

Oxygen Scavenging Plastic Material

The present invention relates to an end-capped polyether-polyester copolymer capable of scavenging oxygen and its use in compositions and articles capable of removing oxygen or functioning as an active oxygen barrier.

Thermoplastic resins such as PET (polyethylene terephthalate) have been widely used to produce several types of packaging and storage containers. PET is mostly involved in the beverage industry because it is as transparent as glass but much lighter; it is also fracture resistant; completely recyclable and has a good flexibility of colour and a variety of PET bottle designs are also made possible. The biggest disadvantage of PET is its permeability to gases and in this case specifically its permeability to oxygen.

It is well known that packaging for electronics, personal care, household, industrial, food and beverage products require high barrier properties to oxygen to preserve the freshness and quality of the package contents. Especially, sauces and beverage products such as juices, beer and tea require packaging material with high barrier properties or the ability to block oxygen ingress and/or remove oxygen trapped inside to avoid oxidation of products and extend shelf life of goods.

To address these limitations and improve shelf life of oxygen sensitive products (beer, juices or tomato sauce) a number of strategies have been used. The packaging industry has developed, for example, multilayer structures comprising mixed polymer layers. These laminated packaging containers offer improved barrier properties approaching, but not comparable to, those of glass and steel while sacrificing many of the recycling benefits associated with single layer containers such as PET, polyethylene naphthalate (PEN) or polyolefin bottles. Furthermore, clarity of the container is often substantially diminished. Maintaining the proper balance of recyclability, barrier properties, and clarity is most critical in bottling applications.

The use of multilayer bottles that contain an inner, sometimes sandwiched, layer of a higher barrier polymer material compared to the outer polymer layers is commonplace. Typically the center layer is a high barrier polymer that slows the permeability of oxygen through the container wall. Examples of such passive high barrier polymers include ethylene-vinyl alcohol (EVOH) and polyamides, preferably a partially aromatic polyamide containing meta-xylylene groups, such as poly (m-xylylene adipamide), MXD6. A common construction for such multilayer structures would comprise inner and outer layers of PET with a center layer of a polyamide, or inner and outer layers of polyolefins with a center layer of ethylene-vinyl alcohol (EVOH) polymer.

A different strategy that can also be combined with the use of passive barriers is the use of an active oxygen scavenger to reduce or remove the oxygen inside of the package. The method of providing oxygen barrier properties where a substance consumes or reacts with the oxygen is known as a (re)active oxygen barrier and differs from the passive oxygen barriers which attempt to hermetically seal a product away from oxygen via the passive approach. Several oxygen scavenging systems are known in the art. Among others, oxygen-scavenging compositions comprising an oxidizable substituted or unsubstituted ethylenically unsaturated hydrocarbon and a transition metal catalyst are well-known viable solutions.

Containers, such as sachets, filled with oxygen scavenging compositions are well-known examples of applications of such materials. However, these applications are generally limited to solid substances and solid foods and, a special care is needed to avoid ingestion.

To solve this issue, oxygen scavengers have been also incorporated into a polymer resin that forms at least one layer of the container and small amounts of transition metal salts can be added to catalyse and actively promote the oxidation of the scavengers, enhancing the oxygen barrier characteristics of the package. This method affords the opportunity to eliminate or reduce oxygen coming from the outside but also unwanted oxygen from the package cavity that may have been inadvertently introduced during packaging or filling.

Modified polyesters have been also widely used as oxygen scavengers. Different modifications of the esters have been found to be active as oxygen scavengers. US 6083585A, WO 98/12127 and WO 98/12244 disclose oxygen scavenging polyester compositions wherein the oxygen scavenger component is polybutadiene.

Other modifications consist on the introduction of ether groups by using poly (alkylene oxide)s, for example.

US 6455620 discloses poly (alkylene glycol)s that act as oxygen scavengers blended with different thermoplastic polymers.

Also WO 01/10947 discloses oxygen scavenging compositions comprising an oxidation catalyst and at least one polyether selected from the group consisting of poly(alkylene glycol)s, copolymers of poly(alkylene glycol)s and blends containing poly(alkylene glycol)s suitable for incorporating into articles containing oxygen-sensitive products.

WO 2009/032560A1 discloses oxygen scavenging compositions comprising an oxidation catalyst and a copolyester ether comprising a polyether segments comprising poly(tetramethylene-co-alkylene ether) having low haze level.

WO 2005/059019 A1 and WO 2005/059020 A2 discloses a composition comprising a copolymer comprising polypropylene oxide segments and a polymer with improved active oxygen barrier properties compared to previously known compositions.

The aforementioned oxygen scavenging systems aim at reducing the oxygen level in the package to a degree as low as possible. This is, however, not always desirable. Not all products have the same needs regarding a suitable atmosphere for extended shelf life. In case of wine, fruits and vegetables the creation of a suitable atmosphere containing a limited oxygen level is desirable to allow the development of a pleasant flavor. In case of meat and fish, a certain low oxygen

level in the atmosphere is necessary to avoid growth of certain pathogen anaerobic bacteria, like *Clostridium botulinum*.

To keep a certain low oxygen level in the package, it is necessary to match the ingress of oxygen into the package with the rate of oxygen consumption by the oxygen scavenging composition. This could potentially be achieved by lowering the content of oxygen scavenging composition in the package. However, this would come at the expense of the overall oxygen scavenging capacity of the package, thereby reducing the shelf life of the contained product article.

It is therefore desirable to provide an oxygen scavenging system, which is able to finely tune the rate of oxygen scavenging reaction to a desired reduced level and to maintain this level over the intended shelf-life of the product, thus providing high scavenging capacity.

It was found surprisingly that certain polyether-polyester copolymers as hereinafter described can effectively be used to effect and control oxygen scavenging in a thermoplastic material.

SUMMARY OF THE INVENTION

In one aspect, there is provided a polyether-polyester copolymer comprising

(i) polyether segments wherein at least one polyether segment contains at least

one polytetramethylene oxide segment,

(ii) polyester segments,

(iii) bridging elements of the structure $-\text{CO}-\text{R}_2-\text{CO}-$, wherein R_2 represents an optionally substituted bivalent hydrocarbon residue consisting of 1 to 100 carbon atoms;

(iv) one or two end-caps $\text{R}_1-\text{O}-(\text{C}_2-\text{C}_4-\text{O})_e^*$, wherein R_1 is an optionally substituted hydrocarbon residue and e is an integer of from 0 to 1000, wherein $*$ represents a bond to a bridging element (iii).

In another aspect, there is provided a method of preparing a polyether-polyester copolymer as described herein comprising a polycondensation of the polyether segments containing at least one polytetramethylenoxide segment, the polyester segments, the bridging elements and the end-caps.

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In another aspect, there is provided an active oxygen barrier composition comprising a polyether-polyester copolymer as described herein and a transition metal catalyst.

- 10 In another aspect, there is provided a plastic material comprising:
 a component a) which is a thermoplastic polymer;
 a component b) which is a polyether-polyester copolymer as described herein; and
 a component c) which is a transition metal catalyst.

15 A subject of the present invention is a polyether-polyester copolymer comprising

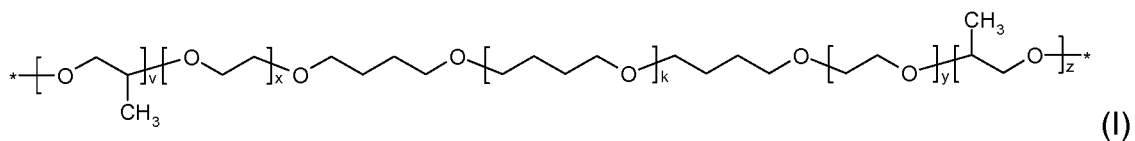
- (i) polyether segments wherein at least one polyether segment contains at least one polytetramethylene oxide segment,
 (ii) polyester segments,
 (iii) bridging elements of the structure $-\text{CO}-\text{R}^2-\text{CO}-$, wherein R^2 represents an optionally substituted bivalent hydrocarbon residue consisting of 1 to 100 carbon atoms wherein the substituents are preferably C_1 - C_5 -alkoxy, nitro, cyano or sulfo or a combination thereof;
 20 (iv) one or two end-caps $\text{R}^1-\text{O}-(\text{C}_2-\text{C}_4-\text{O})_e^*$, wherein R^1 is an optionally substituted hydrocarbon residue and e is an integer of from 0 to 1000.

