

Description

The present invention relates to a process for increasing the molecular weight of hydrocarbons and/or derivatives thereof. The present invention relates in particular to a process for increasing the molecular weight of hydrocarbons containing one or more functional groups as described hereinafter.

Hydrocarbons are used in many applications which depend on the nature of the hydrocarbons concerned. In the present invention emphasis is laid on hydrocarbons suitable in the field of lubricating but the invention is by no means limited to hydrocarbons and/or derivatives thereof which are known to be of interest in said field.

One of the important aspects of lubricating oils is their viscometric behaviour. Well known and widely accepted parameters indicating the viscometric properties are the kinematic viscosity and the so-called viscosity index (VI) which is a measure for the internal resistance of a lubricating oil against changes in performance under respectively cold and hot conditions. Oils having a high VI are of great interest in that they can be used under extreme conditions without deteriorating performance.

There are a number of methods known in the art to increase the VI of lubricating oils such as hydro-isomerization of linear paraffins present in the lubricating oils or by the addition of so-called VI-improvers: polymers which are added to an oil in order to improve its viscosity/temperature relationship.

It is of course possible to increase the molecular weight of a given molecule by subjecting it to a dimerisation or oligomerisation treatment. In order to achieve this normally rather reactive molecules and/or stringent conditions have to be applied. Moreover, the di- or oligomerisation envisaged should be kept under control since otherwise products with undesirable or even unfavourable properties would be obtained in ever increasing amounts.

The use of electric discharges to change the molecular weight of hydrocarbons is another method and of course in principle well known. The production of ethylene, acetylene and carbon black from hydrocarbonaceous materials by subjecting them to electrical discharges has been extensively recorded in the literature and several processes have become commercial. It will be clear that such processes when starting from normally liquid hydrocarbonaceous materials are in essence cleavage processes, i.e. not only carbon-carbon bonds are ruptured but also carbon-hydrogen bonds in order to obtain molecules of lower molecular weight.

It is less frequently reported in the literature to increase the molecular weight of normally liquid hydrocarbonaceous materials by using electrical discharges. When the influence of an electrical discharge is described in the literature for such materials it becomes clear that rather reactive molecules have to be processed whilst using a specific form of electrical discharge, commonly referred to as a corona discharge. In US patent specification 3,356,602 a process is described relating to the dimerisation of carboxylic acids by submitting them to a high electrical field (causing the occurrence of the so-called corona-discharge) together with a group O inert gas and/or hydrogen. It is clear from said specification that good results are only obtained in systems operating under alternate current and containing ethylenic unsaturation. Subjecting a saturated compound such as stearic acid to the process described in said US specification leads only to a fractional increase in molecular weight compared with related unsaturated compounds such as oleic acid and linoleic acid (see Table III of US patent specification 3,356,602).

It would therefore be highly advantageous when the molecular weight of hydrocarbonaceous materials could be increased substantially in a controlled and controllable manner. It would be in particular advantageous when the viscosity and possibly the VI of lubricating base oils could be increased by means of an electric discharge, especially when such lubricating base oils would contain functional groups such as carboxylic groups, ester groups, amino groups and/or amido groups which would continue to be present in substantial amounts in the thus treated lubricating base oils having an increased viscosity and, optionally VI. It would also be very advantageous when such functional groups could be incorporated into the structure of lubricating base oils not containing such functional groups (or only minor amounts thereof) during the process which allows an increase in viscosity and/or VI.

It has now surprisingly been found that an increase in the molecular weight of hydrocarbonaceous material, in particular of hydrocarbonaceous material containing one or more functional groups can be obtained in a controlled and controllable manner when use is made of an active-hydrogen containing system under certain conditions.

Substantial increases in viscosity and optionally VI have been found both for hydrocarbonaceous-type lubricating base oils as well as for hydrocarbonaceous-type materials containing or receiving functional groups without impairing other important physical parameters of the materials thus treated. In some instances even a lower pour point of the treated oils has been observed, which renders the process which allows already an increased molecular weight and a higher viscosity and/or VI even more attractive.

The present invention therefore relates to a process for increasing the molecular weight of hydrocarbons

and/or derivatives thereof by contacting them with an active-hydrogen containing system, which system is not generated by a corona-type discharge, characterized in that the process comprises obtaining the active-hydrogen containing system by generating a hydrogen containing plasma at a pressure of at least 0.007 bar and allowing contact of said hydrocarbons and/or derivatives thereof in liquid form with the plasma-generated system and recovering therefrom a product having an increased average molecular weight.

