

A PROCESS FOR THE BIOTRANSFORMATION OF COLCHICONE  
COMPOUNDS INTO THE CORRESPONDING 3-GLYCOSYL DERIVATIVES

The present invention relates to the biotransformation, effected by means of selected microbial strains, of colchicinoid compounds, into the respective 3-O-glycosyl derivatives. The process of the present invention provides compounds glycosylated exclusively at C-3 of the aromatic ring A, starting from the cited colchicone compounds in high yields and purity.

The compounds obtained by the biotechnological process of the invention, particularly thiocolchicosone (3-O-glucosylthiocolchicone, i.e., with reference to formula (I),  $R_1 = -OCH_3$  e  $R_2 = -SCH_3$ ), are active principles of remarkable pharmacological importance, mainly for the preparation of new antitumor medicaments.

DISCLOSURE OF THE INVENTION

A number of efforts have been made to obtain highly specific glycosydations of compounds of general formula (I) and related colchicinoid compounds, either by means of chemical reactions or by biotransformation.

The chemical route consists in sequences of complex, non-specific reactions which, non-selectively involving different molecular sites, lead to a mixture of glycosydated derivatives, some of which being inactive. Therefore, the conversion yields to the effective product specifically glycosydated at C-3 of the aromatic ring, are very low.

The biological approach substantially relates to the biotransformation of colchicinoid compounds, (which

are indirectly related with colchicone compounds) such as colchicine and thiocolchicine, by culture of Centella Asiatica, into monoglycosydated derivatives at C-2 and at C-3 of the aromatic ring; such a transformation being therefore not highly selective and providing scarce yields and productivity (Solet, J.M., et al., Phytochemistry 33, 4, 817-820, 1993).

Other efforts to biotransform colchicinoid compounds gave simply demethylations of the methoxy groups bound to the aromatic ring (at C-2 and at C-3), anyway always characterized by limited yields and productivity and by a poor regioselectivity.

Thus, Hufford C.D. et al.. (J. Pharm. Sc., 68, 10, 1239-1242, 1979), using Streptomyces griseus and/or Streptomyces spectabilis, and Bellet P. et al.., (GB-923421, 1959), using different strains of Streptomyces and of other species of Bacteria and Fungi, tried to transform colchicine and its derivatives into the corresponding 3-demethylated derivatives. The results of these known methods confirm what stated above in connection with the non-selectivity of the microbial enzymes involved, for example at C-2, C-3 or C-10 of the alkaloid molecule. Moreover, the productivity levels of said catalytic systems are rather poor, due to the low conversion yields, the reduced substrate concentrations which can be used, and the frequent degradation of the tropolone ring.

More recently, Poulev et al.. (J. Ferment. Bioeng. 79, 1, 33-38, 1995) have obtained the specific demethylation by using bacterial microorganisms, but with still rather poor yields and productivity.

Enzyme activity from microorganisms similar to the above mentioned ones (*Streptomyces*, *Bacillus*, etc.) have been applied to the biotransformation of other compounds, such as maytansinoids (US pat. 4 361 650: 5 Izawa, M., et al., J. Antibiotics, 34, 12, 1587-1590, 1981). In this case also the catalysed reaction consists exclusively in a demethylation, characterized by low conversion yields and productivity.

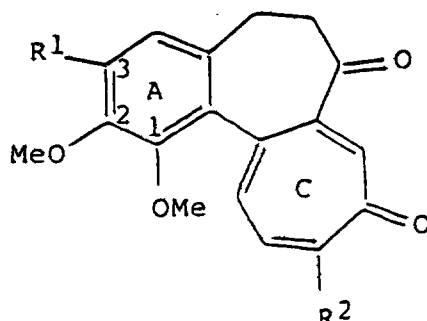
Glycosyl transferase activities of  $\alpha$ -amylase from 10 *Bacillus megaterium* strains have been described (Brumm., P.J., et al., Starch, 43, 8, 319-323, 1991), the acceptor specificity (exclusively glucose or glucosides) being particularly high. Cyclodextrin-glycosyl transferases, produced by the same microbial source, 15 catalyse a  $\alpha$ -1,4-transglucosylation of rubusoside (13-O- $\beta$ -D-glucosyl-steviol  $\beta$ -D-glucosyl ester), starting from starch. Also in this bioconversion the acceptor of the transferase reaction is the substrate glucide fraction (Darise, M., et al., Agric. Bioel. Chem., 48, 10, 2483- 20 2488, 1984). Cyclodextrin-glycosyl transferases were previously used for the preparation of cyclodextrins G6 and G8 from starch (Kitahata, S., Okada, S., Agric. Biol. Chem., 38, 12, 2413-2417, 1974).