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The polyether-ester copolymer of the invention is preferably a non-branched copolymer, but it may also contain small amounts, i.e. up to 10 mol-%, of trifunctional or tetrafunctional comonomers, such as trimellitic anhydride, trimethylpropane, pyromellitic dianhydride, pentaerythritol and other polyacids or polyols generally known in the art.

Beside the polytetramethylene oxide segments, the polyether segments (i) can contain other alkylene oxide segments such as ethylene oxide, propyleneoxide or a combination thereof.

Preferred embodiments of the polyether segments (i) are represented for example, by formulae (I), (Ia), (Ib), and (Ic), and optionally (Id) below:



wherein

k is an integer between 0 and 70, preferably between 0 and 35, particular preferably between 0 and 30;

v is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 50;

x is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 12;

y is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 50;

z is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 12;

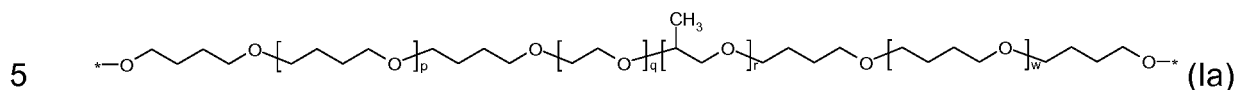
and the sum of k+v+x+y+z is between 0 and 1070, preferably between 0 and 535.

For v+x > 2 and for v and x ≠ 0, and for y+z > 2 and y and z ≠ 0, the resulting

polyethylenoxide / polypropylenoxide-copolymer part can represent a randomly distributed copolymer or a block-copolymer, wherein both blocks (the

polyethylenoxide block alternatively the polypropylenoxide block) can be chemically connected to the polytetramethyleneoxide block.

Formula (Ia):



wherein

p is an integer between 0 and 35, preferably between 0 and 20, particular preferably between 0 and 15;

10 w is an integer between 0 and 35, preferably between 0 and 20, particular preferably between 0 and 15;

q is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 50;

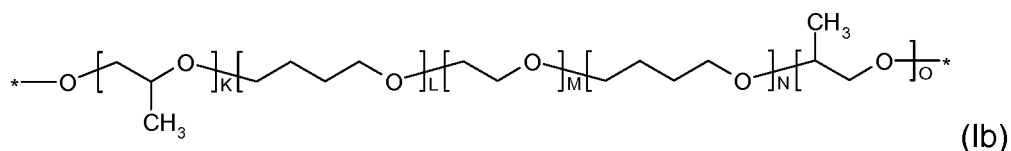
15 r is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 12;

and the sum of p+w+q+r is between 0 and 570, preferably between 0 and 290.

For q+r > 2 and for q and r ≠ 0, the resulting polyethylenoxide / polypropyleneoxide-copolymer part can represent a randomly distributed copolymer or a block-

20 copolymer.

Formula (Ib):



25 wherein

K is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 12;

L is an integer between 0 and 35, preferably between 0 and 20, particular preferably between 0 and 15;

M is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 50;

N is an integer between 0 and 35, preferably between 0 and 20, particular preferably between 0 and 15;

5 O is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 12;

furthermore $L + N$ cannot be chosen as 0;

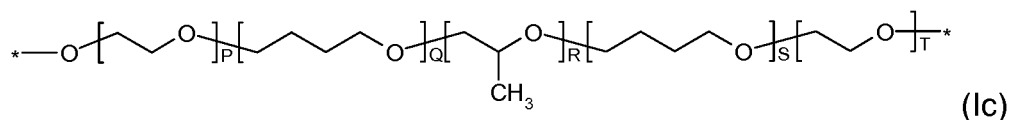
and the sum of $K+L+M+N+O$ is between 1 and 820, preferably between 2 and 415.

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In the case that $K+L > 2$ and for K, L and $M \neq 0$, or in the case that $N+O > 2$ and for N, O and $M \neq 0$, the resulting polypropylene oxide / polytetramethylene oxide-copolymer part can represent a randomly distributed copolymer or a block-copolymer wherein both blocks (the polypropylene oxide block alternatively the

15 polytetramethylene oxide block) can be chemically connected to the polyethylene oxide block.

Formula (Ic):



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wherein

P is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 50;

Q is an integer between 0 and 35, preferably between 0 and 20, particular

25 preferably between 0 and 15;

R is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 12;

S is an integer between 0 and 35, preferably between 0 and 20, particular preferably between 0 and 15;

30 T is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 50;

furthermore $Q + S$ cannot be chosen as 0;

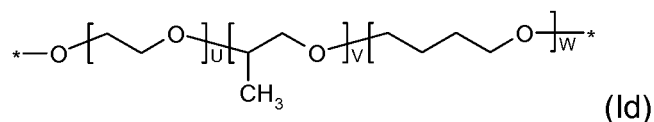
and the sum $P+Q+R+S+T$ is between 1 and 820, preferably between 2 and 415.

In the case that $P+Q > 2$ and for P, Q and $R \neq 0$, or for the case that $S+T > 2$ and

- 5 for S, T and $R \neq 0$, the resulting polyethylene oxide / polytetramethylene oxide-copolymer part can represent a randomly distributed copolymer or a block-copolymer, wherein both blocks (the polyethylene oxide block alternatively the polytetramethylene oxide block) can be chemically connected to the polypropylene oxide block.

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Formula (Id):



15 wherein

U is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 50;

V is an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 12;

20 W is an integer between 0 and 70, preferably between 0 and 35, particular preferably between 0 and 30;

and the sum $U+V+W$ is between 3 and 570, preferably between 5 and 285.

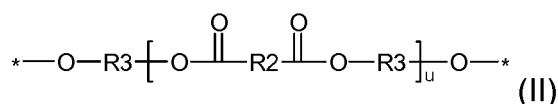
In this embodiment the polyether segment can either be a homopolymer, a

25 randomly distributed copolymer or a block-copolymer.

In all formulae, the asterisk * represents a bond to a bridging element (iii).

Preferably, the polyester segments (ii) are represented by formula (II):

30



wherein

* represents a bond to a bridging element (iii),

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R2 and R3 independently of each other represent an optionally substituted hydrocarbon residue consisting of 1 to 100 carbon atoms wherein the substituents are preferably C₁-C₅-alkoxy, nitro, cyano, and sulfo.

u is an integer between 1 and 50, preferably between 1 and 30, in

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particular between 1 and 25.

Preferably, R2 and R3 independently of each other represent an aliphatic hydrocarbon residue of 1 to 24 carbon atoms, an olefinic hydrocarbon residue of 2 to 24 carbon atoms or an aromatic hydrocarbon residue of 5 to 14 carbon atoms, wherein said hydrocarbon residues are optionally substituted with C₁-C₅-alkoxy, nitro, cyano, or a combination thereof.

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In a preferred embodiment, R2 and R3 are an aliphatic hydrocarbon residue consisting of 2 to 18 carbon atoms and most particular preferably consisting of 2 to 6 carbon atoms. The aliphatic hydrocarbon residue can be linear, branched or cyclic. Furthermore, the aliphatic hydrocarbon residue can be saturated or unsaturated. Preferably, it is saturated.

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Preferred aliphatic residues are ethylene, 1,2-propylene, 1,3-propylene, 2,2'-dimethyl-1,3-propylene, 1,4-butylene, 2,3-butylene, 1,5-pentylene, 1,6-hexamethylene, 1,7-heptamethylene, 1,8-octamethylene and 1,4-cyclohexylene, and mixtures thereof. Particular preferred residues are ethylene, 1,2-propylene, 1,3 propylene, 2,2'-dimethyl-1,3-propylene, 1,4-butylene, 2,3-butylene and 1,6-hexamethylene, and mixtures thereof. The most particular preferred residues are ethylene, 1,2-propylene and 1,4-butylene, and mixtures thereof.

