S.A)

ii) Conditions used for analysis

20 Rate of increase in temperature: 10 °C/min

Range of temperature used for analysis:

Room temperature to 500 °C

Atmosphere used for analysis:

Nitrogen gas atmosphere (purge time: 1 hour)

25



5 of the tungsten, molybdenum and niobium concentrations
is used as the heteropolyacid content of the PTMG.

A. Apparatus:

10 PQQ-type ICP-MS (manufactured and sold by VG
Elemental, England)

B. Method for ICP-Mass Spectrometry:

- ① Approximately 5 g of a sample PTMG is placed in a quartz crucible.
- 15 ② The crucible containing the sample is heated to calcine the sample, thereby obtaining a decomposition product.
- ③ To the decomposition product obtained in step ② above is added 2 ml of 35 % hydrochloric acid solution. Then, the resultant mixture is heated on a hot
20 plate to dissolve the decomposition product in the hydrochloric acid solution, thereby obtaining a sample solution.
- ④ To the sample solution is added 0.1 ml of an aqueous
25 1 ppm indium (In) solution as an internal standard.



C. Preparation of a calibration curve:

- ① A set of standard solutions for preparing a calibration curve is individually prepared for each of tungsten, molybdenum and vanadium. Specifically, a series of solutions containing one metal species in various concentrations (5 to 10000 ppb by weight) is prepared.
- ② 0.1 ml of an aqueous 1 ppm indium (In) solution as an internal standard is added to 5 g of each of the standard solutions prepared in step ① individually, thereby obtaining mixed solutions.
- ③ Water is added to the thus obtained solutions so that the volume of each solution becomes 25 ml.
- ④ The resultant solutions are subjected to ICP-Mass spectrometry so as to prepare a calibration curve.

D. Determination of a heteropolyacid content:

The respective concentrations of tungsten, molybdenum and vanadium of a sample PTMG are determined by using the



Example 1

5 Polyoxytetramethylene glycol (PTMG) was produced using the production system shown in Fig. 1.

First, a heteropolyacid catalyst solution for use as a polymerization catalyst was produced as follows. A 2-liter reaction vessel was prepared, which is
10 provided with a 3-way cock having three respective ends, wherein each end has attached thereto a condenser and an eggplant type flask for collecting and storing a distillate produced by the condenser, so that the contents of the reaction vessel can be distilled. The
15 thus prepared reaction vessel was used for producing a heteropolyacid catalyst solution. 1 liter of tetrahydrofuran (THF) and 600 g of silicotungstic acid dodecahydrate were introduced into the reaction vessel in this order, and stirred at 60 °C, while continuously
20 removing an azeotropic vapor of water and THF from the reaction vessel. The specific gravity of a solution being formed in the reaction vessel was periodically measured while feeding THF to the reaction vessel every 10 minutes so as to compensate for the total amount of
25 water and THF removed from the reaction vessel. When

lyst in a THF/water mixture.

5 Next, polyoxytetramethylene glycol was produced by
the following operation. Reactor 2 having a capacity
of 500 ml was equipped with stirrer 1 and a reflux con-
denser. 110 ml of the above-obtained catalyst solution
(CS) was charged into reactor 2 and 310 ml of THF
10 (monomer) was added thereto to thereby obtain a reac-
tion system comprised of a THF organic phase and an
aqueous THF/catalyst phase. The obtained reaction sys-
tem was stirred at 60 °C while maintaining the motive
power (P/V) applied to the liquid per unit volume of
15 the reactor at 2.0 kW/m³ and while feeding THF to reac-
tor 2 at a rate of 28 ml/hour, to thereby obtain a
polymerization reaction mixture comprising a reaction-
formed THF organic phase containing a polyoxytetra-
methylene glycol and a reaction-formed aqueous
20 THF/catalyst phase. The retention time (V/F) of THF in
reactor 2 was 15 hours. During the reaction, water was
fed to reactor 2 from water feeding tank 3 so as to
maintain the specific gravity of the aqueous
THF/catalyst phase at 2.1. A part of the polymeriza-
25 tion reaction mixture was transferred into first,

methylene glycol and a lower reaction-formed aqueous

5 THF/catalyst phase. The upper phase was withdrawn from first, phase-separation vessel 4 at a rate which is the same as the rate of the feeding of THF, while the lower reaction-formed aqueous THF/catalyst phase (CP) was recycled to reactor 2.

10 The upper phase withdrawn from first, phase-separation vessel 4 (i.e., the reaction-formed THF organic phase containing polyoxytetramethylene glycol) was fed into distillation vessel 5 for removing unreacted THF. The THF concentration of the organic phase
15 was adjusted to 45 to 50 % by weight, thereby obtaining a polyoxytetramethylene glycol concentrate.

The above-mentioned operation for obtaining a polyoxytetramethylene glycol was continuously performed for 50 hours. Approximately 10 g of the polyoxytetramethylene glycol concentrate produced during the stable
20 operation of the reactor was sampled from distillation vessel 5 for GPC analysis. Specifically, low-boiling point substances were distilled off from the sampled polyoxytetramethylene glycol concentrate at 60 °C under
25 1 Torr before subjecting to GPC analysis. The results



5 following operations for adjusting the heteropolyacid
content of the polyoxytetramethylene glycol.

100 g of the polyoxytetramethylene glycol concen-
trate was fed into second, phase-separation vessel 6.
120 g of n-octane (solvent, S) was added to second,
phase-separation vessel 6 and stirred for 5 minutes at
room temperature, thereby obtaining a mixture. The ob-
tained mixture was allowed to stand still for approxi-
mately 5 minutes, so that the mixture was separated in-
to a lower aqueous THF/heteropolyacid catalyst phase
(CP) and an upper organic phase. 200 g of the upper
organic phase which is a solution containing polyoxy-
tetramethylene glycol was placed in a 500 ml eggplant
type flask which was warmed in a water bath maintained
at 50 °C. Subsequently, the solution was applied to
adsorption column 7 at a rate of 100 g/hour using a
pump. Adsorption column 7 was a column packed with 1
kg of an activated carbon (AC) and the column had an
outer jacket in which water heated to 45 °C was circu-
lated so as to maintain the inner temperature of ad-
sorption column 7 at 40 °C or higher.