These examples evidence the high substrate 25 specificity of the glycosyl transferase activities expressed by *Bacillus megaterium*, which involves only glucosyl acceptors, therefore not making it possible to expect any reactions on secondary metabolites having a different, complex molecular structure, such as 30 colchicones. In fact, no examples of the use of said microorganisms for the enzyme conversion of colchicone

compounds to 3-glycosyl derivatives are known.

Now it has been found that strains of Bacillus megaterium capable of growing in the presence of high concentrations of colchicone ( $R_1 = -OCH_3$ ,  $R_2 = -OCH_3$ ),  
5 3-demethyl-colchicone and respective thio derivatives, have an exceedingly high, very specific biotransformation activity of said substrates into derivatives glycosydated exclusively at C-3 of the aromatic ring. Such a transformation takes place in very  
10 short times, and is characterized by surprisingly high yields.

Therefore, the invention relates to a process for the preparation of 3-O-glycosylcolchicone compounds of formula (I):



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wherein  $R_1$  is a glycosyde residue,  $R_2$  is  $C_1-C_6$  alkoxy or  $C_1-C_6$  thioalkyl, which comprises the biotransformation of compounds in which  $R_1$  is OH or methoxy by means of Bacillus megaterium.

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Bacillus megaterium is a Gram-positive spore generating bacterium with a cell diameter higher than 1.0  $\mu m$ ; growing aerobically on a number of culture media; catalase-positive; hydrolysing gelatin. Strains of Bacillus megaterium which can be used according to the invention proved capable of growing satisfactorily



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and of keeping viable also at high concentrations of colchicone, thiocolchicone ( $R_1 = -OCH_3$ ,  $R_2 = -SCH_3$ ) and respective 3-demethyl derivatives (above 2 g/l), as evidenced by the examination of the growth and by  
5 microscope analysis. Congeneric species, such as Bacillus cereus, already at concentrations of substrate of 1 g/l evidence a difficulty in growing (absorbances of 10-15% of the control).

The high selectivity and efficiency of the  
10 biotransformation is surprising and unusual, as the yield levels range from 70% to 95%.

Moreover, the microorganisms used in the bioconversion are capable of maintaining permanently the catalytic activity, even in repeated fermentation steps,  
15 therefore providing the specific bioconversion in fed-batch and continuous processes. Therefore this method provides high productivity and reproducibility levels.

The marked reaction regioselectivity assures, in addition to the remarkable production yields, a high  
20 quality and purity of the resulting product, thus providing it in a 100% purity, with a simple downstream processing.

Further, important advantages are the reduced incidence of the step of purification and recovery of  
25 the product, the economicity of the process and the affidability and safety of use.

The operative sequences usable in the process of the invention comprise:

A) - Selection of cultures of Bacillus megaterium  
30 capable of growing in the presence of high concentrations of colchicone substrate, starting

from natural sources or from collection strains.

- 5 B) - Selection of the isolates from A), to assay the transformation catalytic activity into the corresponding 3-O-glycosyl derivatives, by means of bioconversion assays on the specific substrates, administered in gradually increasing concentrations.
- C) - Microbiological characterization of the strains selected in B).
- 10 D) - Gradual increase in the biotransformation yield, by means of a target-specific selection of the bacterial population from B).
- E) - Study and optimization of the critical fermentation parameters, to optimize the biotransformation.
- 15 F) - Study and optimization of the methods for the conservation of the high-productivity cultures, to guarantee stable, homogeneous inoculum for productive applications on the industrial scale.
- G) - Scale-up of the process in fermenter, in batch, 20 fed-batch and continuous processes.
- H) - Working up and optimization of the methods for the downstream processing and for the recovery of the product.

Specifically, the microorganisms usable in the 25 present invention can be selected starting from collection cultures obtained from strain deposit centers, or from soil samples of various origin, or from preselected industrial strains, by selective recovery on different agar media containing an organic nitrogen 30 source (peptones, yeast extracts, meat extracts, asparagine, etc), a carbon source (glycerin, starch,

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maltose, glucose, etc.), with pH 5 to 8, preferably 6 - 7. The incubation temperature ranges from 20° to 45°C, preferably 28° - 40°C.