It should be noted that the process according to the present invention allows at least an improvement of the viscosity and optionally also of the VI when a lubricating oil is used as feedstock. This means that the (high) viscosity is improved even further whilst maintaining or even increasing also the VI of oils based on already heavy molecules.

Without wishing to be bound to any particular theory it would appear that by carrying out the process according to the present invention in such a way that the hydrocarbons and/or derivatives thereof are not directly submitted to the electrical field generating the hydrogen-containing plasma, it has become possible to control the conditions leading to desired increases in molecular weight whilst reducing or even preventing the amount of cracking which would occur if a hydrocarbon and/or a derivative thereof was placed directly in the influence of the electrical field of the electrical discharge applied.

The process according to the present invention can be carried out by using any hydrocarbon and/or derivative thereof which is liquid or solid under conditions of standard temperature and pressure.

Preference is given to the use of hydrocarbons ranging from the kerosene range to the heaviest grades of lubricating base oils. In particular the process according to the present invention is carried out in order to increase the molecular weight (and therefore the viscosity and optionally the VI) of the so-called XHVI base oils, i.e. base oils having already a VI of at least 140. Various refinery feedstocks such as hydrocracker bottoms, gas oils as well as various kinds of cycle oils can be used in the process according to the invention. Also mixtures of various hydrocarbons (e.g. various base oil compositions) can be used.

It has been found that the process according to the present invention can be carried out in a controllable manner: the molecular weight can be suitably increased by a factor of e.g. 30-150%, without suffering from disadvantages like cracking or coke formation.

If desired, and often preferred, the hydrocarbons to be treated in the process according to the present invention may contain functional groups which will remain substantially unchanged during the molecular weight increase. This is very important since such groups are either of value per se or can be used in further modifications envisaged.

Examples of functional groups which may be present in the hydrocarbons to be treated in accordance with the present invention comprise carboxylic groups, ester groups, amino and/or amido groups. Typical examples of compounds carrying functional groups comprise carboxylic acids and carboxylic acid esters such as stearic acid, linoleic acid, oleic acid and the alkyl esters, in particular the methyl and ethyl esters thereof. If desired, the hydrocarbon derivatives to be treated may contain two or more functional groups like the higher amino carboxylic acids and the corresponding esters. It will be appreciated that when mixtures containing both hydrocarbonaceous materials and hydrocarbon compounds containing one or more functional groups are treated in accordance to the present invention not only the molecular weight of the starting materials will be increased but that functional groups may also be incorporated into said hydrocarbonaceous materials.

It should be noted that also unsaturated compounds may be used together with the hydrocarbonaceous materials and/or derivatives to be treated in accordance with the present invention. Even under such circumstances the process can be carried out in a controllable mode.

In order to account for the possibility that a minor amount of the feedstock to be treated might undergo a (temporarily) molecular weight decrease which would offset the substantial molecular weight increase contemplated by the present invention, the expression "average molecular weight" will be used throughout the specification indicating an overall increase in molecular weight which should be in the order of at least 20%, preferably at least 30% as described hereinbefore.

It is imperative in the process according to the present invention that the hydrocarbon(s) and/or derivatives thereof are contacted in liquid form with an active-hydrogen containing system which is obtained by generating a hydrogen-containing plasma at a pressure of at least 0.007 bar (Hg). A plasma is defined for the purpose of this invention as a gaseous medium containing electrical charges which as a whole are at electric neutrality. It will be clear that a hydrogen-containing plasma therefore does not only consists of hydrogen atoms and hydrogen molecules (e.g. obtained by pure thermal dissociation): H_2 -ions as well as electrons should also be present, provided the electric neutrality is preserved.

Molecular hydrogen is of course a suitable source to produce a hydrogen-containing plasma, but other hydrogen-containing species such as ammonia, hydrogen sulphide, methane and/or H_2O may be present if desired to contribute to the generation of the hydrogen-containing plasma. In general, the hydrogen-source should contain no less than 75% (on a molar basis) of molecular hydrogen. Conventional refinery hydrogen streams can

be suitably applied.

The hydrogen-containing plasmas to be used in the process according to the present invention are suitably produced by so-called plasma torches, which are well-known as such and used in various branches of industry. Typically, plasma-torches having an energy-production in the range up to 8000 kW can be suitably applied. Preference is given to the use of plasma-torches having an energy-production in the range between 500 and 3000 kW.

