

Description

The present invention relates to an alcohol mixture for plasticizer, a method for producing the same and a plasticizer derived from the same.

An alcohol having 10 carbon atoms (hereinafter referred to as "C₁₀ alcohol" or decyl alcohol) is prepared by subjecting a C₄ olefin to hydroformylation, aldol condensation and hydrogenation, and the alcohol thus prepared is mainly used as a starting material for preparing a plasticizer for vinyl chloride resin.

Thus, the present invention relates to a decyl alcohol mixture having generally excellent properties as a starting material for a plasticizer, a plasticizer prepared therefrom and a method for producing the same.

A decyl alcohol is prepared by hydroformylating a fraction containing 4 carbon atoms obtained in a large amount by thermal cracking or catalytic cracking of hydrocarbon oils (hereinafter referred to as "BB fraction") to obtain valeraldehydes, subjecting the valeraldehydes thus obtained to aldol condensation to obtain decenals, and finally hydrogenating the decenals thus obtained. Butenes in BB fraction include three types of 1-butene, 2-butene and isobutene. Accordingly valeraldehydes obtained by hydroformylating these butenes include a mixture of n-valeraldehyde (hereinafter referred to as "n-VAD"), 2-methylbutyraldehyde, 3-methylbutyraldehyde and pivalaldehyde (2,2-dimethylpropionaldehyde). Therefore, condensation products of valeraldehydes obtained by the hydroformylation of the BB fraction and their decyl alcohol products generally comprise mixtures of various types of isomers.

US Patent No. 2921089 and 3121051 disclose 2-propylheptanol derived from condensation products of n-valeraldehyde and decyl alcohol derived from cross-aldol condensation products of n-valeraldehyde and 2-methylbutyraldehyde, and also disclose that methods of condensation and hydrogenation may be generally conducted methods, that 2-propylheptanol is excellent as a decyl alcohol for a plasticizer, and that the cross-aldol condensation product is inferior as a starting material for a plasticizer to 2-propylheptanol but it is comparable to 2-propylheptanol if it is used as a mixture with 2-propylheptanol in an amount of up to ten several %.

Von Bernhard et al, Chemiker-Zeitung 99 Jahrgang (1975), Nr11, P452-458 and Japanese Unexamined Patent Publication No. 127335/1980 disclose about oxo reaction of butenes, and also disclose that valeraldehyde can be produced under normal hydroformylation conditions and that n-valeraldehyde can be produced selectively at a higher yield under special hydroformylation conditions.

Japanese Unexamined Patent Publication No. 206537/1983 discloses the composition of valeraldehydes and the condensation conditions for controlling the amount of the cross-aldol condensation product of n-valeraldehyde and 2-methylbutyraldehyde among 2-propylheptanols to less than 20% in order to prepare decyl alcohols having good plasticizer-aptitude from butenes, and also discloses the performance of two-component type alcohol mixture comprising 2-propylheptanol and the cross-aldol condensation product of n-valeraldehyde and 2-methylbutyraldehyde.

US-A-4426542 discloses a phthalate diester of a ten-carbon alcohol mixture consisting of 2-propylheptanol (≥ 80% of the mixture), 2-propyl-4-methylhexanol and 2-propyl-5-methylhexanol.

BB fraction industrially valuable as a C₄ olefin material includes butenes (1-butene, 2-butene and isobutene) as well as C₃ hydrocarbons, butadiene, butane, the butene concentration of which is generally from 40 to 80% by weight.

The BB fraction includes, so to speak, "spent BB fraction" prepared after extracting a substantial amount of butadiene and, so to speak, "spent spent BB fraction" prepared by further removing a part of isobutene. The butene concentration of the former is from 60 to 90% by weight and that of the latter is from 70 to 90% by weight.

However, in any case, physical properties of butenes are very similar to each other, and therefore it takes much costs to separate 1-butene, 2-butene and isobutene respectively alone, thus leading to industrial demerits.

It is therefore desirable to prepare decyl alcohols having good plasticizer-aptitude from mixed butenes including 1-butene, 2-butene and isobutene as they are.

It is known that the composition of valeraldehyde product can be controlled to some extents by appropriately selecting reaction conditions and catalysts in the hydroformylation of a C₄ olefin mixture. However, there was no method for producing a product without containing undesired specific components, and therefore the product contains all the components including n-valeraldehyde, 2-methylbutyraldehyde, 3-methylbutyraldehyde and pivalaldehyde. Accordingly, the composition of decyl alcohol produced therefrom becomes a mixture of many types of isomers.

It is therefore desired to selectively produce a decyl alcohol mixture comprising isomers having good plasticizer-aptitude from the above four types of valeraldehydes in industrially advantageous manner.

An object of the present invention is to provide a decyl alcohol mixture of isomers having good properties as a starting material for plasticizer.

Another object of the present invention is to provide a method for producing a decyl alcohol mixture of isomers having good plasticizer-aptitude from the above four types of valeraldehydes in industrially advantageous manner.

Still other object of the present invention is to provide a plasticizer having generally excellent properties.

Thus, the present invention, in a broad sense, resides in a C_{10} alcohol mixture for plasticizer, which comprises 2-propylheptanol (hereinafter referred to as "PRH"), an alcohol having a structure of condensation product of n-valeraldehyde and 2-methylbutyraldehyde (hereinafter referred to as "Component A"), an alcohol having a structure of condensation product of n-valeraldehyde and 3-methylbutyraldehyde (hereinafter referred to as "Component B"), an alcohol having a structure of condensation product of n-valeraldehyde and pivalaldehyde (hereinafter referred to as "Component C"), and other C_{10} alcohols (hereinafter referred to as "Component D"), characterized in that the respective components are present in the following molar ratios:

Component A/PRH = 0.04-1

Component B/PRH = 0.002-0.3

Component C/PRH = 0.001-0.3

Component D/PRH $\leq$ 0.3.

The present invention further resides in a plasticizer obtained by esterifying the above C_{10} alcohol mixture with a carboxylic acid.

The present invention still further resides in a method for producing a C_{10} alcohol mixture for plasticizer, which comprises subjecting butene fraction to hydroformylation, aldol condensation and hydrogenation, characterized in that an aldehyde composition participated in said condensation comprises C_5 aldehydes in the following molar ratios,

2-Methylbutyraldehyde/n-VAD = 0.02-0.3

3-Methylbutyraldehyde/n-VAD = 0.001-0.05

Pivalaldehyde/n-VAD = 0.0005-0.05

(wherein n-VAD means n-valeraldehyde)

and that the conversion of each C_5 aldehyde is at least 90%.

The present invention is described in more detail hereinafter.

The C_{10} alcohol mixture of the present invention is characterized in that the above respective Components A to D are present in the following molar ratios:

Component A/PRH = 0.04-1

Component B/PRH = 0.002-0.3

Component C/PRH = 0.001-0.3

Component D/PRH $\leq$ 0.3.

