

HIGHLY POROUS AEROGELS

FIELD OF THE INVENTION

5 **[001]** The present invention lies in the field of highly porous carbon aerogels, their synthesis and use, particularly for the treatment of waste water.

BACKGROUND

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[002] Carbon-based aerogels have attracted much attention due to their low density, high electrical conductivity, porosity, specific surface area, and chemical stability. They demonstrate a great potential for the removal of pollutants and the separation of oil and water. Usually, there are three main methods to fabricate carbon aerogels. The pyrolysis of organic aerogels in an
15 inert atmosphere is a traditional method, which only can produce fragile carbon aerogels with high density. Carbon nanotubes (CNT) sponges or its derivative sponges fabricated by chemical vapor deposition (CVD) show high absorption capacities for oils as well as for organic solvents. However, the expensive precursors and complex equipments dramatically hamper the large-scale production of these carbon-based aerogels for real world applications. Graphene oxide
20 (GO), a precursor for graphene, which can be produced in large scale can be assembled into three dimensional structures through self-gelation. The aerogels show a high adsorption capacity and a good recyclability. However, the use of large amounts of chemicals and production of acidic waste during preparation of GO the methods is not satisfying.

25 **[003]** Natural materials, due to their low cost, rich source, and non-toxicity are attracting more and more attention in producing carbon-based materials. For example, raw cotton fiber contains cellulose as main ingredient and little impurities such as proteinaceous materials, waxes, pectins and small amounts of organic acids and ash producing inorganic materials. Raw cotton fibers have been investigated on adsorbing dyes, heavy metals, and heavy oils as well.
30 However, many disadvantages, such as poor buoyancy characteristics, relatively low oil sorption capacity, low hydrophobicity, and bad recyclability have been observed. These disadvantages hamper its application in removal of pollutants and the separation of oils and water.

35 **[004]** Thus, there is a need for a facile and cost-saving excess to highly porous aerogels with high adsorption capacity and hydrophobicity.

SUMMARY OF THE INVENTION

[005] In a first aspect, the present invention provides a method for manufacturing highly porous aerogels, wherein the method comprises the steps of:

- (i) providing a carbon raw material; and
- (ii) heating the carbon raw material under inert gas atmosphere and reduced pressure up to 900 °C.

[006] In another aspect, the present invention is directed to highly porous aerogels obtainable by the method as disclosed herein.

[007] In a further aspect, the present invention relates to the use of said highly porous aerogels for treating waste water.

[008] In a still further aspect, the present invention relates to a method for the treatment of waste water, comprising

- (i) contacting the highly porous aerogel described herein with the waste water; and
- (ii) separating the treated waste water from the aerogel.

DETAILED DESCRIPTION OF THE FIGURES

[009] **Figure 1: A)** High-magnification image of the cotton and **B)** High-magnification image of the TCF aerogel containing the twisted fiber structure.

[010] **Figure 2:** Sorption efficiency of the TCF aerogel for various organic liquids. The weight gain is defined as the weight ratio of the absorbate to the dried TCF aerogel.

[011] **Figure 3:** Sorption efficiency of the CMB aerogel on various organic liquids. The weight gain here is defined as the weight ratio of the absorbate to the dried CMB aerogel.

DETAILED DESCRIPTION OF THE PRESENT INVENTION

[012] The present invention is based on the inventors' surprising finding that heating a carbon raw material, particularly cotton, under inert gas atmosphere and reduced pressure up to 900 °C provides for a highly porous and hydrophobic, non-toxic aerogel with a high surface. Due to its hydrophobicity the obtained aerogel adsorbs a wide range of organic solvents and oils with excellent recyclability using facile distillation, burning, or squeezing methods. The aerogel still

possesses high adsorption capacity after five cycles. The route to manufacture these aerogels, as described herein, is facile and environmentally sustainable, as no additional expensive and complex purification steps are required and no waste is produced during the manufacture. Additionally, the starting materials, such as cotton and wastepaper, are easy to obtain and cost-effective.