In principle, any means for activating hydrogen to the extent that a hydrogen-containing plasma is formed can be used such as electrode-less discharges and appropriate laser beams.

The amount of activated-hydrogen needed in the process according to the present invention depends to some extent on the scale of the equipment used. In rather small reactors less than 1% of the hydrogen in an activated-system already gives remarkable increases in molecular weight. In larger reactors, directed at the production of rather large amounts of products having an increased average molecular weight, the amount of activated hydrogen could well be more than 40%, preferably more than 70%.

The hydrogen-containing plasma is produced at a hydrogen pressure which may range from as low as 0.007 bar up to several bar.

Preference is given to the use of a hydrogen pressure in the range between 0.40 bar and 1 bar, in particular between 0.53 bar and 0.93 bar. It is preferred not to use a rather low hydrogen pressure since this would reduce the power density and hence the efficiency in generating the plasma whilst requiring a substantial increase in the volumes needed to carry out the process. Although in principle the use of hydrogen at a pressure above e.g. 10 bar is possible, it would require a very high temperature to reach a sufficiently high concentration of atomic hydrogen in the hydrogen-containing plasma under such conditions, which would have serious economic disadvantages.

If desired, inert gases like argon or helium can be present in the hydrogen-containing system which will be used to generate the plasma but they do not contribute substantially to the process, contrary to what is normally observed in corona-type discharges.

The process according to the present invention can be suitably carried out in a discharge-equipment provided with recycle means in order to increase the overall yield of the process.

An embodiment of the process according to the present invention is depicted in Figure 1. The apparatus comprises a high voltage generator 1, a reactor 2 and a recycle pump 3. Hydrogen is introduced into the reactor via inlet 4 and withdrawn from the system via outlet 5 (normally by means of a vacuum pump, not shown). The current necessary to produce the active hydrogen containing plasma is introduced via electrode 6 and leaves the system via electrode 7. The electrodes are normally composed of stainless steel. The hydrocarbon and/or derivative to be treated is introduced via line 8 and sent via line 9 to the top of reactor 2, in this particular case a glass tube provided with external temperature controlling means indicated with 10 and 11. When the power is switched on the discharge can be observed in the apparatus in the form of a bright violet/purple display when the hydrogen is sucked through the reactor.

The hydrocarbon to be treated (12) flows as a thin film along the walls of the reactor 2 and is collected at the bottom part of the reactor 2, indicated by 13. It is removed from the reactor via line 14 and recycled to pump 3 via line 15 with the possibility to withdraw product via line 16.

A further embodiment of the process according to the present invention is depicted in Figure 2. The apparatus comprises a plasma torch 21, an expanding area 22, an oil/gas separating means 23 and a recycle pump 24. Hydrogen is introduced via line 25 into plasma generating device 26.

The plasma generating equipment is operated in such a way that hydrogen is introduced at about 1 bar and has a temperature of about 4500 K when leaving the torch. It is important in the apparatus operating under these conditions of temperature and pressure to allow for expansion of the hydrogen-plasma created.

It has been found that the plasma should be allowed to expand to such an extent that the pressure of the generated plasma in the expansion area 22 (P_2) is at most 0.6 times the initial pressure at which the plasma was generated (P_1). Preferably, the expansion area 22 is constructed in such a way that a P_2 of no more than 0.2, and preferably less than 0.1 of the initial pressure P_1 is achieved. Good results can be obtained when the pressure at the end of the torch is relieved from atmospheric to between 0.027 and 0.067 bar since such pressure drops allow an optimal contact between the species generated in the plasma (but not necessarily having the initial composition of the plasma) and the hydrocarbons and/or derivatives to be treated.

Normally the feedstock to be treated is introduced via line 27 and sent via lines 28, 28^A and 28^B to openings 29 in the expansion area 22 to allow introduction of the feedstock to be treated in liquid form downstream of the generated activated hydrogen-plasma. It will be clear that more inlet openings are possible; the number and design of openings is preferably chosen to allow for the optimal droplet size. After the contact between the oil to be treated and the plasma-generated system has taken place inside area 22 the mixture obtained is sent to oil/gas separation chamber 23 allowing for the gaseous part (consisting mainly of unchanged and re-

combined hydrogen) to be sent to compression in order to be introduced again into the system via line 30 which is linked (not shown) with line 25. The oil phase is sent via line 31 to recycle pump 24 to bring it at the desired pressure level to be recycled via lines 32 and 33 to line 28 for reintroduction within the expanding area. Product can be withdrawn from recycle stream 32 via line 34. It should be noted that the proper dimensions of the expansion area allow for a reduction in temperature to about 2500 K and to a pressure of about 0.40 bar.