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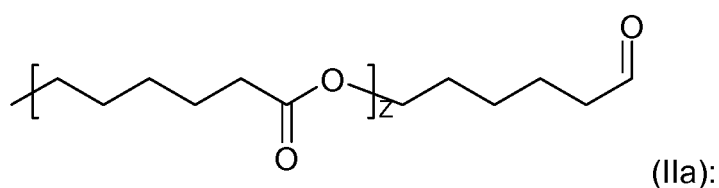
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In a further preferred embodiment, R2 is an aromatic system. The aromatic system can be mono- or polycyclic, such as di- or tricyclic. Preferably, the aromatic system is consisting of 5 to 25 atoms, even more preferably of 5 to 10 atoms. The aromatic system is preferably formed by carbon atoms. In a further embodiment, it consists in addition to carbon atoms of one or more hetero atoms such as nitrogen, oxygen and / or sulfur. Examples of such aromatic systems are benzene, naphthalene, indole, phenanthrene, pyridine, furan, pyrrole, thiophene and thiazole.

Preferred aromatic structure elements for R2 are 1,2-phenylene, 1,3-phenylene, 1,4-phenylene, 1,8-naphtylene, 1,4-naphtylene, 2,2'-biphenylene, 4,4'-biphenylene, 1,3-phenylene-5-sulphonate, 2,5-furanylene and mixtures thereof.

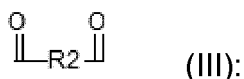
Particularly preferred structure elements for R2 are ethylene, 1,2-propylene, 1,3-propylene, 2,2'-dimethyl-1,3-propylene, 1,4-butylene, 2,3-butylene, 1,6-hexamethylene, 1,4-cyclohexylene, 1,3-phenylene, 1,4-phenylene, 1,8-naphtylene and mixtures thereof. The most particular preferred structure elements for R2 are 1,3-phenylene, 1,4-phenylene, and mixtures thereof.

In another preferred embodiment R3 can be represented by formula (IIa):



wherein Z can be an integer number from 0 to 100.

The bridging elements (iii) may link the polyether segments (i), polyester segments (ii) and/or the end caps (iv). The bridging elements are described by formula (III):



wherein R2 denotes the meanings given above.

- 5 (iv) The end-caps are bonded to a bridging element (iii). The bond is indicated by the asterisk *.

Preferred end-caps can be described by the following general formula



wherein R1 is an aliphatic hydrocarbon residue of 1 to 24 carbon atoms, an olefinic hydrocarbon residue of 2 to 24 carbon atoms, an aromatic hydrocarbon residue of 6 to 14 carbon atoms, wherein said hydrocarbon residues are optionally substituted with C₁-C₅-alkoxy, nitro, cyano, sulfo, or a combination thereof, and e is an integer of from 0 to 1000, preferably an integer between 0 and 500 and most preferably an integer between 0 and 150.

In a preferred embodiment, R1 is an aliphatic hydrocarbon residue consisting of 1 to 18 carbon atoms and more preferably consisting of 1 to 12 carbon atoms. The aliphatic hydrocarbon residue can be linear, branched or cyclic. Furthermore, the hydrocarbon residue can be saturated or unsaturated. Preferably, it is saturated.

Particularly preferred aliphatic residues for R1 are methyl, ethyl, n-propyl, iso-propyl, n-butyl, iso-butyl, sec-butyl, tert-butyl, n-pentyl, iso-pentyl, sec-pentyl, neo-pentyl, 1,2-dimethylpropyl, iso-amyl, n-hexyl, sec-hexyl, n-heptyl, n-octyl, 2-ethyl-hexyl, n-nonyl, n-decyl, tridecyl, isotridecyl, tetradecyl, hexadecyl, octadecyl, methylphenyl cyclopropyl, cyclobutyl, cyclopentyl, cyclohexyl, cycloheptyl, cyclooctyl, cyclononyl, cyclodecyl. Most preferred residues are methyl, ethyl and n-dodecyl. The most particular preferred residue is methyl.

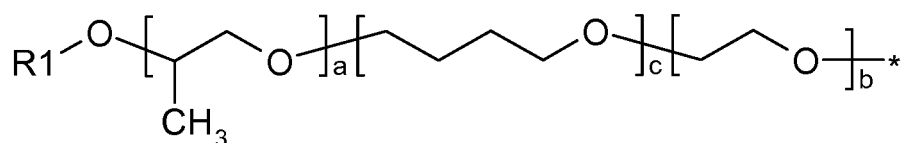
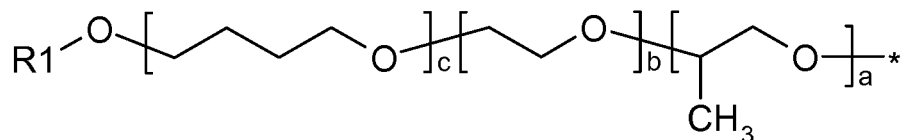
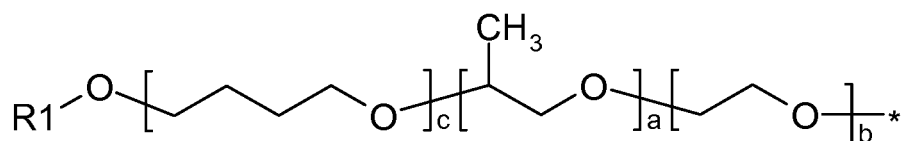
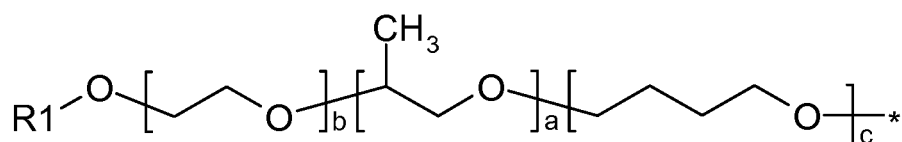
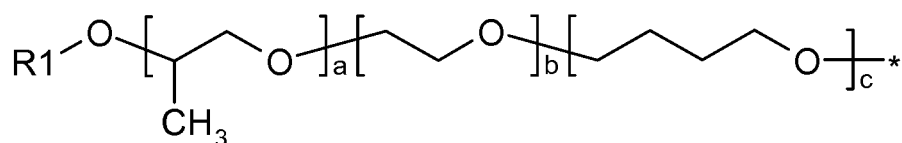
In a further preferred embodiment, R1 can be represented by an aromatic system. The aromatic system can be mono- or polycyclic, such as di- or tricyclic.

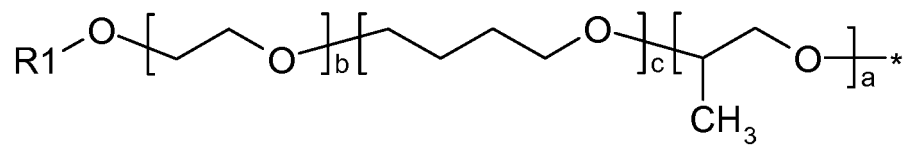
Preferably, the aromatic system is consisting of 6 to 14 carbon atoms, even more preferably of 6 to 10 atoms. The aromatic system is preferably formed by carbon

- 5 atoms. In a further embodiment, it consists in addition to carbon atoms of one or more hetero atoms such as nitrogen, oxygen and / or sulfur. Examples of such aromatic systems are benzene, naphthalene, indole, phenanthrene, pyridine, furan, pyrrole, thiophene and thiazole. In addition, the aromatic system can be chemically connected to one, two, three or more identical or different
- 10 functionalities. Suitable functionalities are for example alkyl-, alkenyl-, alkoxy-, poly (alkoxy), cyano-, and / or nitro-functionalities. These functionalities may be bonded to any position of the aromatic system.

Particularly preferred groups R1-O-(C₂-C₄-O)_e-* correspond to the following

15 formulae





wherein the different monomers are distributed randomly, in blocks or a combination of random and block

- 5 b can be chosen as an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 50
- a can be chosen as an integer between 0 and 250, preferably between 0 and 125, particular preferably between 0 and 12.
- c can be chosen as an integer between 0 and 70, preferably between 0 and 35, particular preferably between 0 and 30, and the sum $a+b+c$ is of from 0 to 570; and
- 10 R1 is as defined above.

15 The number average of the molecular weight for the copolymers of the present invention is preferably between 2000 and 1000000 g/mol, more preferably between 3500 and 100000 g/mol, most preferably between 5000 and 50000 g/mol.