[013] For certain applications, such as in Li-ion batteries and super capacitors, for water splitting, chemical and bio-sensing, nanodevices, and reaction catalysis, the obtained aerogels can further be modified with nanomaterials, such as 2D materials like graphene; metal dichalcogenides including MoS₂, TiS₂, WS₂, TaS₂, WSe₂, TiSe₂, and TaSe₂; metal particles and alloys, such as Au, Ag, Pt, Pd, Cu, AuAg alloy, and PtPd alloy; and metal oxide particles, such as nickel oxide, manganese oxide, iron oxide, zinc oxide, and TiO₂.

[014] For applications in energy storage devices and environmental protection, particularly in waste water treatment, the aerogels can be used without further modifications and purification.

[015] Without wishing to be bound to a specific theory, it is believed that the above outlined advantageous properties of the aerogels are attributable to the specific production method described herein, particularly the features of reduced pressure and inert gas atmosphere, as well as to the selection of the used carbon raw material.

[016] Based on this finding, in a first aspect the present invention thus relates to a method for manufacturing a highly porous aerogel, the method comprising:

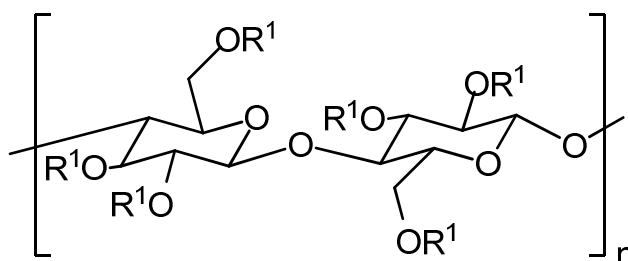
- (i) providing a carbon raw material; and
- (ii) heating the carbon raw material under inert gas atmosphere and reduced pressure up to 900 °C.

[017] The term “highly porous aerogel”, as used herein, relates to aerogels based on the chemical element carbon with open pores and a high porosity (up to ca. 99.5 %) which are flexible and have a sponge-like texture. The structure of the obtained aerogel depends on the carbon raw material used as starting material. In case cotton is used as the carbon raw material, the obtained aerogel has an interconnected twisted carbon fiber (TCF) structure. The fibers in such a TCF aerogel show a diameter of 5 to 10 µm and a twisted morphology with a pitch length in the range of 10 to 20 µm. These fibers are cross-linked. When paper is used as carbon raw material the resulting aerogel shows the same structure as the TCF aerogel, but the fibers of the manufactured aerogel are belt-like and not twisted. Most of the belt-like fibers are 5 to 10 µm wide and are cross-linked with each other resulting in advantageous mechanical properties, such as stiffness. This type of aerogel is referred to herein as a carbon microbelt (CMB) aerogel and is obtained by using paper and/or wastepaper as carbon raw material. The

aerogels have, due to their structure and porosity, a large surface area which makes them particularly suitable for the uses according to the present invention.

[018] The term “carbon raw material”, as used herein, refers to the starting material of the aerogels as disclosed herein. In various embodiments, carbohydrates, in particular polysaccharides are used as the carbon raw material. In various embodiments of the present invention, the carbon raw material is a cellulosic material. In general the term “cellulosic material”, as used herein, relates to cellulose and various cellulose derivatives as well as mixtures thereof.

[019] Cellulose is a polysaccharide with a linear chain consisting of $\beta(1,4)$ linked D-glucose units and has the following Formula (I)

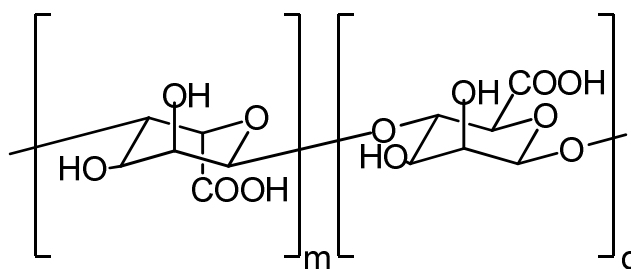


Formula (I)

wherein n is from 25 to 10,000, preferably from 50 to 5,000 and each R^1 is hydrogen.