25 An eluate (approximately 200 g) obtained from ad-



tillation column (number of theoretical plates: 10).

- 5 The eluate in the eggplant type flask was subjected to distillation under atmospheric pressure with stirring to thereby remove THF in the eluate. The residual solution in the flask was transferred to a 300 ml separation funnel used as third, phase-separation vessel 9.
- 10 In third, phase-separation vessel 9, the solution was allowed to separate into two phases, namely a phase containing polyoxytetramethylene glycol as a main component and a phase containing n-octane (S) as a main component. The lower phase (approximately 30 g) containing polyoxytetramethylene glycol was taken out from
- 15 third, phase-separation vessel 9 and subjected to vacuum distillation in vacuum distillation vessel 10 for 20 minutes at 100 °C under a reduced pressure of not more than 0.1 Torr. Low-boiling point substances
- 20 (LBPS), such as n-octane, THF and oligomers, were distilled off to thereby obtain PTMG. The obtained PTMG was approximately 23 g.

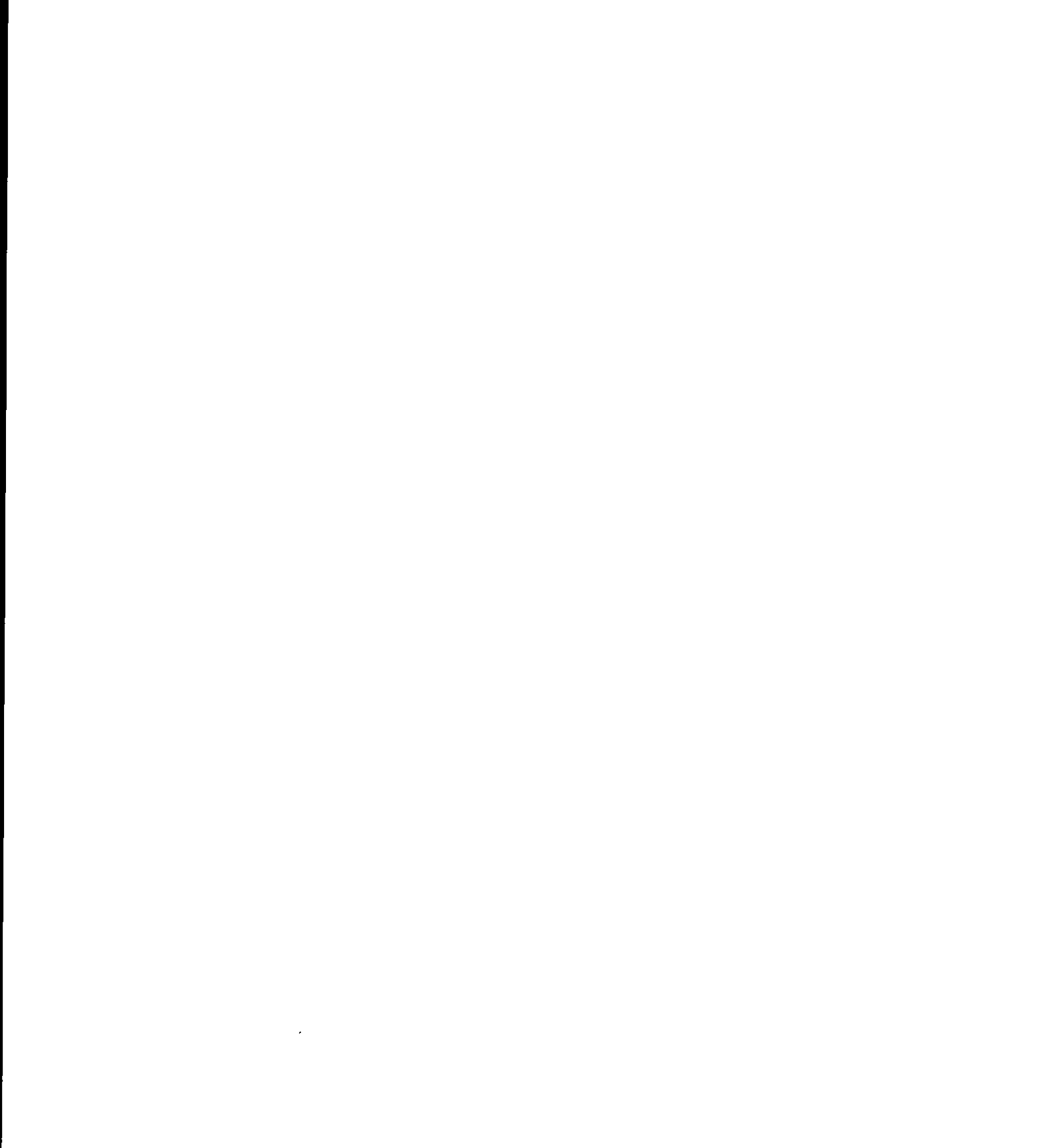
- The number average molecular weight (M_n) and the molecular weight distribution (M_w/M_n) of the obtained
- 25 PTMG was determined by GPC under the conditions men-

described in item (4) above. The heteropolyacid content of the PTMG was 300 ppb by weight.

Example 2

PTMG having a narrower molecular weight distribution than that of the PTMG produced in Example 1 was produced in the following manner. The operation for producing polyoxytetramethylene glycol was effected in the same manner as in Example 1, except that the amount of the silicotungstic acid solution (catalyst solution) charged into the reactor was increased by 50 ml without changing the total volume of the liquid in reactor 2 (thus, the amount of THF charged into the reactor was decreased to 260 ml) and the feeding rate of THF was 42 ml/hour. In addition, the V/F value of THF in the reactor was changed from 15 hours to 10 hours. The P/V value of the reactor was 2.0 kW/m^3 which was the same as that of Example 1.