By properly choosing the recycle ratio of the hydrocarbonaceous material processed and by adjusting the size of the droplets to be introduced via openings 29 into expansion area 22, the reaction can be controlled in such a way that the appropriate average molecular weight increase is achieved. The present invention will now be illustrated by means of the following Examples.

Example 1

An XHVI base oil having the properties as expressed in Table I was processed in the equipment as described in Figure 1. The reactor was operated under the following conditions:

- total pressure	: 0.047 bar (Hg)
- current	: 1-3 mA
- voltage	: 10,000-15,000 V
- distance between stainless steel electrodes	: 40 cm
- inlet water temperature (10)	: 40 °C
- base oil temperature (13)	: 60 °C
- energy input	: 14 Wh/g

The results of this experiment are also given in Table I. No cracking was observed and the average molecular weight increase was no less than 46%. The viscosity in $10^{-6} \text{ m}^2/\text{s}$ (cSt) (at 100 °C) was raised from 8 to 19.6 whilst also an increase in VI and a decrease in pour point was observed.

TABLE I

	XHVI untreated	XHVI treated
viscosity (100 °C)	$8 \times 10^{-6} \text{ m}^2/\text{s}$ (cSt)	$19.6 \times 10^{-6} \text{ m}^2/\text{s}$ (cSt)
viscosity (40 °C)	$46.8 \times 10^{-6} \text{ m}^2/\text{s}$ (cSt)	$153.4 \times 10^{-6} \text{ m}^2/\text{s}$ (cSt)
VI	143	147
Pour Point (°C)	- 16	- 18
Volatility (Noack) (%)	4.1	3.1
Flash Point (°C)	237	237
Average molecular weight	578	846

Example 2

Methyl oleate having an average molecular weight of 292 was processed in the equipment as described in Figure 1. The reactor was operated under the conditions as described in the previous Example but this time with an energy input of 10 Wh/g. No cracking was observed and the average molecular weight measured (by

tonometry) was 493, giving an increase in molecular weight of 66 %. From I.R.-spectroscopy it was found that the ester function was maintained quantitatively in the product as treated.

Example 3

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Squalane (molecular weight 422) was processed as described in Example 1, but using an energy input of 12 Wh/g. No cracking was observed and the average molecular weight of the product was 521 giving an increase in molecular weight of 23%. From the distillation curve it was clear that dimers had been produced. By increasing the energy-input or by extending the run length a higher amount of dimers as well as the formation of trimers and tetramers can be observed.

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Example 4

The process as described in Example 3 was repeated but now in the presence of 10% w of methyl oleate as described in Example 2. Under otherwise identical conditions the product obtained had a substantially increased average molecular weight and it was demonstrated by means of the distillation curve that co-oligomers of squalane and methyl oleate had been formed (comparison with the distillation curves observed for the experiments described in Examples 2 and 3).

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Example 5

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The process as described in Example 3 was repeated but now in the presence of 10 %w of diethyl-dihexylamine. Under otherwise identical conditions the product obtained showed an average molecular weight of 894, ranging from 622 to 1083. The presence of co-oligomers of the amine and squalane was demonstrated by comparison of the appropriate distillation curves.

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Example 6

The process as described in Example 1 was repeated but using the bottom fraction left over after a standard distillation of a commercially produced hydrocrackate.

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Such a bottom fraction is known to be rather unstable during storage which is likely to be caused by the presence of unstable polyaromatic components.

The storage stability, measured after dewaxing at -20 °C, was markedly improved after the treatment with a hydrogen-containing plasma had taken place for a period as short as 3 hours compared with an untreated bottom fraction.