[020] The term “cellulose derivate”, as used herein, relates to an organic compound of Formula (I), wherein n is from 25 to 50,000 and each R^1 in each unit is independently selected from the group consisting of hydrogen, a linear or branched, substituted or unsubstituted alkyl with 1 to 6 carbon atoms, and $-N(R^a)(R^b)$ with the proviso that at least one of R^1 is not hydrogen. Each R^a and R^b is independently selected from the group consisting of linear or branched alkyl with 1 to 6 carbon atoms. In a preferred embodiment each R^1 is independently selected from the group consisting of methyl and ethyl. In a further preferred embodiment each R^a and R^b of $-N(R^a)(R^b)$ is independently selected from the group consisting of methyl and ethyl. In various embodiments, n is from 50 to 5,000.

[021] Alternatively, in another embodiment, the polysaccharide may be alginic acid. Alginic acid is a linear copolymer with homopolymeric blocks of (1,4)-linked β -D-mannuronate and its C-5 epimer α -L-guluronate residues, respectively, covalently linked together in different sequences or blocks. Alginic acid has the Formula (II)



Formula (II)

wherein m and o are independently from each other 1 to 25,000. Alginic acid is distributed widely in the cell walls of brown algae, where it forms together with water a viscous gum.

[022] In accordance with the present invention, all carbon raw materials wherein cellulose or a cellulosic material is the main ingredient can be used. "Main ingredient", as used in this context, means, in various embodiments, that the cellulose/cellulosic material makes up at least 75 weight-% of the carbon raw material. Consequently, in various embodiments, the carbon raw material is selected from the group consisting of cotton, paper, wastepaper, hemp fiber, pulp, starch, brown algae, and mixtures thereof.

[023] According to the present invention, cotton may be used as the carbon raw material. Cotton is a natural fiber obtained from the hair of the seed plants of the genus *Gossypium*. Cotton contains cellulose as main ingredient and further ingredients like proteins, waxes and other plant debris. Cotton as described herein may be used naturally or, alternatively, treated by conventional chemical and/or mechanical methods. Preferably, natural, untreated cotton is used.

[024] In other embodiments, paper may be used as the carbon raw material. Papers are flexible sheets obtained by pressing together moist fibers, typically cellulose pulp derived from wood, rags or grasses, to form sheets and subsequently drying said sheets. Optionally, papers may further comprise glue and fillers and may comprise papers as they are, for example, used in books, documents, newspapers, cardboards, and the like.

[025] Further, in accordance with the present invention, wastepaper may be used as the carbon raw material. "Wastepaper", as used herein, relates to paper as defined above which has been discarded after use, for example originating from discarded books, newspapers, packages and the like.

[026] In still further embodiments, hemp fibers can be used as the carbon raw material. These fibers are fibers from the bast of cannabis which is a genus of flowering plants including the single species *Cannabis sativa*.

5 [027] In another embodiment, pulp may be used as carbon raw material. The term "pulp", as used herein, refers to a fibrous slurry with cellulose as main ingredient prepared by chemical and mechanical separation from wood or wastepaper. Typically, the slurry is an aqueous slurry.

10 [028] In still other embodiments, starch may be used as the carbon raw material. Starch is a carbohydrate consisting of a large number of glucose units joined by glycosidic bonds. This polysaccharide is *inter alia* produced by plants and is contained in large amounts in potatoes, corn, wheat, and rice.

15 [029] In still further embodiments, brown algae can be used as carbon raw material which are a large group of mostly marine multicellular algae including many seaweeds of colder Northern Hemisphere waters, such as *Macrocystis*, *Sargassum*, and *Ascophyllum nodosum*. These algae contain alginic acid in large amounts.

20 [030] The carbon raw material is selected depending on the desired properties of the aerogel. All carbon raw materials disclosed herein are in principle suitable to provide for aerogels with a high hydrophobic property and porosity, but the obtained aerogels may vary with respect to their molecular structure.

