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SPECIFICATION



G00002

TITLE OF THE INVENTION: method for purifying tungsten hexafluoride of high purity

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TECHNICAL FIELD

The present invention relates to a method for purifying tungsten hexafluoride of high purity, and more specifically relates to a method for purifying tungsten hexafluoride of high
10 purity and removing molybdenum hexafluoride, which contaminates tungsten hexafluoride, both cheaply and efficiently.

BACKGROUND OF THE INVENTION

Known methods used as methods for purifying tungsten
15 hexafluoride are reactions of chlorides of tungsten with fluorides such as HF and AsF₃ and reactions of metal tungsten with fluorine.

If it is assumed that impurities, other than molybdenum, which have contaminated tungsten hexafluoride produced by these
20 methods are those of chlorides and fluorides, these impurities can be readily separated and removed from tungsten hexafluoride by using a difference in boiling point and vapor pressure of tungsten hexafluoride from those of these impurities. However, molybdenum has similar properties to those of tungsten because
25 molybdenum is a congener of tungsten and is therefore difficult to separate and remove by distillation.

As the method for removing molybdenum from tungsten, a method is described where a metal piece makes contact with tungsten hexafluoride at a temperature between 100 and 500°C (Japanese

Patent No.2848717). Using this method, it is necessary for all of the tungsten hexafluoride to be converted to tungsten trifluoride and a distillation tower for purification therefore has to keep the temperature in a range from 100 to 500°C. This
5 method is therefore neither suitable nor effective when running costs are taken into consideration.

Moreover, the above described technology carries out heating to a high temperature ranging from 100 to 500°C to cause decomposition of WF_6 by installation of a packed tower made of
10 SUS (stainless steel.)

The present invention provides a method for purifying tungsten hexafluoride of high purity, wherein production of tungsten hexafluoride of higher purity than in the related art is possible in a straightforward manner and at a low cost.

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DISCLOSURE OF THE INVENTION

Taking into consideration that described above, the present inventors subjected tungsten hexafluoride (material to be subject to purification) containing molybdenum hexafluoride as an
20 impurity to solid-gas reaction and / or solid-liquid reaction and solid-liquid contact under specific conditions resulting in the present invention and found a method capable of purifying tungsten hexafluoride of high purity readily, effectively, and economically.

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The present invention provides a method for purifying tungsten hexafluoride of high purity, characterized in that tungsten hexafluoride, which is the material to be purified, containing at least molybdenum hexafluoride as an impurity, makes contact with a metal or alloy containing at least one of molybdenum,

tungsten, copper, nickel, iron, cobalt, zinc, titanium, aluminum, calcium, and magnesium at a temperature ranging from 0 to 100°C.

In the present invention, the temperature at which molybdenum hexafluoride makes contact with the metal or alloy
5 is set to from 0 to 100°C.

At 100°C or higher, the rate at which impurities are removed deteriorates. On the other hand, at temperatures lower than 0°C, tungsten solidifies to cause clogging.

Within a range from 0 to 100°C, 20 to 90°C is therefore
10 preferable, and 40 to 70°C is more preferable.

Generally, a metal or an alloy is packed inside a packed tower having an introducing orifice and a discharging orifice and supplies the material to be purified from the introducing orifice in a gaseous or liquid state.

15 The temperature of the material to be purified introduced into the packed tower preferably ranges from 30 to 80°C. Creating such temperature makes controlling of the temperature within the packed tower straightforward to enable a stable purification reaction. In addition, the influence of the material to be
20 purified on a main portion of the packed tower can be reduced.

The period of time for which the material to be purified is in contact with the metal depends on the surface area of the metal used and the rate of flow of the introduced gas is preferably 5 to 10 minutes.

25 The setting of this range ensures that both reactivity and the amount processed per unit time are both desirable from an economic point of view.

The material to be purified is generally introduced into the packed tower in a gaseous state, but may also be in a liquid

state.

In the case where the material to be purified makes contact with the metal in a gaseous state, as shown in Fig. 1(a), it is preferable that the material to be purified is introduced from the bottom of the packed tower and discharged from the top of the packed tower. On the other hand, when the material to be purified makes contact with the metal in a state where there is a mixture of both gas and liquid, as shown in Fig. 1(b), it is preferable that the material to be purified is introduced from the top of the packed tower and discharged from the bottom of the packed tower.

For packing the metal in the packed tower, it is preferable, as shown in Fig. 2, that the metal 3 is packed in the packed tower 1 to form a space 2 horizontally, which is used as a path for the material to be purified 4. In a vertical-type packed tower shown in Fig. 1, the metal resists the passing of the material to be purified and introduction of the necessary amount of material to be purified (flow rate) requires a higher pressure for supplying the material to be purified. As shown in Fig. 2, if the path (space 2) for the material to be purified 4 is made in advance at the packed tower, a necessary flow can be regulated using low pressure.