A method for producing the alcohol for plasticizer of the present invention is not specially limited so long as the above each component is within the above-mentioned composition ranges. For example, the alcohols for plasticizer of the present invention include C_{10} alcohols obtained by hydroformylation and hydrogenation of C_9 olefins obtained by trimerization of propylene or copolymerization of olefins including the reaction of C_4 olefin with C_5 olefin; C_{10} alcohols obtained by subjecting C_4 olefins to hydroformylation, aldol condensation and hydrogenation; or an alcohol mixture prepared from these products by adjusting the mixing ratio of each component.

A method for producing a decyl alcohol mixture of the present invention in industrially advantageous manner, which comprises subjecting butene fraction as a C_4 olefin to hydroformylation, aldol condensation and hydrogenation, is more concretely explained hereinafter.

"Butene fraction" used as a starting material, includes BB fractions containing butenes as the main component, such as BB fraction obtained by thermal cracking of hydrocarbon oils including naphtha or BB fraction obtained by catalytic cracking (FCC) of hydrocarbon oils including heavy or light oils.

In addition to the above starting materials, spent BB fraction obtained by removing the majority of butadiene from the above-mentioned BB fraction of the thermal cracking or catalytic cracking, spent BB fraction obtained by further removing a part of isobutene therefrom and a mixture thereof can also be favorably used.

The alcohol for plasticizer of the present invention is a C_{10} alcohol mixture having the specific composition, and can be obtained by subjecting the above-mentioned butene fraction to hydroformylation, aldol condensation and hydrogenation.

The hydroformylation is carried out in the accordance with a normal method. The hydroformylating conditions are not specially critical, but any of the conventionally known rhodium method and the cobalt

method can be used. However, it is economically advantageous that the ratio of α -form in the valeraldehyde product is larger. In the case of the rhodium method, any of an organic salt such as rhodium acetate, and an inorganic salt such as rhodium nitrate or a complex such as hydridecarbonyl tris(triphenylphosphine) rhodium can be used as the rhodium source. In the case of the cobalt method, an organic acid salt such as cobalt laurate, an inorganic acid salt such as cobalt nitrate and a complex such as dicobalt octacarbonyl, hydride cobalt tetracarbonyl can be used.

The reaction pressure is generally from normal pressure to 300 kg/cm²G, the reaction temperature being generally from 50 to 150 °C, H₂/CO ratio being generally from 1 to 10 by molar ratio and the catalyst concentration being generally from several ppm to several % by weight. Trivalent organophosphorus compounds such as triphenyl phosphine, triphenyl phosphite or their oxides can be used as a ligand to the abovementioned catalyst in a molar ratio of generally from 1 to 1000 to the catalyst.

A solvent may not be used, but may be used if necessary. Any solvent can be used if it dissolves the catalyst and does not have an adverse influence on the reaction. Examples of the solvent include aromatic hydrocarbons such as benzene, toluene, xylene, dodecylbenzene; cycloaliphatic hydrocarbons such as cyclohexane; ethers such as dibutylether, ethylene glycol dimethylether, diethylene glycol diethylether, triethylene glycol dimethylether, tetrahydrofuran; and esters such as diethylphthalate, dioctylphthalate. Aldehydes or alcohols formed in the hydroformylation can also be used as a solvent. High boiling point by products such as polymerization-condensation products of aldehydes can also be used.

The reaction can be carried out by either continuous or batch wise manner.

By distillation, the valeraldehyde products can be recovered and their composition can be controlled.

It is known that the reaction speed of each component of butenes is different from each other in the hydroformylation and that the ratio of α -aldehyde and isovaldehyde can be varied to some extent by varying the reaction conditions.

Accordingly, the composition of a valeraldehyde mixture can be controlled to some extent by employing appropriate reaction conditions. Each component of the valeraldehyde mixture has a boiling point difference of 10-20 °C, and the composition can be controlled also by normal distillation.

In order to obtain the alcohol mixture for plasticizer of the present invention, the valeraldehyde mixture participated in aldol condensation should preferably have the following molar ratios,

2-Methylbutyraldehyde/n-VAD = 0.02-0.3, preferably 0.05-0.3,

3-Methylbutyraldehyde/n-VAD = 0.001-0.05, preferably 0.001-0.03, and

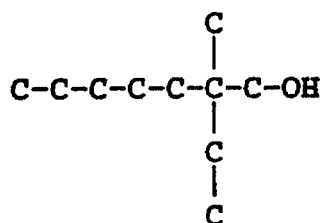
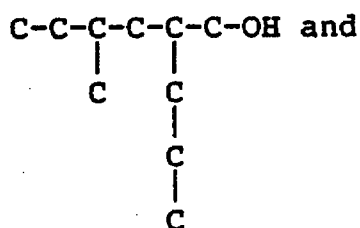
Pivalaldehyde/n-VAD = 0.0005-0.05, preferably 0.001-0.03.

The aldol condensation is usually carried out by using an alkaline aqueous solution such as sodium hydroxide, potassium hydroxide as a catalyst, but amines also can be used. The reaction temperature is generally from 50 to 150 °C, the reaction pressure being generally from normal pressure to several kg/cm²G and the reaction time being from several minutes to several hours. The conversion rate of each component of the valeraldehyde mixture should preferably be about at least 90%, more preferably at least 95%.

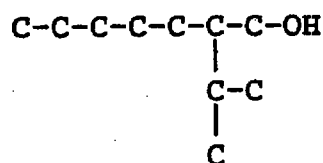
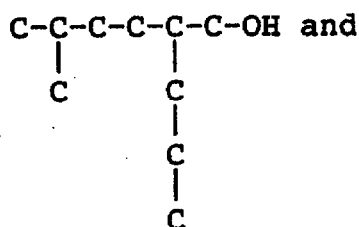
The condensation speeds of valeraldehydes other than n-valeraldehyde are relatively slow, and therefore the mutual condensation of valeraldehydes other than n-valeraldehyde or the dimerization of the other valeraldehydes themselves do not substantially occur. However, the cross-aldol condensation with n-valeraldehyde in the above-mentioned C₅ aldehyde composition relatively speedily occurs, thereby producing a decenal mixture having the desired composition. The decenal mixture is thereafter subjected to hydrogenation. The hydrogenation can be carried out in usual manner. That is, the hydrogenation is carried out in the presence of a usual hydrogenation catalyst such as Ni, Cr, Cu, under a pressure of from normal pressure to 150 kg/cm²G at a temperature of from 40 to 300 °C.

Thereafter, the C₁₀ alcohol mixture of the present invention can be obtained by general distillation refining.