25 [031] In step (i) of the method described herein, a carbon raw material is provided. This step may comprise treatments necessary to prepare the carbon raw material for the heating in step (ii). Consequently, the providing step may for example include washing and drying the raw material. Thus, in a preferred embodiment of the invention, the providing step (i) comprises washing and/or drying the carbon raw material. The carbon raw material can be washed with any solvent or solvent mixtures which are suitable to remove undesired compounds and
30 substances, such as without limitation contaminants, from said raw materials. Washing as used herein includes contacting the material with a detergent, including water, by, for instance, wetting, rinsing, or dipping. The purpose of washing the carbon raw material is to remove compounds and substances from the carbon raw material which may have a negative impact during the subsequent steps, for example in that they decrease porosity or interfere with the
35 aerogel formation. The compounds and materials that are to be removed include any kind of dirt, dust, and/or inorganic or organic contamination. In a preferred embodiment the carbon raw material is washed with deionized water. If desired, the washing may be carried out at elevated temperature.

[032] If the contaminating substance, as described above, is volatile, the organic raw material may also be purified by heating. Such contaminants which may be removed by a heating step may include, for example, organic solvents. The heating temperature can be adjusted depending on the actual contaminant.

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[033] In various embodiments, the washed carbon raw material is dried and the solvent used for washing is removed. In a preferred embodiment, drying in step (i) is conducted at a temperature from about 10 °C to about 200 °C. In a more preferred embodiment drying in step (i) is conducted at a temperature from about 20 °C to about 150 °C and in an even more preferred embodiment drying is conducted at a temperature from about 40 °C to about 90 °C.

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[034] Optionally, the drying in step (i) can be conducted under reduced pressure, for example, when the carbon raw material is temperature sensitive. Therefore, the drying in step (i) can be conducted in a glove-box.

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[035] As a further option the drying step of step (i) can be conducted by freeze-drying.

[036] "About", as used herein, refers to the numerical value it relates to $\pm 10\%$.

[037] In step (ii) of the method disclosed herein, the carbon raw material is heated under inert gas atmosphere and reduced pressure. In general, an "inert gas", as used herein, refers to a gas that does not undergo chemical reactions with the carbon raw material under a set of given reaction conditions. Thus, in principle all gases that satisfy this requirement can be used, including without limitation noble gases, such as helium or argon, and nitrogen. Preferably, nitrogen or argon is used.

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[038] Before the carbon raw material is heated the carbon raw material is inserted into a reaction vessel suitable for carrying out step (ii). The reaction vessel has to be an airtight and heatable reaction vessel, chamber, furnace, or the like. For example, an airtight furnace can be used as reaction vessel. Preferably, a tubular furnace is used.

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[039] In general, the heating in step (ii) can be conducted by all known methods, techniques, and equipment. Before the carbon raw material is heated the reaction vessel is flushed with the used inert gas at least once, for example 2, 3, 4, 5, or even more times, to ensure that no air, in particular oxygen, or water remains in the reaction vessel. Such techniques and methods are known in the art. In various embodiments the reaction temperature of step (ii) is from about 200 °C to about 900 °C. Preferably, the reaction temperature of step (ii) is from about 400 °C to about 900 °C and more preferably from about 600 °C to about 900 °C or from about 700 °C to

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about 900 °C. In an even more preferred embodiment the reaction temperature of step (ii) is from about 750 °C to about 850 °C.

[040] Further, step (ii) is carried out under reduced pressure. The term “reduced pressure”, as used herein, refers to pressure substantially less than 1013 mbar. In a preferred embodiment of the present invention, the pressure is of from about 0.1 mbar to about 500 mbar. In a more preferred embodiment, step (ii) is conducted at a pressure of from about 0.25 mbar to about 250 mbar. In most preferred embodiments, step (ii), as described herein, is conducted at a pressure of from about 0.5 mbar to about 100 mbar. The pressure can be reduced prior to or during the heating and the reduced pressure is preferably maintained during step (ii), for example by using a suitable vacuum pump connected to the reaction chamber. Due to the absence of oxygen and water the carbon raw material is thermochemically decomposed and burning of said material is prevented. The reduced pressure supports the pyrolysis and the molecules generated during the decomposition can be separated from the developing aerogel.

[041] In various embodiments, steps (i) and (ii) are conducted in the same reaction vessel.

