

DESCRIPTION

TITLE OF INVENTION: PROCESSING AID, MASTER BATCH,
THERMOPLASTIC RESIN COMPOSITION, AND FILM

5

TECHNICAL FIELD

[0001]

The disclosure relates to processing aids,
masterbatches, thermoplastic resin compositions, and films.

10

BACKGROUND ART

[0002]

In processing of melt-fabricable thermoplastic resin,
rapid extrusion is required to achieve improved
15 productivity and low cost. Still, melt-fabricable
thermoplastic resin compositions inevitably have a critical
shear rate and extrusion at a rate higher than this
critical shear rate causes a rough surface called melt
fracture, resulting in a failure in providing a good molded
20 article.

[0003]

Patent Literatures 1 and 2 propose techniques of
improving the processibility of thermoplastic resin,
specifically processing aids containing a high molecular
25 weight polyethylene glycol. However, the effects thereof
are insufficient.

CITATION LIST

- Patent Literature

30 [0004]

Patent Literature 1: JP 2017-538833 T

Patent Literature 2: US 2005/0070644

SUMMARY OF INVENTION

35 - Technical Problem

[0005]

The disclosure aims to provide a processing aid and masterbatch capable of improving the processibility of a thermoplastic resin, as well as a thermoplastic resin
5 composition and film formed therefrom.

- Solution to Problem

[0006]

The disclosure (1) relates to a processing aid
10 containing a biodegradable polymer having a melting point of 65°C or higher.

[0007]

The disclosure (2) relates to the processing aid according to the disclosure (1), wherein the melting point
15 of the biodegradable polymer is 190°C or lower.

[0008]

The disclosure (3) relates to the processing aid according to the disclosure (1) or (2), wherein the biodegradable polymer includes an aliphatic polyester.

20 [0009]

The disclosure (4) relates to the processing aid according to the disclosure (3), wherein the aliphatic polyester includes at least one selected from the group consisting of polylactic acid and polybutylene succinate.

25 [0010]

The disclosure (5) relates to the processing aid according to any one of the disclosures (1) to (4), wherein the biodegradable polymer has a melt flow rate of 0.01 to 500 g/10 min at 190°C and a 2.16 kgf load.

30 [0011]

The disclosure (6) relates to the processing aid according to any one of the disclosures (1) to (5), further containing a synergist that includes at least one selected from the group consisting of polyol, polycaprolactone,
35 silicone, and a polyamide-polyether block copolymer each of

which has a melting point of 80°C or lower.

[0012]

The disclosure (7) relates to the processing aid according to the disclosure (6), wherein the polyol
5 includes polyethylene glycol and/or polyethylene oxide.

[0013]

The disclosure (8) relates to the processing aid according to the disclosure (7), wherein the polyethylene glycol has a number average molecular weight of 1000 to
10 50000, the polyethylene oxide has a viscosity average molecular weight of 100000 to 10000000, and the polycaprolactone has a weight average molecular weight of 2000 to 100000.

[0014]

15 The disclosure (9) relates to the processing aid according to any one of the disclosures (6) to (8), wherein the biodegradable polymer and the synergist have a mass ratio (biodegradable polymer:synergist) of 99.9:0.1 to 10:90.

20 [0015]

The disclosure (10) relates to the processing aid according to any one of the disclosures (1) to (9), further containing an ethylene-vinyl alcohol copolymer.

[0016]

25 The disclosure (11) relates to the processing aid according to the disclosure (10), wherein the ethylene-vinyl alcohol copolymer has a melt flow rate of 40 g/10 min or lower at 190°C and a 2.16 kgf load.

[0017]

30 The disclosure (12) relates to the processing aid according to the disclosure (10) or (11), wherein the ethylene-vinyl alcohol copolymer has an ethylene content of 10 to 50 mol%.

[0018]

35 The disclosure (13) relates to the processing aid

according to any one of the disclosures (10) to (12),
wherein the biodegradable polymer and the ethylene-vinyl
alcohol copolymer have a mass ratio (biodegradable
polymer:ethylene-vinyl alcohol copolymer) of 95:5 to 10:90.

5 [0019]

The disclosure (14) relates to the processing aid
according to any one of the disclosures (10) to (13),
wherein the biodegradable polymer and the ethylene-vinyl
alcohol copolymer have a mass ratio (biodegradable
10 polymer:ethylene-vinyl alcohol copolymer) of 92:8 to 70:30.
[0020]

The disclosure (15) relates to the processing aid
according to any one of the disclosures (10) to (14),
wherein the biodegradable polymer, the ethylene-vinyl
15 alcohol copolymer, and the synergist have a mass ratio
(biodegradable polymer:ethylene-vinyl alcohol
copolymer:synergist) of (1 to 98):(1 to 98):(1 to 98).
[0021]

The disclosure (16) relates to the processing aid
20 according to any one of the disclosures (10) to (15),
wherein the biodegradable polymer, the ethylene-vinyl
alcohol copolymer, and the synergist have a mass ratio
(biodegradable polymer:ethylene-vinyl alcohol
copolymer:synergist) of (25 to 90):(5 to 70):(5 to 70).
25 [0022]

The disclosure (17) relates to the processing aid
according to any one of the disclosures (1) to (16),
further containing a lubricant (A) that includes at least
one selected from the group consisting of a wax, an
30 alcohol, and a surfactant.
[0023]

The disclosure (18) relates to the processing aid
according to the disclosure (17), wherein the biodegradable
polymer and the lubricant (A) have a mass ratio
35 (biodegradable polymer:lubricant (A)) of 99:1 to 1:99.

[0024]

The disclosure (19) relates to the processing aid according to the disclosure (17) or (18), wherein the biodegradable polymer and the lubricant (A) have a mass ratio (biodegradable polymer:lubricant (A)) of 90:10 to 40:60.

[0025]

The disclosure (20) relates to the processing aid according to any one of the disclosures (17) to (19), wherein the biodegradable polymer, the ethylene-vinyl alcohol copolymer, and the lubricant (A) have a mass ratio (biodegradable polymer:ethylene-vinyl alcohol copolymer:lubricant (A)) of (1 to 98):(1 to 98):(1 to 98).

[0026]

The disclosure (21) relates to the processing aid according to any one of the disclosures (17) to (20), wherein the biodegradable polymer, the ethylene-vinyl alcohol copolymer, and the lubricant (A) have a mass ratio (biodegradable polymer:ethylene-vinyl alcohol copolymer:lubricant (A)) of (25 to 93):(5 to 70):(2 to 70).

[0027]

The disclosure (22) relates to the processing aid according to any one of the disclosures (1) to (21), wherein the processing aid is substantially free from fluorine.

[0028]

The disclosure (23) relates to a masterbatch containing the processing aid according to any one of the disclosures (1) to (22) and a thermoplastic resin (A).

[0029]

The disclosure (24) relates to the masterbatch according to the disclosure (23), wherein the thermoplastic resin (A) includes a polyolefin resin.

[0030]

The disclosure (25) relates to the masterbatch

according to the disclosure (24), wherein the polyolefin resin includes polyethylene.

[0031]

5 The disclosure (26) relates to the masterbatch according to any one of the disclosures (23) to (25), wherein the thermoplastic resin (A) and the processing aid have a mass ratio (thermoplastic resin (A):processing aid) of 99:1 to 5:95.

[0032]

10 The disclosure (27) relates to the masterbatch according to any one of the disclosures (23) to (26), wherein the masterbatch has a melt flow rate of 0.01 to 100 g/10 min at 190°C and a 2.16 kgf load.

[0033]

15 The disclosure (28) relates to a thermoplastic resin composition containing: the processing aid according to any one of the disclosures (1) to (22) and/or the masterbatch according to any one of the disclosures (23) to (27); and a thermoplastic resin (B).

20 [0034]

The disclosure (29) relates to the thermoplastic resin composition according to the disclosure (28), wherein the thermoplastic resin (B) includes a polyolefin resin.

[0035]

25 The disclosure (30) relates to the thermoplastic resin composition according to the disclosure (29), wherein the polyolefin resin includes polyethylene.

[0036]

30 The disclosure (31) relates to the thermoplastic resin composition according to any one of the disclosures (28) to (30), wherein the processing aid is contained in an amount of 0.001 to 5% by mass.

[0037]

35 The disclosure (32) relates to a film containing the thermoplastic resin composition according to any one of the

disclosures (28) to (31).

[0038]

The disclosure (33) relates to a method for producing the processing aid according to any one of the disclosures
5 (1) to (22), including a mixing step and an ejecting step.

[0039]

The disclosure (34) relates to a method for producing the masterbatch according to any one of the disclosures
(23) to (27), including a mixing step and an ejecting step.

10 [0040]

The disclosure (35) relates to a method for producing the thermoplastic resin composition according to any one of the disclosures (28) to (31), including a mixing step and an ejecting step.

15 [0041]

The disclosure (36) relates to a method for producing the film according to the disclosure (32), including a molding step.

20 - Advantageous Effects of Invention

[0042]

The disclosure can improve the processibility of thermoplastic resin.

25 DESCRIPTION OF EMBODIMENTS

[0043]

The disclosure will be specifically described hereinbelow.

[0044]

30 <Processing aid>

The processing aid of the disclosure contains a biodegradable polymer having a melting point of 65°C or higher.

[0045]

35 The biodegradable polymer herein means a polymer that

has biodegradability, i.e., that is degradable into low molecular weight compounds owing to involvement of microorganisms in the natural world. Known examples thereof include: aliphatic polyesters such as polylactic acid (PLA), polybutylene succinate (PBS), polyhydroxy butyrate, polycaprolactone, polybutylene succinate/adipate, polyethylene succinate, polymalic acid, polyglycolic acid, polydioxanone, and poly(2-oxetanone); aromatic aliphatic polyesters such as polybutylene succinate/terephthalate, polybutylene adipate/terephthalate (PBAT), and polytetramethylene adipate/terephthalate; natural polymers such as starch, cellulose, chitin, chitosan, gluten, gelatin, zein, soy protein, collagen, and keratin; and polyhydroxy alkanol (PHA). Examples of the PHA include poly(3-hydroxybutyrate) (PHB), poly(3-hydroxybutyrate/3-hydroxyvalerate) (PHBV), poly(3-hydroxybutyrate/3-hydroxyhexanoate) (PHBH), and poly(3-hydroxybutyrate/4-hydroxybutyrate).

[0046]

The polylactic acid is a polymer containing L-lactic acid and/or D-lactic acid as main components, and may further contain a copolymerized component different from the lactic acids. Examples of this different monomer unit include glycol compounds such as ethylene glycol, propylene glycol, butanediol, heptanediol, hexanediol, octanediol, nonanediol, decanediol, 1,4-cyclohexanedimethanol, neopentyl glycol, glycerol, pentaerythritol, bisphenol A, polyethylene glycol, polypropylene glycol, and polytetramethylene glycol; dicarboxylic acids such as oxalic acid, adipic acid, sebacic acid, azelaic acid, dodecanedioic acid, malonic acid, glutaric acid, cyclohexanedicarboxylic acid, terephthalic acid, isophthalic acid, phthalic acid, naphthalenedicarboxylic acid, bis(p-carboxyphenyl)methane, anthracenedicarboxylic acid, 4,4'-diphenyl ether dicarboxylic acid, sodium 5-

sulfoisophthalate, and tetrabutylphosphonium 5-isophthalate; hydroxycarboxylic acids such as glycolic acid, hydroxypropionic acid, hydroxybutyric acid, hydroxyvaleric acid, hydroxycaproic acid, and
5 hydroxybenzoic acid; and lactones such as caprolactone, valerolactone, propiolactone, undecalactone, and 1,5-oxepan-2-one.

[0047]

10 The biodegradable polymer may have any molecular weight and molecular weight distribution that substantially enable extrusion molding.

[0048]

The processing aid of the disclosure has been completed by the finding that a biodegradable polymer
15 having a melting point of 65°C or higher among the biodegradable polymers can significantly improve the processibility of thermoplastic resin. The biodegradable polymer having a melting point of 65°C or higher is preferably an aliphatic polyester such as PLA or PBS,
20 particularly preferably PLA or PBS.

[0049]

The melting point of the biodegradable polymer is at least 65°C or higher, preferably 70°C or higher, more preferably 75°C or higher, still more preferably 80°C or
25 higher, while preferably 190°C or lower, more preferably 185°C or lower, still more preferably 180°C or lower. The biodegradable polymer having a melting point within this range can lead to a better effect of improving the processibility.

30 The melting point herein is the temperature corresponding to the maximum value on a heat-of-fusion curve with a temperature-increasing rate of 10°C/min using a differential scanning calorimeter (DSC).

[0050]

35 The biodegradable polymer has a melt flow rate (MFR)

of preferably 0.01 g/10 min or higher, more preferably 0.05 g/10 min or higher, still more preferably 0.1 g/10 min or higher, while preferably 500 g/10 min or lower, more preferably 300 g/10 min or lower, still more preferably 150 g/10 min or lower. The biodegradable polymer having a MFR within this range can lead to a better effect of improving the processibility.

The MFR herein is determined under conditions of 190°C and a 2.16 kgf load in conformity with ASTM D1238.

10 [0051]

The processing aid of the disclosure contains the biodegradable polymer in an amount of preferably 60% by mass or more, more preferably 70% by mass or more, still more preferably 80% by mass or more. The upper limit may be, but is not limited to, 100% by mass. In the case of combination use with a synergist to be described later, this upper limit is preferably 99% by mass or less, more preferably 95% by mass or less.

[0052]

20 The biodegradable polymer preferably contains a structural unit represented by the following formula 1:

$$-X-(CR^1R^2)_n-Y-(CR^3R^4)_m-Z-$$
 (formula 1)

wherein X is a single bond or a divalent group optionally containing a functional group;

25 Y and Z are each independently a group constituted by at least one selected from the group consisting of a single bond, -O-, -C(=O)-, -C(=O)O-, -OC(=O)O-, -C(=NR')-, -C(=NR')O-, -OC(=NR')O-, -S-, -S(=O)-, -S(=O)O-, -OS(=O)O-, -S(=O)₂-, -S(=O)₂O-, -OS(=O)₂O-, -P(=O)-, -P(=O)O-, -OP(=O)O-, -P(=O)₂-, -P(=O)₂O-, -OP(=O)₂O-, -NR'-, and -C(OR')R'-, wherein R's at respective occurrences are each independently a hydrogen atom or a C1-C10 hydrocarbon group;

35 R¹, R², R³, and R⁴ are each independently a hydrogen atom or a C1-C10 hydrocarbon group; and

n and m are each independently an integer of 0 to 10,
with at least one of X, Y, or Z being -C(=O)-, -
C(=O)O-, -OC(=O)O-, or -C(OR')R'-.