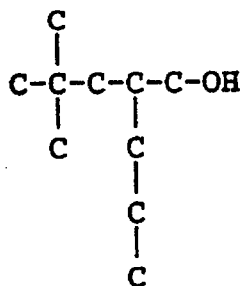
The C₁₀ alcohol mixture for plasticizer of the present invention comprises not only 2-propylheptanol (PRH) but also an alcohol having a structure of condensation and hydrogenation product of n-valeraldehyde and 2-methylbutyraldehyde (Component A):



an alcohol having a structure of condensation and hydrogenation product of n-valeraldehyde and 3-methylbutyraldehyde (Component B):



an alcohol having a structure of condensation and hydrogenation product of n-valeraldehyde and pivalaldehyde (Component C):



and other C₁₀ alcohols (Component D)

(In the above chemical structural formulas, every hydrogen atoms bonded to carbon atoms are omitted), the respective components being present in the following molar ratios:

Component A/PRH = 0.04-1.0, preferably 0.05-1.0, more preferably 0.1-0.7;

Component B/PRH = 0.002-0.3 preferably 0.002-0.3, more preferably 0.002-0.1;

Component C/PRH = 0.001-0.3 preferably 0.002-0.3, more preferably 0.002-0.1; and

Component D/PRH ≤ 0.3 , preferably not more than 0.1.

The above prepared decyl alcohol mixture is then esterified with phthalic anhydride in the presence of a titanium type catalyst, acidic catalyst (p-toluene sulfonic acid) in usual manner to produce phthalic acid ester usable as a plasticizer. Examples of other plasticizers derived from the C₁₀ alcohol mixture of the present invention include aromatic carboxylic acid esters prepared by the esterification reaction of the C₁₀ alcohol mixture with aromatic carboxylic acids such as pyromellitic anhydride, trimellitic anhydride or the like, and aliphatic dibasic acid esters prepared by the esterification reaction of the C₁₀ alcohol mixture with aliphatic dibasic acids such as adipic acid, azelaic acid, sebacic acid.

It is known that decyl alcohol containing 2-propylheptanol as the main component is generally superior in heat resistance to widely used 2-ethylhexanol for plasticizer, but is inferior in electric resistance and plasticizing efficiency.

The performance of plasticizer should be totally evaluated in view of

- ① Plasticizing efficiency (100% modulus)
- ② Evaporation loss (heat resistance)
- ③ Cold flex temperature (cold resistance)
- ④ Kerosine extraction (oil resistance) and
- ⑤ Electric resistance (electrical insulating properties)

It should not be evaluated from single property, for example, heat resistance only.

Among the above properties, some properties, for example, properties ② and ⑤ tend to be contrary each other, and are complicated. The decyl alcohol mixture prepared by the present invention include structures of 2- or 3-methylbutyraldehyde and pivalaldehyde in a small amount, thus providing an alcohol for plasticizer having generally excellent properties.

[EXAMPLE]

Now, the present invention will be described in detail with reference to Examples. However, it should be understood that the present invention is by no means restricted to such specific Examples.

REFERENCE EXAMPLE 1

(1) Synthesis of 2-propylheptanol

Commercially available genuine n-valeraldehyde was subjected to condensation reaction. The condensation was carried out batch wise for 30 minutes at 95°C under normal pressure in the presence of 3% sodium hydroxide aqueous solution/n-valeraldehyde = 1 (weight ratio).

The conversion of n-valeraldehyde was 99.9%.

Decenal obtained after liquid-liquid separation was hydrogenated in the presence of a nickel type solid catalyst. The hydrogenation was batch wise conducted for 3.0 hours at 100°C under pressure of 100 kg/cm²G in the presence of the catalyst/decenal = 0.1 (weight ratio). The conversion of decenal was 99.9%.

The crude 2-propylheptanol thus obtained was rectified by a glass-made Oldershaw type distillation tower having 30 plates, thereby obtaining the refined 2-propylheptanol under the conditions of initial cut 1%, main fraction 96% and ending cut 4%.

(2) Synthesis of plasticizer and evaluation thereof

2-Propylheptanol obtained in the above step (1) and phthalic anhydride were esterified in usual manner to prepare a plasticizer.

The plasticizer thus prepared was mixed with vinyl chloride resin in a ratio of plasticizer/vinyl chloride resin = 67/100 (weight ratio) in usual manner to prepare a soft type vinyl chloride resin, and the vinyl chloride resin was subjected to various tests by a usual method to evaluate various properties of the resin.

The test results are shown in Table 1. The same test results with regard to commonly used plasticizer, di-2-ethylhexylphthalate (DOP) are also shown in Table 1.

EXAMPLE 1

Spent spent BB fraction having the following composition prepared by removing the majority of butadiene and isobutene from BB fraction produced from a naphtha cracker was continuously hydroformylated under the following conditions.

Composition: 1-butene 43 wt%

2-butene 22
isobutene 4
butadiene 1.3
C₃'s 0.3
others 29.4

Reaction Conditions:

Total pressure 7kg/cm²G
Oxo gas partial pressure 4 kg/m²G (H₂/CO = 1),
Reaction temperature: 100 °C

Catalyst liquor

Rhodium catalyst (concentration 300
ppm (calculation as Rh atom))
Triphenylphosphine (concentration
30 % by weight)
Solvent: xylene

Feed/catalyst liquor = 10 (weight ratio)

Reactor residence time: 2.0 hours

After depressurizing the reaction liquor, the valeraldehyde mixture thus produced was recovered by distillation in substantially total amount, the molar ratios of which were as follows:

2-Methylbutyraldehyde/n-VAD = 0.1

3-Methylbutyraldehyde/n-VAD = 0.02

Pivalaldehyde/n-VAD = 0.01

The resultant valeraldehyde mixture, as it is, was then subjected to condensation reaction in a 10 l autoclave for 1.5 hours at 95 °C under normal pressure in the presence of 3% sodium hydroxide aqueous solution/aldehyde = 1 (weight ratio).

The conversion of each aldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	99.8
3-Methylbutyraldehyde	99.8
Pivalaldehyde	98.2

The decenal mixture thus obtained was hydrogenated in the same manner as in Reference Example 1 to obtain a decyl alcohol mixture, and the resultant decyl alcohol mixture was refined. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 1.

The composition of this decyl alcohol mixture was analyzed by capillary gaschromatography, and had the following molar ratio as a result.

Component A/PRH = 0.22

Component B/PRH = 0.045

Component C/PRH = 0.022

Component D/PRH = 0.01

EXAMPLE 2

The same starting material as used in Example 1 was hydroformylated in the same manner as in Example 1, except that the total pressure was 18 kg/cm²G and the oxo gas partial pressure was 15 kg/cm² (H₂/CO = 1). The molar ratio of the valeraldehyde mixture thus produced was as follows:

2-Methylbutyraldehyde/n-VAD = 0.5

3-Methylbutyraldehyde/n-VAD = 0.1

Pivalaldehyde/n-VAD = 0.1

The resultant valeraldehyde mixture was rectified by a glass-made Oldershaw type distillation tower having 90 plates to distill out a part of the respective pivalaldehyde, 2-methylbutyraldehyde and 3-methylbutyraldehyde, thereby obtaining a mixture having the following molar ratio.