With respect to the produced polyoxytetramethylene glycol, the number average molecular weight was 1940; the molecular weight distribution was 1.65; and the content of high molecular weight PTMG molecules was



the number average molecular weight thereof, by de-

5 creasing the V/F value of THF in the reactor.

 The heteropolyacid (silicotungstic acid) content
of the produced polyoxytetramethylene glycol was ad-
justed in the same manner as in Example 1, thereby ob-
taining PTMG. The heteropolyacid content of the PTMG
10 was 230 ppb by weight. Further, the PTMG obtained by
adjusting the heteropolyacid content of the polyoxy-
tetramethylene glycol was analyzed by GPC. The results
are shown in Table 4.

15 Example 3

 The operation for producing polyoxytetramethylene
glycol was effected in substantially the same manner as
in Example 1, except that 80 ml of a phosphomolybdic
acid solution having a specific gravity of 1.8 was used
20 as a catalyst solution, the initial amount of THF
charged in the reactor was 340 ml, the V/F value of THF
in the reactor was 10 hours, and the feeding rate of
water was controlled so as to maintain the specific
gravity of the aqueous THF/catalyst phase in the reac-
25 tor at 1.8. In addition, the P/V value was 2.3 kW/m^3 .

content of high molecular weight PTMG molecules was

5 4.35 % by weight.

 The heteropolyacid (phosphomolybdic acid) content of the produced polyoxytetramethylene glycol was adjusted in the same manner as in Example 1, thereby obtaining PTMG. The heteropolyacid content of the PTMG
10 was 600 ppb by weight. Further, the PTMG obtained by adjusting the heteropolyacid content of the polyoxytetramethylene glycol was analyzed by GPC. The results are shown in Table 4.

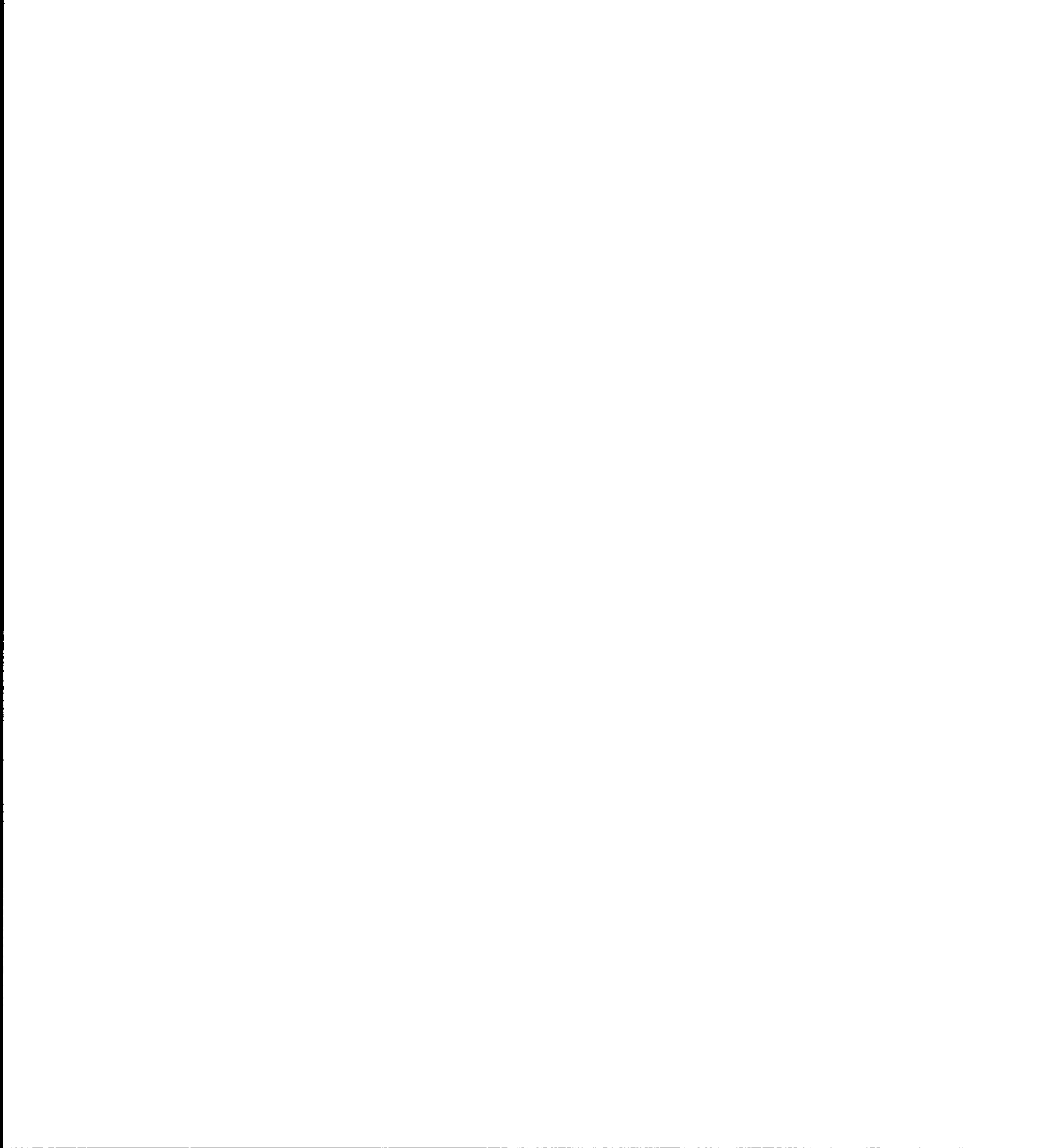
15 Example 4

 PTMG having a broader molecular weight distribution than that of the PTMG produced in Example 3 was produced in the following manner. The operation for producing polyoxytetramethylene glycol was effected in
20 substantially the same manner as in Example 3, except that the volume of the catalyst phase in the reactor was 60 ml, the volume of the THF organic phase was 360 ml, and the V/F value of THF in the reactor was 13 hours. With respect to the produced polyoxytetra-
25 methylene glycol, the number average molecular weight

5 The heteropolyacid content of the produced poly-
oxytetramethylene glycol was adjusted in the same man-
ner as in Example 1, thereby obtaining PTMG. The
heteropolyacid content of the PTMG was 690 ppb by
weight. Further, the PTMG obtained by adjusting the
heteropolyacid content of the polyoxytetramethylene
10 glycol was analyzed by GPC. The results are shown in
Table 4.