The mass ratio Ω , defined as the mass ratio between the poly(tetramethyleneoxide) content and the overall content of all dicarbonyl structure elements, i.e. in (ii) and (iii), of the copolymers of the present invention is preferably between 0.1 and 10, more preferably between 0.2 and 5 and most preferably between 0.5 and 2.

The mass ratio Θ , defined as the mass ratio between the endcap content and the overall content of all dicarbonyl structure elements, i.e. in (ii) and (iii), of the copolymers of the present invention is preferably between 0.001 and 100, more preferably between 0.005 and 50 and most preferably between 0.01 and 2.

30 The copolymers of the present invention can be prepared by polycondensation of at least one polyether segment containing at least one polytetramethylenoxide

segment, at least one polyester segment, at least one bridging element and at least one end-cap $R1-O-(C_2-C_4-O)_e-^*$.

Starting compounds providing polyether segments (i) according to the invention can be homo or copolymers, copolymers may be block, random or segmented.

Examples for starting compounds are: poly(tetrahydrofuran)-diol, poly(propyleneglycol)-diol, poly(ethyleneglycol)-diol, poly(ethylenglycol)-co-poly(propylenglycol)-diol, poly(ethylenglycol)-co-poly(tetrahydrofuran)-diol, poly(propylenglycol)-co-poly(tetrahydrofuran)-diol and poly(ethyleneglycol)-co-poly(propylenglycol)-co-poly(tetrahydrofuran)-diol.

The polyester segment can be synthesized in-situ during the polycondensation reaction or introduced as pre-synthesized building block at the beginning of the reaction. Preferred polyester segments are those resulting from the condensation reaction of dibasic acids, or esters or anhydrides thereof, and diols.

Examples for starting compounds providing polyester segments (ii) according to the invention are dimethyl terephthalate, terephthalic acid, dimethyl isophthalate, isophthalic acid, dimethyl adipate, adipic acid, azelaic acid, sebacic acid, dodecanoic diacid, 1,2 cyclohexane dicarboxylic acid, dimethyl-1,4-cyclohexane dicarboxylate ester, and ethyleneglycol, 1,2-propanediol, 1,3-propanediol, 1,4-butanediol, 1,4-cyclohexanedimethanol, 2,2-dimethyl-1,3-propanediol, 1,6-hexanediol, diethyleneglycol, triethyleneglycol, poly(ethylene terephthalate) and poly(butylene terephthalate).

Examples for starting compounds providing bridging elements (iii) according to the invention are dimethyl terephthalate, terephthalic acid, dimethyl isophthalate, isophthalic acid, dimethyl adipate, adipic acid, azelaic acid, sebacic acid, dodecanoic diacid, 1,2 cyclohexane dicarboxylic acid, dimethyl-1,4-cyclohexane dicarboxylate ester.

Examples for starting compounds providing end caps are mono methoxylated poly(ethyleneglycol)-monool, mono methoxylated poly(ethylenglycol)-co-

poly(propylenglycol)-monool, lauryl-alcohol ethoxylate, oleyl-alcohol ethoxylate, nonyl-phenol ethoxylate, n-dodecanol, oleyl-alcohol.

5 For the preparation of the copolymers of the present invention, typically a two stage process is used of either direct esterification of diacids and diols or transesterification of diesters and diols, followed by a polycondensation reaction under reduced pressure.

10 A suitable process for the preparation of the copolymers of the present invention comprises heating suitable starting compounds for segments (i) to (iv) with the addition of a catalyst, to temperatures of 160 to 220 °C, expediently beginning at atmospheric pressure, and then continuing the reaction under reduced pressure at temperatures of from 160 to 240 °C.

15 Reduced pressure preferably means a pressure of from 0.1 to 900 mbar and more preferably a pressure of from 0.5 to 500 mbar.

Typical transesterification and condensation catalysts known in the art can be used for the preparation of the copolymers, such as antimony, germanium and
20 titanium based catalysts. Preferably, tetraisopropyl orthotitanate (IPT) and sodium acetate (NaOAc) are used as the catalyst system in the process.

The present invention further provides for a method of providing an active oxygen barrier in a plastic material of a packaging article comprising incorporating an
25 effective amount of the polyether-polyester copolymer and a transition metal catalyst into a thermoplastic polymer material which is preferably a polyester, a polyolefin, a polyolefin copolymer or a polystyrene.

Therefore, a further subject of the present invention is an active oxygen barrier
30 composition comprising a polyether-polyester copolymer as described before and a transition metal catalyst, preferably in a concentration of 0.001 to 5 wt.-%, more preferably 0.01 to 0.5 %, based on the total weight of the oxygen barrier composition.

Without being bound by any theory, it is believed that the polyether-polyester copolymer is an oxidisable substrate in which the end-caps at the end of the chains are capable of controlling the oxygen ingress and providing a controlled active oxygen barrier. The speed of the oxygen scavenging reaction can be modified by the amount and the chemical constitution of the end-caps.

The transition metal catalyst also initiates and accelerates the rate of oxygen consumption. The mechanism by which this transition metal functions is not certain. The catalyst may or may not be consumed with oxygen, or if consumed, may only be consumed temporarily by converting back to a catalytically active state.

More preferably, the transition metal catalyst is in the form of a salt, with the transition metal selected from the first, second or third transition series of the Periodic Table of the Elements. Suitable metals and their oxidation states include, but are not limited to, manganese II or III, iron II or III, cobalt II or III, nickel II or III, copper I or II, rhodium II, III or IV, and ruthenium. The oxidation state of the metal when introduced does not need to be that of the active form. The metal is preferably iron, nickel, manganese, cobalt or copper; more preferably manganese or cobalt; and even more preferably cobalt. Suitable counterions for the metal include, but are not limited to, chloride, acetate, acetylacetonate, propionate, oleate, stearate, palmitate, 2-ethylhexanoate, octanoate, neodecanoate or naphthenate.

The metal salt can also be an ionomer, in which case a polymeric counterion is employed. Such ionomers are well known in the art.

Even more preferably, the salt, the transition metal, and the counterion are either compliant with country regulations in the matter of food contact materials or, if part of a packaging article, exhibit substantially no migration from the oxygen barrier composition to the packaged contents. Particularly preferable salts include cobalt oleate, cobalt propionate, cobalt stearate, and cobalt neodecanoate.

A further subject of the invention is a plastic material comprising:

a component a) which is a thermoplastic polymer, preferably selected from the group consisting of polyesters, polyolefins, polyolefin copolymers and polystyrenes;

5 a component b) which is a polyether-polyester copolymer as described in the foregoing; and

a component c) which is a transition metal catalyst as described in the foregoing.

The plastic material can be a masterbatch, a compound or a formed article.

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Depending on its use the plastic material can contain component b) in an amount of from 0.5 to 99.995 wt.-% or more preferably 1 to 99,8 wt.-%, and component c) expressed as concentration of transition metal element, in an amount of from 0.001 to 5 wt.-% or more preferably 0.002 to 4 % wt.-%, based on the total weight of the plastic material.

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Preferred components a) within the meaning of the invention are polyesters. The intrinsic viscosity values of the polyesters are set forth in dL/g units as calculated from the inherent viscosity measured at 25 °C in 60/40 wt/wt

20 phenol/tetrachloroethane. The intrinsic viscosity of the polyesters preferably ranges from about 0.55 to about 1.14 dL/g.

Preferred polyesters are the ones resulting from the condensation reaction of dibasic acids and glycols.

25 Typically, the dibasic acid comprises an aromatic dibasic acid, or ester or anhydride thereof, and is selected from the group consisting of isophthalic acid, terephthalic acid, naphthalene-1,4-dicarboxylic acid, naphthalene-2,6,-dicarboxylic acid, phthalic acid, phthalic anhydride, tetrahydrophthalic anhydride, trimellitic anhydride, diphenoxyethane-4,4'-dicarboxylic acid, diphenyl-4,4'-dicarboxylic acid, 30 2,5-furandicarboxylic acid and mixtures thereof. The dibasic acid also can be an aliphatic dibasic acid or anhydride, such as adipic acid, sebacic acid, decan-1,10-dicarboxylic acid, fumaric acid, succinic anhydride, succinic acid, cyclohexanediacetic acid, glutaric acid, azeleic acid, and mixtures thereof. Other

aromatic and aliphatic dibasic acids known to persons skilled in the art also can be used. More preferably, the dibasic acid comprises an aromatic dibasic acid, optionally further comprising up to about 20 % by weight of the dibasic acid component, of an aliphatic dibasic acid.