5 The ability of the culture of growing in the presence of toxic concentrations of the colchiconic substrate to be transformed is evaluated by techniques of scalar dilution and plating in parallel, on different agarized substrates, a part of which having previously been added with the colchiconic compound (e.g.: 3-

10 demethylthiocolchicone) in concentrations from 0.1 to 3 g/l (so as to inhibit the growth of the main part of the microorganisms).

The colonies capable of growing in the described conditions are withdrawn in sterile and placed on

15 different agarized media, to verify their purity and the homogeneity of growth.

The culture media used for the conservation of the culture are typical microbiological substrates, containing organic nitrogen sources (peptones, yeast

20 extracts, tryptone, meat extracts, etc.), a carbon source (glucose, maltose, glycerin, etc.), at pH 5 to 8, preferably 6 - 7. The incubation temperature ranges from 20° to 45°C, preferably 28° - 40°C.

The selected microorganisms are then assayed for

25 the capability of growing in submerged culture, in the presence of colchiconic compounds, and of transforming the latter into the corresponding 3-glycosyl derivatives.

Said assays were carried out in 100 ml flasks

30 containing 20 ml of liquid medium, with different medium formulations, comprising one or more organic

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nitrogen sources (yeast extracts, peptones, tryptone, casein hydrolysates, meat extract, corn-steep liquor, etc.), one or more carbon sources (glucose, glycerol, starch, saccharose, etc.), inorganic phosphorous and  
5 nitrogen sources, and inorganic salts of various ions ( $K^+$ ,  $Na^+$ ,  $Mg^{++}$ ,  $Ca^{++}$ ,  $Fe^{++}$ ,  $Mn^{++}$ , etc.).

The culture samples can optionally be subjected to mutagenic treatments, by means of the conventional mutagenesis techniques (irradiation with UV rays, etc.)  
10 to induce mutants having a specific bioconversion activity which can be evaluated with the same procedure as above.

Culture samples from each bioconversion assay, were analyzed to evaluate the production of 3-glycosyl  
15 derivatives, by means of TLC and HPLC analysis.

The capability of the selected microorganism of transforming colchicone substrates into the respective 3-glycosyl derivatives was confirmed by means of bioconversion assays in flasks, in a 300 ml scale, in  
20 the same culture broths as used in the selection step.

The microorganisms which gave a positive response were used in tests for the optimization of the bioconversion, in different culture broths, in a 300 ml scale. The main cultural and fermentation parameters  
25 studied are: organic nitrogen sources, carbon sources, mineral salts, temperature, stirring-aeration, pH, incubation time, inoculum ratio, subculture steps, time and form of addition of the substrate to be transformed. The selected bacterial microorganisms, capable of  
30 effecting the biotransformation of the present invention, can grow on both solid and liquid culture

substrates, containing one or more organic nitrogen sources, preferably yeast extract, meat extract, peptone, tryptone, casein hydrolysates, corn-steep liquor; etc.. Carbon sources useful for the growth and the biotransformation are glucose, fructose, saccharose, glycerol, malt extract, etc., preferably glucose, fructose and glycerin. The culture medium contains moreover inorganic phosphorous sources and salts of  $K^+$ ,  $Na^+$ ,  $Mg^{++}$ ,  $NH_4^+$ , etc..

The selected microorganisms can grow at temperatures from  $20^\circ$  to  $45^\circ C$ , preferably from  $28^\circ$  to  $40^\circ C$ , at pH between 5 and 8, preferably 6 - 7. In the same conditions, the considered microorganisms are capable of transforming the colchiconic compounds into the corresponding 3-glycosyl derivatives. Said transformations occur in submerged culture, in flasks incubated on a rotating shaker, with stirring from 150 to 250 rpm.

Due to the particular kinetics of the biotransformation concerned, which is related to the microbial growth, the optimum conditions for the purposes of biotransformation are the same conditions which are optimum for the growth. Therefore, culture media useful to promote a good microbial growth, such as those based on the organic and inorganic components cited above, are also useful for a good activity of biotransformation of the concerned substrate. The latter is added to the culture in the starting fermentation step, or in fractional aliquots starting from the beginning of fermentation.

The biotransformation of the invention is based on

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an enzyme conversion, which starts during the growth exponential phase and continues with a parallel progression to that of the growth; the maximum levels of conversion to 3-glycosyl derivative (very high: up to 5 95%) are reached within the first 48-72 hours, depending on the addition time of the substrate. The regioselectivity of the biotransformation is absolute: no presence of 2-glycosyl derivatives has ever been evidenced in the culture samples. The resulting products 10 are exclusively extracellular.