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Claims

- 40 1. Process for increasing the molecular weight of hydrocarbons and/or derivatives thereof by contacting them with an active-hydrogen containing system, which system is not generated by a corona-type discharge, characterized in that the process comprises obtaining the active-hydrogen containing system by generating a hydrogen-containing plasma at a pressure of at least 0.007 bar and allowing contact of said hydrocarbons and/or derivatives thereof in liquid form with the plasma-generated system and recovering therefrom a product having an increased average molecular weight.
- 45 2. Process according to claim 1, wherein use is made of a hydrocarbon and/or derivative which is liquid or solid under conditions of standard temperature and pressure.
- 50 3. Process according to claim 2, wherein use is made of a hydrocarbon ranging from the kerosene grade to the heaviest grades of the lubricating base oils.
4. Process according to claim 3, wherein use is made of an XHVI base oil.
- 55 5. Process according to claim 1 or 2, wherein use is made of a hydrocarbon containing one or more functional groups which will remain substantially unchanged during the process.
6. Process according to claim 5, wherein use is made of hydrocarbons containing carboxylic groups, ester



tonometry) was 493, giving an increase in molecular weight of 66 %. From I.R.-spectroscopy it was found that the ester function was maintained quantitatively in the product as treated.

Example 3

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Squalane (molecular weight 422) was processed as described in Example 1, but using an energy input of 12 Wh/g. No cracking was observed and the average molecular weight of the product was 521 giving an increase in molecular weight of 23%. From the distillation curve it was clear that dimers had been produced. By increasing the energy-input or by extending the run length a higher amount of dimers as well as the formation of trimers and tetramers can be observed.

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Example 4

The process as described in Example 3 was repeated but now in the presence of 10% w of methyl oleate as described in Example 2. Under otherwise identical conditions the product obtained had a substantially increased average molecular weight and it was demonstrated by means of the distillation curve that co-oligomers of squalane and methyl oleate had been formed (comparison with the distillation curves observed for the experiments described in Examples 2 and 3).

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Example 5

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The process as described in Example 3 was repeated but now in the presence of 10 %w of diethyl-di-hexylamine. Under otherwise identical conditions the product obtained showed an average molecular weight of 894, ranging from 622 to 1083. The presence of co-oligomers of the amine and squalane was demonstrated by comparison of the appropriate distillation curves.

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Example 6

The process as described in Example 1 was repeated but using the bottom fraction left over after a standard distillation of a commercially produced hydrocrackate.

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Such a bottom fraction is known to be rather unstable during storage which is likely to be caused by the presence of unstable polyaromatic components.

The storage stability, measured after dewaxing at -20 °C, was markedly improved after the treatment with a hydrogen-containing plasma had taken place for a period as short as 3 hours compared with an untreated bottom fraction.

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Claims

- 40 1. Process for increasing the molecular weight of hydrocarbons and/or derivatives thereof by contacting them with an active-hydrogen containing system, which system is not generated by a corona-type discharge, characterized in that the process comprises obtaining the active-hydrogen containing system by generating a hydrogen-containing plasma at a pressure of at least 0.007 bar and allowing contact of said hydrocarbons and/or derivatives thereof in liquid form with the plasma-generated system and recovering therefrom a product having an increased average molecular weight.
- 45 2. Process according to claim 1, wherein use is made of a hydrocarbon and/or derivative which is liquid or solid under conditions of standard temperature and pressure.
- 50 3. Process according to claim 2, wherein use is made of a hydrocarbon ranging from the kerosene grade to the heaviest grades of the lubricating base oils.
4. Process according to claim 3, wherein use is made of an XHVI base oil.
- 55 5. Process according to claim 1 or 2, wherein use is made of a hydrocarbon containing one or more functional groups which will remain substantially unchanged during the process.
6. Process according to claim 5, wherein use is made of hydrocarbons containing carboxylic groups, ester



groups, amino and/or amido groups.

7. Process according to claim 6, wherein use is made of stearic acid, linoleic acid, oleic acid and/or the appropriate alkyl esters.
8. Process according to claim 7, wherein use is made of methyl oleate.
9. Process according to one or more of claims 1-8, wherein use is made of a hydrocarbon and a hydrocarbon containing one or more functional groups.
10. Process according to one or more of claims 1-9, wherein additionally use is made of unsaturated compounds.
11. Process according to one or more of claims 1-10, which is carried out using molecular hydrogen as source for the hydrogen-containing plasma.
12. Process according to claim 10, wherein use is made of molecular hydrogen containing up to 25% (on a molar basis) of ammonia, hydrogen sulphide, methane and/or water.
13. Process according to one or more of claims 1-12, wherein use is made of a plasma torch to generate the hydrogen-containing plasma.
14. Process according to claim 13, wherein use is made of a torch having an energy-production within the range 500-3000 kW.
15. Process according to one or more of claims 11-14, wherein use is made of a hydrogen-containing plasma containing at least 40% activated hydrogen.
16. Process according to one or more of claims 1-15, wherein the hydrogen-plasma is produced at a hydrogen-pressure in the range between 0.40 and 1 bar.
17. Process according to claim 16, wherein the hydrogen-plasma is produced at a hydrogen-pressure between 0.53 and 0.93 bar.
18. Process according to one or more of claims 1-17, wherein the plasma generated is expanded to a value of at most 0.6 times the initial pressure at which the plasma was generated.
19. Process according to claim 18, wherein the plasma is expanded to a value of at most 0.2, and preferably less than 0.1 times the initial pressure at which the plasma was generated.