Example 5

15 The operation for producing polyoxytetramethylene
glycol was effected in substantially the same manner as
in Example 3, except that 200 ml of a phosphomolybdic
acid solution having a specific gravity of 1.8 was used
as a catalyst solution, the volume of the THF organic
phase in the reactor was 220 ml, the V/F value of THF
20 in the reactor was 10 hours, and the P/V value of the
reactor was 2.2 kW/m³. With respect to the produced
polyoxytetramethylene glycol, the number average mo-
lecular weight was 1300; the molecular weight distribu-
tion was 1.7; and the content of high molecular weight
25 PTMG molecules was 3.98 % by weight.



heteropolyacid content of the PTMG was 450 ppb by weight. Further, the PTMG obtained by adjusting the heteropolyacid content of the polyoxytetramethylene glycol was analyzed by GPC. The results are shown in Table 4.

10 Comparative Example 1

15 A polyoxytetramethylene glycol having a broader molecular weight distribution than that of the PTMG produced in Example 4 was produced in the following manner. The operation for producing a polyoxytetramethylene glycol was effected in substantially the same manner as in Example 4, except that the P/V value was decreased to 1.2 kW/m^3 . With respect to the produced polyoxytetramethylene glycol, the number average molecular weight was 1295; the molecular weight distribution was 1.85; and the content of high molecular weight polyoxytetramethylene glycol molecules was 4.8 % by weight.

25 The heteropolyacid content of the produced polyoxytetramethylene glycol was adjusted in the same manner as in Example 1. The heteropolyacid content of the

Examples 6 to 10 and Comparative Example 2

THF was polymerized using a phosphotungstic acid solution having a specific gravity of 2.07 as a catalyst solution. Specifically, the operation for producing polyoxytetramethylene glycol was effected in substantially the same manner as in Example 1, except that the reaction conditions shown in Tables 2 and 3 were employed. In addition, the volume (V) of the liquid in the reactor was maintained at 420 ml and the feeding rate of water was controlled so as to maintain the specific gravity of the aqueous THF/catalyst phase at 2.07.

In order to elucidate the correlation between the molecular weight distribution and the V/F value of THF in the reactor, in Examples 6 to 8, polyoxytetramethylene glycols were produced under the reaction conditions where the P/V value was fixed at 1.95 kW/m^3 . With respect to other reaction conditions, the conditions shown in Table 2 were employed. The number average molecular weights and the molecular weight dis-

5 The heteropolyacid (phosphotungstic acid) contents
of the produced polyoxytetramethylene glycols were ad-
justed in the same manner as in Example 1, thereby ob-
taining PTMG's. The heteropolyacid contents of the
PTMG's obtained in Examples 6 to 8 were 260 ppb, 310
ppb and 220 ppb by weight, respectively. Further, each
10 PTMG obtained by adjusting the heteropolyacid content
of the polyoxytetramethylene glycol was analyzed by GPC.
The results are shown in Table 5.

Table 2

Reaction condi- tions	Hetero- polyacid	Volume of the liquid in the reactor: V (ml)	Feeding rate of THF: F (ml/Hr)	V/F (Hr)	Volume of the cata- lyst phase (ml)	Mn	Mw/Mn
Ex. 6	Phospho- tungstic acid	420	64	6.6	180	1810	1.60
Ex. 7	ditto	420	42	10	120	1800	1.69
Ex. 8	ditto	420	28	15	80	1805	1.79

Fig. 2 is a chromatogram of the PTMG produced in
Example 6 (PTMG obtained by adjusting the heteropoly-
acid content of the polyoxytetramethylene glycol) which
20 shows the molecular weight distribution of the PTMG.



5 tical straight broken line and the abscissa shows the
logarithm of the number average molecular weight. The
area of a hatched portion shows the amount of the PTMG
molecules having molecular weights (10860 or more; $\log$
10 (molecular weight) = 4.04 or more), which are at least
six times as large as the number average molecular
weight ($M_n = 1810$; $\log M_n = 3.26$) of all PTMG molecules.
The ratio of the area of the hatched portion to the to-
tal area of the peak is 2.29 %.

15 Next, in order to elucidate the correlation be-
tween the molecular weight distribution and the P/V
value applied to the liquid in the reactor, in Compara-
tive Example 2 and Examples 9 and 10, polyoxytetra-
methylene glycols were produced under the reaction con-
20 ditions in which the V/F value and the volume of the
catalyst phase were fixed at 9 hours and 133.3 ml, re-
spectively. With respect to other reaction conditions,
the conditions shown in Table 3 were employed. The
number average molecular weight and the molecular
weight distribution of the produced polyoxytetra-
25 methylene glycols were determined. The results are

manner as in Example 1. The heteropolyacid contents of the resultant polyoxytetramethylene glycols produced in Comparative Example 2 and Examples 9 and 10 were 330 ppb, 280 ppb and 270 ppb by weight, respectively. Further, the polyoxytetramethylene glycols obtained after adjusting the heteropolyacid contents were analyzed by GPC. The results are shown in Table 5.