The substrate to be transformed can be added in acetone or alcohol solution, in alcohol-water mixtures, in dioxane, etc. The biotransformation of the invention can be scaled up to fermenter level, keeping the culture 15 conditions unchanged, in particular as far as culture medium, temperature and processing times are concerned. In order to obtain good growths, adequate levels of stirring-aeration are important, in particular aeration levels of 1 - 2 litres of air per litre of culture per 20 minute (vvm), preferably of 1,5-2 vvm, are required.

The products resulting from the bioconversion are extracted from the culture broths after separation of the biomass from the liquid fraction by centrifugation and recovery of the supernatant, or microfiltration and 25 recovery of the permeate. The culture can be treated with alcohols, in view of an optimum recovery of the product.

The purification and the recovery of the biotransformation products can be carried out using 30 chromatographic techniques for the separation on absorption resins and elution with alcohols, preferably

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with methanol. The hydromethanol solutions containing the product can further be purified by extraction with lipophilic organic solvents, preferably with methylene chloride. After further treatments with mixtures of  
5 alcohols and organic solvents, the product can be obtained in the pure state from the resulting alcohol solutions by crystallization. Glucose can be replaced by other sugars, such as fructose or galactose, without causing the loss of the glycosyl transferase activity.

10 The following examples disclose the invention in further detail.

#### EXAMPLE 1

Aliquots of cultures of Bacillus megaterium, isolated from agriculture soil, are resuspended in 20  
15 ml of sterile saline, and subjected to a scalar dilution to a 1:10.000.000 dilution factor. The suspensions at various dilutions are plated on LB-Agar culture medium and on LB-Agar added respectively with thiocolchicone or 3-demethylthiocolchicone, to a final concentration of 2  
20 g/l (see Table). The cultures are incubated at +28°C, for 3-4 days, in the dark. The colonies grown on the selective medium, added with the colchicone compound, are isolated and purified by means of plating on non-selective medium; said samples are incubated as above,  
25 but for a shorter time (24 hours).

Subsequently the cultures are transferred to the same agar medium, in a test-tube, and incubated as above for 24 hours.

Aliquots of cultures, selected as described, are  
30 used to inoculate 100 ml Erlenmeyer flasks containing 20 ml of culture medium ST (Table), added with

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thiocolchicone or 3-demethylthiocolchicone, to a 0.4 mg/ml final concentration. Said cultures are incubated overnight at 28°C, on a rotary shaker, at 200 rpm.

5 The transformation of the colchicone substrate is checked by analysis of aliquots of culture broths, taken every 3 - 4 hours, by TLC on silica gel, with an acetone:ethyl acetate:water 5 : 4 : 1 eluent system.

10 After 4 day incubation, aliquots of the cultures, which proved an evident catalytic activity towards the 3-glycosyl derivative, are recovered on plates, by means of scalar dilution as described above, for the preparation of novel inocula in test-tube. The biotransformation assay in the flask is repeated in the same conditions as above, but using markedly higher  
15 final concentrations of thiocolchicone and 3-demethylthiocolchicone (1 mg/ml). The most active single cultures (substrate conversion equal to or higher than 70%) are used for the preparation of inocula in frozen cryotubes.

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Table

## Formulation of the culture media

1) LB-Agar

|               |        |
|---------------|--------|
| Tryptone      | 10 g/l |
| Yeast extract | 5 g/l  |
| 25 NaCl       | 10 g/l |
| Agar Agar     | 15 g/l |
| pH 7          |        |

Sterilization: 121°C x 20'

2) Broth ST

|            |        |
|------------|--------|
| 30 Glucose | 20 g/l |
| Glycerol   | 10 g/l |

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|   |                                       |         |
|---|---------------------------------------|---------|
|   | Peptone                               | 15 g/l  |
|   | Yeast extract                         | 5 g/l   |
|   | NaCl                                  | 3 g/l   |
|   | NH <sub>4</sub> Cl                    | 3 g/l   |
| 5 | K <sub>2</sub> HPO <sub>4</sub>       | 8 g/l   |
|   | KH <sub>2</sub> PO <sub>4</sub>       | 3 g/l   |
|   | MgSO <sub>4</sub> · 7H <sub>2</sub> O | 0,5 g/l |
|   | pH 7                                  |         |

Sterilization: 121°C x 20'

10 EXAMPLE 2

The procedure described in Example 1 is repeated, starting from Bacillus megaterium cultures, deriving from the following collection strains (Deutsche Sammlung von Mikroorganismen, Braunschweig, Germany):

- 15 DSM 90  
DSM 322  
DSM 333  
DSM 1667  
DSM 1670  
20 DSM 1671.