2-Methylbutyraldehyde/n-VAD = 0.2

3-Methylbutyraldehyde/n-VAD = 0.03

Pivalaldehyde/n-VAD = 0.02

The resultant mixture having the above molar ratio was subjected to condensation under the same conditions as in Example 1.

The conversion of each aldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	99.0
3-Methylbutyraldehyde	98.5
Pivalaldehyde	98.0

The decenal mixture thus obtained was hydrogenated in the same manner as in Reference Example 1 to obtain a decyl alcohol mixture, and the resultant decyl alcohol mixture was refined. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 1.

The composition of this decyl alcohol mixture was analyzed by capillary gaschromatography, and had the following molar ratio as a result.

Component A/PRH = 0.48

Component B/PRH = 0.073

Component C/PRH = 0.05

Component D/PRH = 0.02

EXAMPLE 3

Spent BB fraction having the following composition prepared by removing butadiene from BB fraction produced from a naphtha cracker was hydroformylated to produce a valeraldehyde mixture under the same conditions as in Example 1, except that the reaction temperature was 110 °C.

The composition of the starting material:

1-butene 24.3 wt%

2-butene 13.1

isobutene 51.5

butadiene 0.02

C₃'s 0.15

others 10.93

The molar ratios of the valeraldehyde mixture thus produced were as follows:

2-Methylbutyraldehyde/n-VAD = 0.3

3-Methylbutyraldehyde/n-VAD = 0.03

Pivalaldehyde/n-VAD = 0.04

The resultant valeraldehyde mixture was then subjected to condensation reaction under the same conditions as in Example 1, except that the concentration of sodium hydroxide aqueous solution was made 5%.

The conversion of each aldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	99.1
3-Methylbutyraldehyde	98.3
Pivalaldehyde	97.8

The decenal mixture thus obtained was hydrogenated in the same manner as in Example 1 to obtain a decyl alcohol mixture, and the resultant decyl alcohol mixture was refined. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 1.

The composition of this decyl alcohol mixture was analyzed by capillary gaschromatography, and had the following molar ratio as a result.

Component A/PRH = 0.93
 Component B/PRH = 0.09
 Component C/PRH = 0.12
 Component D/PRH = 0.03

REFERENCE EXAMPLE 2

The valeraldehyde mixture (before rectified) obtained by the hydroformylation in Example 2 was subjected to condensation, hydrogenation and refining to produce a decyl alcohol mixture. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 1.

The conversion of each aldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	92.2
3-Methylbutyraldehyde	93.5
Pivalaldehyde	91.8

The composition of the decyl alcohol mixture had the following molar ratio as a result.

Component A/PRH = 1.3
 Component B/PRH = 0.3
 Component C/PRH = 0.3
 Component D/PRH = 0.03

REFERENCE EXAMPLE 3

A decyl alcohol mixture was prepared in the same manner as in Reference Example 1, except that a commercially available mixture of n-valeraldehyde and 2-methylbutyraldehyde (1:0.1 weight ratio) was used as a starting material for condensation. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 1.

The conversion of each valeraldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	99.2

The composition of the decyl alcohol mixture had the following molar ratio.

Component A/PRH = 0.22
 Component B/PRH = 0
 Component C/PRH = 0
 Component D/PRH = 0.01

REFERENCE EXAMPLE 4

A decyl alcohol mixture was prepared in the same manner as in Reference Example 1, except that a commercially available mixture of n-valeraldehyde: 2-methylbutyraldehyde: 3-methylbutyraldehyde (1:0.3:0.02 weight ratio) was used as a starting material for condensation and hydrogenation. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 1.

The conversion of each valeraldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	99
3-Methylbutyraldehyde	98.5

The composition of the decyl alcohol mixture had the following molar ratio.

Component A/PRH = 0.88

Component B/PRH = 0.058

Component C/PRH = 0

Component D/PRH = 0.03

Table 1

	Refer- ence Exam- ple 1	Refer- ence Exam- ple 1 (DOP)	Exam- ple 1	Exam- ple 2	Exam- ple 3	Refer- ence Exam- ple 2	Refer- ence Exam- ple 3	Refer- ence Exam- ple 4
	Refer- ence Exam- ple 1							
	n-VAD (genuine)							
Composition of VAD participated in condensation (molar ratio)	2-Methylbutyr- aldehyde/n-VAD		0.1	0.2	0.3	0.5	0.1	0.3
	3-Methylbutyr- aldehyde/n-VAD		0.02	0.03	0.03	0.1	0	0.02
	Pivalaldehyde/ n-VAD		0.01	0.02	0.04	0.1	0	0
Alcohol composition (molar ratio)	Component A/ PRH	2-Ethyl- hexanol	0.22	0.48	0.93	1.3	0.22	0.88
	Component B/ PRH		0.045	0.073	0.09	0.3	0	0.058
	Component C/ PRH		0.022	0.05	0.12	0.3	0	0
	Component D/ PRH		0.01	0.02	0.03	0.03	0.01	0.03

Table 1 (continued)

	Refer- ence Exam- ple 1	Refer- ence Exam- ple 1 (DOP)	Exam- ple 1	Exam- ple 2	Exam- ple 3	Refer- ence Exam- ple 2	Refer- ence Exam- ple 3	Refer- ence Exam- ple 4
Evaluation of plasticizer properties	100% Modulus (kg/cm ²)	77	64	68	68	65	70	68
	Evapo- ration loss (%) 1 day	0.9	4.2	0.9	1.2	1.3	3.8	1.1
	loss (%) 6 days (87°C)	4.5	19.8	4.9	5.8	5.7	18.9	5.0
	Cold flex temperature (°C)	-39	-38	-39	-37	-36	-30	-38
	Kerosine extraction (%) (23°C x 1 day)	61	44.6	42.1	40.3	38.2	53	60
	Electric resistance (x 10 ¹² Ω·m)	6.3	12.5	13.5	15.3	18.4	18.2	7.4

EXAMPLE 4

Spent spent BB fraction having the following composition prepared by removing the majority of butadiene and isobutene from BB fraction produced from a naphtha cracker was continuously hydrofor-

mylated under the following conditions.