Melting points and a boiling points of individual components are as shown below.

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Melting point 2°C; boiling point 17°C



Melting point 17°C; boiling point 32°C



Melting point 67; boiling point 214°C



Sublimation point 800°C

In the present invention, if the temperature at which
5 contact is made is set to the boiling point or lower of the material
to be purified, introducing the material to be purified in a
gaseous state allows the material to be purified to become a
mixture of gas and liquid, and molybdenum hexafluoride, which
has contaminated the tungsten hexafluoride, is reduced by the
10 solid-gas reaction and the solid-liquid reaction to yield stable
molybdenum pentafluoride and molybdenum trifluoride.

If the contact temperature is set to the boiling point
or lower of the material to be purified, introducing the material
to be purified in a liquid state allows the material to be purified
15 to become a liquid, and molybdenum hexafluoride, which is
contaminated with tungsten hexafluoride, is reduced by the
solid-liquid reaction to yield stable molybdenum pentafluoride
and molybdenum trifluoride.

On the other hand, if the contact temperature is set to
20 the boiling point or higher of the material to be purified,
introducing the material to be purified in the gas state allows
the material to be purified to become a gas and molybdenum
hexafluoride, which has contaminated tungsten hexafluoride, is
reduced by the solid-gas reaction to yield stable molybdenum
25 pentafluoride and molybdenum trifluoride.

If the contact temperature is set to the boiling point
or higher of the material to be purified, introducing the material
to be purified in the liquid state allows the material to be
purified to become a mixture of gas and liquid and molybdenum

hexafluoride, which has contaminated the tungsten hexafluoride, is reduced by the solid-gas reaction and solid-liquid reaction to yield stable molybdenum pentafluoride and molybdenum trifluoride.

5 Molybdenum, tungsten, copper, nickel, iron, cobalt, zinc, titanium, aluminium, calcium, and magnesium react selectively with molybdenum hexafluoride, but molybdenum hexafluoride does not react under the above described conditions.

As described above, in the present invention, it was found
10 that tungsten hexafluoride can be purified to a high degree at a temperature of 100°C or lower, which, conventionally, does not permit the yielding of tungsten hexafluoride of a high purity.

According to the present invention, molybdenum hexafluoride produces molybdenum pentafluoride and molybdenum
15 trifluoride due to a solid-gas reaction and / or solid-liquid reaction with molybdenum. However, within such a temperature range, molybdenum pentafluoride and molybdenum trifluoride exhibit a stable state and a low vapor pressure to allow molybdenum to be deposited on a packed layer resulting in collection.

20 Molybdenum hexafluoride exhibits the same reaction with tungsten, copper, nickel, iron, cobalt, zinc, titanium, aluminium, calcium, and magnesium to produce molybdenum pentafluoride and molybdenum trifluoride. Fluorides of these metals are also produced simultaneously. All these metals except tungsten
25 exhibit stable solid states and can be collected from the layer in which the metal is packed. Tungsten is not problematic because it becomes tungsten fluoride.

According to the present invention, solid-liquid contact of the material in the liquid state for purification with the

metal allows easy separation and collection of fluorides of molybdenum exhibiting a solid state at such temperatures.

According to the present invention, the metal used for removal of molybdenum hexafluoride contaminating tungsten
5 hexafluoride is not restricted in quality, but used generally in a linear, swarf, and particle state. Powder and particulate states are preferable in order that contact of the gas taken as the material to be purified and a liquefied material to be purified with the metal is improved.

10 Excessive particle size causes reactivity to be poor and a particle size of 1mm or smaller is therefore preferred. If particle size exceeds 1 mm, spaces occur between granular metals that allow fluid constituting the material to be purified to flow easily. If the fluid does not flow in a turbulent manner, the fluid will
15 always flow through the same path and will therefore always react with the same metal, which means that the reaction is not performed in a sufficient manner.

A lower limit of the particle size is preferably 1 μ m. If the particle size is smaller than 1 mm, surface area becomes large
20 excessively and causes an increase in an amount of an oxide film formed on the surface which inhibits the reaction.

Particle distribution is not restricted. Because molybdenum pentafluoride and molybdenum trifluoride produced by the reduction reaction of molybdenum hexafluoride with the metal
25 (or alloy) covers the metal (or alloy), the surface area of the metal used is preferably large. The larger the surface area of the metal (or alloy) the more molybdenum hexafluoride is collected. The particles of metal used for the packed tower are therefore preferably small in size.