[0053]

5 In the formula 1, preferably, X is a divalent group
constituted by at least one selected from the group
consisting of X¹ and X²,

wherein X¹ is a group constituted by at least one
selected from the group consisting of -C(=O)-, -C(=NR')-, -
10 S(=O)₂-, -NR'-, -CR'R'-, and -C(OR')R'- (wherein R's at
respective occurrences are each independently a hydrogen
atom or a C1-C10 hydrocarbon group); and

X² is a C1-C12 aromatic hydrocarbon group optionally
containing a substituent.

15 [0054]

In the formula 1, X is more preferably a divalent
group containing at least one selected from the group
consisting of -C(=O)-, -CR'R'-, and -C(OR')R'-, wherein R's
at respective occurrences are each independently a hydrogen
20 atom or a C1-C10 hydrocarbon group.

[0055]

In the formula 1, R's at respective occurrences are
preferably each independently a hydrogen atom or a C1-C7
hydrocarbon group, more preferably a hydrogen atom or a C1-
25 C4 hydrocarbon group, still more preferably a hydrogen atom
or a C1 hydrocarbon group.

[0056]

In the formula 1, Y and Z are preferably each
independently a group constituted by at least one selected
30 from the group consisting of a single bond, -O-, -C(=O)-, -
C(=O)O-, -C(=NR')-, -C(=NR')O-, -S-, -S(=O)₂-, -S(=O)₂O-, -
NR'-, and -C(OR')R'-, wherein R's at respective occurrences
are each independently a hydrogen atom or a C1-C10
hydrocarbon group.

35 [0057]

In the formula 1, Y and Z are preferably each independently a group constituted by at least one selected from the group consisting of a single bond, -O-, -C(=O)-, and -C(=O)O-.

5 [0058]

In the formula 1, R¹, R², R³, and R⁴ are preferably each independently a hydrogen atom or a C1-C7 hydrocarbon group, more preferably a hydrogen atom or a C1-C4 hydrocarbon group, still more preferably a hydrogen atom or a C1 hydrocarbon group.

10

[0059]

In the formula, n and m are preferably each independently an integer of 0 to 8, more preferably an integer of 0 to 6, still more preferably an integer of 0 to 4, particularly preferably an integer of 0 to 2.

15

[0060]

The processing aid of the disclosure preferably contains a synergist that includes at least one selected from the group consisting of polyol having a melting point of 80°C or lower, polycaprolactone, silicone, and a polyamide-polyether block copolymer, more preferably contains a synergist that includes at least one selected from the group consisting of polyol having a melting point of 80°C or lower and polycaprolactone. This can lead to a better effect of improving the processibility. To achieve an excellent effect of improving the processibility, the synergist is preferably such a polyol.

20

25

[0061]

The melting point of the polyol is at least 80°C or lower, preferably 75°C or lower, more preferably 70°C or lower, still more preferably 68°C or lower, while preferably 10°C or higher, more preferably 20°C or higher, still more preferably 25°C or higher. The polyol having a melting point within this range can lead to a better effect of improving the processibility.

30

35

[0062]

The polyol can be represented by $A[(OR^{11})_{x2}OR^{12}]_{y2}$, wherein A is commonly alkylene having one or more ether bonds; $y2$ is 2 or 3, $(OR^{11})_{x2}$ is a poly(oxyalkylene) chain having multiple ($x2$) oxyalkylene groups OR^{11} ; R^{11} s are each independently C2-C5 alkylene or, in some embodiments, C2-C3 alkylene; R^{12} is hydrogen, alkyl, aryl, arylalkenyl, alkylarylenyl, -C(O)-alkyl, -C(O)-aryl, -C(O)-arylalkenyl, or -C(O)-alkylarylenyl, where -C(O)- bonds to O of OR^{12} ; and $x2$ is 10 to 230000.

[0063]

The polyol may be a homopolymer such as poly(oxyethylene) in which R^{11} s are each $-CH_2CH_2-$ or poly(oxypropylene) and R^{11} s are each $-C_3H_6-$.

[0064]

The polyol may be a chain of randomly distributed oxyalkylene groups (e.g., $-OC_2H_4-$ and $-OC_3H_6-$ units which are copolymers) or a chain including alternating blocks of repeated oxyalkylene groups (e.g., a polymer including a $(-OC_2H_4-)_{a1}$ block and a $(-OC_3H_6-)_{b1}$ block, where $a1 + b1$ is 10 to 230000).

[0065]

In some embodiments, A in the polyol is ethylene, $-CH_2-CH(-)-CH_2-$ (derived from glycerol), $CH_3CH_2C(CH_2-)_3$ (derived from 1,1,1-trimethylolpropane), poly(oxypropylene), $-CH_2CH_2-O-CH_2CH_2-$, or $-CH_2CH_2-O-CH_2CH_2-O-CH_2CH_2-$; and R^{12} is hydrogen, methyl, butyl, phenyl, benzyl, acetyl, benzoyl, or stearyl.

[0066]

The polyol may be polyester prepared from a dicarboxylic acid and a poly(oxyalkylene) polymer represented by $A[(OR^{11})_{x2}OR^{12}]_{y2}$, wherein A, R^{11} , and $x2$ are as defined above; R^{12} is hydrogen; and $y2$ is 2.

[0067]

One of the polyols may be used alone or two or more

thereof may be used in combination. To achieve an excellent effect of improving the processibility, polyethylene glycol or polyethylene oxide is preferred, and polyethylene glycol is particularly preferred.

5 [0068]

The polyethylene glycol has a number average molecular weight (M_n) of preferably 1000 or higher, more preferably 3000 or higher, still more preferably 5000 or higher, while preferably 50000 or lower, more preferably 45000 or lower, still more preferably 40000 or lower. The polyethylene glycol having a number average molecular weight within this range can lead to a better effect of improving the processibility.

The number average molecular weight herein is determined by calculation from the hydroxyl value determined in conformity with JIS K0070.

[0069]

The polyethylene oxide has a viscosity average molecular weight (M_v) of preferably 100000 or higher, more preferably 120000 or higher, still more preferably 140000 or higher, while preferably 10000000 or lower, more preferably 1600000 or lower, still more preferably 500000 or lower. The polyethylene oxide having a viscosity average molecular weight within this range can lead to a better effect of improving the processibility.

The viscosity average molecular weight herein is calculated as follows.

An Ostwald viscometer is used to determine at 35°C the specific viscosities η_{sp} of aqueous solutions containing a polymer at various concentrations c (g/dl) in pure water; each specific viscosity is divided by the corresponding polymer concentration to provide the reduced viscosity; based on the relationship between the resulting reduced viscosity (η_{sp}/c) and the polymer concentration c , with the polymer concentration c being extrapolated to 0,

the $[\eta]$ value is calculated. The $[\eta]$ value is substituted into the following formula, whereby the viscosity average molecular weight M is calculated.

$$\text{Formula: } [\eta] = 6.4 \times 10^{-5} M^{0.82}$$

5 [0070]

The polycaprolactone may be a homopolymer of ϵ -caprolactone or may be a modified polycaprolactone. Examples of the modified polycaprolactone include those modified with, for example, 1,4-butanediol combined during
10 ring-opening polymerization of ϵ -caprolactone and those modified with, for example, an ether or ester group at an end of a polymer.

[0071]

The polycaprolactone has a weight average molecular
15 weight (M_w) of preferably 2000 or higher, more preferably 10000 or higher, still more preferably 25000 or higher, while preferably 100000 or lower, more preferably 95000 or lower, still more preferably 90000 or lower. The polycaprolactone having a weight average molecular weight
20 within this range can lead to a better effect of improving the processibility.

The weight average molecular weight herein is determined in polystyrene equivalent by gel permeation chromatography (GPC).

25 [0072]

The polycaprolactone has a melting point of preferably 80°C or lower, more preferably 75°C or lower, still more preferably 70°C or lower, further preferably 68°C or lower, while preferably 10°C or higher, more
30 preferably 20°C or higher, still more preferably 45°C or higher. The polycaprolactone having a melting point within this range can lead to a better effect of improving the processibility.

[0073]

35 The silicone may be basically any organic silicon

compound known to those skilled in the art with the term silicone polymer. An appropriate definition of the silicone is found in Winnacker/Kuchler: "Chemische Technik" [Chemical Technology], R. Dittmeyer, W. Keim, G. Kreysa, A. Oberholz (editor), Vol. 5: "Organische Zwischenverbindungen, Polymere" [Organic Intermediates, Polymers], Chapter: "Silicones", Wiley-VCH, Weinheim, 2005. [0074]

The silicone may be a substituted or unsubstituted linear oligo- or polydiorganosiloxane, a branched silicone polymer, silicone resin, or a crosslinked silicone polymer. A mixture of various silicone polymers may also be used, of course. As described above, a silicone-containing copolymer may be used, such as a polyether functional silicone, a silicone containing a urea or urethane unit, or a silicone block copolymer with an organic polymer. To achieve better additivity, particularly preferred is to use a high molecular weight polydiorganosiloxane that can contain a non-silicone component, such as filler, e.g., fine silicic acid particulate, chalk, talc, or a sheet-shaped silicic acid salt. [0075]

Preferably, the silicone polymer corresponds to the formula A $[R^{13}_3SiO_{1/2}]_{a2}[SiR^{13}_2O_{2/2}]_{b2}[R^{13}SiO_{3/2}]_{c2}[SiO_{4/2}]_{d2}$, wherein R^{13} is hydrogen, -OH, or a C1-C18 substituted or unsubstituted hydrocarbon residue; and $a2$, $b2$, $c2$, and $d2$ each mean 0 or an integer, with $a2 + b2 + c2 + d2$ being an integer of 5 to 15000. [0076]

Examples of the C1-C18 hydrocarbon residue R^{13} include alkyl residues, such as methyl, ethyl, n-propyl, isopropyl, n-butyl, 2-butyl, isobutyl, tert-butyl, n-pentyl, isopentyl, neopentyl, a tert-pentyl residue, hexyl residues, e.g., a n-hexyl residue, heptyl residues, e.g., a n-heptyl residue, octyl residues, e.g., a n-octyl residue

and an isooctyl residue, a 2,2,4-trimethylpentyl residue, nonyl residues, e.g., a n-nonyl residue, decyl residues, e.g., a n-decyl residue, cycloalkyl residues, e.g., a cyclopentyl residue, a cyclohexyl residue, a 4-ethylcyclohexyl residue, and a cycloheptyl residue, a norbornyl residue, and a methylcyclohexyl residue. Preferred among the alkyl residues are C1-C6 residues, such as methyl and ethyl residues, particularly a methyl residue.

10 [0077]

Examples of R^{13} also include C1-C18 unsaturated hydrocarbon residues such as alkenyl residues, e.g., a vinyl residue, a 2-propen-2-yl residue, an allyl residue, a 3-buten-1-yl residue, a 5-hexen-1-yl residue, and a 10-undecen-1-yl residue, as well as cycloalkenyl residues (a 2-cyclohexenyl residue, a 3-cyclohexenyl residue, a cyclopentadienyl residue, and a 2-(cyclohex-3-en-1-yl)ethyl residue); aryl residues, e.g., a phenyl residue, a biphenyl residue, and a naphthyl residue; alkaryl residues, e.g., o-, m-, or p-tolyl residue and phenethyl residues (a 2-phenylethyl residue and a 1-phenylethyl residue); as well as aralkyl residues, e.g., a benzyl residue. Preferred C1-C18 unsaturated hydrocarbon residues R^{13} are a vinyl residue and a phenyl residue.

25 [0078]

Examples of a substituted hydrocarbon residue as the residue R^{13} include halogenated hydrocarbons such as a chloromethyl residue, a 3-chloropropyl residue, a 3-bromopropyl residue, a 3,3,3-trifluoropropyl residue, and a 5,5,5,4,4,3,3-heptafluoropentyl residue, as well as a chlorophenyl residue, a dichlorophenyl residue, and a trifluorotolyl residue.

[0079]

The residue R^{13} is preferably coupled with a silicone polymer represented by the formula A via a Si-C bond, and

35

may be coupled with the silicone polymer via an oxygen atom
-O-.

[0080]

R^{13} preferably contains 1 to 6 carbon atoms.

5 Particularly preferred are an ethyl residue, a phenyl
residue, a vinyl residue, and a methyl residue.

[0081]

Preferably, the number represented by $a^2 + b^2 + c^2 +$
 d^2 means at least 10, more preferably at least 100,
10 particularly preferably at least 1000 and at most 15000,
still more preferably at most 10000, particularly
preferably at most 7000.

[0082]

Preferably, the number represented by $c^2 + d^2$ means <
15 $0.1 \times (a^2 + b^2 + c^2 + d^2)$, particularly $c^2 + d^2 < 0.05 \times$
 $(a^2 + b^2 + c^2 + d^2)$.

[0083]

Preferably at least 50%, more preferably at least
70%, particularly preferably at least 80% of all residues
20 R^{13} mean a methyl residue.

[0084]

In principle, every silicone polymer corresponding to
the formula A may be used. Still, preferred is a silicone
polymer having a dynamic viscosity of higher than 1000
25 mPa·s, which is measured using a plate-cone system (cone
CP50-2) having an opening angle of 2° and a diameter of 50
mm with a rheometer "MCR 302" available from Anton Paar at
a measurement temperature of $25.00^\circ\text{C} \pm 0.05^\circ\text{C}$ and a shear
rate of 1 sec^{-1} , preferably in conformity with DIN EN
30 ISO3219:1994 and DIN 53019.

[0085]

Among these silicones, a silicone polymer having a
very high molecular weight may be used, such as UHMW
polysiloxane (ultra-high molecular weight; described in K.
35 J. Ryan, et al., Journal of Vinyl & Additive Technology,

March 2000, Vol. 6, No. 1, pp. 7-19).

[0086]

UHMW polysiloxane has a degree of polymerization within a range from > 1000 to about 14000, which
5 corresponds to a number average molecular weight from 74 kg/mol to 1000 kg/mol.

[0087]

Typical UHMW polysiloxane has a dynamic viscosity from 10 kPa·s to 50 kPa·s, preferably from 15 kPa·s to 30
10 kPa·s, which is determined using an airborne rotational rheometer preferably in conformity with DIN EN ISO3219:1994 and DIN 53019, where a plate-plate system (diameter 25 mm) having a measurement gap of 0.5 mm is used. The measurement temperature is 25.00°C +/- 0.1°C. The shear
15 rate gradient is 0.1 sec⁻¹. The viscosity described refers to an arithmetic mean of three distinct, independently measured values.