Table 3

Reaction conditions	Heteropolyacid	Volume of the liquid in the reactor: V (ml)	Motive power applied to the liquid in the reactor: P (mW)	P/V (kW/m ³)	Mn	Mw/Mn
Comp. Ex. 2	Phosphotungstic acid	420	462	1.1	1800	1.91
Ex. 9	ditto	420	756	1.8	1800	1.71
Ex. 10	ditto	420	1092	2.6	1805	1.62

The following formulae (5) and (6) showing the correlation between the molecular weight distribution (Mw/Mn) and the retention time (V/F) of THF and the motive power (P/V) applied to the liquid per unit volume of the reactor were obtained from the results shown in Ta-

The operation for producing polyoxytetramethylene glycol was effected in substantially the same manner as in Example 2, except that 180 ml of a phosphotungstic acid solution having a specific gravity of 1.80 was used as a catalyst solution, the feeding rate of THF was 100 ml/hour, the V/F value of THF in the reactor was 4.2 hours, the P/V value of the reactor was 2.1 kW/m³, and the volume of the THF organic phase was 240 ml. With respect to the produced polyoxytetramethylene glycol, the number average molecular weight was 852; the molecular weight distribution was 1.68; and the content of high molecular weight PTMG molecules was 4.35 % by weight.

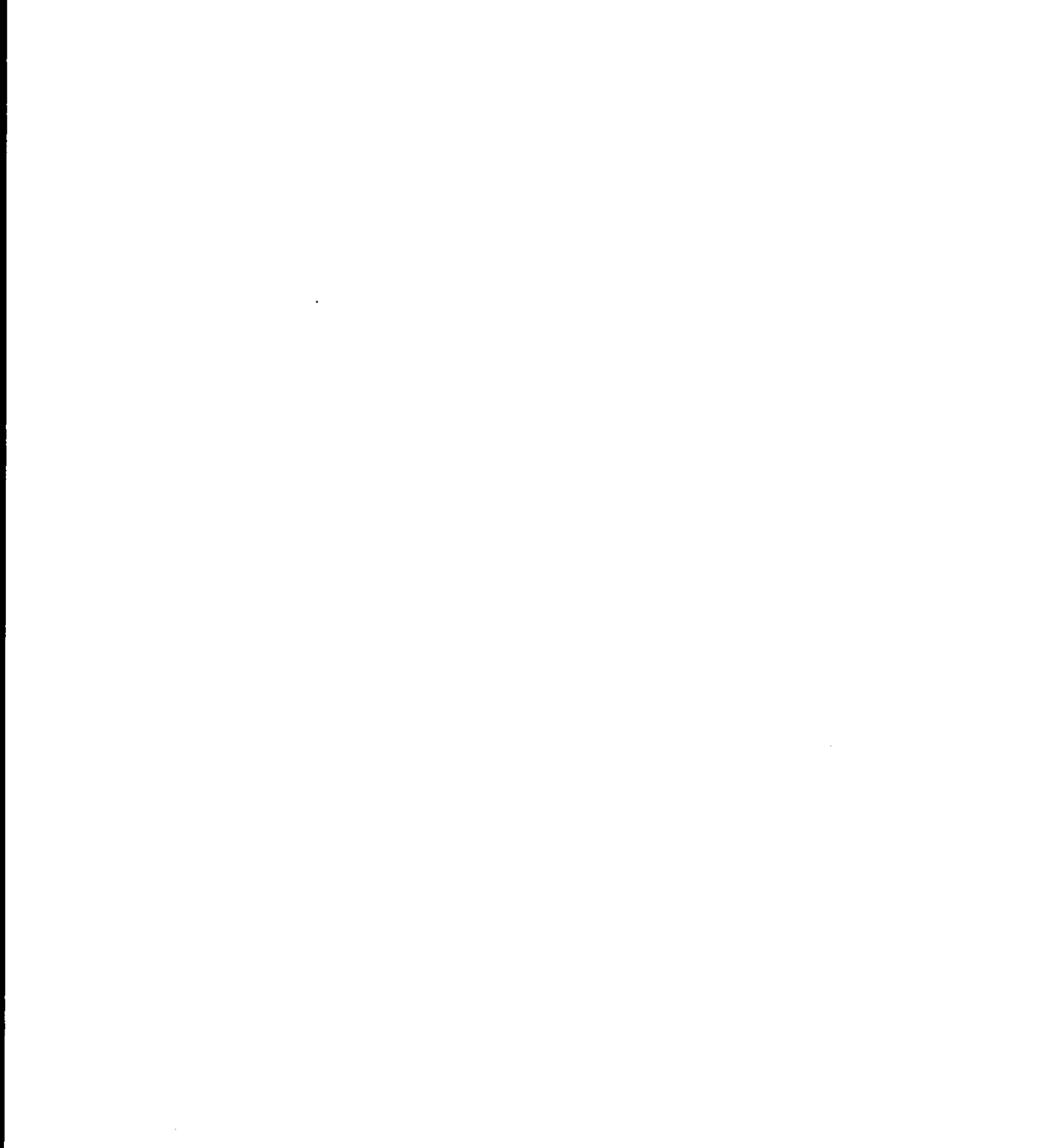
Further, the heteropolyacid content of the produced polyoxytetramethylene glycol was adjusted in the same manner as in Example 1, thereby obtaining PTMG. The heteropolyacid content of the PTMG was 590 ppb by weight. Further, the PTMG obtained by adjusting the heteropolyacid content of the polyoxytetramethylene glycol was analyzed by GPC. The results are shown in

1 to 11 and Comparative Examples 1 and 2 was determined
5 by E-type viscometer under the conditions mentioned in
item (2) above. The viscosities of the PTMG's are
shown in Tables 4 and 5 together with other character-
istics.