Composition: 1-butene 43 wt%
2-butene 22
isobutene 0.71
butadiene 1.3
C₃'s 0.3
others 32.7

Reaction Conditions: Total pressure 9 kg/cm²G
Oxo gas partial pressure 4 kg/cm²G (H₂/CO = 1);
Reaction temperature: 100 °C

Catalyst liquor { Rhodium catalyst (concentration 300
ppm (calculation as Rh atom))
Triphenylphosphine (concentration
30% by weight)
Solvent: xylene

Feed/catalyst liquor = 10 (weight ratio)

Reactor residence time: 2.0 hours

After depressurizing the reaction liquor, the valeraldehyde mixture thus produced was recovered by distillation in substantially total amount, the molar ratios of which were as follows:

2-Methylbutyraldehyde/n-VAD = 0.1

3-Methylbutyraldehyde/n-VAD = 0.0030

Pivalaldehyde/n-VAD = 0.0048

The resultant valeraldehyde mixture, as it is, was then subjected to condensation reaction in a 10 l autoclave for 1.7 hours at 95 °C under normal pressure in the presence of 3% sodium hydroxide aqueous solution/aldehyde = 1 (weight ratio).

The conversion of each aldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	99.8
3-Methylbutyraldehyde	97.5
Pivalaldehyde	99.4

The decenal mixture thus obtained was hydrogenated in the same manner as in Reference Example 1 to obtain a decyl alcohol mixture, and the resultant decyl alcohol mixture was refined. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 2.

The composition of this decyl alcohol mixture was analyzed by capillary gaschromatography, and had the following molar ratio as a result.

Component A/PRH = 0.22

Component B/PRH = 0.004

Component C/PRH = 0.011

Component D/PRH = 0.01

EXAMPLE 5

Spent spent BB fraction having the following composition prepared by removing the majority of butadiene and isobutene from BB fraction produced from a naphtha cracker was continuously hydroformylated under the following conditions.

Composition: 1-butene 43 wt%

2-butene 22
isobutene 0.68
butadiene 1.3
C₃'s 0.3
others 32.7

Reaction Conditions: Total pressure 8 kg/cm²G
Oxo gas partial pressure 4 kg/cm²G (H₂/CO = 1),
Reaction temperature: 100 °C

Catalyst liquor { Rhodium catalyst (concentration 300
ppm (calculation as Rh atom))
Triphenylphosphine (concentration
30% by weight)
Solvent: xylene

Feed/catalyst liquor = 10 (weight ratio)

Reactor residence time: 2.0 hours

After depressurizing the reaction liquor, the valeraldehyde mixture thus produced was recovered by distillation in substantially total amount, the molar ratios of which were as follows:

2-Methylbutyraldehyde/n-VAD = 0.1

3-Methylbutyraldehyde/n-VAD = 0.003

Pivalaldehyde/n-VAD = 0.0026

The resultant valeraldehyde mixture, as it is, was then subjected to condensation reaction in a 10 l autoclave for 1.8 hours at 95 °C under normal pressure in the presence of 3% sodium hydroxide aqueous solution/aldehyde = 1 (weight ratio).

The conversion of each aldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	99.8
3-Methylbutyraldehyde	97.5
Pivalaldehyde	99.4

The decenal mixture thus obtained was hydrogenated in the same manner as in Reference Example 1 to obtain a decyl alcohol mixture, and the resultant decyl alcohol mixture was refined. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 2.

The composition of this decyl alcohol mixture was analyzed by capillary gaschromatography, and had the following molar ratio as a result.

Component A/PRH = 0.22

Component B/PRH = 0.004

Component C/PRH = 0.006

Component D/PRH = 0.01

EXAMPLE 6

Spent spent BB fraction having the following composition prepared by removing the majority of butadiene and isobutene from BB fraction produced from a naphtha cracker was continuously hydroformylated under the following conditions.

Composition: 1-butene 57.9 wt%
2-butene 7.1
isobutene 0.68

Reaction Conditions:

butadiene 1.3
 C₃'s 0.3
 others 32.7
 Total pressure 7 kg/cm²G
 Oxo gas partial pressure 4 kg/cm²G (H₂/CO = 1),
 Reaction temperature: 100 °C

Catalyst liquor

Rhodium catalyst (concentration 300
 ppm (calculation as Rh atom))
 Triphenylphosphine (concentration
 30% by weight)
 Solvent: xylene

Feed/catalyst liquor = 10 (weight ratio)

Reactor residence time: 2.0 hours

After depressurizing the reaction liquor, the valeraldehyde mixture thus produced was recovered by distillation in substantially total amount, the molar ratios of which were as follows:

2-Methylbutyraldehyde/n-VAD = 0.04

3-Methylbutyraldehyde/n-VAD = 0.0025

Pivalaldehyde/n-VAD = 0.0025

The resultant valeraldehyde mixture, as it is, was then subjected to condensation reaction in a 10 l autoclave for 1.8 hours at 95 °C under normal pressure in the presence of 3% sodium hydroxide aqueous solution/aldehyde = 1 (weight ratio).

The conversion of each aldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	99.8
3-Methylbutyraldehyde	97.0
Pivalaldehyde	98.2

The decenal mixture thus obtained was hydrogenated in the same manner as in Reference Example 1 to obtain a decyl alcohol mixture, and the resultant decyl alcohol mixture was refined. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 2.

The composition of this decyl alcohol mixture was analyzed by capillary gaschromatography, and had the following molar ratio as a result.

Component A/PRH = 0.08

Component B/PRH = 0.004

Component C/PRH = 0.006

Component D/PRH = 0.01

EXAMPLE 7

Spent spent BB fraction having the following composition prepared by removing the majority of butadiene and isobutene from BB fraction produced from a naphtha cracker was continuously hydroformylated under the following conditions.

Composition: 1-butene 59 wt%
 2-butene 6.0
 isobutene 1.2
 butadiene 1.3
 C₃'s 0.3

Reaction Conditions: others 32.2
Total pressure 5 kg/cm²G
Oxo gas partial pressure 4 kg/cm²G (H₂/CO = 1),
Reaction temperature: 100 °C

Catalyst liquor { Rhodium catalyst (concentration 300
ppm (calculation as Rh atom))
Triphenylphosphine (concentration
30% by weight)
Solvent: xylene

Feed/catalyst liquor = 10 (weight ratio)

Reactor residence time: 2.0 hours

After depressurizing the reaction liquor, the valeraldehyde mixture thus produced was recovered by distillation in substantially total amount, the molar ratios of which were as follows:

2-Methylbutyraldehyde/n-VAD = 0.03

3-Methylbutyraldehyde/n-VAD = 0.005

Pivalaldehyde/n-VAD = 0.0014

The resultant valeraldehyde mixture, as it is, was then subjected to condensation reaction in a 10 l autoclave for 1.8 hours at 95 °C under normal pressure in the presence of 3% sodium hydroxide aqueous solution/aldehyde = 1 (weight ratio).