According to the present invention, materials used for the packed tower and a collector are, for example, stainless steel, nickel, and copper. The packed tower is preferably cylindrical because a cylindrical shape is easy to make. Stainless steel and copper are used as the material of the pipe.

According to the present invention, the amount of molybdenum hexafluoride contaminating tungsten hexafluoride before and after purification is measured by ICP MS. The amount of molybdenum can be measured up to 0.04 ppm (detection limit.)

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BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 is a conceptual view showing a method for introducing the material to be purified to the packed tower.

Fig. 2 is a conceptual view showing a method for packing a metal in the packed tower and a method for introducing the material to be purified to the packed tower.

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BEST MODE FOR CARRYING OUT THE INVENTION

The following is a specific description of the embodiments of the present invention.

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Embodiment 1-14; Comparative Example 1-2

In a purifying step of the present invention, the source gas to be purified is passed through a metal packed tower so as to make contact and molybdenum impurities are collected. Next, purified gas is collected by a collector to yield purified tungsten hexafluoride.

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The metal-made packed tower used is made of stainless steel (SUS 316L) and has an internal diameter of 50 mm and is 1000mm

long.

1700cc of metal is packed in the packed tower.

Metals used were (1) molybdenum, (2) tungsten, (3) copper, (4) nickel, (5) iron, (6) cobalt, (7) zinc, (8) titanium, (9) aluminium, (10) calcium, and (11) magnesium.

These metals are prepared for packing in the packed tower as power with a particle size of 1 μ m.

The source gas to be purified is supplied at a rate of 1 L/ min.

10 The collector used for a purified product is cylindrical, is made of stainless steel and has an inner diameter of 75mm and a length of 500mm (SUS304).

The temperature of the collector is kept in a range from 0 to 10°C.

15 Tungsten hexafluoride is purified under the conditions shown in Table 1.

The results are shown in Table 1.

It can be seen that purification according to the method of the present invention provides very preferable removal of molybdenum hexafluoride contaminating tungsten hexafluoride.

20 After the collector is heated to 20°C and tungsten hexafluoride is vaporized to be discarded from the collector, molybdenum impurities are not collected by the collector, but are collected completely by the metal packed tower.

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Embodiment 15-26

In a purifying step of the present invention, a source gas to be purified is passed through a metal packed tower so as to make contact with the metal and molybdenum impurities are

collected. Next, the collector collects purified gas to yield purified tungsten hexafluoride.

The metal packed tower used is made of stainless steel (SUS 316L) with an inner diameter of 50 mm and a length of 1000
5 mm and the packed amount was 1700 cc.

Metals used were (1) molybdenum, (2) tungsten, and 7(3) aluminum.

These metals are prepared as grains of powder or grains of a particle size of 0.1 μ m to 1 mm.

10 The temperature for purification is 50°C.

The source gas to be purified is supplied at a rate of 1 L/ min.

The collector used for the purified product is cylindrical, and made of stainless steel with an inner diameter of 75mm and
15 a length of 500mm (SUS304).

The temperature of the collector is kept in a range from 0 to 10°C.

Tungsten hexafluoride is purified under the conditions shown in Table 2.

20 The results are shown in Table 2 and It can be seen that purification according to the method of the present invention provides very preferable removal of molybdenum hexafluoride contaminating tungsten hexafluoride.

After the collector is heated to 20°C and tungsten
25 hexafluoride is vaporized so as to be discarded from the collector, molybdenum impurities are not collected by the collector, but rather collected completely by the metal packed tower.

(Embodiments 27-36)

In the purifying step of the present invention, the material to be purified is passed in a liquid state through a metal packed tower so as to make contact with the metal and molybdenum impurities are collected. Next, the collector collects purified gas to yield
5 purified tungsten hexafluoride.

The metal packed tower used is made of stainless steel (SUS 316L) and has an inner diameter of 50 mm and is 1000 mm long, and the packed amount is 1700 cc.

Metals used are (1) hastelloy, (2) monel, (3) stainless
10 steel, (4) molybdenum, and (5) tungsten.

These metals are prepared as powder 10 μ m in size and 1 mm particle grains.

The temperature for purification is 50°C.

The source gas for purification is supplied at a rate of
15 1 L/ min.

The collector used for a purified product is cylindrical, made of stainless steel, and has an inner diameter of 75 mm and a length of 500 mm (SUS304).

The temperature of the collector is kept to a range from 0 to
20 10°C.

Tungsten hexafluoride is purified under the conditions shown in Table 3.

The results are shown in Table 3 and it can be seen that purification according to the method of the present invention
25 provides very preferable removal of molybdenum hexafluoride contaminating tungsten hexafluoride.

After the collector heated to 20 °C and tungsten hexafluoride was vaporized to discard from the collector, molybdenum impurities are not collected by the collector, but

are collected in their entirety by the metal packed tower.