Catalyst		Sulfuric acid		Triisopropylamine			
Specific gravity of the catalyst solution		2.1	2.1	1.8	1.8	1.8	1.8
Volume of the liquid in the reactor: V (ml)		420	420	420	420	420	420
Volume of the catalyst phase (ml)		110	160	80	60	200	200
Volume of the THF organic phase (ml)		310	260	340	360	220	220
Reaction temperature (°C)		60	60	60	60	60	60
Feeding rate of THF: F (ml/Hr)		28	42	42	32.3	42	42
V/F (Hr)		15	10	10	13	10	10
P/V (kW/m ³)		2	2	2.3	2.3	2.2	1.2
Before adjustment of heteropolyacid content	Mn	1940	1940	1060	1055	1300	1295
	Mw/Mn	1.8	1.65	1.7	1.8	1.7	1.85
	Content of high molecular weight PTMG molecules* ¹ (% by weight)	4.1	2.98	4.35	4.94	3.98	4.8
After adjustment of heteropolyacid content	Heteropolyacid content (ppb by weight)	300	230	600	690	450	590
	Viscosity (cP)	836	725	332	356	451	510
	Mn	1960	1950	1070	1060	1310	1300
	Mw/Mn	1.79	1.65	1.7	1.8	1.68	1.85
	Content of high molecular weight PTMG molecules* ¹ (% by weight)	4.0	2.90	4.36	4.95	3.80	4.85

*) High molecular weight PTMG molecules are defined as PTMG molecules having molecular weights which are at least six times as large as the number average molecular weight of all PTMG molecules.



Specific gravity of the catalyst solution		2.07	2.07	2.07	2.07	2.07	2.07	1.80
Volume of the liquid in the reactor: V (ml)		420	420	420	420	420	420	420
Volume of the catalyst phase (ml)		180	120	80	133.3	133.3	133.3	180
Volume of the THF organic phase (ml)		240	300	340	286.7	286.7	286.7	240
Reaction temperature (°C)		60	60	60	60	60	60	60
Feeding rate of THF: F (ml/Hr)		64	42	28	28	46.7	46.7	100
V/F (Hr)		6.5625	10	15	9	9	9	4.2
P/V (kW/m ³)		1.95	1.95	1.95	1.1	1.8	2.6	2.1
Before adjustment of heteropolyacid content	Mn	1810	1800	1805	1800	1800	1805	852
	Mw/Mn	1.6	1.69	1.79	1.91	1.71	1.62	1.68
	Content of high molecular weight PTMG molecules* ¹ (% by weight)	2.29	3.05	3.89	4.73	3.24	2.89	4.35
After adjustment of heteropolyacid content	Heteropolyacid content (ppb by weight)	270	310	220	330	280	270	590
	Viscosity (cP)	638	698	761	838	695	638	242
	Mn	1800	1810	1820	1800	1795	1820	856
	Mw/Mn	1.6	1.68	1.78	1.90	1.7	1.60	1.66
	Content of high molecular weight PTMG molecules* ¹ (% by weight)	2.28	3.00	3.80	4.81	3.19	2.70	4.45

*) High molecular weight PTMG molecules are defined as PTMG molecules having molecular weights which are at least six times as large as the number average molecular weight of all PTMG molecules.



50 hours, thereby obtaining 1.25 kg of a polyoxytetramethylene glycol concentrate in which a THF concentration has been adjusted to 45 to 50 % by weight. The polyoxytetramethylene glycol concentrate was subjected to vacuum distillation in a vacuum distillation vessel at 60 °C under a reduced pressure of not more than 1 Torr to distill off low-boiling point substances (such as THF), thereby obtaining polyoxytetramethylene glycol. With respect to the obtained polyoxytetramethylene glycol, the number average molecular weight was 1810; the molecular weight distribution was 1.6; and the content of high molecular weight polyoxytetramethylene glycol molecules (the molecules having molecular weights which are at least six times as large as the number average molecular weight of all polyoxytetramethylene glycol molecules) was 2.29 % by weight. The polyoxytetramethylene glycol was subjected to the following operations for adjusting the content of the residual heteropolyacid catalyst.

To 550 g of the polyoxytetramethylene glycol were added 400 g of THF, 2 g of water and 1500 g of n-octane, and the resultant mixture was stirred vigorously for 10

phases (containing polyoxytetramethylene glycol, THF, water and n-octane) were transferred to a vessel and 80 g of an activated carbon was added thereto, followed by stirring at 40 °C for 15 minutes. The activated carbon was removed by filtration using a membrane filter, thereby obtaining 2420 g of a solution containing 530 g of polyoxytetramethylene glycol, 390 g of THF and 1500 g of n-octane.

Half the amount (i.e., 1210 g) of the obtained solution was heated in an oil bath maintained at 100 °C to thereby distill off a part of THF contained in the solution. Next, the solution was allowed to stand still to thereby separate the solution into two phases, namely a polyoxytetramethylene glycol phase and an n-octane phase, and the upper n-octane phase was eliminated. The remaining lower polyoxytetramethylene glycol phase was subjected to distillation at 60 °C under 1 Torr. The low-boiling point substances (such as THF and n-octane) were distilled off to thereby obtain 256 g of PTMG.

weight PTMG molecules (the molecules having molecular weights which are at least six times as large as the number average molecular weight of all PTMG molecules) was 2.28 % by weight. The heteropolyacid content of the PTMG was 270 ppb.

10 Example 13

Using the reaction conditions of Example 11, a polymerization operation was continuously performed for 150 hours, thereby obtaining 1.2 kg of polyoxytetramethylene glycol concentrate in which a THF concentration has been adjusted to 45 to 50 %. The polyoxytetramethylene glycol concentrate was subjected to vacuum distillation in a vacuum distillation vessel at 60 °C under a reduced pressure of not more than 1 Torr to distill off low-boiling point substances (such as THF), thereby obtaining polyoxytetramethylene glycol. With respect to the obtained polyoxytetramethylene glycol, the number average molecular weight was 852; the molecular weight distribution was 1.68; and the content of high molecular weight polyoxytetramethylene glycol molecules (the molecules having molecular weights which



5 the heteropolyacid content of the polyoxytetra-
methylene glycol was adjusted in the same manner as in
Example 12, thereby obtaining PTMG.

 With respect to the obtained PTMG, the number av-
erage molecular weight was 856; the molecular weight
distribution was 1.66; and the content of high molecu-
10 lar weight PTMG having molecular weights which are at
least six times as large as the number average molecu-
lar weight was 4.45 % by weight. The heteropolyacid
content of PTMG was 590 ppb.