[0088]

Owing to its inexpensiveness and effectiveness,
20 particularly preferred among the UHMW polysiloxanes is a high molecular weight polydimethylsiloxane having a dynamic viscosity from 1 kPa·s to 50 kPa·s, preferably from 10 to 40 kPa·s, particularly preferably from 15 to 30 kPa·s (preferably determined by the aforementioned method).

25 [0089]

Examples of the UHMW polysiloxane include commercially available UHMW polysiloxanes such as MULTIBASE® MB50-001 and MULTIBASE® MB50-002 available from Dupont, GENIOPLAST® PELLET S, GENIOPLAST® PELLET P PLUS,
30 GENIOPLAST® PE50S08, and GENIOPLAST® PP50S12 available from Wacker Asahikasei Silicone Co., Ltd., and mixtures of any of these, with MB50-002 and GENIOPLAST® PELLET S being preferred.

[0090]

35 The silicone polymer can be commercially available in

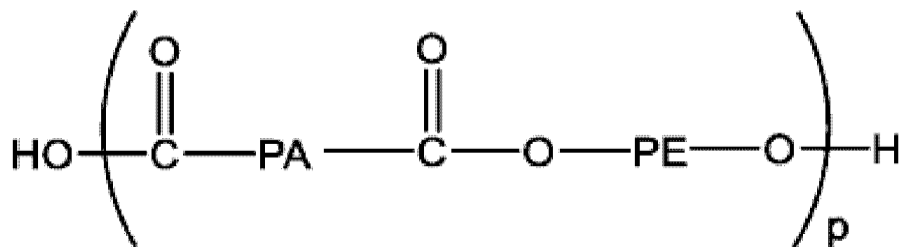
the form of pellets or granules or masterbatch for ready-to-use, which may be mixed with thermoplastic granules before additional processing.

[0091]

5 The polyamide-polyether block copolymer is a copolymer including a polyamide block and a polyether block in the polymer backbone. In the disclosure, such a block copolymer including a polyamide block and a polyether block can also be referred to as a "polyamide/polyether block
10 copolymer". This may also be abbreviated to "PEBA copolymer" or "PEBA".

In some embodiments of the disclosure, the PEBA copolymer can be represented by the following formula:

[Chem. 1]

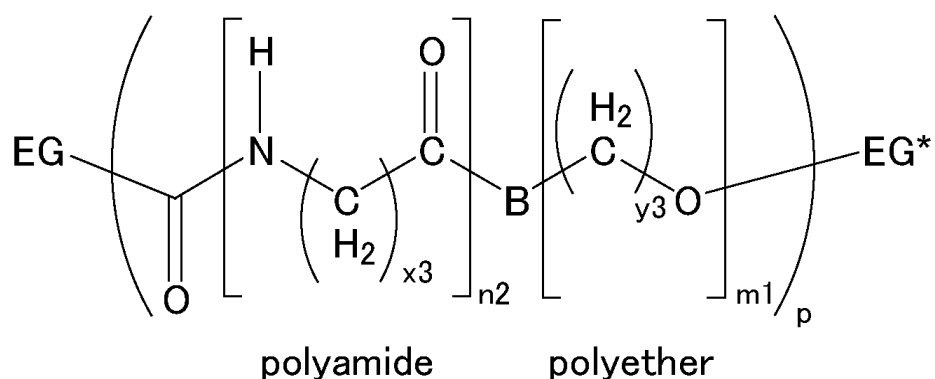


15

[0092]

wherein PA represents a polyamide block, PE represents a polyether block, and p represents the length of the PEBA copolymer, which represents the total number of the
20 polyamide and polyether blocks. In some embodiments of the disclosure, the PEBA copolymer can be represented by the following formula:

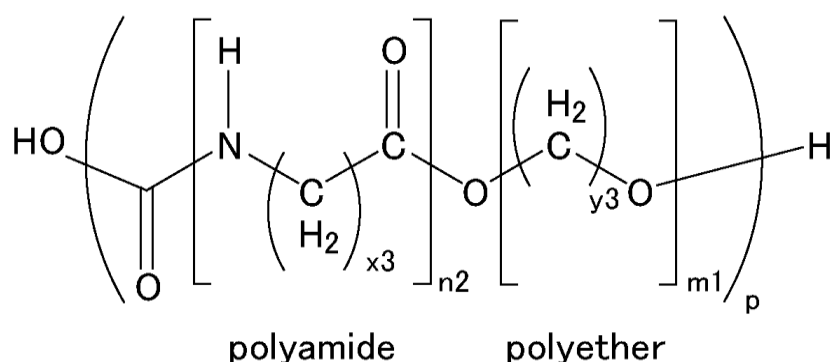
[Chem. 2]



[0093]

wherein EG represents a first unspecified end group; B represents an unspecified crosslinking group; and EG* represents a second unspecified end group, where EG, B, and EG* are determined by a synthesis method used for producing a PEBA copolymer, wherein n2 represents the length of the polyamide block; x3 represents the length of an amide component in the polyamide block; m1 represents the length of the poly(ether) block; y3 represents the length of an ether component in the poly(ether) block; and p represents the total number of the polyamide and polyether blocks.

In some embodiments of the disclosure, the PEBA copolymer can be represented by the following formula:
[Chem. 3]



[0094]

wherein n2 represents the length of the polyamide block; x3 represents the length of an amide component in the polyamide block; m1 represents the length of the

poly(ether) block; y3 represents the length of an ether component in the poly(ether) block; and p represents the length of the PEBA copolymer, which represents the total number of the polyamide and polyether blocks.

5 [0095]

The polyamide block in the PEBA copolymer is derived from polyamide-12 (PA-12), polyamide-11 (PA-11), polyamide-6 (PA-6), or polyamide-66 (PA-66).

[0096]

10 The weight average molecular weight (e.g., Mw and Mn) of the PEBA copolymer can be determined, for example, by gel permeation chromatography using a narrow molecular weight polymer standard based on a known technique in the technical field (i.e., by size-exclusion chromatography).

15 [0097]

In an embodiment, the polyamide block in the PEBA copolymer has a number average molecular weight Mn of about 100 to about 15000 g/mol, or about 300 to about 15000 g/mol, or about 600 to about 10000 g/mol, or about 600 to
20 about 5000 g/mol.

The polyether block in the PEBA copolymer has a number average molecular weight Mn of about 100 to about 15000 g/mol, about 100 to about 10000 g/mol, about 100 to about 6000 g/mol, about 100 to about 3000 g/mol, about 200
25 to about 6000 g/mol, about 200 to about 3000 g/mol, about 250 to about 2000 g/mol, about 750 to about 3500 g/mol, or about 1000 to about 3000 g/mol.

[0098]

The PEBA copolymer has a number average molecular
30 weight Mn of 10000 to 500000 g/mol, including any subrange within these ranges and any number within these ranges. In an embodiment of the disclosure, for example, the number average molecular weight Mn of the PEBA copolymer is 10000 to 400000 g/mol, or 10000 to 300000 g/mol, 10000 to 250000
35 g/mol, or 15000 to 300000 g/mol, or 20000 to 300000 g/mol,

or 15000 to 200000 g/mol, or 20000 to 200000 g/mol, or 30000 to 250000 g/mol, or about 25000 to about 75000 g/mol, or about 50000 to about 75000 g/mol, or about 100000 to about 150000 g/mol.

5 The number average molecular weight M_n of the PEBA copolymer is at least 10000 g/mol, at least 20000 g/mol, at least 25000 g/mol, exceeding 25000 g/mol, at least 30000 g/mol, exceeding 30000 g/mol, at least 35000 g/mol, exceeding 35000 g/mol, at least 50000 g/mol, or exceeding
10 50000 g/mol.
[0099]

 In an embodiment, the PEBA copolymer has a weight average molecular weight M_w of 25000 to 500000 g/mol, including any subrange within these ranges and any number
15 within these ranges. In an embodiment of the disclosure, for example, the weight average molecular weight M_w of the PEBA copolymer is about 100000 to about 250000 g/mol, or about 100000 to about 150000 g/mol, or about 125000 to about 150000 g/mol.

20 The polyamide and polyether blocks in the PEBA copolymer may be randomly distributed.
[0100]

 The PEBA copolymer contains a polyamide block and a polyether block and the polyamide block occupies at least
25 50% by mass of the copolymer. The PEBA copolymer contains a polyamide block and a polyether block and the polyether block occupies at least 50% by mass of the copolymer. The PEBA copolymer contains a polyamide block and a polyether block and the ratio by mole of the polyamide block to the
30 polyether block may fall within a range of 1:3 to 3:1, or 1:2 to 2:1, or 3:2 to 1:3, or 2:3 to 3:1, or about 1:1.
[0101]

 The PEBA copolymer containing a polyamide block and a polyether block can be prepared by reacting precursors of
35 the polyamide and polyether blocks. For example, a lactam,

a polyether diol, and a chain-limiting dioic acid may be reacted together in the presence of a small amount of water, thereby producing a length-variable PEBA copolymer containing a polyamide block and a polyether block
5 statistically randomly distributed in the block copolymer chain.

The polyether block may be derived from poly(oxyethylene), poly(oxypropylene), or poly(tetramethylene ether)glycol, each of which in the
10 natural state may be co-condensed with a polyamide block having a carboxylic acid chain end. A chain-limiting agent may be present during the polycondensation reaction to provide a PEBA copolymer containing a polyamide block and a polyether block randomly distributed in the block
15 copolymer.

The polyether block is derived from poly(oxyethylene), poly(oxypropylene), or poly(tetramethylene ether)glycol, each of which are first aminated into polyether diamine and then co-condensed with
20 a polyamide block having a carboxylic acid chain end. A chain-limiting agent may be present during the polycondensation reaction to provide a PEBA copolymer containing a polyamide block and a polyether block randomly distributed in the block copolymer.

25 The polyether block can be derived from poly(oxyethylene), which is also known as polyethylene glycol (PEG).

The polyether block can be derived from poly(oxypropylene), which is also known as polypropylene
30 glycol (PPG).

The polyether block can be derived from poly(tetramethylene ether)glycol (PTMG), which is also known as polytetramethylene oxide (PTMEO) or polytetrahydrofuran (PTHF).

35 [0102]

The PEBA copolymer contains i) a polyamide block selected from polyamide-12 (PA-12), polyamide-11 (PA-11), polyamide-6 (PA-6), or a mixture of any of these and ii) a polyether block selected from polyethylene glycol (PEG), polypropylene glycol (PPG), polytetrahydrofuran (PTHF), or a mixture of any of these.

[0103]

The PEBA copolymer contains i) a polyamide block selected from polyamide-12 (PA-12), polyamide-11 (PA-11), polyamide-6 (PA-6), or a mixture of any of these and ii) a polyether block which is polyethylene glycol (PEG). In an embodiment of the disclosure, the PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG).

[0104]

The PEBA copolymer contains 10 to 20 polyamide blocks and 10 to 20 polyether blocks.

[0105]

The PEBA copolymer contains a single species of the polyamide block and a single species of the polyether block.

[0106]

The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG), wherein the polyamide-12 block occupies about 30% by mass to 70% by mass of the copolymer and the polyethylene glycol block occupies about 70% by mass to 30% by mass of the copolymer.

[0107]

The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG), wherein the polyamide-12 block occupies about 40% by mass to 60% by mass of the copolymer and the polyethylene glycol block occupies about 60% by mass to 40% by mass of the copolymer.

[0108]

The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG), wherein the polyamide-
5 12 block represents about 45% by mass of the copolymer and the polyethylene glycol block represents about 55% by mass of the copolymer.

[0109]

The PEBA copolymer contains i) 10 to 20 polyamide
10 blocks each of which is polyamide-12 (PA-12) and ii) 10 to 20 polyether blocks each of which is polyethylene glycol (PEG).

[0110]

The PEBA copolymer contains i) a polyamide block
15 which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG), and has a number average molecular weight Mn of about 25000 to about 75000 g/mol.

[0111]

20 The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG), and has a number average molecular weight Mn of about 50000 to about 75000 g/mol. The PEBA copolymer contains i) a polyamide block
25 which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG), and has a number average molecular weight Mn of about 66100 g/mol.

[0112]

The PEBA copolymer contains i) a polyamide block
30 which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG), and has a weight average molecular weight Mw of about 100000 to about 150000 g/mol.

[0113]

35 The PEBA copolymer contains i) a polyamide block

which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG), and has a weight average molecular weight Mw of about 125000 to about 150000 g/mol.

5 [0114]

The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polyethylene glycol (PEG), and has a weight average molecular weight Mw of about 134000 g/mol.

10 [0115]

In an embodiment of the disclosure, the PEBA copolymer contains i) a polyamide block which is polyamide-6 (PA-6) and ii) a polyether block which is polyethylene glycol (PEG).

15 The PEBA copolymer contains i) a polyamide block which is polyamide-6 (PA-6) and ii) a polyether block which is polyethylene glycol (PEG), wherein the polyamide-6 block represents about 30% by mass to 60% by mass of the copolymer and the polyethylene glycol block represents about 70% by mass to 40% by mass of the copolymer.

20 [0116]

The PEBA copolymer contains i) a polyamide block which is polyamide-6 (PA-6) and ii) a polyether block which is polyethylene glycol (PEG), wherein the polyamide-6 block represents about 50% by mass to 35% by mass of the copolymer and the polyethylene glycol block represents about 50% by mass to 65% by mass of the copolymer.

25 [0117]

The PEBA copolymer contains i) 10 to 20 polyamide blocks each of which is polyamide-6 (PA-6) and ii) 10 to 20 polyether blocks each of which is polyethylene glycol (PEG).

[0118]

35 The PEBA copolymer contains i) a polyamide block which is polyamide-11 (PA-11) and ii) a polyether block

which is polyethylene glycol (PEG). In an embodiment of the disclosure, the PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polytetrahydrofuran (PTHF).

5 [0119]

The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polytetrahydrofuran (PTHF), wherein the polyamide-12 block represents about 75% by mass to 10% by mass of the
10 copolymer and the polytetrahydrofuran block represents about 25% by mass to 90% by mass of the copolymer.

[0120]

The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block
15 which is polytetrahydrofuran (PTHF), wherein the polyamide-12 block represents about 80% by mass to 60% by mass of the copolymer and the polytetrahydrofuran block represents about 20% by mass to 40% by weight of the copolymer.

[0121]

20 The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polytetrahydrofuran (PTHF), wherein the polyamide-12 block represents about 40% by mass to 60% by mass of the copolymer and the polytetrahydrofuran block represents
25 about 60% by mass to 40% by mass of the copolymer.