[042] In various embodiments, the reaction time of step (ii) is from about 0.1 hour to about 12 hours. The reaction time can also be from about 0.1 hour to about 8 hours or from about 0.25 hour to about 6 hours. Preferably, the reaction time of step (ii) is from about 0.5 hour to about 4 hours, more preferably from about 1 hour to about 3 hours, and even more preferably about 2 hours. The term “reaction time”, as used herein, relates to the time period over which the desired reaction conditions, i.e. elevated temperature and reduced pressure are maintained. Any warming up phase needed to reach the desired reaction temperature is however not included in the given reaction time.

[043] In various embodiments of the present invention, the heating rate in step (ii) is from about 0.1 °C/min to about 20 °C/min. The heating rate can also be from about 1 °C/min to about 15 °C/min. Preferably, the heating rate in step (ii) is from about 1.5 °C/min to about 10 °C/min or from about 2 °C/min to about 8 °C/min. More preferably, the heating rate in step (ii) is from about 4 °C/min to about 6 °C/min and most preferably about 5 °C/min.

[044] Cotton fibers naturally possess a twisted structure with 3.9 to 6.5 twists per millimeterlength.^[1] The density of the twists is increased by the present method, wherein a heating rate of 5 °C/min generates more twists than 15 °C/min. However, a heating rate of 15 °C/min will shorten the fabrication process thereby saving energy cost. As a result, the heating rate may be selected on the basis of the individual preferences. Generally, the more twists are generated the more rigid and mechanical stable is the obtained aerogel.

[045] Further, it is advantageous that by-products, which are generated during the heating, are continuously removed during carrying out the method, in particular step (ii). Low pressure pyrolysis with constant removal of the by-products is ideal. It has been demonstrated that pyrolysis under an argon atmosphere generates the described twisted structure. Ideally, argon should be continuously flow through the reaction chamber, for example from an inlet to an outlet, at a sufficient flow rate in order to increase the diffusion rate and remove generated by-products. On the other hand, the gas flow rate should not be too high, as the flow of gas will cause undesired temperature fluctuations at the fiber surface.

[046] In a preferred embodiment of the present invention the method comprises pretreating the carbon raw material. In a preferred embodiment the carbon raw material is pretreated with water and/or an aqueous solution. The aqueous solution may comprise an acid. The acid may be selected from the group consisting of hydrochloric acid, sulfuric acid, phosphorous acid, nitric acid, acetic acid, and mixtures thereof. Preferably, the acid is hydrochloric acid. Optionally, the pretreatment may comprise treatment with both, water and an aqueous solution of an acid, at least once. The time of the pretreatment may vary and depends on the carbon raw material. In various embodiments, the pretreatment is carried out for about 0.1 hour to about 80 hours, about 1 hour to about 72 hours or about 6 hours to about 60 hours.

[047] When the carbon raw material is selected from the group consisting of paper, wastepaper, and mixtures thereof the carbon raw material is preferably pretreated with an aqueous solution comprising an acid. Preferably, the used acid is hydrochloric acid. In a preferred embodiment, paper and/or wastepaper are pretreated for about 6 hours to about 24 hours. The pretreating procedure softens the raw material and certain ingredients of the paper and/or wastepaper, such as fillers, glue, and ingredients other than cellulose, are dissolved. Subsequently, the cellulose is separated from the pretreatment solution and optionally dried before the pretreated raw material is further processed in step (i) as disclosed herein. Such a pretreatment may also include one or more washing steps using water. If necessary, each pretreatment step may be repeated several times. For example, the raw material may be subjected to acid solution treatment twice, a water treatment, and a subsequent drying step.

[048] The present invention also encompasses the highly porous aerogel obtainable by the method as described herein.

[049] In a preferred embodiment the highly porous aerogel is a twisted carbon fiber (TCF) aerogel.

[050] In another preferred embodiment the highly porous aerogel is a carbon microbelt (CMB) aerogel. The CMB aerogel can absorb a wide range of organic solvents and oils with a

maximum sorption capacity up to 188 times the weight of the pristine CMB aerogel. Moreover, the CMB aerogel exhibits the excellent recyclability (up to 5 times), and maintains a high sorption capacity even after five cycles through distillation or squeezing.

5 **[051]** As already outlined herein, the type of obtained aerogel depends on the used carbon raw material.

10 **[052]** In a further aspect, the present invention is directed to the use of the highly porous aerogel for treating waste water or methods for the treatment of waste water comprising the use of the aerogels described herein.