The cultures selected as in Example 1 and added with thiocolchicone (1 mg/ml) are incubated for 4 days in liquid culture: the TLC analysis detects the occurred transformation of the substrate into thiocolchicosone,  
25 with conversion yields varying from 30 to 70%.

EXAMPLE 3

Aliquots of culture samples in test-tube, selected as described in the above example, are used to inoculate 100 ml Erlenmeyer flasks containing 20 ml of broth ST.

30 The broth cultures are incubated at +30°C, on a rotary shaker at 200 rpm, overnight. After incubation,

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the cultures are added with a glycerol sterile solution to a 20% final concentration. The cultures are then dispensed into 2 ml cryotubes and immediately immersed in liquid nitrogen.

5       After some days, 10% of the cultures are thawed quickly at 37°C. Aliquots of each cryotube are used to inoculate 100 ml Erlenmeyer flasks containing 20 ml of medium ST, which are subsequently incubated at +28°C, overnight (preculture), at 200 rpm. After incubation, 2  
10       ml of each preculture are transferred in sterile into 20 ml of fresh medium ST, added with 3-demethylthiocolchicone to a 1 g/l final concentration. The biotransformation is carried out and checked in the conditions described in Example 1. The analysis  
15       confirmed that the transformation of the substrate into the 3-glycosyl derivative occurred in the quantitative terms described above (70% and higher), thus proving the catalytic stability of the frozen cultures.

Parallel controls of the broth cultures, plated on  
20       LB Agar immediately after thawing, confirm the viability, homogeneity and purity of the frozen cultures.

#### EXAMPLE 4

Aliquots of cultures in cryotube, after thawing,  
25       are used to inoculate 300 ml Erlenmeyer flasks containing 50 ml of medium ST (preculture). After incubation overnight at 30°C, 250 rpm, 5 ml of preculture are transferred into 50 ml of the same medium added with 3-demethyl-thiocolchicone to a 1 g/l final  
30       concentration. The cultures are incubated for 4 days, in the same conditions as described above.

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Every 4 hours, samples are taken to evaluate the growth level (measuring the absorbance at 600 nm), the thiocolchicosone production (TLC and HPLC), the sterility (on LB Agar), and for the microscope morphological examination.

TLC analysis is carried out as described in Example 1. For the HPLC analysis, 1 ml fractions of culture broths are added with 9 ml of methanol and centrifuged at 13,000 rpm for 2 minutes. The content in 3-glucosyl derivative of the supernatant is analyzed by reverse phase HPLC, with isocratic elution, by means of the water:acetonitrile 80 : 20

eluent system.

The HPLC analysis proves that, after 72-96 hours, the bioconversion of substrate to thiocolchisone is substantially completed.

The final yields to 3-glucosyl derivative, obtained by the bioconversion range from 70 to 85%.

#### EXAMPLE 5

The procedure described in Example 4 is repeated, but 3-demethylthiocolchicone is added to the cultures in two fractions: 0.25 g/l at the beginning and 0.74 g/l after 24 hours.

The growth and production responses of the cultures are similar to those obtained in Example 4, with thiocolchisone yields of about 90%.

#### EXAMPLE 6

One liter of ST broth in Erlenmeyer flask (inoculum) is inoculated with a cryotube culture. The flasks are incubated overnight at +30°C, 250 rpm. The inoculum is transferred in sterile into a 14 l

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fermenter, containing 9 l of sterile broth STL. 3-demethylthiocolchicone is added to a 1 g/l final concentration (25% at the beginning, the remainder after 20 hours). The fermentation is carried out keeping  
5 suitable levels of stirring-aeration (stirring up to 900 rpm; aeration 1 to 1.5 vvm, depending on the culture growth).

Every 2 hours, samples from the culture broths are taken and subjected to the following analysis:

- 10 - Optical density (OD) at 600 nm,
- Sterility and purity analysis of the strain (on LB Agar);
- Microscope morphology (Gram stain);
- Analysis of the thiocolchicosone content, by TLC  
15 and HPLC, as described in Examples 1 and 4, respectively.