[0122]

The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is polytetrahydrofuran (PTHF), wherein the polyamide-
30 12 block represents about 30% by mass to 10% by mass of the copolymer and the polytetrahydrofuran block represents about 70% by mass to 90% by mass of the copolymer.

The PEBA copolymer contains i) 10 to 20 polyamide blocks each of which is polyamide-12 (PA-12) and ii) 10 to
35 20 polyether blocks each of which is polytetrahydrofuran

(PTHF).

[0123]

The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block
5 which is polytetrahydrofuran (PTHF), and has a number average molecular weight Mn of about 25000 to about 75000 g/mol.

The PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block
10 which is polytetrahydrofuran (PTHF), and has a number average molecular weight Mn of about 40000 to about 60000 g/mol. In an embodiment of the disclosure, the PEBA copolymer contains i) a polyamide block which is polyamide-12 (PA-12) and ii) a polyether block which is
15 polytetrahydrofuran (PTHF), and has a number average molecular weight Mn of about 50000 g/mol.

[0124]

The PEBA copolymer contains i) a polyamide block which is polyamide-6 (PA-6) and ii) a polyether block which
20 is polytetrahydrofuran (PTHF).

The PEBA copolymer contains i) a polyamide block which is polyamide-11 (PA-11) and ii) a polyether block which is polytetrahydrofuran (PTHF).

The PEBA copolymer is a commercially available elastomer and is marketed under the trade name of PEBAX®.

[0125]

The PEBA copolymer is a commercially available elastomer selected from the group consisting of: PEBAX 2533 SA 01, PEBAX 2533 SA 01 MED, PEBAX 2533 SD 02, PEBAX 3533
30 SA 01, PEBAX 3533 SA 01 MED, PEBAX 3533 SP01, PEBAX 4011, PEBAX 4033 SA 01, PEBAX 4033 SA 01 MED, PEBAX 4033 SP01, PEBAX 4533 SA 01, PEBAX 4533 SA 01 MED, PEBAX 4533 SP01, PEBAX 5513 SA 01, PEBAX 5513 SP01, PEBAX 5533 SA 01, PEBAX 5533 SA 01 MED, PEBAX 5533 SN 70 BLACK, PEBAX 5533 SP01,
35 PEBAX SA 01, PEBAX 6333 SA 01 MED, PEBAX SP01, PEBAX 6333

SP01, PEBAX 6333 SA 01, PEBAX, PEBAX 3533 SA 01, PEBAX 3533
SA 01 MED, PEBAX 3533 SP01, PEBAX 4011 SA 01, PEBAX 4033 SA
01 MED, PEBAX 4033 SP01, PEBAX 4033 SA 01 MED, PEBAX Clear
2533, PEBAX ES 2533 UV, PEBAX MH 2533, PEBAX MH2030, PEBAX
5 MV 5513 SA 01, PEBAX MV 5513 SA 01 MED, PEBAX MV 5533 SP01,
PEBAX MV 5533, PEBAX MV 5533 SP01, PEBAX RNEW® 30R51 SA 01,
PEBAX RNEW 35R53 SP01, PEBAX RNEW 70R53 SP01, PEBAX RNEW
55R53 SP01, PEBAX RNEW 63R53 SP01, PEBAX RNEW 70R53 SP01,
PEBAX RNEW 70R53 SP01, PEBAX, PEBAX RNEW 72R53 SP01, PEBAX
10 RNEW 80R53 SP 02, and a mixture of any of these.

The PEBA copolymer is a commercially available
elastomer and is marketed under the trade name of VESTAMID®
or VESTAMID E.

[0126]

15 The PEBA copolymer is a commercially available
elastomer selected from the group consisting of VESTAMID D,
VESTAMID DX, VESTAMID E, VESTAMID EX, VESTAMID Care,
VESTAMID Care ML, VESTAMID Care ME, VESTAMID Care ME-B,
VESTAMID L, VESTAMID LX, VESTAMID NRG, VESTAMID Terra,
20 VESTAMID X, and a mixture of any of these. Preferred among
these is Pebax MV 1072.

[0127]

The PEBA copolymer may be used in the form of
semisolid or viscous liquid, or in the form of powder,
25 pellets, or granules.

[0128]

The processing aid of the disclosure contains the
synergist in an amount of preferably 0.1% by mass or more,
more preferably 0.5% by mass or more, still more preferably
30 1% by mass or more, while preferably 40% by mass or less,
more preferably 30% by mass or less, still more preferably
20% by mass or less of the composition.

[0129]

In the processing aid of the disclosure, the
35 biodegradable polymer and the synergist have a mass ratio

(biodegradable polymer:synergist) of preferably 99.9:0.1 to 10:90. The mass ratio is more preferably 99.5:0.5 to 30:70, still more preferably 99:1 to 50:50, particularly preferably 98:2 to 60:40. The mass ratio may be 99.5:0.5 to 70:30, or may be 99:1 to 85:15, or may be 98:2 to 92:8. In the case where the processing aid of the disclosure contains no ethylene-vinyl alcohol copolymer, the mass ratio may be 99.9:0.1 to 10:90, or may be 99.5:0.5 to 70:30, or may be 99:1 to 85:15, or may be 98:2 to 92:8.

10 [0130]

The processing aid of the disclosure contains the biodegradable polymer and the synergist in a total amount of preferably 70% by mass or more, more preferably 80% by mass or more, still more preferably 85% by mass or more, particularly preferably 90% by mass or more. The total amount of the biodegradable polymer and the synergist may be 80% by mass or more, or may be 90% by mass or more, or may be 95% by mass or more, or may be 100% by mass.

[0131]

20 The processing aid of the disclosure may further contain a component different from the biodegradable polymer and the synergist.

[0132]

The processing aid of the disclosure preferably contains an ethylene-vinyl alcohol copolymer. This can lead to a better effect of improving the processibility.

[0133]

The ethylene-vinyl alcohol copolymer has a melt flow rate (MFR) of preferably 0.001 g/10 min or higher, more preferably 0.1 g/10 min or higher, still more preferably 0.5 g/10 min or higher, while preferably 40 g/10 min or lower, more preferably 20 g/10 min or lower, still more preferably 10 g/10 min or lower. The ethylene-vinyl alcohol copolymer having a melt flow rate within this range can lead to a better effect of improving the

35

processibility.

[0134]

The ethylene-vinyl alcohol copolymer has an ethylene content of preferably 5 mol% or more, more preferably 10
5 mol% or more, still more preferably 15 mol% or more, while preferably 50 mol% or less, more preferably 40 mol% or less. The ethylene-vinyl alcohol copolymer having an ethylene content within this range can lead to a better effect of improving the processibility.

10 The ethylene content herein is determined by nuclear magnetic resonance (NMR) analysis.

[0135]

The ethylene-vinyl alcohol copolymer is preferably one obtained by saponifying an ethylene-vinyl ester
15 copolymer, and is particularly preferably one obtained by saponifying an ethylene-vinyl acetate copolymer.

[0136]

The ethylene-vinyl alcohol copolymer has a degree of saponification of preferably 80 to 100 mol%.

20 [0137]

Copolymerization of ethylene and vinyl acetate may involve use of a different fatty acid vinyl ester (e.g., vinyl propionate or vinyl pivalate). The ethylene-vinyl alcohol copolymer may contain 0.0002 to 0.2 mol% of a
25 vinylsilane compound as a copolymerized component.

Examples of the vinylsilane compound include vinyltrimethoxysilane, vinyltriethoxysilane, vinyltri(β -methoxy-ethoxy)silane, and γ -methacryloxypropylmethoxysilane. Preferably used among
30 these are vinyltrimethoxysilane and vinyltriethoxysilane.

[0138]

Copolymerization of ethylene and vinyl acetate may involve the presence of a small amount of a monomer different from the aforementioned fatty acid vinyl ester or
35 vinylsilane compound, such as any of α -olefins such as

propylene, isobutylene, α -octene, and α -dodecene;
unsaturated acids such as acrylic acid, methacrylic acid,
crotonic acid, maleic acid, and itaconic acid, and
anhydrides, salts, and mono- or dialkyl esters thereof;
5 nitriles such as acrylonitrile and methacrylonitrile;
amides such as acrylamide and methacrylamide; olefin
sulfonic acids such as ethylene sulfonic acid, allyl
sulfonic acid, and methallyl sulfonic acid and salts
thereof; alkyl vinyl ethers, vinyl ketones, N-
10 vinylpyrrolidone, vinyl chloride, and vinylidene chloride.
[0139]

The ethylene-vinyl alcohol copolymer contains a
polymerized unit based on a monomer different from ethylene
and vinyl alcohol in an amount of preferably 10 mol% or
15 less, more preferably 5 mol% or less, still more preferably
1 mol% or less. The lower limit may be, but is not limited
to, 0% by mass.

The amount of the polymerized unit based on a monomer
different from ethylene and vinyl alcohol herein is
20 determined by nuclear magnetic resonance (NMR) analysis.
[0140]

The processing aid of the disclosure contains the
ethylene-vinyl alcohol copolymer in an amount of preferably
0.1% by mass or more, more preferably 0.5% by mass or more,
25 still more preferably 1% by mass or more, while preferably
90% by mass or less, more preferably 70% by mass or less,
still more preferably 50% by mass or less.
[0141]

In the processing aid of the disclosure, the
30 biodegradable polymer and the ethylene-vinyl alcohol
copolymer have a mass ratio (biodegradable
polymer:ethylene-vinyl alcohol copolymer) of preferably
99:3 to 50:50. The mass ratio is more preferably 95:5 to
60:40, still more preferably 92:8 to 70:30, particularly
35 preferably 90:10 to 75:25. The mass ratio may be 95:5 to

10:90, or may be 90:10 to 75:25, or may be 80:20 to 60:40,
or may be 60:40 to 40:60.

[0142]

In the processing aid of the disclosure, the
5 biodegradable polymer, the ethylene-vinyl alcohol
copolymer, and the synergist have a mass ratio
(biodegradable polymer:ethylene-vinyl alcohol
copolymer:synergist) of preferably (1 to 98):(1 to 98):(1
to 98), more preferably (25 to 90):(5 to 70):(5 to 70),
10 most preferably (56 to 88):(7 to 39):(5 to 37).

[0143]

The processing aid of the disclosure contains the
biodegradable polymer and the ethylene-vinyl alcohol
copolymer in a total amount of preferably 10% by mass or
15 more, more preferably 50% by mass or more, still more
preferably 70% by mass or more. The total amount of the
biodegradable polymer and the ethylene-vinyl alcohol
copolymer may be 80% by mass or more, or may be 90% by mass
or more, or may be 95% by mass or more, or may be 100% by
20 mass.

[0144]

The processing aid of the disclosure preferably
contains a lubricant (A).

[0145]

25 The lubricant (A) is an additive for reducing the
friction and improving the lubricity, and examples thereof
include a wax, an alcohol, and a surfactant. One selected
therefrom may be used alone, or two or more selected
therefrom may be used in combination.

30 The lubricant (A) preferably includes at least one
selected from the group consisting of a wax, an alcohol,
and a surfactant.

[0146]

35 Examples of the wax include pure hydrocarbon waxes
such as liquid paraffin, natural paraffin, microwax,

synthetic paraffin, polyethylene wax, and polyethylene/polypropylene wax; fatty acid waxes such as higher fatty acid and oxy fatty acid; fatty acid amide waxes such as fatty acid amide and bis fatty acid amide; 5 and fatty acid ester waxes such as fatty acid lower alcohol esters, fatty acid polyhydric alcohol esters, e.g., glyceride, fatty acid polyglycol esters, and fatty acid fatty alcohol esters (ester waxes). Preferred among these is a pure hydrocarbon wax or a fatty acid ester wax. The 10 pure hydrocarbon wax is preferably polyethylene wax or polyethylene/polypropylene wax, and the fatty acid ester wax is preferably adipic acid ester or glycerol fatty acid ester.

[0147]

15 Examples of the fatty acid ester wax include a phthalic acid ester, dimethyl or diethyl succinate and esters related thereto, glycerol monoacetate, glycerol diacetate, glycerol triacetate, glycerol monoacid ester, citric acid ester, adipic acid ester, stearic acid ester, 20 and oleic acid ester. One of these may be used alone or two or more thereof may be used.

[0148]

An example of the adipic acid ester is an adipic acid diester. Specific examples thereof include dimethyl 25 adipate, dibutyl adipate, bis[2-(2-methoxyethoxy)ethyl]adipate, bis(butyldiglycol)adipate, bis(methyldiglycol)adipate, benzyl[2-(2-methoxyethoxy)ethyl]adipate, di-n-butyl adipate, dioctyl adipate, methyldiglycol butyldiglycol adipate, benzylmethyl 30 glycol adipate, benzylbutyl diglycol adipate, and diisononyl phthalate. One of these may be used alone or two or more thereof may be used. Preferred among these is diisononyl phthalate or dioctyl adipate.

[0149]

35 Examples of the glycerol fatty acid ester include

glycerol monostearate, glycerol monobehenate, glycerol
mono(12-hydroxystearate), glycerol monooleate, glycerol
monocaprylate, glycerol monocaprate, glycerol monolaurate,
glycerol diacetomonolaurate, succinic acid fatty acid
5 monoglyceride, citric acid fatty acid monoglyceride,
diacetyltartaric acid fatty acid monoglyceride, diglycerol
laurate, diglycerol stearate, diglycerol oleate, diglycerol
monolaurate, diglycerol monomyristate, diglycerol
monostearate, diglycerol monooleate, tetraglycerol
10 stearate, decaglycerol laurate, decaglycerol stearate,
decaglycerol oleate, polyglycerol polyricinoleate,
propylene glycol monolaurate, propylene glycol
monopalmitate, propylene glycol monostearate, propylene
glycol monooleate, and propylene glycol monobehenate. One
15 of these may be used alone or two or more thereof may be
used. Preferred among these is glycerol diacetomonolaurate
or decaglycerol stearate.

[0150]

Examples of the alcohol include fatty alcohols such
20 as higher alcohol and polyhydric alcohols such as
polyglycol and polyglycerol.

[0151]

Examples of the fatty alcohols include lauryl
alcohol, myristyl alcohol, cetyl alcohol, stearyl alcohol,
25 oleyl alcohol, and behenyl alcohol. One of these may be
used alone or two or more thereof may be used.