15 **[053]** The term “waste water”, as used herein, refers to water which is contaminated with any organic material, which may be liquid under standard conditions (20°C, 1013 mbar). While in principle any weight ratio of water and the organic contaminant may be used, in various embodiments the weight ratio of water and the organic material ranges from about 1 : 1 to about 1.000.000 : 1 or more. In a preferred embodiment of the present invention, the waste water comprises water and an organic liquid. The organic liquid can be any hydrophobic organic liquid which is suitable to penetrate into the aerogel due to its hydrophobic character, and includes, without limitation, liquid hydrocarbons, such as (crude) oil and oil-based products, such as refined oil products, including kerosene, gasoline and the like. Other examples include without limitation chloroform, benzylalcohol, DMF, toluene, octadecylene, hexane, heptane, acetone, ethanol, petroleum, pump oil, colza oil, and olive oil.

25 **[054]** “Treating”, as used herein in relation to waste water treatment, includes at least partially purifying the waste water by separating contaminants that adsorb to the aerogels from the waste water, thus, after separation of the aerogel from the treated water, providing at least partially purified water, i.e. water wherein at least part of the contaminants have been removed. The contaminants are preferably liquid organic contaminants, as described above.

30 **[055]** In various embodiments, the use of the aerogels as disclosed herein comprises bringing the highly porous aerogel into contact with the waste water by, for example, dipping the aerogel into the waste water. The waste water can also be flowed over the aerogel, with the aerogel being fixated, for example in a device, on a plate, or in a pipe. In case the organic contamination and the water form a biphasic system, the aerogel needs to contact the organic phase in order to adsorb the organic material.

35 **[056]** Due to its excellent adsorbing properties the aerogels as disclosed herein are suitable for cleanup and recovery of oil spills.

[057] The absorption capacity of the aerogels can reach up to 192 times the weight of the pristine TCF aerogels. The CMB aerogel possesses an adsorption capacity of 188 times the weight of the pristine CMB aerogel. The aerogel can be simply recycled by distilling, burning, or squeezing methods. Moreover, after five adsorption/recycling cycles, TCF and CMB aerogels still maintain their high adsorption capacity.

[058] The following examples are provided to better illustrate the claimed invention and are not be interpreted in any way as limiting the scope of the invention. All specific compounds, materials, and methods described below, in whole or in part, fall within the scope of the invention. These specific compounds, materials, and methods are not intended to limit the invention, but merely to illustrate specific embodiments falling within the scope of the invention. One skilled in the art may develop equivalent compounds, materials, and use without the exercise of inventive capacity and without departing from the scope of the invention. It is the intention of the inventors that such variations are included in the scope of the present invention.

[059] All references cited herein are incorporated by reference in their entirety.

EXAMPLES

General information

[060] Preparation of twisted carbon fibers (TCF) aerogels:

Cylindrical shaped pieces of raw cotton were rinsed several times by deionized water, and then dried in vacuum at 60 °C for 12 h. After that, the dried cotton was transferred to a tubular furnace for pyrolysis. In order to remove the air trapped in the cotton completely, we first evacuated the furnace, and then introduced argon gas, followed by evacuating the furnace again. After that, the furnace was heated up to 800 °C at a heating rate of 5 °C/min and held at 800 °C for 2 h in argon atmosphere at a low pressure of ~0.5 mbar. Finally, the furnace was cooled down to room temperature naturally to obtain the low-density TCF aerogels.

[061] Characterization of raw cotton and TCF aerogel:

All samples were characterized by a field emission scanning electron microscope (FESEM, JEOL, JSM-7600F), and Fourier transform infrared spectroscopy (FTIR, Perkin Elmer Instruments Spectra, GX FTIR spectrometer).

[062] Sorption of oils and organic solvent of TCF aerogel:

In a typical sorption test, a TCF aerogel was placed in contact with an organic liquid until the aerogel was filled with the organic liquid completely, and then taken out for weight measurement. In order to avoid evaporation of the absorbed organic liquid, especially for those

with low boiling points, the weight measurement should be done quickly. The weight of a piece of TCF aerogel before and after sorption was recorded for calculating the weight gain.