15 (Heat resistance test of PTMG)

Test Examples 1 to 11

 Various sample polyoxytetramethylene glycols hav-
ing different number average molecular weights, molecu-
lar weight distributions, different contents of high
20 molecular weight PTMG molecules (the molecules having
molecular weights which are at least six times as large
as the number average molecular weight of all PTMG
molecules), and different heteropolyacid contents, were
subjected to TGA analysis under nitrogen atmosphere, to
25 thereby determine the temperatures at which the weights



the viscosity of sample polyoxytetramethylene glycols.

5 Sample polyoxytetramethylene glycol used in Test
Example 1 was PTMG produced in Example 13 and sample
polyoxytetramethylene glycol used in Test Example 2 was
PTMG produced in Example 12. Sample polyoxytetra-
methylen glycols used in Test Examples 3 and 4 were
10 manufactured and sold by BASF AG, Germany; sample poly-
oxytetramethylene glycols used in Test Examples 5 and 6
were manufactured and sold by Du Pont, USA; sample
polyoxytetramethylene glycols used in Test Examples 7
to 9 were manufactured and sold by Hodogaya Chemical
15 Co., Ltd., Japan; and sample polyoxytetramethylene gly-
cols used in Test Examples 10 and 11 were manufactured
and sold by Mitsubishi Chemical Corporation, Japan.



Table 6

Heat resistance and viscosity of various PTMG's

	Test Example 1	Test Example 2	Test Example 3	Test Example 4	Test Example 5	Test Example 6	Test Example 7	Test Example 8	Test Example 9	Test Example 10
Mn (determined by GPC)	856	1800	891	1787	922	1826	596	898	1846	93
Mw/Mn (determined by GPC)	1.66	1.60	1.87	2.44	1.89	2.47	1.45	1.78	2.51	2.0
Content of high molecu- lar weight PTMG mole- cules (% by weight)	4.45	2.28	5.21	10.85	5.81	11.62	1.47	3.78	13.39	7.0
Heteropoly- acid content (ppb by weight)	590	270	80	22	0	0	27	7	0	0
Heat resis- tance (5 wt % re- duction tem- perature) (°C)	281.5	289.9	255.7	275.8	273.4	244.0	244.9	267.2	275.2	251
Viscosity (E-type viscometer) (cP)	242	630	287	1175	292	1257	138	269	1345	32



and a content of high molecular weight PTMG molecules

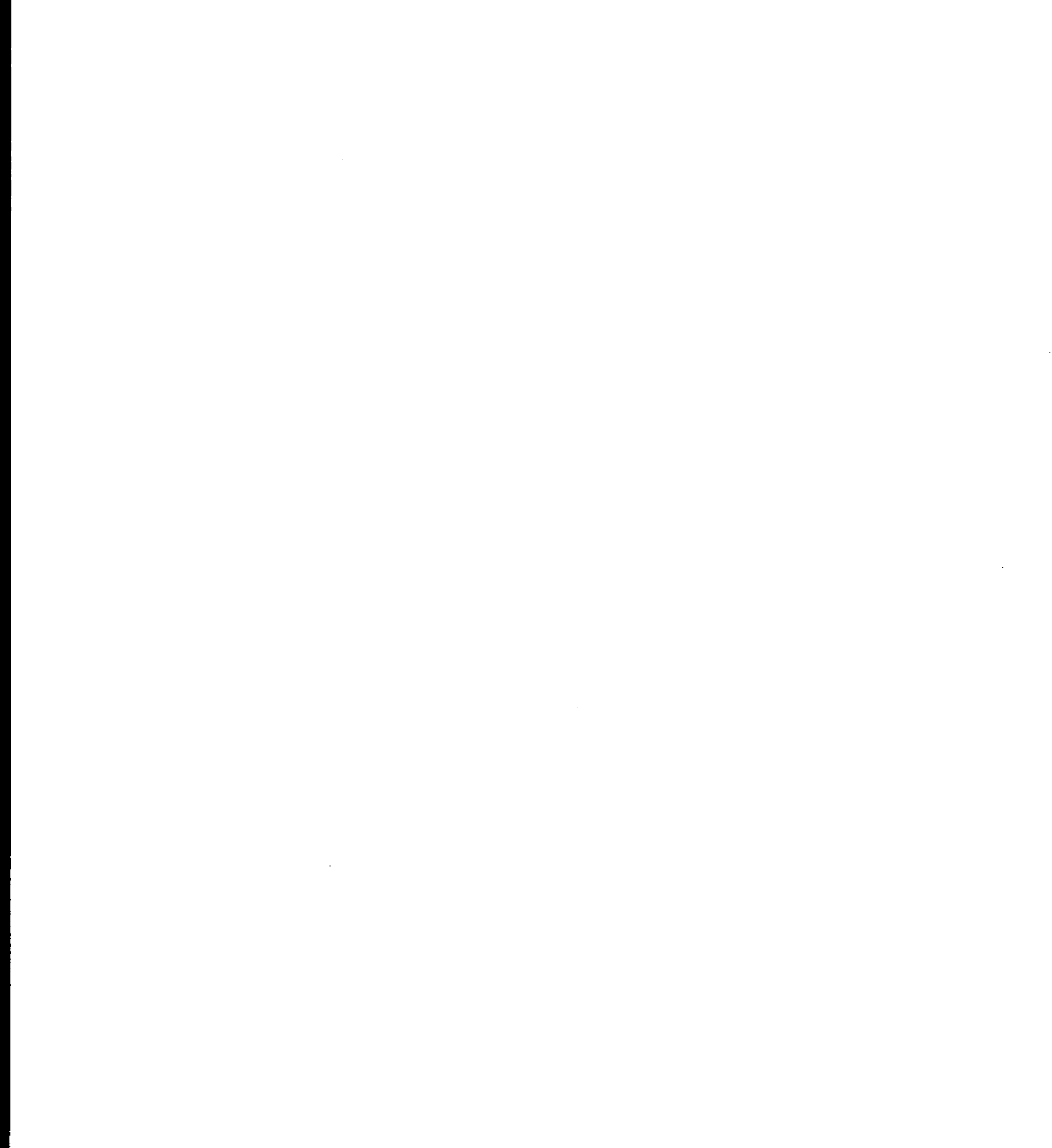
5 (PTMG molecules having molecular weights which are at
least six times as large as the number average molecu-
lar weight of all PTMG molecules) of 2 to 5 % by weight,
but also a heteropolyacid content of from 10 to 900 ppb
by weight, exhibit higher heat resistance than the con-
10 ventional polyoxytetramethylene glycols used in Test
Examples 3 to 11 which do not satisfy all of the char-
acteristics required for the present invention.