[0152]

Examples of the surfactant include anionic
surfactants such as metal soap and an ammonium salt
30 surfactant; cationic surfactants such as an alkyl amine
salt and a quaternary ammonium salt; nonionic surfactants
such as ester-based, ether-based, ester/ether-based, and
amide-based surfactants; and amphoteric surfactants such as
an aminocarboxylic acid salt, an alkyl betaine, and an
35 alkyl imidazoline derivative. Preferred among these is an

anionic surfactant or a nonionic surfactant. The anionic surfactant is preferably metal soap, specifically preferably a carboxylic acid salt, a sulfuric acid salt, a sulfonic acid salt, or a phosphoric acid ester salt. The nonionic surfactant is preferably an ester/ether-based surfactant, specifically preferably a sugar-based surfactant.

[0153]

Examples of the metal soap include a fatty acid salt, polysulfonic acid salt, polycarboxylic acid salt, alkyl sulfate salt, alkylaryl sulfonate salt, alkyl naphthalenesulfonate salt, dialkyl sulfonate salt, dialkyl sulfosuccinate salt, alkyl phosphate salt, polyoxyethylene alkyl ether sulfate, polyoxyethylene alkylaryl ether sulfate, and polyoxyethylene alkyl phosphate sulfonate salt, and specific examples thereof include sodium dodecylbenzenesulfonate, sodium laurylsulfate, sodium polyoxyethylene lauryl ether sulfate, and a polyoxyethylene nonylphenyl ether sulfate salt. One of these may be used alone or two or more thereof may be used.

[0154]

The metal soap may be preferably, for example, a compound represented by the following formula:



wherein R^5 is a hydrogen atom or a C1-C21 alkyl group; $n1$ is an integer of 1 to 4; and M^1 is lithium, sodium, potassium, rubidium, caesium, boron, magnesium, aluminum, calcium, manganese, iron, cobalt, nickel, tin, antimony, copper, silver, zinc, molybdenum, vanadium, strontium, zirconium, barium, bismuth, lead, gold, platinum, or any rare-earth element.

[0155]

In the case where $n1$ is an integer of 2 or greater in the formula (1), multiple R^5 s may be the same as or different from each other.

[0156]

The C1-C21 alkyl group for R⁵ may be a linear alkyl group, or may be a branched alkyl group, or may contain an alicyclic structure.

5 [0157]

The C1-C21 alkyl group for R⁵ corresponds to a carboxylic acid residue resulting from removing the carboxyl group (COOH) from a C1-C22 carboxylic acid represented by R⁵COOH used for production of a fatty acid
 10 metal salt. Examples of the carboxylic acid residue include an acetic acid residue, propionic acid residue, butanoic acid residue, pentanoic acid residue, acrylic acid residue, methacrylic acid residue, octylic acid residue (2-ethylhexanoic acid residue), neodecanoic acid residue,
 15 naphthenic acid residue, isononanoic acid residue, eleostearic acid residue, tall oil fatty acid residue, coconut oil fatty acid residue, soybean oil fatty acid residue, linseed oil fatty acid residue, safflower oil fatty acid residue, dehydrated castor oil fatty acid
 20 residue, tung oil fatty acid residue, lauric acid residue, myristic acid residue, palmitic acid residue, stearic acid residue, isostearic acid residue, oleic acid residue, and 12-hydroxystearic acid residue.

[0158]

25 To improve the processibility, the C1-C21 alkyl group for R⁵ is preferably a C12-C21 alkyl group, more preferably a C16-C21 alkyl group, still more preferably a stearic acid residue or 12-hydroxystearic acid residue.

[0159]

30 M¹ is lithium, sodium, potassium, rubidium, caesium, boron, magnesium, aluminum, calcium, manganese, iron, cobalt, nickel, tin, antimony, copper, silver, zinc, molybdenum, vanadium, strontium, zirconium, barium, bismuth, lead, gold, or platinum.

35 [0160]

In the formula, n_1 is a value determined in accordance with the ionic valence of the metal atom M^1 ; for example, when M^1 is boron, n_1 is 3; and when M^1 is cobalt, n_1 is 2.

5 [0161]

The metal soap encompasses the form of a fatty acid boric acid metal salt. The fatty acid boric acid metal salt may be, for example, a compound represented by the following formula (2):

10 $(R^6COO-M^2-O)_3B$ (2)

wherein R^6 is a hydrogen atom or a C1-C21 alkyl group; M^2 is boron, magnesium, aluminum, calcium, manganese, iron, cobalt, nickel, tin, antimony, copper, zinc, molybdenum, vanadium, strontium, zirconium, barium, bismuth, lead, gold, or platinum.

15 [0162]

In the formula (2), the C1-C21 alkyl group for R^6 is defined as described for the C1-C21 alkyl group for R^5 in the formula (1). Similarly, the metal for M^2 in the formula (2) is defined as described for the metal for M^1 in the formula (1).

20 [0163]

One metal soap may be used alone, or two or more metal soaps having different structures may be used.

25 [0164]

Specific examples of the metal soap include metal salts of stearic acid and metal salts of hydroxystearic acid. The metal soap preferably includes at least one selected from the group consisting of a metal salt of stearic acid and a metal salt of hydroxystearic acid, more preferably at least one selected from the group consisting of zinc stearate, magnesium hydroxystearate, and calcium stearate.

35 Examples of the metal constituting the metal salt include zinc, magnesium, and calcium, and the metal

preferably includes at least one selected from the group consisting of zinc, magnesium, and calcium, more preferably at least one selected from the group consisting of zinc and magnesium. The metal soap can be produced by a known
5 method, and may be a commercially available product.
[0165]

An example of the ammonium salt anionic surfactant is a fatty acid ammonium salt. Examples thereof include ammonium laurylsulfate and ammonium polyoxyethylene lauryl
10 ether sulfate. One anionic surfactant may be used, or two or more anionic surfactants may be used.
[0166]

Examples of the cationic surfactant include alkylamine salts and quaternary ammonium salts. Specific
15 examples thereof include stearylamine acetate, trimethylcocoammonium chloride, tallow trimethylammonium chloride, dimethyldioleylammonium chloride, methyloleyldiethanol chloride, tetramethylammonium chloride, laurylpyridinium chloride, laurylpyridinium bromide,
20 laurylpyridinium disulfate, cetyltrimethylammonium chloride, cetylpyridinium bromide, 4-alkyl mercaptopyridine, poly(vinylpyridine)-dodecyl bromide, and (dodecylbenzyl)triethylammonium chloride. One cationic surfactant may be used, or two or more cationic surfactants
25 may be used.
[0167]

Examples of the amphoteric surfactant include an aminocarboxylic acid salt, an alkyl betaine surfactant, and an alkyl imidazoline derivative, and a specific example
30 thereof is lauric acid amidopropylbetaine. One amphoteric surfactant may be used, or two or more amphoteric surfactants may be used.
[0168]

Examples of the ether-based nonionic surfactant
35 include a polyoxyethylene alkyl ether, a polyoxyalkylene

derivative, a polyoxyethylene phenyl ether, and an alkyl allyl ether. Specific examples thereof include polyoxyethylene lauryl ether, polyoxyethylene oleyl ether, and polyoxyethylene octylphenyl ether.

5 An example of the ester/ether-based nonionic surfactant is a sugar-based surfactant. Specific examples thereof include a sorbitan fatty acid ester, sorbitol, and a polyoxyethylene sorbitan fatty acid ester.

10 One nonionic surfactant may be used, or two or more nonionic surfactants may be used.
[0169]

Examples of the sugar-based surfactant include a sucrose fatty acid ester, a sorbitan acid ester, and a polysorbate.

15 Specific examples of the sugar-based surfactant include sorbitol fatty acid esters such as sorbitol monolaurate, sorbitol monostearate, sorbitol monooleate, sorbitol trioleate, sorbitol tristearate, and sorbitol monoisostearate; sorbitan fatty acid esters such as
20 sorbitan isostearate, sorbitan oleate, sorbitan caprylate, sorbitan dioleate, sorbitan distearate, sorbitan stearate, sorbitan sesquiisostearate, sorbitan sesquioleate, sorbitan sesquicaprylate, sorbitan sesquistearate, sorbitan triisostearate, sorbitan trioleate, sorbitan tristearate,
25 sorbitan palmitate, sorbitan coconut fatty acid ester, sorbitan laurate, and sorbitan olive fatty acid ester; sucrose fatty acid esters such as sucrose acetate isobutylate, sucrose octaacetate, sucrose oleate, sucrose distearate, sucrose dilaurate, sucrose stearate, sucrose tetraisostearate, sucrose tetrahydroxystearate, sucrose
30 tristearate, sucrose tribehenate, sucrose trilaurate, sucrose tetrastearate triacetate, sucrose palmitate, sucrose hexaerucate, sucrose hexapalmitate, sucrose pentaerucate, sucrose pentahydroxystearate, sucrose
35 polyoleate, sucrose polystearate, sucrose polysoyate,

sucrose polypalmitate, sucrose polybehenate, sucrose
 polylaurate, sucrose polylinoleate, sucrose
 polycottonseedate, sucrose myristate, sucrose cocoate,
 sucrose laurate, sucrose ricinoleate, sucrose benzoate,
 5 sucrose distearate acetate, and sucrose stearate acetate;
 and alkyl glucosides such as coconut fatty acid glucoside,
 lauryl glucoside, decyl glucoside, myristyl glucoside,
 palmityl glucoside, stearyl glucoside, and cocoglucoside.
 Each of these may be used alone or two or more of these may
 10 be used in combination.

[0170]

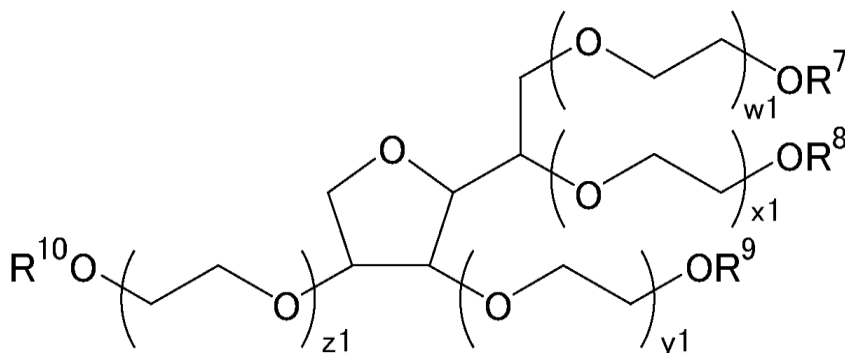
The sugar-based surfactant is preferably a sorbitan
 ester containing a polar sorbitan group (hydrophilic group)
 and a nonpolar carboxylic acid (lipophilic group) bonded
 15 thereto via an ester bond. Also preferred are
 polyoxyethylene derivatives of sorbitan esters and a
 plurality of polyoxyethylene oligomers which are chemical
 substituents on a sorbitan group.

[0171]

20 These polyoxyethylene derivatives of sorbitan esters
 are referred to as polysorbates.

Specifically, a polyoxyethylene derivative of a
 sorbitan ester (also referred to as a polysorbate) may be
 represented by the following formula (I):

25 [Chem. 4]



[0172]

wherein

one of R^7 to R^{10} is a linear fatty acid portion while the other three of R^7 to R^{10} are each hydrogen;

w_1 , x_1 , y_1 , and z_1 are integers satisfying $10 < w_1 + x_1 + y_1 + z_1 < 40$, preferably $15 < w_1 + x_1 + y_1 + z_1 < 25$,
5 more preferably $w_1 + x_1 + y_1 + z_1 = 20$;

the linear fatty acid portion is preferably represented by $(C=O)(CH_2)_aCH_3$, and

the fatty acid portion may instead contain a double bond along a hydrocarbon chain (i.e., optionally contains a
10 monovalent unsaturated portion) so as to be represented by the formula $(C=O)(CH_2)_b(CH)=(CH)(CH_2)_cCH_3$,

where a is an integer of 10 to 25, preferably an integer of 12 to 18, and the linear fatty acid may contain an unsaturated bond;

15 $b + c$ is an integer of 8 to 23, preferably an integer of 10 to 18; and

the number of unsaturated bonds may be such that the hydrocarbon chain contains two or more unsaturated portions, and this number of unsaturated portions is
20 preferably four or less, more preferably three or less, and is particularly preferably maintained at 0, 1, or 2.

[0173]

Specific examples of the polysorbate include polysorbate 20 (polyoxyethylene (20) sorbitan monolaurate),
25 polysorbate 40 (polyoxyethylene (20) sorbitan monopalmitate), polysorbate 60 (polyoxyethylene (20) sorbitan monostearate), and polysorbate 80 (polyoxyethylene (20) sorbitan monooleate).

[0174]

30 The figures 20, 40, 60, and 80 following the "polysorbate" each mean the fatty acid portion ("lipophilic group" of the molecule) added to the polyoxyethylene sorbitan portion ("hydrophilic group" in the molecule); 20 refers to monolaurate; 40 refers to monopalmitate; 60
35 refers to monostearate; and 80 refers to monooleate

(examples of monovalent unsaturated fatty acid portions).
[0175]

The name "polysorbate #" means that 20 oxyethylene
portions $-(\text{CH}_2\text{CH}_2\text{O})-$ are added to the solvate.

5 [0176]

In a specific embodiment, the sugar-based surfactant
may be or may include one or more of polysorbate 20,
polysorbate 40, polysorbate 60, and/or polysorbate 80. For
example, the surfactant may be polysorbate 60 or may
10 include a different polysorbate.
[0177]

Instead of the aforementioned polysorbates, a
surfactant used may be a variation of any aforementioned
specific polysorbate.

15 For example, with reference to the formula I, two,
three, or all of R^7 to R^{10} each may be a linear fatty acid
portion (and the other(s) of R^7 to R^{10} , when present, is
hydrogen).

Examples of this compound include polyoxyethylene
20 sorbitan tristearate in which three of R^7 to R^{10} are each a
fatty acid portion, stearic acid, while the other of R^7 to
 R^{10} is hydrogen.
[0178]

The processing aid of the disclosure contains the
25 lubricant (A) in an amount of preferably 1% by mass or
more, more preferably 2% by mass or more, still more
preferably 4% by mass or more, while preferably 99% by mass
or less, more preferably 60% by mass or less, still more
preferably 40% by mass or less.

30 [0179]

In the processing aid of the disclosure, the
biodegradable polymer and the lubricant (A) have a mass
ratio (biodegradable polymer:lubricant (A)) of preferably
99:1 to 1:99, more preferably 90:10 to 40:60, most
35 preferably 80:20 to 60:40.