5

Preferably, the glycol or diol component of the polyester is selected from the group consisting of ethylene glycol, propylene glycol, butane-1,4-diol, diethylene glycol, a polyethylene glycol, a polypropylene glycol, neopentyl glycol, a polytetramethylene glycol, 1,6-hexylene glycol, pentane-1,5-diol, 3-methylpentanediol-(2,4),

10 2-methylpentanediol-(1,4), 2,2,4-trimethylpentane-diol-(1,3), 2-ethylhexanediol-(1,3), 2,2-diethylpropanediol-(1,3), hexanediol-(1,3), 1,4-di-(hydroxy-ethoxy) benzene, 2,2-bis-(4-hydroxycyclohexyl) propane, 2,4-dihydroxy-1,1,3,3-tetramethylcyclobutane, 2,2-bis-(3-hydroxyethoxyphenyl) propane, 2,2-bis-(4-hydroxypropoxyphenyl) propane, 1,4-dihydroxymethyl-cyclohexane, and mixtures
15 thereof. Additional glycols known to persons skilled in the art also can be used as the glycol component of the polyester.

Two preferred polyesters are polyethylene terephthalate (PET) and polyethylene naphthalate (PEN). The PET and PEN can be homopolymers, or copolymers
20 further containing up to 10 mole percent of a dibasic acid different from terephthalic acid or a naphthalene dicarboxylic acid, and/or up to 10 mole percent of a glycol different from ethylene glycol.

PEN is preferably selected from the group consisting of polyethylene naphthalene
25 2, 6-dicarboxylate, polyethylene naphthalene 1,4-dicarboxylate, polyethylene naphthalene 1,6-dicarboxylate, polyethylene naphthalene 1,8-dicarboxylate, and polyethylene naphthalene 2,3-dicarboxylate. More preferably, PEN is polyethylene naphthalene 2,3-dicarboxylate.

30 More preferably the plastic material is selected from the group consisting of PET, e.g. virgin bottle grade PET and postconsumer PET (PC-PET), cyclohexane dimethanol/PET copolymer (PETG), polyethylene naphthalate (PEN), polybutylene terephthalate (PBT), and mixtures thereof.

Also preferred plastic materials are biobased polymers, preferably polyethylene furanoate (PEF) and also biodegradable polyester, preferably selected from the group consisting of PLAs (Polylactic acid), polycaprolactones (PCL) and

- 5 polyhydroxybutyrates (PHB).; and bio-based polyesters, which are derived from renewable resources such as corn and sugar cane and the by-products associated with their harvesting and processing but are not biodegradable.

Preferred polyolefins and polyolefin copolymers, i.e. component a) within the meaning of the invention, are thermoplastic polyolefins known in the art and are selected from the group consisting of

- polyethylene (PE), preferably selected from the group consisting of high density polyethylene (HDPE), medium density polyethylene (MDPE), low density polyethylene (LDPE), linear low density polyethylene (LLDPE),
15 metallocene low density polyethylene (mLDPE) and metallocene linear low density polyethylene (mLLDPE),
- polypropylene (PP), preferably selected from the group consisting of polypropylene homopolymer (PPH), polypropylene random copolymer (PP-R) and polypropylene block copolymers (PP-block-COPO),
- 20 - PE copolymers, preferably selected from the group consisting of ethylene-vinyl acetate copolymers (EVA), copolymers of ethylene and methyl acrylate (EMA), copolymers of ethylene and butyl acrylate (EBA), copolymers of ethylene and ethyl acrylate (EEA), and cycloolefin copolymers (COC),
- 25 - general purpose polystyrene (GPPS) and high impact polystyrene (HIPS); more preferably of
- high density polyethylene (HDPE) and low density polyethylene (LDPE)
- polypropylene homopolymer (PPH),
- general purpose polystyrene (GPPS).

30

Preferred polystyrenes, i.e. component a) within the meaning of the invention, can be a styrene homopolymer, an alkylstyrene homopolymer, preferably a

C₁-C₄-alkylstyrene homopolymer, for example α -methylstyrene homopolymer; a styrene copolymer, especially a high impact polystyrene (HIPS).

High impact polystyrenes (HIPS) are generally prepared by polymerization by grafting mixtures of styrene and optionally of one or more copolymerizable vinyl monomers, preferably mixtures of styrene, methylstyrene, ethylstyrene, butylstyrene, halostyrenes, vinylalkylbenzenes, such as vinyltoluene, vinylxylene, acrylonitrile, methacrylonitrile, lower alkyl esters of methacrylic acid, in the presence of a rubbery polymer trunk comprising copolymers chosen from polybutadiene, polyisoprene, rubbery styrene-diene copolymers, acrylic rubber, nitrile rubber and olefinic rubbers, such as propylene diene monomer rubber (PDM) and propylene rubber (PR). In the high impact polystyrene, the rubbery polymer trunk normally constitutes from 5 to 80 % by weight, preferably 5 to 50 % by weight, of the total weight of the grafted polymer.

Optionally, the active oxygen barrier composition and the plastic material of the present invention comprises one or more further substances (component d), which are selected from the group consisting of

- natural colorants derived from plants or animals and synthetic colorants, preferred synthetic colorants being synthetic organic and inorganic dyes and pigments,
 - preferred synthetic organic pigments being azo or disazo pigments, laked azo or disazo pigments or polycyclic pigments, particularly preferably phthalocyanine, diketopyrrolopyrrole, quinacridone, perylene, dioxazine, anthraquinone, thioindigo, diaryl or quinophthalone pigments;
 - preferred synthetic inorganic pigments being metal oxides, mixed oxides, aluminium sulphates, chromates, metal powders, pearlescent pigments (mica), luminescent colours, titanium oxides, cadmium lead pigments, iron oxides, carbon black, silicates, nickel titanates, cobalt pigments or chromium oxides;
- surfactants;

- auxiliaries, preferably acid scavengers, processing aids, coupling agents, lubricants, stearates, blowing agents, polyhydric alcohols, nucleating agents, or antioxidants, e.g. stearates, or oxides such as magnesium oxide;
- antioxidants, preferably primary or secondary antioxidants;
- 5 - antistatic agents;
- compatibilizers for polyester/polyamide blends;
- UV absorbers, slip agents, anti-fogging agents, anti-condensation agents, suspension stabilizers, anti-blocking agents, waxes, and a mixture of these substances.

10

More preferably, component d) is selected from the group consisting of compatibilizers, UV absorbers, antioxidants and colorants.

15

Component d) can be present in an amount of from 0 to 60 wt.-%, preferably 0.001 to 50 wt.-%, more preferably 0.1 to 30 wt.-%, most preferably 1 to 25 wt.-%, based on the total weight of the plastic material.

The plastic material of the present invention is expediently formed, e.g. blow molded, into a plastic article.

20

Therefore, another subject of the present invention is a formed plastic article comprising said plastic material.

25

The formed plastic article according to the invention can be a packaging material, preferably a container, a film or a sheet, especially for use in packaging of personal care, cosmetics, household, industrial, food and beverage products where a high oxygen barrier is needed.

30

Packaging materials can be flexible, rigid, semi-rigid or combinations thereof. Rigid packaging articles typically have wall thicknesses in the range of 100 to 1000 micrometers. Typical flexible packages typically have thicknesses of 5 to 250 micrometers.

Rigid packaging articles or flexible films of the invention can consist of a single layer or may comprise multiple layers.

When a packaging article or film comprises an oxygen scavenging layer, it can further comprise one or more additional layers, one or more of the additional layers comprising an oxygen barrier layer or being permeable to oxygen. Further additional layers, such as adhesive layers, can also be used in a multi-layer packaging article or film.

Another subject of the invention is a method for the manufacture of a plastic article as defined above, characterized in that the components a), b), c), and optionally d), are physically mixed with one another and subjected to a shape forming process.