Patentansprüche

1. Verfahren zur Erhöhung des Molekulargewichtes von Kohlenwasserstoffen und/oder ihren Derivaten durch Kontaktieren mit einem aktiven Wasserstoff enthaltenden System, welches System nicht durch eine Entladung vom Corona-Typ generiert ist, dadurch gekennzeichnet, daß das Verfahren ein Erhalten des aktiven Wasserstoff enthaltenden Systems durch Generieren eines Wasserstoff enthaltenden Plasmas bei einem Druck von wenigstens 0,007 bar und ein Kontaktierenlassen der genannten Kohlenwasserstoffe und/oder ihrer Derivate in flüssiger Form mit dem Plasma-generierten System und ein Gewinnen eines Produktes mit erhöhtem mittlerem Molekulargewicht umfaßt.
2. Verfahren nach Anspruch 1, worin ein Kohlenwasserstoff und/oder Derivat verwendet wird, das unter Standardbedingungen von Temperatur und Druck flüssig oder fest ist.
3. Verfahren nach Anspruch 2, worin ein Kohlenwasserstoff im Bereich von der Kerosinqualität bis zu den schwersten Qualitäten der Schmiermittelgrundöle eingesetzt wird.
4. Verfahren nach Anspruch 2, worin ein XHVI-Grundöl eingesetzt wird.
5. Verfahren nach Anspruch 1 oder 2, worin ein ein oder mehrere funktionelle Gruppen enthaltender Koh-



lenwasserstoff eingesetzt wird, welche Gruppen während des Verfahrens im wesentlichen unverändert aufrecht erhalten bleiben.

- 5 6. Verfahren nach Anspruch 5, worin Carbonsäuregruppen, Estergruppen, Amino- und/oder Amidogruppen enthaltende Kohlenwasserstoffe eingesetzt werden.
7. Verfahren nach Anspruch 6, worin Stearinsäure, Linolsäure, Ölsäure und/oder die entsprechenden Alkyl-ester eingesetzt werden.
- 10 8. Verfahren nach Anspruch 7, worin Methyloleat eingesetzt wird.
9. Verfahren nach einem oder mehreren der Ansprüche 1 bis 8, worin ein Kohlenwasserstoff und ein eine oder mehrere funktionelle Gruppen enthaltender Kohlenwasserstoff eingesetzt werden.
- 15 10. Verfahren nach einem oder mehreren der Ansprüche 1 bis 9, worin zusätzlich ungesättigte Verbindungen eingesetzt werden.
11. Verfahren nach einem oder mehreren der Ansprüche 1 bis 10, welches unter Verwendung von molekularem Wasserstoff als Quelle für das Wasserstoff enthaltende Plasma ausgeführt wird.
- 20 12. Verfahren nach Anspruch 10, worin molekularer Wasserstoff mit einem Gehalt an bis zu 25 % (auf Molbasis bezogen) an Ammoniak, Schwefelwasserstoff, Methan und/oder Wasser eingesetzt wird.
13. Verfahren nach einem oder mehreren der Ansprüche 1 bis 12, worin eine Plasmafackel zum Generieren des Wasserstoff enthaltenden Plasmas angewendet wird.
- 25 14. Verfahren nach Anspruch 13, worin eine Plasmafackel mit einer Energieproduktion im Bereich von 500-3000 kW eingesetzt wird.
15. Verfahren nach einem oder mehreren der Ansprüche 11 bis 14, worin ein Wasserstoff enthaltendes Plasma eingesetzt wird, das wenigstens 40 % aktivierten Wasserstoff enthält.
- 30 16. Verfahren nach einem oder mehreren der Ansprüche 1 bis 15, worin das Wasserstoffplasma bei einem Wasserstoffdruck im Bereich von 0,40 bis 1 bar ausgebildet wird.
17. Verfahren nach Anspruch 16, worin das Wasserstoffplasma bei einem Wasserstoffdruck zwischen 0,53 und 0,93 bar ausgebildet wird.
- 35 18. Verfahren nach einem oder mehreren der Ansprüche 1 bis 17, worin das gebildete Plasma auf einen Wert von höchstens dem 0,6-fachen des Anfangsdrucks, bei welchem das Plasma gebildet worden ist, expandiert wird.
- 40 19. Verfahren nach Anspruch 18, worin das Plasma auf einem Wert von höchstens dem 0,2-fachen, und vorzugsweise weniger als dem 0,1-fachen des Anfangsdrucks, bei welchem das Plasma gebildet worden ist, expandiert wird.