[0180]

In the processing aid of the disclosure, the biodegradable polymer, the ethylene-vinyl alcohol copolymer, and the lubricant (A) have a mass ratio
5 (biodegradable polymer:ethylene-vinyl alcohol copolymer:lubricant (A)) of preferably (1 to 98):(1 to 98):(1 to 98), more preferably (25 to 93):(5 to 70):(2 to 70), most preferably (72 to 86):(10 to 24):(4 to 18).

[0181]

10 A preferred combination of the biodegradable polymer, the ethylene-vinyl alcohol copolymer, and the lubricant (A) may be a combination of polylactic acid and/or polybutylene succinate, which corresponds to the biodegradable polymer, an ethylene-vinyl alcohol copolymer, and at least one
15 selected from the group consisting of zinc stearate, magnesium hydroxystearate, and calcium stearate, which corresponds to the lubricant (A). The combination may be different from the above.

[0182]

20 The processing aid of the disclosure preferably contains a degradation inhibitor.

[0183]

The degradation inhibitor suitably used may be a compound containing at least one skeleton selected from the
25 group consisting of a phenol skeleton and a phosphate skeleton.

[0184]

In the case where the degradation inhibitor has a phenol skeleton, the number thereof is preferably, but not
30 limited to, 1 or more, more preferably 2 or more, still more preferably 3 or more, particularly preferably 4 or more, while preferably 100 or less, more preferably 10 or less, still more preferably 6 or less.

[0185]

35 Specific examples of the degradation inhibitor having

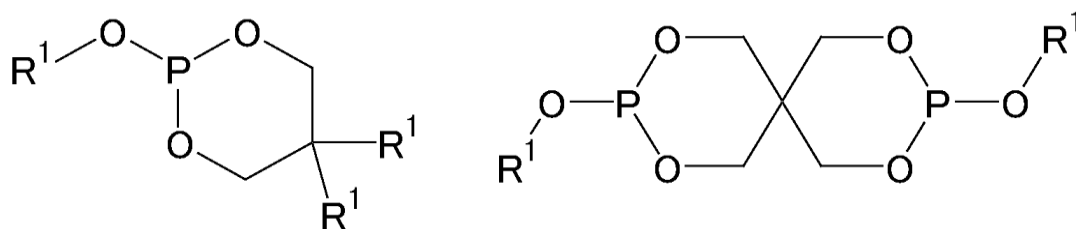
a phenol skeleton include compounds having one phenol skeleton (monocyclic phenol compounds) such as 2,6-di-t-butyl-p-cresol, 2,6-di-t-butyl-4-ethylphenol, 2,6-dicyclohexyl-4-methylphenol, 2,6-diisopropyl-4-ethylphenol, 2,6-di-t-amyl-4-methylphenol, 2,6-di-t-octyl-4-n-propylphenol, 2,6-dicyclohexyl-4-n-octylphenol, 2-isopropyl-4-methyl-6-t-butylphenol, 2-t-butyl-4-ethyl-6-t-octylphenol, 2-isobutyl-4-ethyl-6-t-hexylphenol, 2-cyclohexyl-4-n-butyl-6-isopropylphenol, a styrenated cresol mixture, DL- α -tocopherol, stearyl β -(3,5-di-t-butyl-4-hydroxyphenyl)propionate, and 2,6-di-t-butyl-4-(4,6-bis(octylthio)-1,3,5-triazin-2-ylamino)phenol; compounds having two phenol skeletons (bicyclic phenol compounds) such as 2,2'-methylenebis(4-methyl-6-t-butylphenol), 4,4'-butylidenebis(3-methyl-6-t-butylphenol), 4,4'-thiobis(3-methyl-6-t-butylphenol), 2,2'-thiobis(4-methyl-6-t-butylphenol), 4,4'-methylenebis(2,6-di-t-butylphenol), 2,2'-methylenebis[6-(1-methylcyclohexyl)-p-cresol], 2,2'-ethylidenebis(4,6-di-t-butylphenol), 2,2'-butylidenebis(2-t-butyl-4-methylphenol), 3,6-dioxaoctamethylenebis[3-(3-t-butyl-4-hydroxy-5-methylphenyl)propionate], triethylene glycol bis[3-(3-t-butyl-5-methyl-4-hydroxyphenyl)propionate], 1,6-hexanediol bis[3-(3,5-di-t-butyl-4-hydroxyphenyl)propionate], and 2,2'-thiodiethylenebis[3-(3,5-di-t-butyl-4-hydroxyphenyl)propionate]; compounds having three phenol skeletons (tricyclic phenol compounds) such as 1,1,3-tris(2-methyl-4-hydroxy-5-t-butylphenyl)butane, 1,3,5-tris(2,6-dimethyl-3-hydroxy-4-t-butylbenzyl)isocyanurate, 1,3,5-tris[(3,5-di-t-butyl-4-hydroxyphenyl)propionyloxyethyl]isocyanurate, tris(4-t-butyl-2,6-dimethyl-3-hydroxybenzyl)isocyanurate, 1,3,5-trimethyl-2,4,6-tris(3,5-di-t-butyl-4-hydroxybenzyl)benzene; and compounds having four phenol skeletons (tetracyclic phenol compounds) such as

tetrakis[methylene-3-(3,5-di-t-butyl-4-hydroxyphenyl)propionate]methane and pentaerythritoltetrakis[3-(3,5-di-tert-butyl-4-hydroxyphenyl)propionate]. Preferred among these are
 5 tetracyclic phenol compounds, more preferred are tetrakis[methylene-3-(3,5-di-t-butyl-4-hydroxyphenyl)propionate]methane and pentaerythritoltetrakis[3-(3,5-di-tert-butyl-4-hydroxyphenyl)propionate], still more preferred is
 10 pentaerythritoltetrakis[3-(3,5-di-tert-butyl-4-hydroxyphenyl)propionate].
 [0186]

The phosphate skeleton refers to one having a structure in which one to four O (oxygen) atoms are bonded
 15 to one P (phosphorus) atom. Preferred is one in which three O (oxygen) atoms are bonded to one P (phosphorus) atom.
 [0187]

In the case where the degradation inhibitor has a
 20 phosphate skeleton, the number thereof is preferably, but not limited to, 1 or more, more preferably 2 or more, still more preferably 3 or more, while preferably 100 or less, more preferably 10 or less, still more preferably 6 or less.
 25 [0188]

Specific examples of the degradation inhibitor having a phosphate skeleton include:
 [Chem. 5]



30 (wherein R¹ is selected from the group consisting of a C1-C16 linear or branched alkyl group and an aryl group, where

R¹s are the same as or different from each other), and a compound represented by the formula P(OR¹)₃ (wherein R¹ is selected from the group consisting of C4-C32 linear or branched alkyl groups). More specific examples thereof
5 include trilauryl phosphite, triisodecyl phosphite, tridecyl phosphite, trihexadecyl phosphite, trioctadecyl phosphite, tribehenyl phosphite, trirachidyl phosphite, triceryl phosphite, trioleyl phosphite, tris(2-ethylhexyl)phosphite, phosphorous acid diposphoric acid
10 salts and polymer homologs such as monostearyl phosphite (or its tautomer, monostearyl phosphonate) and distearyl phosphite (distearyl phosphonate), partially esterified phosphonic acid compounds, and alkali salts, alkaline-earth salts, aluminum salts, and zinc salts thereof.

15 [0189]

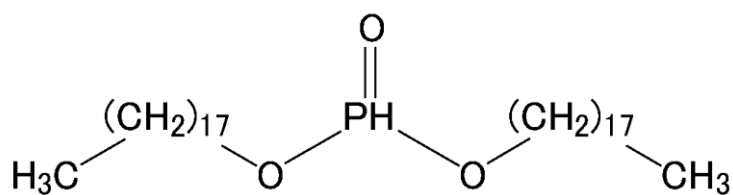
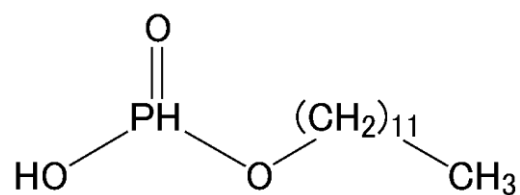
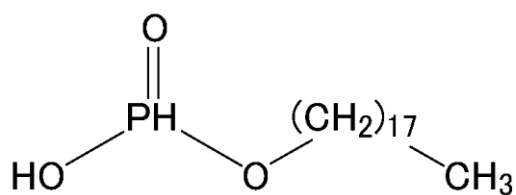
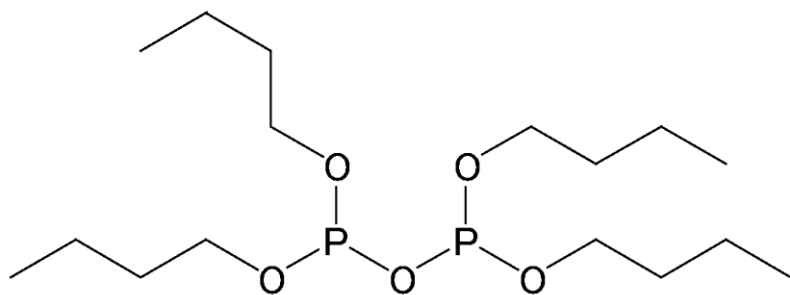
Examples of diposphorous acid include tetraethyl diposphite and tetrapropyl diposphite. Examples of triphosphorous acid include triphosphorigenic acid P,P'-bis(2-hydroxyethyl) ester.

20 [0190]

Oligophosphites and polyphosphites (oligomer phosphites and polymer phosphites) are disclosed in WO 2011/102861, WO 2014/20519, and WO 2020/123986, for example. Compounds disclosed in these documents may also
25 be used. Examples thereof include the following compounds.

[0191]

[Chem. 6]

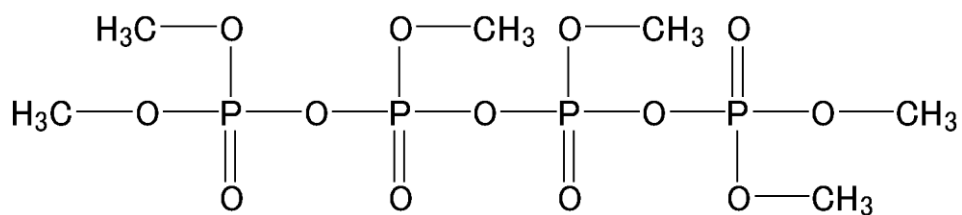
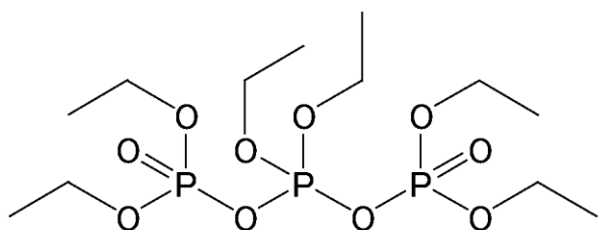
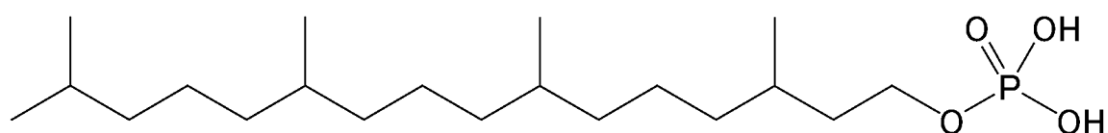
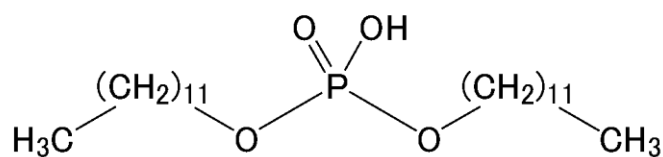
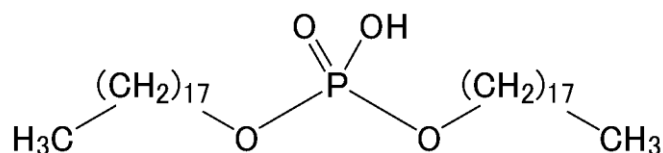


[0192]

Examples also include phosphoric acid esters, diposphoric acid esters, metaphosphoric acid esters, and polyphosphoric acid esters derived from any of the
 5 aforementioned phosphorous acid esters, such as trilauryl phosphate, triisodecyl phosphate, tridecyl phosphate, trihexadecyl phosphate, trioctadecyl phosphate, tribehenyl phosphate, triarachidyl phosphate, triceryl phosphate, and
 10 trioleyl phosphate, the following structures and salts derived therefrom, and any mixture of at least two phosphoric acid esters selected from the group consisting of a monoalkyl phosphoric acid ester, a dialkyl phosphoric acid ester, and a trialkyl phosphoric acid ester.