Test Examples 12 to 14

15 Three sample polyoxytetramethylene glycols having
different number average molecular weights, different
molecular weight distributions, different contents of
high molecular weight PTMG molecules and different het-
eropolyacid contents were subjected to heat resistance
20 test at 120 °C.

Each of sample polyoxytetramethylene glycols shown
in Table 7 was tested as follows. 60 g of a polyoxy-
tetramethylene glycol was placed in an autoclave
equipped with a pressure gauge. After replacing air
25 inside the autoclave with nitrogen gas, the autoclave

was cooled to room temperature. Deterioration of sample polyoxytetramethylene glycol after the heat resistance test was detected by evaluating its chromaticity, appearance (i.e., evaluation with naked eye), and the number average molecular weight as measured by GPC. The results are shown in Table 7.



Mw/Mn	1.60	1.60	1.74
Content of high molecular weight PTMG molecules (% by weight)	2.28	2.28	8.32
Heteropolyacid content (ppb by weight)	270	2880	200
Results of heat resistance test			
Internal pressure (kg/cm ² ·G)	0.22	0.32	0.30
Chromaticity (APHA)	<10	30	20
Evaluation with naked eye	No change	Black substances were floating in the PTMG	No change
Mn after the heat resistance test	1760	1700	1820

5 From Table 7 it is understood that, in Test Example 12 which used the PTMG produced in Example 6, both the increase in the inner pressure and the change in the number average molecular weight of the PTMG after the heat resistance test were small because only a

10 small amount of low-boiling point substances were generated by the decomposition of the PTMG. The results of Test Example 12 are excellent over the results of



oxytetramethylene glycol having a content of high molecular weight PTMG molecules of more than 5 % by weight).



weight of from 500 to 5000, a molecular weight distribution (Mw/Mn) of 1.8 or less, a content of high molecular weight PTMG molecules of from 2 to 5 % by weight, wherein the high molecular weight PTMG molecules are defined as PTMG molecules having molecular weights which are at least six times as large as the number average molecular weight of all PTMG molecules, and a heteropolyacid content of from 10 to 900 ppb by weight, exhibits improved properties with respect to heat resistance and low viscosity. By virtue of these improved properties, not only can decomposition of the PTMG during the storage be suppressed, but also occurrence of the thermal decomposition during the polymerization for producing the PTMG can be suppressed. Therefore, the PTMG of the present invention can be advantageously used for producing a high performance elastic fiber, such as a polyurethane urea elastic fiber having excellent physical and chemical properties, a polyurethane elastic fiber and a polyester elastic fiber.

following characteristics:

5 (1) a number average molecular weight of from 500
to 3000;

 (2) a molecular weight distribution of 1.8 or less
in terms of the Mw/Mn ratio, wherein Mw represents the
weight average molecular weight of PTMG and Mn repre-
10 sents the number average molecular weight of PTMG;

 (3) a content of high molecular weight PTMG mo-
lecules of from 2 to 5 % by weight, based on the total
weight of all PTMG molecules, wherein said high molecu-
lar weight PTMG molecules are defined as PTMG molecules
15 having molecular weights which are at least six times
as large as the number average molecular weight of all
PTMG molecules; and

 (4) a heteropolyacid content of from 10 to 900 ppb
by weight.

20

2. The polyoxytetramethylene glycol according to
claim 1, which has a molecular weight distribution of
1.7 or less.

25

3. The polyoxytetramethylene glycol according to



5 4. The polyoxytetramethylene glycol according to
claim 1, which has a heteropolyacid content of 30 to
800 ppb by weight.

10 5. A method for producing the polyoxytetramethylene
glycol (PTMG) of claim 1, which comprises subjecting
tetrahydrofuran to a polymerization reaction in a con-
tinuous polymerization reactor with a stirrer in the
presence of a heteropolyacid catalyst, while feeding
tetrahydrofuran to the continuous polymerization reac-
15 tor,

 said polymerization reaction being continuously
performed in the presence of water, wherein said water
is present in an amount sufficient to form a tetrahy-
drofuran organic phase and an aqueous tetrahydrofu-
20 ran/catalyst phase which comprises a solution of the
heteropolyacid catalyst in a tetrahydrofuran/water mix-
ture and which has a specific gravity of from 1.8 to
2.3,

 while maintaining a V/F value at 0.5 to 20 hours where-
25 in V represents the volume (m^3) of the liquid in said

5 value at 1.3 kW or more wherein P represents the motive
power (kW) applied to the liquid in said reactor and V
is as defined above so that the P/V value represents
the motive power (kW/m³) applied to the liquid per unit
volume thereof,

10 to thereby obtain a polymerization reaction mixture
comprising a reaction-formed tetrahydrofuran organic
phase containing a polyoxytetramethylene glycol having
a number average molecular weight of from 500 to 3,000
and a reaction-formed aqueous tetrahydrofuran/catalyst
15 phase,

 separating said reaction-formed tetrahydrofuran
organic phase containing said polyoxytetramethylene
glycol from said polymerization reaction mixture, and

 adjusting the heteropolyacid content of said poly-
20 oxytetramethylene glycol to a level of 10 to 900 ppb by
weight.