For physical mixing, it is possible to use a mixing apparatus customary in the plastics industry. Preferably, the mixing apparatus can be one used to make a liquid masterbatch or a solid masterbatch or can be a combination of those apparatuses.

A mixing apparatus for a liquid masterbatch can be a high speed dispersor (e.g. of CowlesTM type), a media mill, a three-roll mill, a submill or a rotor-stator type dispersor.

A mixing apparatus used to make solid masterbatches MB or compounds CO can be a mixer, extruder, kneader, press, mill, calender, blender, injection moulding machine, injection and stretch blow moulding machine (ISBM), extrusion blow moulding machine (EBM), compression moulding machine, compression and stretch blow moulding machine; more preferably a mixer, extruder, injection moulding machine, injection and stretch blow moulding machine, compression moulding machine, compression and stretch blow moulding machine; even more preferably a mixer, extruder, injection and stretch blow moulding machine and extrusion blow moulding machine.

The shape forming process for the article is dependent on the desired shape of article to be manufactured.

Containers are preferably made by blow moulding, injection moulding, injection and stretch blow moulding, extrusion blow moulding, compression moulding, compression and stretch blow moulding processes.

Films and sheets are preferably made by cast or blown film extrusion or co-extrusion processes, depending on the thickness required and on the number of layers needed to obtain specific properties, eventually followed by post-extrusion shaping processes like thermoforming or stretching. In the thermoforming process, the plastic sheet is heated to a pliable forming temperature, formed to a specific shape in a mold, and trimmed to create a final article. If vacuum is used, this process is generally called vacuum forming. In post-extrusion stretching processes an extruded film can be, for example, biaxially oriented by drawing. All the above listed processes are well-known in the art.

10

The mixing of the components can occur in one step, two steps or in a plurality of steps.

Mixing can occur in one step when the components a), b), c), and optionally component d) or only b), c) and optionally component d), are directly metered

15

and/or let down in a form of liquid or solid concentrates or as pure components, for example in an injection and stretch blow molding machine.

The mixing can also occur in two or three steps, wherein in a first step components b), c) and optionally d) are predispersed into component a), and in one or more consecutive steps are added to component a).

20

Mixing can also occur in two or three steps, wherein in a first step components c) and optionally component d) are predispersed into component a) and the component b) is directly metered and/or let down as pure component, for example in an injection and stretch blow molding machine.

25

Preferably, component b) and component c) are predispersed into component a) to form two separate masterbatches, and then these masterbatches are combined with components a) and optionally d).

30

In one preferred embodiment, in a first step, component b) and optionally component d) are dispersed into component a) while component c) is dispersed into component a) to provide two separate masterbatches. After being melt compounded, for example in a single or twin screw extruder, the extrudates are withdrawn in strand form, and recovered as pellets according to the usual way,

such as cutting. In a second step, the obtained masterbatches are metered and let down by a converter/compounder into the main stream of component A pellets, for example in an injection and stretch blow molding machine. These extrudates can be metered and let down into the main stream of component a) directly into an injection process avoiding the compounding process.

In another embodiment, in a first step, component b), c) and optionally component d) are dispersed into component a) to provide a masterbatch. After being melt compounded, for example in a single or twin screw extruder, the extrudate is withdrawn in strand form, and recovered as pellets according to the usual way such as cutting. In a second step, the obtained solid masterbatch is metered and let down by a converter/compounder into the main stream of component a) of e.g. an injection and stretch blow molding machine, at a rate corresponding to the final desired concentration of component b) and c) in the article.

Mixing preferably occurs continuously or batchwise, more preferably continuously; in case of a solid masterbatch MB preferably by extrusion, mixing, milling or calendaring, more preferably by extrusion; in case of a liquid masterbatch MB preferably by mixing or milling; in case of a compound CO preferably by extrusion or calendaring, more preferably by extrusion.

Mixing is preferably carried out at a temperature of from 0 to 330 °C.

The mixing time is preferably of from 5 sec to 36 h, preferably 5 sec to 24 h.

The mixing time in the case of continuous mixing is preferably of from 5 sec to 1 h.

The mixing time in the case of batchwise mixing is preferably of from 1 sec to 36 h.

In the case of a liquid masterbatch MB, mixing is preferably carried at a temperature of from 0 to 150 °C with a mixing time of from 0.5 minutes to 60 minutes.

In the case of a solid masterbatch MB or a compound CO, mixing is preferably carried out at a temperature of from 80 to 330 °C with a mixing time of from 5 sec to 1 h.

Specific articles of the present invention include preforms, containers, films and sheets for packaging of food, beverages, cosmetics, and personal care products where a high oxygen barrier is needed. Examples of beverage containers are:

bottles for juices, sport drinks, beer or any other beverage where oxygen
5 detrimentally affects the flavour, fragrance, performance (prevent vitamin degradation), or colour of the drink. The compositions of the present invention are also particularly useful as a sheet for thermoforming into rigid packages and films for flexible structures. Rigid packages include food trays and lids. Examples of food tray applications include dual ovenable food trays, or cold storage food trays,
10 both in the base container and in the lidding (whether a thermoformed lid or a film), where the freshness of the food contents can decay with the ingress of oxygen.

Preferred articles of the present invention are rigid packaging articles, such as
15 bottles and thermoformed sheets and flexible films.

Further aspect of the present invention concerns monolayer films. The term monolayer film or monolayer cast film or monolayer sheet indicates the semi-finished product consisting of the sheet (preform) usually obtained by means of
20 extrusion of the films forming the layer. The sheet obtained has not undergone any preferential orientation process and is therefore unoriented. The sheet can be afterwards transformed into a finished article such as a container by means of known processes which do not induce orientation, usually by means
thermoforming. The term "container" refers any article having an opening for the
25 introduction of a product, particularly food products.

To determine the oxygen scavenging capabilities of the copolymers of the invention, the rate of oxygen scavenging can be calculated by measuring the time elapsed until the article has depleted a certain amount of oxygen from a sealed
30 container.

Another definition of acceptable oxygen scavenging is derived from testing actual packages.

The oxygen scavenging capacity of an article comprising the invention can be measured by determining the amount of oxygen consumed until the article becomes ineffective as a scavenger.

- 5 The plastic material of the present invention provides an oxygen scavenging system with high oxygen scavenging capacity, exact fine-tuning of oxygen transmission rate into the inner of the package and satisfactory transparency of the final plastic articles.

10

TEST METHODS

The product properties are determined by the following methods, unless indicated otherwise:

- 15 Values of density are determined in accordance with ASTM D792 (g/cm³).

Values of melt flow rate (MFR) are determined in accordance with ASTM D1238 (g/10 min at specified temperature and weight).

- 20 Measurement method for oxygen scavenging activity

A cast film containing suitable scavenging composition is introduced into a glass bottle equipped with an optical sensor and a rubber cap.

Measurement of the oxygen level in the free headspace of the bottle is then carried out using two different techniques. One of them is a non-invasive oxygen

- 25 measurement sensor and a Fibox[®] transmitter. The other one is CheckMate 3 O₂ (Zr) CO₂-100 %.

For both of them, data are collected in parallel for at least two samples of the same composition, at regular time intervals. For each sample, the oxygen

- 30 consumption at a certain time is calculated as the difference between the oxygen content measured at that time and the oxygen measured at time 0 which was near 21 %. The oxygen consumption is then averaged over the number of samples measured for each composition and plotted against the time.

EXAMPLES

- 5 % by weight mentioned in the following examples are based on the total weight of the mixture, composition or article; parts are parts by weight;

“ex” means example; “cpex” means comparative example; MB means masterbatch; CO means compound, “D” means direct metering in the respective
10 additives.

Equipment used

The equipment used to perform the production tests of the PET cast film described below consisted of

- 15 - single screw extruder, screw diameter 25 mm
 - 1 filter changer with 40 micron filter mesh
 - 1 flat head die width 350 mm for producing a monolayer film
 - 1 horizontal calender with 3 rollers

20 Substances used

Component a: A1:

Polyethylene terephthalate (PET) having a density from 1.35 to 1.45 g/cm³ and intrinsic viscosity from 0.74 to 0.78 dl/g (ASTM D3236-88).