15 [0193]

[Chem. 7]



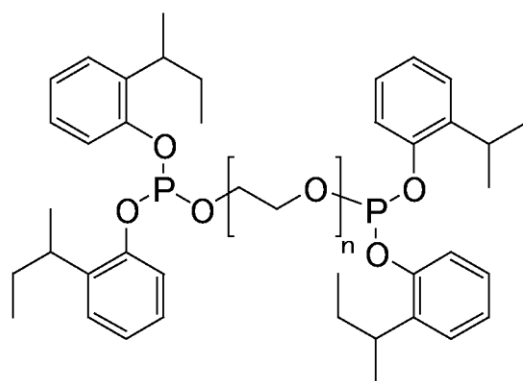
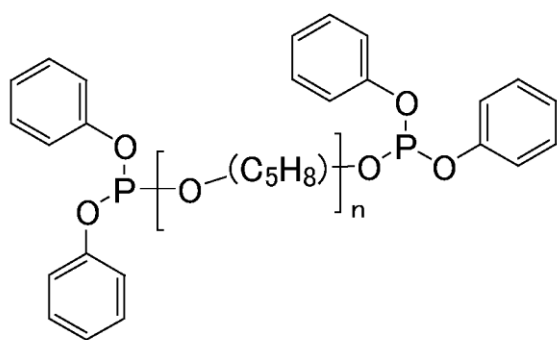
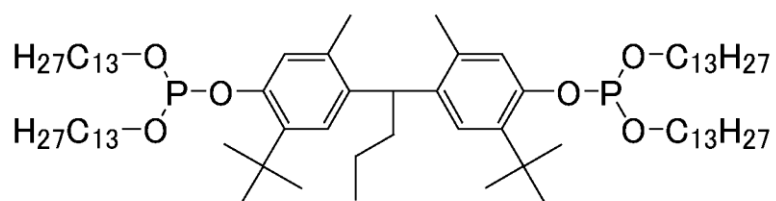
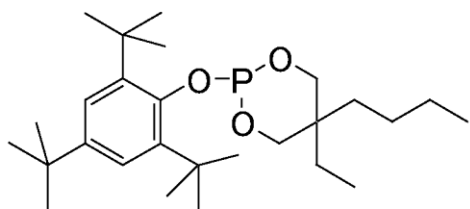
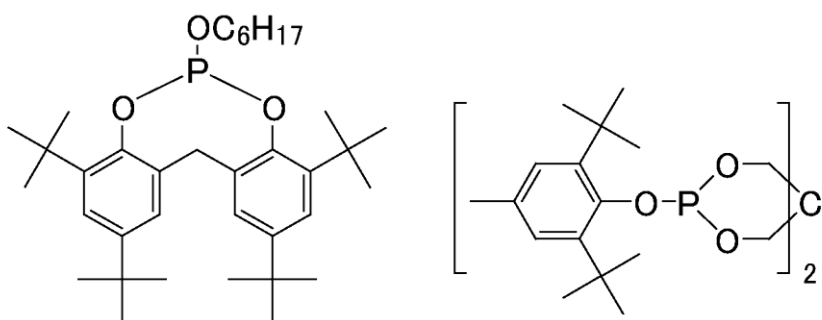
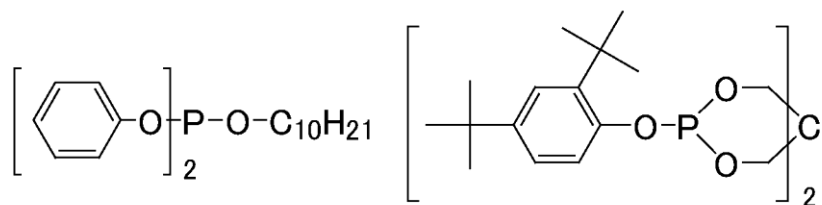
In the case of the aforementioned phosphoric acid ester, diphosphoric acid ester, metaphosphoric acid ester, or polyphosphoric acid ester, i.e., any of the
5 aforementioned phosphorous acid ester derivatives, the phosphorus atoms are present not with an oxidation number of +III as in the case of a phosphorous acid ester, but with an oxidation number of +V.

[0195]

The degradation inhibitor having a phosphate skeleton is preferably a phosphorous acid salt. Examples of the phosphorous acid salt include the following compounds.

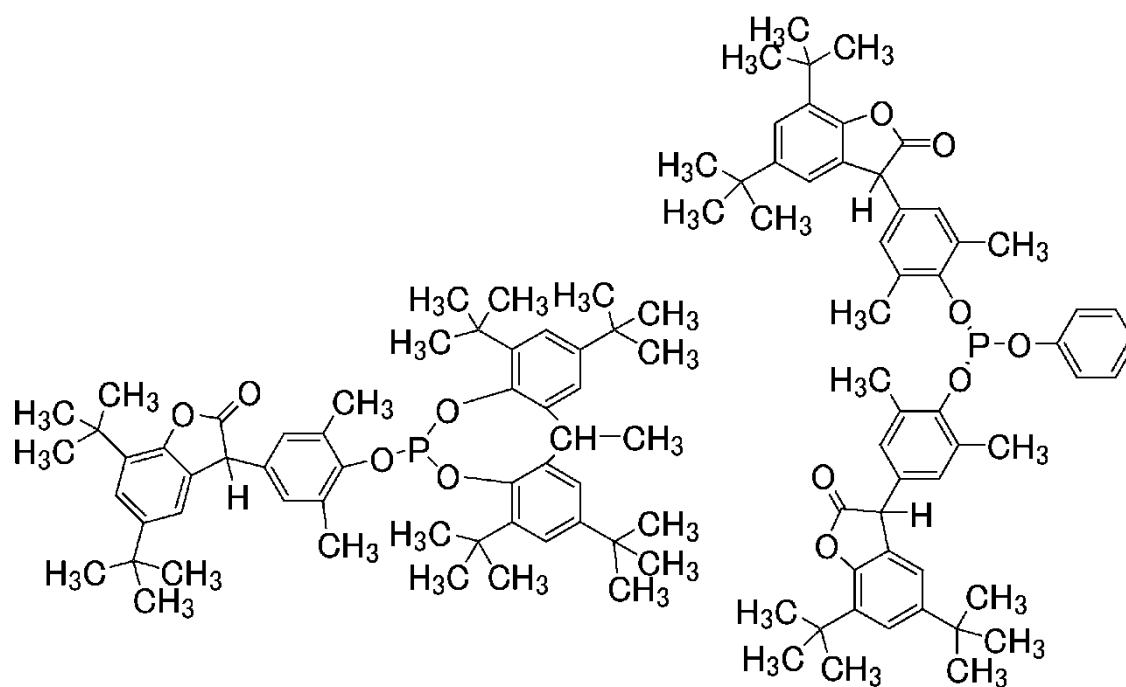
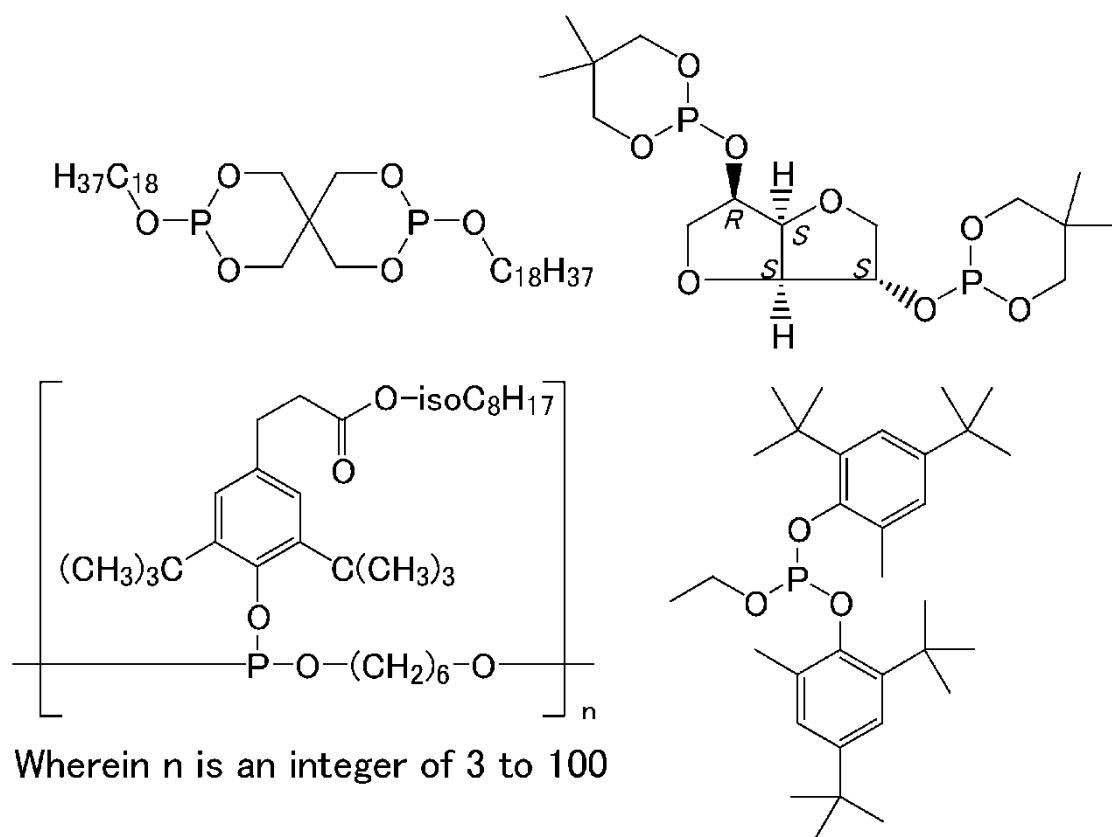
5 [0196]

[Chem. 8]



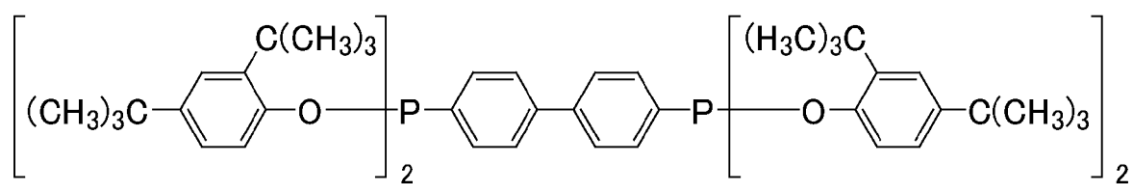
[0197]

[Chem. 9]



[0198]

[Chem. 10]



[0199]

An example of a particularly preferred phosphorous acid salt is tris(2,4-di-tert-butylphenyl)phosphite.

5 [0200]

Specific examples of the degradation inhibitor having a phenol skeleton and a phosphate skeleton include phosphorus-containing phenol compounds such as calcium bis(ethyl 3,5-di-tert-butyl-4-hydroxybenzylphosphonate) and nickel bis(ethyl 3,5-di-tert-butyl-4-hydroxybenzylphosphonate).

10

[0201]

The degradation inhibitor may have either a phenol skeleton or a phosphate skeleton, or may have both a phenol skeleton and a phosphate skeleton, and preferably has either a phenol skeleton or a phosphate skeleton.

15

[0202]

The degradation inhibitor used is preferably a combination of one having a phenol skeleton alone (phenol degradation inhibitor) and one having a phosphate skeleton alone (phosphate degradation inhibitor). This can lead to good pressure stability during extrusion.

20

[0203]

In the case where the degradation inhibitor used is a combination of a phenol degradation inhibitor and a phosphate degradation inhibitor, they have a mass ratio (phenol degradation inhibitor:phosphate degradation inhibitor) of preferably 20:80 to 80:20. The mass ratio is more preferably 30:70 to 70:30, still more preferably 40:60 to 60:40, particularly preferably 50:50.

25

30 [0204]

The processing aid of the disclosure contains the degradation inhibitor in an amount of preferably 10% by

mass or more, more preferably 30% by mass or more, still more preferably 40% by mass or more, while preferably 80% by mass or less, more preferably 70% by mass or less, still more preferably 60% by mass or less.

5 [0205]

The processing aid of the disclosure is substantially free from fluorine. The phrase "substantially free from fluorine" means that the processing aid has a fluorine content of 10 ppm or less, preferably 1 ppm or less, more
10 preferably 0.1 ppm or less. More preferably, the processing aid of the disclosure is free from fluorine (has a fluorine content of 0% by mass).

[0206]

The processing aid of the disclosure may be
15 obtainable by a mixing step of mixing the biodegradable polymer fed to a mixer and an ejecting step of ejecting the mixture from the mixer, for example. The disclosure also relates to a method for producing the aforementioned processing aid including a mixing step and an ejecting
20 step.

[0207]

The process in the mixing step may be, but is not limited to, mixing (kneading) with a shear force or mixing without a shear force. To effectively achieve the molding
25 processibility, kneading is preferred, and melt-kneading is more preferred.

In the case of melt-kneading, the components may be melted in the mixing step or may be melted before the mixing step.

30 [0208]

In the production method, the ejecting step may be followed by a molding step of molding the ejected matter using a molding machine, for example.

Examples of the process in the molding step include,
35 but are not limited to, extrusion molding, injection

molding, and blow molding. To effectively achieve the molding processibility, extrusion molding is preferred among these.

[0209]

5 The extrusion molding is performed using an extruder. Examples of the extruder include a single-screw extruder, a twin-screw extruder, and a tandem extruder. The extruder commonly includes a cylinder, a screw housed in the cylinder, a die attached to the tip of the cylinder, and a
10 hopper for feeding pellets to the cylinder.

[0210]

 The conditions relating to the molding are not limited and may be set as appropriate in accordance with, for example, the compositional ratio and amount of the
15 composition as well as the shape and size of a desired molded article. The processing aid of the disclosure may be in any form such as powder, granules, or pellets; to achieve excellent handleability and easy molding, pellets are preferred.

20 [0211]

 The processing aid of the disclosure is particularly useful as a processing aid for thermoplastic resin (particularly, polyolefin resin).

[0212]

25 <Masterbatch>

 The masterbatch of the disclosure contains the processing aid of the disclosure and a thermoplastic resin (A).

 The processing aid of the disclosure as it is may be
30 added to a target such as a thermoplastic resin; still, adding the processing aid in the form of masterbatch can lead to weighing stability and good dispersibility, i.e., a better effect of improving the processibility.

[0213]

35 Examples of the thermoplastic resin (A) include a

polyolefin polymer (e.g., polyethylene (PE), polypropylene (PP), and an ethylene-propylene copolymer), polystyrene (PS), AS (acrylonitrile styrene) resin (AS), ABS (acrylonitrile butadiene styrene) resin (ABS), methacrylic resin (PMMA), polymethyl pentene (PMP), polybutadiene resin (BDR), polybutene-1 (PB-1), polyvinyl alcohol (PVA), polyacrylonitrile (PAN), polystyrene methacrylate (MS), an ethylene-vinyl acetate copolymer (EVA), an ethylene-vinyl alcohol copolymer, and polyvinyl chloride (PVC). Each of these may be used alone or two or more of these may be used in combination. To achieve a better effect of improving the processibility, a polyolefin polymer (polyolefin resin) is preferred.

[0214]

15 An example of the polyolefin polymer is a homopolymer (e.g., a homopolymer of a C2-C10 α -olefin, preferably a C2-C6 α -olefin). Specific examples of the homopolymer include homo-polyethylene and homo-polypropylene (hPP). In the case of homo-polyethylene, for example, this polymer can be produced by free-radical polymerization in a high-pressure process and is typically known as a highly branched ethylene homopolymer, which is often referred to as LDPE (low-density polyethylene), having a density of lower than 0.945 g/cm³, often 0.935 g/cm³ or lower, e.g., within a range from 0.900, 0.905, or 0.910 g/cm³ to 0.920, 0.925, 0.927, 0.930, 0.935, or 0.945 g/cm³. Unless otherwise described herein, the densities of all polymers are determined in conformity with ASTM D1505. A sample is formed through the step C of ASTM D4703-10a and left under the conditions in ASTM D618-08 (23 $\pm$ 2°C and relative humidity 50 $\pm$ 10%) for 40 hours before testing.

[0215]

35 In another example, an ethylene monomer can be polymerized in a phase of a known gas, slurry, and/or solution (using, e.g., a catalyst such as chromium catalyst

or a single site catalyst such as Ziegler-Natta and/or metallocene catalyst), each of which is well known in the polymerization technique and is therefore not elaborated herein. In the case of producing a more highly linear ethylene homopolymer (e.g., using gas-phase or slurry-phase polymerization with any of the above catalysts), this is referred to as HDPE (high-density polyethylene), which typically has a density of 0.945 g/cm³ or higher, e.g., within a range from 0.945 to 0.970 g/cm³.