[063] Preparation of carbon microbelt (CMB) aerogels:

5 60 mg of wastepaper scraps were mixed with 40 mL of distilled water and left still for 24 h. Then
10 10 mL of hydrochloric acid (10 %) was added to the aforementioned mixture, which was left
undisturbed for another 12 h. The solid in the mixture was washed by centrifugation for several
times with distilled water to remove chloride ions, and then dried overnight in an oven at 60 °C.
The dried sample was poured into 30 mL of distilled water followed by strong agitation under
vigorous magnetic stirring to form a uniform mixture which is called pulp. The pulp was then
subjected to freeze-drying to form pulp fiber aerogel. After that, the pulp fiber aerogel was
transferred into a tubular furnace for pyrolysis. In order to remove the air trapped in the pulp
fiber aerogel completely, evacuated the furnace before introduction of argon gas, followed by
evacuation of the furnace again. After that, the furnace was heated up to 850 °C at a heating
rate of 5 °C min⁻¹ and kept at 850 °C for 2 h in argon atmosphere at pressure of ~0.5 mbar.
Finally, the furnace was cooled down to room temperature naturally to obtain the low-density
CMB aerogels.

[064] Characterization of pulp fiber aerogels and CMB aerogels:

20 All samples were characterized by a field emission scanning electron microscope (FESEM,
JEOL, JSM-7600F), and Fourier transform infrared spectroscopy (FTIR, Perkin Elmer
Instruments Spectra, GX FTIR spectrometer).

[065] Sorption of oils and organic solvents of carbon microbelt (CMB) aerogels:

25 In a typical sorption test, a CMB aerogel was placed in contact with an organic liquid until the
aerogel was filled with the organic liquid completely, which was then taken out for weight
measurement. In order to avoid evaporation of the absorbed organic liquid, especially for those
with low boiling points, the weight measurement should be done quickly. The weight of a piece
of CMB aerogel before and after sorption was recorded for calculation of the weight gain.

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[066] References:

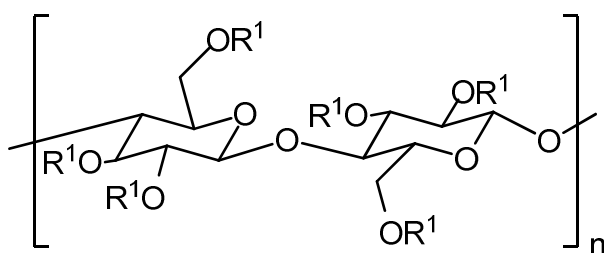
[1] N. Le Moigne, J. Bikard, P. Navard, *Cellulose* **2010**, 17, 507.

35 **[067]** While particular preferred and alternative embodiments of the present invention have
been disclosed, it will be apparent to one of ordinary skill in the art that many various
modifications and extensions of the above described technology may be implemented using the

teaching of this invention described herein. All such modifications and extensions are intended to be included within the true spirit and scope of the invention as discussed in the appended claims.

CLAIMS

1. Method for manufacturing a highly porous aerogel, the method comprising:
 - (i) providing a carbon raw material; and
 - (ii) heating the carbon raw material under inert gas atmosphere and reduced pressure up to 900 °C.
2. Method according to claim 1, wherein the carbon raw material is a polysaccharide or a cellulosic material.
3. Method according to claim 2, wherein the cellulosic material is selected from the group consisting of cellulose and cellulose derivatives.
4. Method according to claim 3, wherein the cellulose is of Formula (I)



Formula (I)

- wherein,
 n is from 25 to 10.000, and
 R¹ is hydrogen.
5. Method according claim 4, wherein n in Formula (I) is from 50 to 5.000.
 6. Method according to claim 3, wherein the cellulose derivate is of Formula (I), wherein n is from 25 to 50.000 and R¹ is selected from the group consisting of hydrogen, a linear or branched, substituted or unsubstituted alkyl with 1 to 6 carbon atoms, and -N(R^a)(R^b) wherein each of R^a and R^b is independently selected from the group consisting of linear or branched alkyl with 1 to 6 carbon atoms with the proviso that at least one of R¹ is not hydrogen.