25 Component a: A2:

Polybutylene terephthalate (PBT) having a density from 1.28 to 1.32 g/cm³ and intrinsic viscosity from 0.90 to 1.00 dl/g (ASTM D3236-88).

Component b: B1 - B13:

- 30 The polyester-ethers were prepared using the following general procedure:

In a 500 ml multinecked flask equipped with a KPG-stirrer, a vigreux column, a vacuum supply and a distillation bridge, the chemicals according to Table 1 are

placed into the reactor under a nitrogen atmosphere and in an amount as given in Table 1. The mixture is heated to an internal temperature of 60 °C, followed by the addition of 200 µl tetraisopropyl orthotitanate.

Within 2 hours, the temperature of the reaction mixture is continuously increased to 230 °C under a weak nitrogen flow (5 l/h) and held at this temperature for 2 hours. After reaching 70 °C, methanol starts to distill off. After reaching 190 °C, ethylene glycol continuously starts to distill off. Thereafter, the N₂-flow is stopped and the pressure of the reaction mixture is continuously decreased to 400 mbar at 230 °C within 165 minutes, followed by a further continuous pressure decrease to 1 mbar within 90 minutes. In the next step, the reaction mixture is stirred at a pressure of 1 mbar and an inner temperature of 230 °C for additional 4 hours. After the end of this time period, the inner pressure of the reaction flask is set back to 1 bar using N₂ and the polymer melt is subsequently removed from the reactor and allowed to solidify.

To determine the molecular weight of the Polyester-ether, GPC measurements were done under the following conditions:

Columns:	1 x PSS SDV Guard, 5µm, 50 mm x 8.0 mm ID
	1 x PSS SDV 100 Å, 5 µm, 300 mm x 8.0 mm ID
	1 x PSS SDV 1000 Å, 5 µm, 300 mm x 8.0 mm ID
	1 x PSS SDV 100000 Å, 5 µm, 300 mm x 8.0 mm ID
Detector:	RI
Oven temperature:	40 °C
Flow:	1 ml/min
Injection volume:	50 µl
Eluent:	THF
Evaluation:	PSS-WinGPC Version 8.2
Calibration:	Polystyrene standards in the range from 682 -
	1,670,000 Dalton
Internal Standard:	Toluene
Injection concentration:	4 g/l in THF

Table 1

Sample	DMT/g	DMI/g	Poly-THF 1000/g	Poly-THF 2000/g	PEG 1000/g	PR-1000/g	MPEG 750/g	M41/g	ϵ -Caprolactone/g	1,4 Butandiol/g	EG/g	PG/g	Na-Acetate/g	ϕ	Ω	$M_w/g^{mol^{-1}}$	$M_n/g^{mol^{-1}}$
B1	48.5			50.0	25.0		25.0				125.0		0.3	0.8	1.5	17311	8073
B2	48.5			50.0	37.5		12.5				125.0		0.3	0.4	1.5	28398	12019
B3	48.5			50.0	43.8		6.3				125.0		0.3	0.2	1.5	35318	16430
B4*	48.5			50.0	50.0						125.0		0.3	0.0	1.5	39852	18412
B5	43.7	4.9		50.0	37.5		12.5				125.0		0.3	0.4	1.5	27623	11783
B6	43.7	4.9		50.0	43.8		6.3				125.0		0.3	0.2	1.5	36165	15054
B7	43.7	4.9		50.0	46.9		3.1				125.0		0.3	0.1	1.5	24979	10948
B8	48.5		50.0		37.5		12.5				125.0		0.3	0.4	1.5	27986	13604
B9	48.5			50.0		37.5	12.5				125.0		0.3	0.4	1.5	26281	11626
B10	48.5			50.0	37.5			12.5			125.0		0.3	0.4	1.5	38476	17954
B11	48.5			50.0			12.5		37.5		37.5		0.3	0.4	1.5	32345	11853
B12	48.5			50.0	37.5		12.5			29.3			0.3	0.4	1.5	28894	13465
B13	48.5			50.0			18.8		31.3		37.5		0.3	0.6	1.5	25310	10501

*B4 Comparative sample → no endcap was used for the synthesis of this polymer

5

DMT	=	Dimethyl terephthalate	MPEG 750	=	Mono methoxylated poly(ethyleneglycol)-monool
DMI	=	Dimethyl isophthalate			(average molecular weight (M_n) = 0,75 KDa)
Poly-THF 1000	=	Poly-THF-diol	M41	=	Mono methoxylated poly(ethyleneglycol)-co-poly(propyleneglycol)-monool
		(average molecular weight (M_n) = 1 KDa)			(average molecular weight (M_n) = 2000 KDa)
10 Poly-THF 2000	=	Poly-THF-diol			
		(average molecular weight (M_n) = 2 KDa)			
PEG 1000	=	Poly(ethyleneglycol)-diol	EG	=	Ethylene glycol
		(average molecular weight (M_n) = 1 KDa)	PG	=	Propylene glycol
PR 1000	=	Poly(ethyleneglycol)-co-poly(propyleneglycol)-diol			
		(average molecular weight (M_n) = 1 KDa)			

15

Component c: C1:

Cobalt stearate solid form (9.5 % Elemental cobalt concentration).

5

Component d: D1:

Surfactant

10 Masterbatches MB1 to MB10

The components were homogenized together on a Leistritz® ZSE18HP extruder at the temperature of 260 °C to obtain solid masterbatches MB; Table 2 gives the details.

Table 2

[illegible]

Preparation of cast films:

As an example of operational mode, 200 μ m cast films were obtained via extrusion by using the Colling E 25 PK by inserting the component A1, pre-dried for 18 hours at 120 °C, into the main hopper of the machine, and by adding the other components (MB and/or pure additives directly dosed) through dosing units applied to the main stream of component A1 before entering the injection unit barrel. Extruder temperatures can be kept at 260 °C and flat die temperature is 270 °C.

- 5 The operating conditions during the test were: T1 = 60 °C / T2 = 240 °C / T3 = 260 °C / T4 = 260 °C / T5 = 260 °C / T_{die} = 270 °C / T_{calenderrollers} = 70 °C/ screw revolutions 80 rpm

Table 3

15

ex-cpex	Type of material	Composition (%)		
cpex1		100 PET		
cpex2	MB	86.3 PET +	12 MB1 +	1.7 MB10
ex2	CO	7.3 PET +	91 MB2 +	
ex3	D	96.3 PET +	2 B1 +	
ex4	D		2 B2 +	
ex5	D		2 B3 +	
cpex6	D		2 B4 +	
ex7	MB	78.3 PET +	20 MB3 +	
ex8	MB		20 MB4 +	
ex9	MB		20 MB5 +	
ex10	MB		20 MB6 +	
ex11	MB		20 MB7 +	
ex12	MB		20 MB8 +	
ex13	MB		20 MB9 +	

The oxygen scavenging activity (in ml O₂ consumed per gram of scavenging composition) corresponding to the cast films was measured by the methods described above. Table 4 reports the oxygen consumption of compositions with different copolymer structures and different amount of end caps.

5

Table 4

Θ	0.0	0.2	0.4	0.8	0.4	0.6
Sample	cpex6	ex5	ex4	ex3	ex11	ex13
Day						
0	0,0	0,0	0,0	0,0	0,0	0,0
2	6,2	6,2	4,7	2,0		
3					0,8	0,6
6	24,0	20,8	17,9	6,4		
7	29,1	24,8	21,8	7,8	4,5	3,1
9	37,5	32,1	27,4	9,2		
10					13,0	6,5
12	44,7	42,2	36,0	11,8		
14	52,0	50,6	42,2	14,8	28,2	13,2
17					39,4	19,7
19	68,3	64,4	55,6	23,0		
21	71,9	70,5	60,1	27,2	50,7	26,4
23	76,8	70,5	64,5	31,4		
26	82,2	76,5	68,1	36,9		
28	91,8	78,8	71,6	40,9		

By comparison between ex3 to ex5 and cpex6 a significant dependence of the oxygen consumption rate with respect to the amount of end-caps present is observed. In general, the amount of consumed oxygen decreases when a higher amount of end-caps are introduced. The oxygen consumption rate is strongly dependent on the quantity of end-caps contained into the polyester-copolyether,

10

so one can fine-tune and control the the amount of oxygen being scavenged by increasing or reducing the amount of end-caps.