After about 48 hour fermentation, the transformation of the substrate into thiocolchisone is almost finished. The final yield is about 85%.

#### 20 EXAMPLE 7

The procedure described in Example 6 is repeated, but after 48 hour fermentation, only 90% of the culture broths are recovered, to extract the product (fraction 1). The residual 10% is added in sterile in the fermenter with 9 l of fresh sterile medium ST containing 10 g  
25 of 3-demethylthiocolchicone. The fermentation is carried out as described in Example 6. After 48 hours, 9 l of culture broths are collected and extracted (fraction 2). The residual volume of culture broths is added sterilely  
30 with 9 more l of sterile fresh medium ST containing fresh 3-demethylthiocolchicone (10 g). The fermentation

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is carried out as above. After 48 hours the culture broth is collected completely and extracted (fraction 3). The biotransformation activity of the strain remained stable for all of the three runs, with  
5 conversion yields of about 80%.

#### EXAMPLE 8

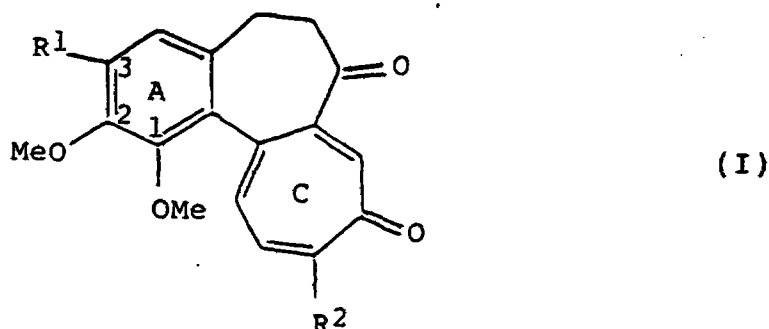
The final culture broth from the fermentation (total volume: about 27 l) is concentrated under vacuum to a soft residue and taken up with ethanol.

10 After separation by filtration, the water-ethanol fraction is concentrated to water, under vacuum, and purified by repeated extractions with methylene chloride. The aqueous fractions are concentrated and, after adjusting pH to 10 with sodium hydroxide,  
15 extracted with chloromethylene-ethanol mixtures.

The combined organic phases are concentrated under vacuum. The resulting suspension is added with ethanol, concentrated and left to crystallize. A second crystallization with ethanol is carried out after  
20 further redissolution steps of the solid in chloromethylene-ethanol mixtures.

CLAIMS

1. A process for the preparation of 3-O-glycosylcolchicone compounds of formula (I):



wherein  $R^1$  is a glycoside residue,  $R^2$  is  $C_1-C_6$  alkoxy or  $C_1-C_6$  thioalkyl, which comprises the biotransformation of compounds in which  $R_1$  is OH or methoxy by means of Bacillus megaterium.

2. A process for the preparation of the compounds of formula (I) in which  $R_1$  is an O-glucoside residue.

3. A process according to claims 1-2, wherein the Bacillus megaterium strains are selected for their capability of growing in the presence of high concentrations of colchicone substrate to be transformed.

4. A process according to claim 3 wherein said concentrations range from 0.1 to 3 g/l.

5. A process according to claims 1-4, wherein Bacillus megaterium is cultured in a solid or liquid medium.

6. A process according to claim 5, wherein said medium comprises at least one organic nitrogen source.

7. A process according to claim 6, wherein said organic nitrogen source is selected from the group consisting of meat extract, peptone, tryptone, casein



hydrolysates, corn-step water.

8. A process according to claim 5, wherein the medium comprises at least one carbon source.

5 9. A process according to claim 8, wherein said carbon source is selected from the group consisting of glucose, fructose, glycerol.

10. A process according to claim 5, wherein said medium comprises at least one source of inorganic salts of  $K^+$ ,  $Na^+$ ,  $Mg^{++}$ ,  $NH_4^+$ .

10 11. A process according to claims 1-10, which is carried out at a pH ranging from 5 to 8.

12. A process according to claim 11, wherein said pH ranges from 6 to 7.

15 13. A process according to claims 1-12, which is carried out at a temperature ranging from 20° to 45°C.

14. A process according to claim 13, wherein said temperature ranges from 28° to 40°C.

20 15. A process according to claims 1-14, which is carried out at a maximum aeration level from 1 to 2 litres of air per litre of culture per minute (vvm).

16. A process according to claim 15 wherein said level ranges from 1.5 to 2 vvm.