45 Revendications

50 1. Procédé pour augmenter le poids moléculaire d'hydrocarbures et/ou de leurs dérivés en les mettant en contact avec un système contenant de l'hydrogène actif, lequel système n'est pas produit par une décharge du type corona, caractérisé en ce que le procédé comprend l'obtention du système contenant de l'hydrogène actif par génération d'un plasma contenant de l'hydrogène à une pression d'au moins 0,007 bar et en permettant un contact desdits hydrocarbures avec le système où le plasma a été produit et on recueille à partir de ce système un produit ayant un poids moléculaire moyen accru.

55 2. Procédé selon la revendication 1, dans lequel on utilise un hydrocarbure et/ou un dérivé d'hydrocarbure qui est liquide ou solide dans des conditions de température et pression normales.

3. Procédé selon la revendication 2, dans lequel on utilise un hydrocarbure allant du domaine du kérosène aux qualités les plus lourdes des huiles lubrifiantes de base.

4. Procédé selon la revendication 3, dans lequel on utilise une huile de base XHVI.



5. Procédé selon la revendication 1 ou 2, dans lequel on utilise un hydrocarbure contenant un ou plusieurs groupes fonctionnels qui resteront substantiellement inchangés durant le procédé.

6. Procédé selon la revendication 5, dans lequel on utilise des hydrocarbures contenant des groupes carboxyliques, des groupes ester, des groupes amino et/ou amido.

5 7. Procédé selon la revendication 6, dans lequel on utilise l'acide stéarique, l'acide linoléique, l'acide oléique et/ou les esters d'alcyle appropriés.

8. Procédé selon la revendication 7, dans lequel on utilise l'oléate de méthyle.

9. Procédé selon une ou plusieurs des revendications 1-8, dans lequel on utilise un hydrocarbure et un hydrocarbure contenant un ou plusieurs groupes fonctionnels.

10 10. Procédé selon une ou plusieurs des revendications 1-9, dans lequel on utilise en outre des composés insaturés.

11. Procédé selon une ou plusieurs des revendications 1-10, qui est mis en oeuvre en utilisant de l'hydrogène moléculaire comme source pour le plasma contenant de l'hydrogène.

12. Procédé selon la revendication 10, dans lequel on utilise de l'hydrogène moléculaire contenant jusqu'à 15 25 % (sur une base molaire) d'ammoniac, de sulfure d'hydrogène, de méthane et/ou d'eau.

13. Procédé selon une ou plusieurs des revendications 1-12, dans lequel on utilise une torche à plasma pour engendrer le plasma contenant de l'hydrogène.

14. Procédé selon la revendication 13, dans lequel on utilise une torche ayant une production d'énergie comprise entre 500 et 3000 kW.

20 15. Procédé selon une ou plusieurs des revendications 11-14, dans lequel on utilise un plasma contenant de l'hydrogène qui contient au moins 40 % d'hydrogène activé.

16. Procédé selon une ou plusieurs des revendications 1-15, dans lequel le plasma contenant de l'hydrogène est produit à une pression d'hydrogène comprise entre 0,40 et 1 bar.

25 17. Procédé selon la revendication 16, dans lequel le plasma contenant de l'hydrogène est produit à une pression d'hydrogène comprise entre 0,53 et 0,93 bar.

18. Procédé selon une ou plusieurs des revendications 17, dans lequel le plasma engendré est expansé à une valeur d'au maximum 0,6 fois la pression initiale à laquelle le plasma a été engendré.

19. Procédé selon la revendication 18, dans lequel le plasma est expansé à une valeur d'au maximum 0,2 fois, et de préférence moins de 0,1 fois la pression initiale à laquelle le plasma a été engendré.

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