5 This effect is observed when polyester-copolyether additives are dosed together with the resin directly into the hooper of the extruder as well as when a MB is prepared.

10 Ex11 and ex13 which refer to end-cap polyesters which are different from those in ex3 to ex5 and cpex6, show exactly the same behavior: higher amounts of end-caps reflect a reduction in oxygen consumption.

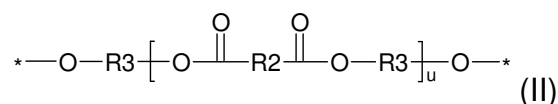
Patent Claims

1. A polyether-polyester copolymer comprising
- (i) polyether segments wherein at least one polyether segment contains at
 5 least one polytetramethylene oxide segment,
- (ii) polyester segments,
- (iii) bridging elements of the structure $-\text{CO}-\text{R}_2-\text{CO}-$, wherein R_2 represents an optionally substituted bivalent hydrocarbon residue consisting of 1 to 100 carbon atoms;
- 10 (iv) one or two end-caps $\text{R}_1-\text{O}-(\text{C}_2-\text{C}_4-\text{O})_e-$, wherein R_1 is an optionally substituted hydrocarbon residue and e is an integer of from 0 to 1000, wherein $*$ represents a bond to a bridging element (iii).

2. The polyether-polyester copolymer as claimed in claim 1, wherein the
 15 polyether segments (i) contain ethylene oxide segments, propylene oxide segments or a combination thereof.

3. The polyether-polyester copolymer as claimed in claim 1 or 2, wherein the polyester segments (ii) are represented by formula (II):

20

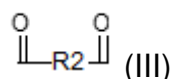


wherein

$*$ represents a bond to a bridging element (iii),

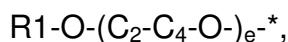
- 25 R_2 and R_3 independently of each other represent an optionally substituted hydrocarbon residue consisting of 1 to 100 carbon atoms, and u is an integer between 1 and 50.

4. The polyether-polyester copolymer as claimed in any of the preceding
 30 claims, wherein bridging elements are described by formula (III)



wherein R2 represents an optionally substituted hydrocarbon residue consisting of 1 to 100 carbon atoms.

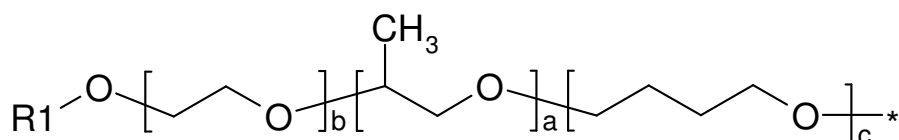
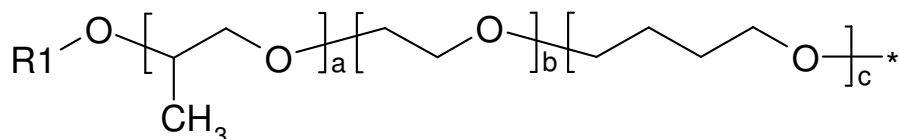
- 5 5. The polyether-polyester copolymer as claimed in any of the preceding claims, wherein end-caps are described by the following general formula



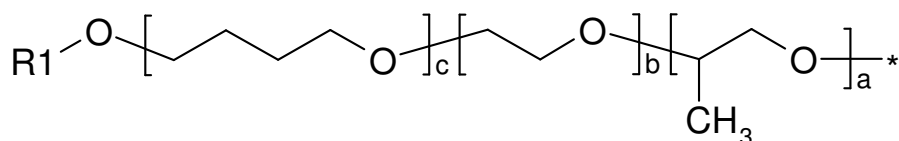
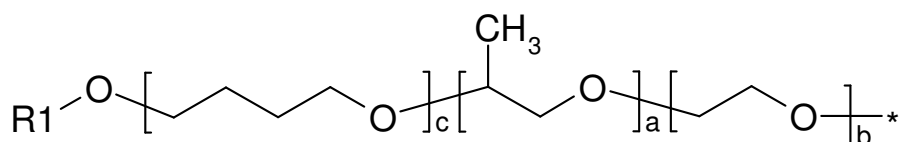
- 10 wherein R1 is an aliphatic hydrocarbon residue of 1 to 24 carbon atoms, an olefinic hydrocarbon residue of 2 to 24 carbon atoms, an aromatic hydrocarbon residue of 6 to 14 carbon atoms, wherein said hydrocarbon residues are optionally substituted with C₁-C₅-alkoxy, nitro, cyano, sulfo, or a combination thereof, and e is an integer of between 0 and 500.

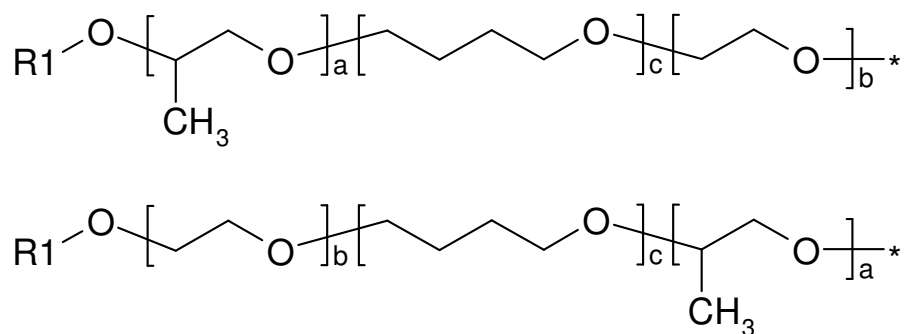
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6. The polyether-polyester copolymer as claimed in any of the preceding claims, wherein R1-(C₂-C₄-O)_e-* correspond to the following formulae



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wherein the different monomers are distributed randomly, in blocks or a

5 combination of random and block, and

b is an integer between 0 and 250,

a is an integer between 0 and 250,

c is an integer between 0 and 70,

and the sum $a+b+c$ is of from 0 to 570; and

10 R1 is as defined in claim 5.

7. The polyether-polyester copolymer as claimed in any of the preceding claims, wherein R1 denotes methyl, ethyl, n-propyl, iso-propyl, n-butyl, iso-butyl, sec-butyl, tert-butyl, n-pentyl, iso-pentyl, sec-pentyl, neo-pentyl,

15 1,2-dimethylpropyl, iso-amyl, n-hexyl, sec-hexyl, n-heptyl, n-octyl, 2-ethyl-hexyl, n-nonyl, n-decyl, tridecyl, isotridecyl, tetradecyl, hexadecyl, octadecyl, methylphenyl cyclopropyl, cyclobutyl, cyclopentyl, cyclohexyl, cycloheptyl, cyclooctyl, cyclononyl, or cyclodecyl.

20 8. The polyether-polyester copolymer as claimed in any of the preceding claims, wherein the number average of the molecular weight is between 2000 and 1000000 g/mol.

25 9. The polyether-polyester copolymer as claimed in any of the preceding claims, wherein the mass ratio Ω , defined as the mass ratio between the poly(tetramethyleneoxide) content and the overall content of all dicarbonyl structure elements (ii) and (iii) is between 0.1 and 10.

10. The polyether-polyester copolymer as claimed in any of the preceding claims, wherein the mass ratio Θ , defined as the mass ratio between the endcap content and the overall content of all dicarbonyl structure elements (ii) and (iii) is between 0.001 and 100.

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11. A method of preparing a polyether-polyester copolymer as claimed in any of the preceding claims comprising a polycondensation of the polyether segments containing at least one polytetramethylenoxide segment, the polyester segments, the bridging elements and the end-caps.

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12. An active oxygen barrier composition comprising a polyether-polyester copolymer as claimed in claims 1 to 10 and a transition metal catalyst.

13. A plastic material comprising:

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a component a) which is a thermoplastic polymer;

a component b) which is a polyether-polyester copolymer as claimed in any of claims 1 to 10; and

a component c) which is a transition metal catalyst.

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14. The plastic material as claimed in claim 13, which is a masterbatch, a compound or a formed article.

15. The plastic material as claimed in claims 13 or 14 which is or is part of a container or a film.

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