7. Method according to claim 6, wherein each R¹ is independently selected from the group consisting of methyl and ethyl.
- 5 8. Method according to claim 6, wherein each R^a and R^b is independently selected from the group consisting of methyl and ethyl.
9. Method according to any one of claims 6 to 8, wherein n is from 50 to 5.000.
- 10 10. Method according to claim 2, wherein the polysaccharide is alginic acid.
11. Method according to any one of claims 1 to 10, wherein the carbon raw material is selected from the group consisting of cotton, paper, wastepaper, hemp fiber, pulp, starch, brown algae, and mixtures thereof.
- 15 12. Method according to any one of claims 1 to 11, wherein step (ii) is conducted at a pressure of about 0.1 mbar to about 500 mbar, of about 0.25 mbar to about 250 mbar, or of about 0.5 mbar to about 100 mbar.
- 20 13. Method according to any one of claims 1 to 12, wherein step (i) comprises washing and/or drying the carbon raw material.
14. Method according to claim 13, wherein deionized water is used for washing in step (i).
- 25 15. Method according to claim 13 or 14, wherein drying in step (i) is conducted at a temperature from about 10 °C to about 200 °C, from about 20 °C to about 150 °C, or from about 40 °C to about 90 °C.
- 30 16. Method according to any one of claims 13 to 15, wherein drying is conducted under reduced pressure.
- 35 17. Method according to any one of claims 1 to 16, wherein the reaction temperature of step (ii) is from about 200 °C to about 900 °C, from about 400 °C to about 900 °C, from about 600 °C to about 900 °C, from about 700 °C to about 900 °C, from about 750 °C to about 850 °C or about 800 °C.
18. Method according to any one of claims 1 to 17, wherein the reaction time of step (ii) is from about 0.1 hour to about 12 hours, from about 0.1 hour to about 8 hours, from about 0.25 hour to about 6 hours, from about 0.5 hour to about 4 hours, from about 1 hour to about 3 hours, or about 2 hours.

19. Method according to any one of claims 1 to 18, wherein the heating rate in step (ii) is from about 0.1 °C/min to about 20 °C/min, from about 1 °C/min to about 15 °C/min, from about 1.5 °C/min to about 10 °C/min, from about 2 °C/min to about 8 °C/min, from about 4 °C/min to about 6 °C/min, or about 5 °C/min.
20. Method according to any one of claims 1 to 19, wherein the method comprises pretreating the carbon raw material.
21. Method according to claim 20, wherein pretreating comprises pretreating the carbon raw material with water and/or an aqueous solution.
22. Method according to claim 21, wherein the aqueous solution comprises an acid.
23. Method according to claim 22, wherein the acid is selected from the group consisting of hydrochloric acid, sulfuric acid, phosphorous acid, nitric acid, acetic acid, and mixtures thereof.
24. Method according to claim 22 or 23, wherein the acid is hydrochloric acid.
25. Method according to any one of claims 20 to 24, wherein the pretreating time is about 0.1 hour to about 80 hours, about 1 hour to about 72 hours, or about 6 hours to about 60 hours.
26. Method according to any one of claims 20 to 25, wherein the carbon raw material is selected from the group consisting of paper, wastepaper, and mixtures thereof and is pretreated with an aqueous solution comprising acid.
27. Method according to claim 26, wherein the acid is hydrochloric acid.
28. Method according to claim 26 or 27, wherein the pretreating time is from about 6 hours to about 24 hours.
29. Highly porous aerogel obtainable by the method according to any one of claims 1 to 28.
30. Highly porous aerogel according to claim 29, wherein the aerogel is a twisted carbon fiber (TCF) aerogel.

31. Highly porous aerogel according to claim 29, wherein the aerogel is a carbon microbelt (CMB) aerogel.

32. Use of the highly porous aerogel according to claim 29 for the treatment of waste water.

33. Use according to claim 32, wherein treating the highly porous aerogel comprising bringing the aerogel into contact with the waste water.

34. Use according to claim 32 or 33, wherein the waste water comprises water and an organic liquid contaminant.

35. Method for the treatment of waste water, comprising
(i) contacting the highly porous aerogel according to claim 29 with the waste water; and
(ii) separating the treated waste water from the aerogel.