INDUSTRIAL APPLICABILITY

According to the present invention, tungsten hexafluoride
5 of high purity can be obtained readily, effectively, and economically.

(Table 1)

	Purification condition		Mo concentration in WF_6	
	Temp. (°C)	Metal used	Pretreatment (ppm)	Post-treatment (ppm)
Embodiment 1	20	Molybdenum	300	<0.04
Embodiment 2	100	Molybdenum	2000	<0.04
Embodiment 3	20	Tungsten	3500	<0.04
Embodiment 4	50	Tungsten	3500	<0.04
Embodiment 5	80	Tungsten	3500	<0.04
Embodiment 6	50	Tungsten	3500	<0.04
Embodiment 7	50	Nickel	3500	<0.04
Embodiment 8	50	Iron	3500	<0.04
Embodiment 9	50	Cobalt	3500	<0.04
Embodiment 10	50	Zinc	3500	<0.04
Embodiment 11	50	Titanium	3500	<0.04
Embodiment 12	50	Aluminum	3500	<0.04
Embodiment 13	50	Calcium	3500	<0.04
Embodiment 14	50	Magnesium	3500	<0.04
Comparative Example 1	300	Tungsten	2200	10
Comparative Example 2	150	Molybdenum	300	100

(Table 2)

	Purification condition		Mo concentration in WF_6	
	Particle size	Metal used	Pretreatment (ppm)	Post-treatment (ppm)
Embodiment 15	0.1 μm	Molybdenum	300	<0.04
Embodiment 16	0.5 μm	Molybdenum	300	<0.04
Embodiment 17	1 μm	Tungsten	3500	<0.04
Embodiment 18	0.5 μm	Tungsten	3500	<0.04
Embodiment 19	1 μm	Tungsten	3500	<0.04
Embodiment 20	2 μm	Tungsten	3500	<0.04
Embodiment 21	5 μm	Tungsten	3500	<0.04
Embodiment 22	15 μm	Tungsten	3500	<0.04
Embodiment 23	1 mm	Tungsten	3500	<0.04
Embodiment 24	2 μm	Aluminum	3500	<0.04
Embodiment 25	15 μm	Aluminum	3500	<0.04
Embodiment 26	1 mm	Aluminum	3500	<0.04
Comparative Example 3	2 mm	Tungsten	2000	10
Comparative Example 4	3 mm	Molybdenum	300	30

Table 3

	Purification condition		Mo concentration in WF_6	
	Particle size	Metal used	Pretreatment (ppm)	Post-treatment (ppm)
Embodiment 27	10 μm	Hastelloy	300	<0.04
Embodiment 28	1 mm	Hastelloy	300	<0.04
Embodiment 29	10 μm	Monel	3500	<0.04
Embodiment 30	1 mm	Monel	3500	<0.04
Embodiment 31	10 μm	Stainless steel	3500	<0.04
Embodiment 32	1 mm	Stainless steel	3500	<0.04
Embodiment 33	10 μm	Tungsten	3500	<0.04
Embodiment 34	1 mm	Tungsten	3500	<0.04
Embodiment 35	10 μm	Molybdenum	3500	<0.04
Embodiment 36	1 mm	Molybdenum	3500	<0.04

WHAT IS CLAIMED IS:

1. A method for purifying tungsten hexafluoride of high purity, characterized in that tungsten hexafluoride, constituting a material to be purified, containing at least molybdenum hexafluoride as an impurity, makes contact with a metal or an alloy containing at least one of molybdenum, tungsten, copper, nickel, iron, cobalt, zinc, titanium, aluminum, calcium, and magnesium at a temperature ranging from 0 to 100°C.
2. The method for purifying tungsten hexafluoride of high purity according to claim 1, characterized in that said material to be purified makes contact with a powdered and/ or granular metal or alloy.
3. The method for purifying tungsten hexafluoride of high purity according to claim 2, characterized in that a particle size of said powdered and/ or granular metal or alloy is 1 mm or smaller.
4. The method for purifying tungsten hexafluoride of high purity according to any one of claim 1 to claim 3, characterized in that said material of purification makes contact with a metal or an alloy that is a mixture of a gas and a liquid.
5. The method for purifying tungsten hexafluoride of high purity according to any one of claim 1 to claim 3, characterized in that said tungsten hexafluoride containing molybdenum hexafluoride as an impurity makes contact with a metal or an alloy.

6. The method for purifying tungsten hexafluoride of high purity according to any one of claim 1 to claim 5, characterized in that said powdered and/ or granular metal or alloy is packed in a packed tower to create a space laterally and the space is used
5 as a path for the material to be purified.