The conversion of each aldehyde was as follows:

n-Valeraldehyde	99.9%
2-Methylbutyraldehyde	99.8
3-Methylbutyraldehyde	99.8
Pivalaldehyde	98.2

The decenal mixture thus obtained was hydrogenated in the same manner as in Reference Example 1 to obtain a decyl alcohol mixture, and the resultant decyl alcohol mixture was refined. Various properties of a plasticizer prepared from this decyl alcohol mixture were evaluated and the results are shown in Table 2.

The composition of this decyl alcohol mixture was analyzed by capillary gaschromatography, and had the following molar ratio as a result.

Component A/PRH = 0.06

Component B/PRH = 0.01

Component C/PRH = 0.003

Component D/PRH = 0.001

Table 2

	Exam- ple 4	Exam- ple 5	Exam- ple 6	Exam- ple 7
2-Methylbutyr- aldehyde/n-VAD	0.1	0.1	0.04	0.03
3-Methylbutyr- aldehyde/n-VAD	0.0030	0.0030	0.0025	0.0050
Pivalaldehyde/ n-VAD	0.0048	0.0026	0.0025	0.0014
Component A/ PRH	0.22	0.22	0.08	0.06
Component B/ PRH	0.004	0.004	0.004	0.01
Component C/ PRH	0.011	0.006	0.006	0.003
Component D/ PRH	0.01	0.01	0.01	0.001
Composition of VAD participated in condensation (molar ratio)				
Alcohol composition (molar ratio)				

Table 2 (continued)

	Exam- ple 4	Exam- ple 5	Exam- ple 6	Exam- ple 7
Evaluation of plasticizer properties	100% Modulus (kg/cm ²)	72	70	69
	Evapo- ration loss (%)	0.9	0.95	0.85
	1 day			
	6 days	5.0	4.9	4.9
	Cold flex temperature (°C)	-39	-39	-40
	Kerosine extraction (%) (23°C x 1 day)	45.1	45.0	45.8
	Electric resistance (x 10 ¹² Ω·m)	13.2	10.9	11.0
				9.2

REFERENCE EXAMPLE 5

A plasticizer was prepared in the same manner as in Reference Example 1, except that the esterification in the step (2) was carried out by using adipic acid in place of phthalic anhydride.

The plasticizer thus prepared was then mixed with vinyl chloride resin in a ratio of plasticizer/vinyl chloride resin = 43/100 (weight ratio) in usual manner to prepare a soft type vinyl chloride resin, and the vinyl chloride resin was subjected to various tests by a usual method to evaluate various properties of the resin.

The test results are shown in Table 3. The same test results with regard to commonly used plasticizer, di-2-ethylhexyladipate (DOA) are also shown in Table 3.

EXAMPLE 8

A plasticizer was prepared by esterifying the decyl alcohol mixture produced in Example 1 with adipic acid as used in Reference Example 5. Various properties of the plasticizer thus prepared were evaluated in the same manner as above, and the results are shown in the following Table 3.

EXAMPLE 9

A plasticizer was prepared by esterifying the decyl alcohol mixture produced in Example 4 with adipic acid as used in Example 8. Various properties of the plasticizer thus prepared were evaluated in the same manner as above, and the results are shown in the following Table 3.

REFERENCE EXAMPLE 6

A plasticizer was prepared by esterifying the decyl alcohol mixture produced in Reference Example 2 with adipic acid as used in Example 8. Various properties of the plasticizer thus prepared were evaluated in the same manner as above, and the results are shown in the following Table 3.

Table 3

	Refer- ence Exam- ple 5	Refer- ence Exam- ple 5 (DOA)	Exam- ple 8	Exam- ple 9	Refer- ence Exam- ple 6
	(n-VAD genuine)		0.1	0.1	0.5
2-Methylbutyr- aldehyde/n-VAD					
3-Methylbutyr- aldehyde/n-VAD			0.02	0.0030	0.1
Pivalaldehyde/ n-VAD			0.01	0.0048	0.1
A Component/ PRH	PRH	2-Ethyl- hexanol	0.22	0.22	1.3
B Component/ PRH			0.045	0.004	0.3
Component C/ PRH			0.022	0.011	0.3
Component D/ PRH			0.01	0.01	0.03
Composition of VAD participated in condensation (molar ratio)					
Alcohol composition (molar ratio)					

Table 3 (continued)

	Refer- ence Exam- ple 5	Refer- ence Exam- ple 5 (DOA)	Exam- ple 8	Exam- ple 9	Refer- ence Exam- ple 6
Evaluation of plasticizer properties	100% Modulus (kg/cm ²)	129	85	87	113
	Evapo- ration loss (%) 1 day	2.3	14.0	2.1	10.9
	loss (%) 6 days	12.7	72.8	12.5	60.7
	Cold flex temperature (°C)	-43	-46	-44	-39
	Kerosine extraction (%) (23°C x 1 day)	65.0	67.1	59.1	72.4
	Electric resistance (x 10 ¹⁰ Ω·m)	1.9	3.5	5.1	10.1

As mentioned above, alcohol having generally excellent properties as a starting material for plasticizer can be prepared in accordance with the method of the present invention.



Claims

1. A C₁₀ alcohol mixture for plasticizer, which comprises 2-propylheptanol (hereinafter referred to as "PRH"), an alcohol having a structure of condensation and hydrogenation product of n-valeraldehyde and 2-methylbutyraldehyde (hereinafter referred to as "Component A"), an alcohol having a structure of condensation and hydrogenation product of n-valeraldehyde and 3-methylbutyraldehyde (hereinafter referred to as "Component B"), an alcohol having a structure of condensation and hydrogenation product of n-valeraldehyde and pivalaldehyde (hereinafter referred to as "Component C"), and other C₁₀ alcohols (hereinafter referred to as "Component D"), characterized in that the respective components are present in the following molar ratios:
 Component A/PRH = 0.04-1.0
 Component B/PRH = 0.002-0.3
 Component C/PRH = 0.001-0.3
 Component D/PRH ≤ 0.3.
2. The C₁₀ alcohol mixture for plasticizer according to Claim 1, wherein the molar ratios of the respective components are:
 Component A/PRH = 0.05-1.0
 Component B/PRH = 0.002-0.3
 Component C/PRH = 0.002-0.3
 Component D/PRH ≤ 0.1.
3. The C₁₀ alcohol mixture for plasticizer according to Claim 1, wherein said C₁₀ alcohol mixture is obtained by subjecting butene fraction to hydroformylation, aldol condensation and hydrogenation.
4. A plasticizer obtained by esterifying a carboxylic acid with a C₁₀ alcohol mixture which comprises 2-propylheptanol (hereinafter referred to as "PRH"), an alcohol having a structure of condensation and hydrogenation product of n-valeraldehyde and 2-methylbutyraldehyde (hereinafter referred to as "Component A"), an alcohol having a structure of condensation and hydrogenation product of n-valeraldehyde and 3-methylbutyraldehyde (hereinafter referred to as "Component B"), an alcohol having a structure of condensation and hydrogenation product of n-valeraldehyde and pivalaldehyde (hereinafter referred to as "Component C"), and other C₁₀ alcohols (hereinafter referred to as "Component D"), wherein the respective components are present in the following molar ratios:
 Component A/PRH = 0.04-1
 Component B/PRH = 0.002-0.3
 Component C/PRH = 0.001-0.3
 Component D/PRH ≤ 0.3.
5. The plasticizer according to Claim 4, wherein the molar ratios of the respective components in said C₁₀ alcohol mixture are:
 Component A/PRH = 0.05-1.0
 Component B/PRH = 0.002-0.3
 Component C/PRH = 0.002-0.3
 Component D/PRH ≤ 0.1.
6. The plasticizer according to Claim 4, wherein said carboxylic acid is at least one selected from the group consisting of phthalic acid, aromatic carboxylic acid and aliphatic dibasic acid.
7. A method for producing a C₁₀ alcohol mixture for plasticizer, which comprises subjecting butene fraction to hydroformylation, aldol condensation and hydrogenation, characterized in that an aldehyde composition participated in said condensation comprises C₅ aldehydes in the following molar ratios,
 2-Methylbutyraldehyde/n-VAD = 0.02-0.3
 3-Methylbutyraldehyde/n-VAD = 0.001-0.05
 Pivalaldehyde/n-VAD = 0.0005-0.05
 (wherein n-VAD means n-valeraldehyde)
 and that the conversion of each C₅ aldehyde is at least 90%.



8. The method according to Claim 7, wherein said butene fraction is selected from the group consisting of BB fraction obtained by thermal cracking of hydrocarbon oil and BB fraction obtained by catalytic cracking of hydrocarbon oil.
9. The method according to Claim 7, wherein said hydroformylation is carried out in the presence of a rhodium catalyst.
10. The method according to Claim 7, wherein said aldol condensation is carried out in the presence of an alkali catalyst.
11. The method according to Claim 7, wherein said aldehyde composition participated in said condensation comprises C_5 aldehydes in the following molar ratios,
 $2\text{-Methylbutyraldehyde/n-VAD} = 0.05\text{-}0.3$
 $3\text{-Methylbutyraldehyde/n-VAD} = 0.001\text{-}0.03$
 $\text{Pivalaldehyde/n-VAD} = 0.001\text{-}0.03$
 (wherein n-VAD means n-valeraldehyde).
12. The method according to Claim 7, wherein the conversion of each C_5 aldehyde in the condensation is at least 95%.

Patentansprüche

1. Ein C_{10} -Alkoholgemisch für Weichmacher, umfassend 2-Propylheptanol (im folgenden als "PRH" bezeichnet), einen Alkohol mit einer Struktur des Produkts der Kondensation und Hydrierung von n-Valeraldehyd und 2-Methylbutyraldehyd (im folgenden als "Komponente A" bezeichnet), einen Alkohol mit einer Struktur des Produkts der Kondensation und Hydrierung von n-Valeraldehyd und 3-Methylbutyraldehyd (im folgenden als "Komponente B" bezeichnet), einen Alkohol mit einer Struktur des Produkts der Kondensation und Hydrierung von n-Valeraldehyd und Pivalaldehyd (im folgenden als "Komponente C" bezeichnet) und andere C_{10} -Alkohole (im folgenden als "Komponente D" bezeichnet), dadurch gekennzeichnet, daß die jeweiligen Komponenten in den folgenden molaren Verhältnissen vorliegen:
 $\text{Komponente A/PRH} = 0,04\text{-}1,0$
 $\text{Komponente B/PRH} = 0,002\text{-}0,3$
 $\text{Komponente C/PRH} = 0,001\text{-}0,3$
 $\text{Komponente D/PRH} \leq 0,3$
2. C_{10} -Alkoholgemisch für Weichmacher gemäß Anspruch 1, wobei die molaren Verhältnisse der jeweiligen Komponenten wie folgt sind:
 $\text{Komponente A/PRH} = 0,05\text{-}1,0$
 $\text{Komponente B/PRH} = 0,002\text{-}0,3$
 $\text{Komponente C/PRH} = 0,002\text{-}0,3$
 $\text{Komponente D/PRH} \leq 0,1$
3. C_{10} -Alkoholgemisch für Weichmacher gemäß Anspruch 1, wobei das erwähnte C_{10} -Alkoholgemisch erhalten wurde, indem man eine Butenfraktion der Hydroformylierung, Aldolkondensation und Hydrierung unterwirft.
4. Weichmacher, erhalten durch Veresterung einer Carbonsäure mit einem C_{10} -Alkoholgemisch, umfassend 2-Propylheptanol (im folgenden als "PRH" bezeichnet), einen Alkohol mit einer Struktur des Produkts der Kondensation und Hydrierung von n-Valeraldehyd und 2-Methylbutyraldehyd (im folgenden als "Komponente A" bezeichnet), einen Alkohol mit einer Struktur des Produkts der Kondensation und Hydrierung von n-Valeraldehyd und 3-Methylbutyraldehyd (im folgenden als "Komponente B" bezeichnet), einen Alkohol mit einer Struktur des Produkts der Kondensation und Hydrierung von n-Valeraldehyd und Pivalaldehyd (im folgenden als "Komponente C" bezeichnet) und andere C_{10} -Alkohole (im folgenden als "Komponente D" bezeichnet), dadurch gekennzeichnet, daß die jeweiligen Komponenten in den folgenden molaren Verhältnissen vorliegen:
 $\text{Komponente A/PRH} = 0,04\text{-}1,0$
 $\text{Komponente B/PRH} = 0,002\text{-}0,3$



Komponente C/PRH = 0,001-0,3
 Komponente D/PRH $\leq$ 0,3

5. Weichmacher gemäß Anspruch 4, wobei die molaren Verhältnisse der jeweiligen Komponenten in dem C₁₀-Alkoholgemisch wie folgt sind:
 Komponente A/PRH = 0,05-1,0
 Komponente B/PRH = 0,002-0,3
 Komponente C/PRH = 0,002-0,3
 Komponente D/PRH $\leq$ 0,1
6. Weichmacher gemäß Anspruch 4, wobei die Carbonsäure mindestens eine ist, ausgewählt aus der Gruppe, bestehend aus Phthalsäure, aromatische Carbonsäure und aliphatische dibasische Säure.
7. Verfahren zur Herstellung eines C₁₀-Alkoholgemisches für Weichmacher, wobei eine Butenfraktion der Hydroformylierung, Aldolkondensation und Hydrierung unterworfen wird, dadurch gekennzeichnet, daß eine an der Kondensation teilnehmende Aldehydzusammensetzung C₅-Aldehyde in den folgenden molaren Verhältnissen umfaßt:
 2-Methylbutyraldehyd/n-VAD = 0,02-0,3
 3-Methylbutyraldehyd/n-VAD = 0,001-0,05
 Pivalaldehyd/n-VAD = 0,0005-0,05
 (wobei n-VAD für n-Valeraldehyd steht), und daß die Umwandlung des jeweiligen C₅-Aldehyds mindestens 90 % beträgt.
8. Verfahren gemäß Anspruch 7, wobei die Butenfraktion ausgewählt ist aus der Gruppe, bestehend aus durch thermisches Cracken von Kohlenwasserstofföl erhaltene BB-Fraktion und durch katalytisches Cracken von Kohlenwasserstofföl erhaltene BB-Fraktion.
9. Verfahren gemäß Anspruch 7, wobei die Hydroformylierung in Gegenwart eines Rhodiumkatalysators durchgeführt wird.
10. Verfahren gemäß Anspruch 7, wobei die Aldolkondensation in Gegenwart eines Alkali-Katalysators durchgeführt wird.
11. Verfahren gemäß Anspruch 7, wobei die an der Kondensation teilnehmende Aldehydzusammensetzung C₅-Aldehyde in den folgenden molaren Verhältnissen umfaßt:
 2-Methylbutyraldehyd/n-VAD = 0,05-0,3
 3-Methylbutyraldehyd/n-VAD = 0,001-0,03
 Pivalaldehyd/n-VAD = 0,001-0,03
 (wobei n-VAD für n-Valeraldehyd steht).
12. Verfahren gemäß Anspruch 7, wobei die Umwandlung jedes C₅-Aldehyds in der Kondensation mindestens 95 % beträgt.

Revendications

1. Mélange d'alcools en C₁₀ pour plastifiant, comprenant du propyl-2 heptanol (dénommé ci-après "PRH"), un alcool ayant une structure de produit de condensation et d'hydrogénation de n-valéraldéhyde et méthyl-2 butyraldéhyde (dénommé ci-après "Composant A"), un alcool ayant une structure de produit de condensation et d'hydrogénation de n-valéraldéhyde et méthyl-3 butyraldéhyde (dénommé ci-après "Composant B"), un alcool ayant une structure de produit de condensation et d'hydrogénation de n-valéraldéhyde et pivalaldéhyde (dénommé ci-après "Composant C"), et d'autres alcools en C₁₀ - (dénommés ci-après "Composant D"), caractérisé en ce que les composants respectifs sont présents dans les rapports molaires suivants:
 Composant A/PRH = 0,04-1,0
 Composant B/PRH = 0,002-0,3
 Composant C/PRH = 0,001-0,3
 Composant D/PRH $\leq$ 0,3.



2. Mélange d'alcools en C₁₀ pour plastifiant selon la revendication 1, dans lequel les rapports molaires des composants respectifs sont:
Composant A/PRH = 0,05-1,0
Composant B/PRH = 0,002-0,3
Composant C/PRH = 0,002-0,3
Composant D/PRH ≤ 0,1.
3. Mélange d'alcools en C₁₀ pour plastifiant selon la revendication 1, dans lequel ledit mélange d'alcools en C₁₀ est obtenu en soumettant la fraction butène à l'hydroformylation, l'aldolisation et l'hydrogénation.
4. Plastifiant obtenu par estérification d'un acide carboxylique avec un mélange d'alcools en C₁₀ qui comprend du propyl-2 heptanol (dénommé ci-après "PRH"), un alcool ayant une structure de produit de condensation et d'hydrogénation de n-valéraldéhyde et méthyl-2 butyraldéhyde (dénommé ci-après "Composant A"), un alcool ayant une structure de produit de condensation et d'hydrogénation de n-valéraldéhyde et méthyl-3 butyraldéhyde (dénommé ci-après "Composant B"), un alcool ayant une structure de produit de condensation et d'hydrogénation de n-valéraldéhyde et pivalaldéhyde (dénommé ci-après "Composant C"), et d'autres alcools en C₁₀ (dénommés ci-après "Composant D"), caractérisé en ce que les composants respectifs sont présents dans les rapports molaires suivants:
Composant A/PRH = 0,04-1
Composant B/PRH = 0,002-0,3
Composant C/PRH = 0,001-0,3
Composant D/PRH ≤ 0,3.
5. Plastifiant selon la revendication 4, dans lequel les rapports molaires des composants respectifs dudit mélange d'alcools en C₁₀ sont:
Composant A/PRH = 0,05-1,0
Composant B/PRH = 0,002-0,3
Composant C/PRH = 0,002-0,3
Composant D/PRH ≤ 0,1.
6. Plastifiant selon la revendication 4, dans lequel ledit acide carboxylique est au moins un acide sélectionné dans le groupe comprenant l'acide phthalique, l'acide carboxylique aromatique et l'acide dibasique aliphatique.
7. Méthode de production d'un mélange d'alcools en C₁₀ pour plastifiant, qui comprend l'hydroformylation, l'aldolisation et l'hydrogénation de la fraction butène, caractérisée en ce qu'une composition d'aldéhydes, intervenant dans ladite condensation, comprend des aldéhydes en C₅ dans les rapports molaires suivants:
Méthyl-2 butyraldéhyde/n-VAD = 0,02-0,3
Méthyl-3 butyraldéhyde/n-VAD = 0,001-0,05
Pivalaldéhyde/n-VAD = 0,0005-0,05
(où n-VAD signifie n-valéraldéhyde)
et que la conversion de chaque aldéhyde en C₅ est au moins de 90%.
8. Méthode selon la revendication 7, dans laquelle ladite fraction butène est sélectionnée dans le groupe comprenant une fraction BB obtenue par craquage thermique d'huile d'hydrocarbure, et une fraction BB obtenue par craquage catalytique d'huile d'hydrocarbure.
9. Méthode selon la revendication 7, dans laquelle l'hydroformylation est réalisée en présence d'un catalyseur au rhodium.
10. Méthode selon la revendication 7, dans laquelle l'aldolisation est réalisée en présence d'un catalyseur comprenant un alcali.
11. Méthode selon la revendication 7, dans laquelle ladite composition d'aldéhydes, intervenant dans ladite condensation, comprend des aldéhydes en C₅ dans les rapports molaires suivants:
Méthyl-2 butyraldéhyde/n-VAD = 0,05-0,3



Méthyl-3 butyraldéhyde/n-VAD = 0,001-0,03
Pivalaldéhyde/n-VAD = 0,001-0,03
(où n-VAD signifie n-valéraldéhyde)

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12. Méthode selon la revendication 7, dans laquelle la conversion de chaque aldéhyde en C₅ dans la condensation est au moins de 95%.

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