10 [0216]

Examples of the polymer also include copolymers of two or more C₂-C₄₀ α -olefins, e.g., C₂-C₂₀ α -olefins, such as ethylene- α -olefin copolymers and propylene- α -olefin copolymers (e.g., a propylene-ethylene copolymer and a propylene-ethylene-diene terpolymer (also known as EPDM and PEDM)). Specific examples intended herein include an ethylene copolymer and one or more C₃-C₂₀ α -olefin comonomer such as a C₄-C₁₂ α -olefin comonomer (1-butene, 1-hexene, 1-octene, or a mixture of any two or more of these is preferred in a variety of embodiments). The ethylene copolymer (e.g., a copolymer of ethylene and one or more C₃-C₂₀ α -olefins) may contain an ethylene-derived unit in an amount of at least 90, 94, 95, or 96% by weight (e.g., within a range from a lower value of 80, 85, 90, 80, 85, 93, 93, 95, 96, or 97 wt% to a higher value of 94, 95, 95.5, 91, 92, 97, 94, 97.5, or 98 wt%; at least 96 wt% or 96.5 wt%), and may contain the unit in an amount within the range from any of the lower values to any of the higher values based on the total amount of the ethylene-derived unit and a comonomer-derived unit. For example, the ethylene copolymer may contain 94 or 95% by mass to 97 or 98% by mass of an ethylene-derived unit based on the total amount of the ethylene-derived unit and a comonomer-derived unit. The balance of the copolymer (based on the ethylene-derived unit and the comonomer-derived unit) consists of

the comonomer-derived unit. For example, a comonomer unit (e.g., a unit derived from a C2-C20 α -olefin such as a unit derived from butene, hexene, and/or octene) may be present in an amount within a range from a lower value of 2, 2.5, 3, 3.5, 4, 4.5, 5, or 6% by mass to a higher value of 3, 4, 5, 6, 7, 8, 9, 10, 15, or 20% by mass, and the range thereof is from any of the above lower values to any intended value among the above higher values (provided that the higher value is greater than the lower value).

10 [0217]

Some appropriate comonomers have already been known for ethylene-based, propylene-based, or other α -olefin-based copolymers; in various embodiments, other α -olefin comonomers are intended. For example, the α -olefin comonomer may be linear or branched, and two or more comonomers may be used as appropriate. Examples of appropriate comonomers include C3-C20 linear α -olefins (e.g., butene, hexene, and octene, as described above) and α -olefins having one or more C1-C3 alkyl branches or aryl groups. Examples include: propylene; 3-methyl-1-butene; 3,3-dimethyl-1-butene; 1-pentene; 1-pentene having one or more methyl, ethyl, or propyl substituents; 1-hexene having one or more methyl, ethyl, or propyl substituents; 1-heptene having one or more methyl, ethyl, or propyl substituents; 1-octene having one or more methyl, ethyl, or propyl substituents; 1-nonene having one or more methyl, ethyl, or propyl substituents; ethyl-, methyl- or dimethyl-substituted 1-decene; 1-dodecene; and styrene. The above list of comonomers shows mere examples and is not intended to set any limitation. In some embodiments, the comonomer includes propylene, 1-butene, 1-pentene, 4-methyl-1-pentene, 1-hexene, 1-octene, and styrene.

[0218]

In a specific embodiment, the polymer may include an ethylene copolymer or may be an ethylene copolymer

35

(according to the above description). The ethylene copolymer can be produced by gas, slurry, or solution phase polymerization. Some particularly preferred ethylene copolymers can be produced by gas or slurry phase
5 polymerization. Specific examples include linear low-density polyethylene (LLDPE) and a copolymer of ethylene and one or more α -olefins, which are polymerized in the presence of one or more single site catalysts, e.g., one or more Ziegler-Natta catalysts, one or more metallocene
10 catalysts, or combination of any of these. This LLDPE may have a density within a range from a lower concentration of 0.900, 0.905, 0.907, or 0.910 g/cm³ to a higher concentration of 0.920, 0.925, 0.930, 0.935, 0.940, or 0.945 g/cm³. The density of the LLDPE may be from 0.902 to
15 0.945, or may be 0.906 to 0.932, or may be from 0.908 to 0.926. LLDPE is distinguishable from the aforementioned LDPE in some respects, many of which are well-known in the technical field, including the degree of branching (in many cases, there are few branches, if present) in the polymer
20 produced. It should be noted that LLDPE has substantially a small number of long chain branches. In a specific embodiment, the polymer of the polymer composition is or includes a metallocene catalyst LLDPE (mLLDPE). In other embodiments, the polymer of the polymer composition is or
25 includes a Ziegler-Natta catalyst LLDPE (or ZN-LLDPE).
[0219]

In some embodiments, the density of the polymer falls within a range from 0.905 to 0.945 g/cm³, e.g., from a lower value of 0.905, 0.907, 0.908, 0.910, 0.911, 0.912,
30 0.913, 0.914, or 0.915 g/cm³ to a higher value of 0.916, 0.917, 0.918, 0.919, 0.920, 0.924, 0.926, 0.930, 0.935, 0.940, or 0.945 g/cm³, and the range thereof is from any of the above lower values to any of the above higher values intended herein (e.g., from 0.910 to 0.925 or 0.935 g/cm³,
35 e.g., from 0.912 to 0.925 or from 0.915 to 0.918 g/cm³).

In other embodiments, the polymer may be a higher-density one (e.g., HDPE) having a density within a range from 0.945 g/cm³ to 0.970 g/cm³.

[0220]

5 The rheological characteristics of a polymer can have influence on the processing aid composition for forming a molded article. In common cases, a PPA composition is preferably used in a polymer having a melt index (MI or I2 is measured at 190°C and a 2.16 kg load in conformity with
10 ASTM D1238) of 1.5 g/2.0 min or lower, preferably 2.5 g/3.0 min or lower, such as within a range from 0.1, 0.2, or 0.5 g/10 min to 1.0, 1.2, 5.0, 10, 2.5, 10, 4.0, or 5.0 g/10 min. In some embodiments, the polymer may commonly have a melt index ratio (MIR) (MIR herein is defined as the ratio
15 of the high-load melt index (HLMI) (determined at 190°C and a 21.6 kg load per ASTM D1238) to the melt index or as HLMI/MI) within a range from 10, 12, or 15 to 19, 20, 21, 22, 25, 27, 30, 35, 40, 45, 50, 60, 65, 70, 75, 80, 85, 90, 95, or 100. If necessary, this polymer may have a MI of
20 lower than 1.5 g/10 min, such as 1.0 g/10 min or lower (e.g., from 0.1, 0.2, or 0.5 g/10 min to 1.0; or any of 1.1, 1.2, 1.3, or 1.4, or lower than 1.5 g/10 min).

[0221]

 The LLDPE preferably includes at least one selected
25 from the group consisting of a Ziegler-Natta catalyst LLDPE and a metallocene catalyst LLDPE. Particularly preferred is a metallocene catalyst LLDPE.

[0222]

 The thermoplastic resin (A) may have crystallinity or
30 may have no crystallinity. The thermoplastic resin (A) having crystallinity has a melting point of preferably 80°C to 300°C, more preferably 100°C to 200°C. The thermoplastic resin (A) having no crystallinity preferably has a processing temperature substantially equal to that of
35 a thermoplastic resin (A) whose melting point range is

indicated by its crystallinity.

[0223]

In the masterbatch of the disclosure, the thermoplastic resin (A) and the processing aid have a mass ratio (thermoplastic resin (A):processing aid) of
5 preferably 99:1 to 1:99. The mass ratio is more preferably 97:3 to 50:50, still more preferably 95:5 to 60:40, particularly preferably 92:8 to 70:30. The mass ratio may be 99:1 to 5:95, or may be 90:10 to 7:93, or may be 75:35
10 to 8:92, or may be 30:70 to 10:90.

[0224]

The masterbatch of the disclosure contains the thermoplastic resin (A) and the processing aid in a total amount of preferably 80% by mass or more, more preferably
15 90% by mass or more, still more preferably 95% by mass or more, particularly preferably 100% by mass.

[0225]

The masterbatch of the disclosure has a melt flow rate (MFR) of preferably 0.01 g/10 min or higher, more
20 preferably 0.1 g/10 min or higher, still more preferably 1.0 g/10 min or higher, while preferably 100 g/10 min or lower, more preferably 50 g/10 min or lower, still more preferably 20 g/10 min or lower. The masterbatch having a MFR within this range can lead to a better effect of
25 improving the processibility.

The MFR herein is determined under conditions of 190°C and a 2.16 kgf load in conformity with ASTM D1238.

[0226]

The masterbatch of the disclosure may contain a
30 component different from the thermoplastic resin (A) and the processing aid.

[0227]

The masterbatch of the disclosure may be obtainable by a mixing step of mixing the processing aid of the
35 disclosure, which is prepared in advance, and the

thermoplastic resin (A) fed to a mixer and an ejecting step of ejecting the mixture from the mixer, or may be obtainable by a mixing step of mixing the thermoplastic resin (A) and the biodegradable polymer fed to a mixer and an ejecting step of ejecting the mixture from the mixer, for example. The disclosure also relates to a method for producing the aforementioned masterbatch including a mixing step and an ejecting step.

[0228]

In the method for producing a masterbatch of the disclosure, the ejecting step may be followed by a molding step of molding the ejected matter using a molding machine, for example.

[0229]

The mixing step, the ejecting step, and the molding step in the method for producing a masterbatch of the disclosure are the same as those described for the method for producing a processing aid of the disclosure. The masterbatch of the disclosure may be in any form such as powder, granules, or pellets; to achieve excellent handleability and easy molding, pellets are preferred.

[0230]

The masterbatch of the disclosure is particularly useful as a masterbatch for improving the processibility of thermoplastic resin (particularly, polyolefin resin).

[0231]

<Thermoplastic resin composition>

The thermoplastic resin composition of the disclosure contains the processing aid of the disclosure and/or the masterbatch of the disclosure, and a thermoplastic resin (B). This leads to good processibility (particularly, extrusion processibility).

[0232]

The thermoplastic resin (B) used may be the same as the thermoplastic resin (A), and a preferred form thereof

is also the same as that of the thermoplastic resin (A).

[0233]

The thermoplastic resin composition of the disclosure at least contains at least one of the processing aid of the disclosure or the masterbatch of the disclosure, and
5 preferably contains the masterbatch of the disclosure to achieve better processibility.

[0234]

In the case where the thermoplastic resin composition
10 of the disclosure contains the masterbatch of the disclosure, the thermoplastic resin (A) and the thermoplastic resin (B) may be the same as or different from each other.

[0235]

15 The thermoplastic resin composition of the disclosure contains the processing aid in an amount of preferably 0.001% by mass or more, more preferably 0.01% by mass or more, still more preferably 0.06% by mass or more, further preferably 0.10% by mass or more, particularly preferably
20 0.15% by mass or more, while preferably 5.0% by mass or less, more preferably 3.0% by mass or less, still more preferably 2.0% by mass or less, particularly preferably 1.5% by mass or less. The amount may be 0.001% by mass or more, may be 0.01% by mass or more, may be 0.1% by mass or
25 more, may be 0.3% by mass or more, or may be 0.5% by mass or more, while may be 5% by mass or less, may be 2% by mass or less, may be 1.5% by mass or less, or may be 1.0% by mass or less.

[0236]

30 The thermoplastic resin composition of the disclosure may contain a component different from the processing aid, the masterbatch, and the thermoplastic resin (B).

Examples of the component different from the processing aid, the masterbatch, and the thermoplastic
35 resin (B) include an anti-agglomerating agent; an

ultraviolet absorber; a flame retarder; a reinforcing material such as glass fiber or glass powder; a stabilizer such as mineral or flaky material; a lubricant such as silicone oil or molybdenum disulfide; a pigment such as titanium dioxide or red iron oxide; a conductive agent such as carbon black; an impact resistance improver such as rubber; an antioxidant such as a hindered phenol- or phosphorus-based antioxidant; a nucleating agent such as metal salt or acetal of sorbitol; an antiblocking agent; and the aforementioned lubricant (A).

[0237]

The thermoplastic resin composition of the disclosure may be obtainable by a mixing step of mixing the masterbatch of the disclosure, which is prepared in advance, and the thermoplastic resin (B) fed to a mixer and an ejecting step of ejecting the mixture from the mixer, or may be obtainable by a mixing step of mixing the thermoplastic resin (B) and the biodegradable polymer, optionally the thermoplastic resin (A), fed to a mixer and an ejecting step of ejecting the mixture from the mixer, for example. The disclosure also relates to a method for producing the aforementioned thermoplastic resin composition including a mixing step and an ejecting step.

[0238]

In the method for producing a thermoplastic resin composition of the disclosure, the ejecting step may be followed by a molding step of molding the ejected matter using a molding machine, for example.

[0239]

The mixing step, the ejecting step, and the molding step in the method for producing a thermoplastic resin composition of the disclosure are the same as those described for the method for producing a processing aid of the disclosure.

[0240]

<Molded article>

The molded article of the disclosure is obtainable from the thermoplastic resin composition of the disclosure and may be obtainable by, for example, a molding step of
5 molding the thermoplastic resin composition of the disclosure.

The disclosure also relates to a method for producing a molded article including a molding step.

The thermoplastic resin composition of the disclosure
10 is suitable for a molded article in the form of tube, film, or sheet, and may be applicable to a molded article in a different form.

[0241]

The molding step is the same as that described for
15 the method for producing a processing aid of the disclosure.

[0242]

In the molding step, the molding temperature (extruding temperature) during molding is commonly equal to
20 or higher than the melting point of the thermoplastic resin (B) and lower than the decomposition temperature of the biodegradable polymer. To allow the processing aid to significantly exert its effects, the molding temperature preferably falls within a range of 160°C or higher and
25 270°C or lower.

The molding temperature may also be referred to as the extrusion temperature in the case of extrusion molding.

[0243]

Examples of applications of the molded article of the
30 disclosure include, but are not limited to, bags, coating materials, dishware such as drink containers, electric wires, cables, pipes, fibers, bottles, gasoline tanks, and other industrial molded articles.

[0244]

35 <Film>

The film of the disclosure is obtainable from the thermoplastic resin composition of the disclosure and may be obtainable by, for example, a molding step of molding the thermoplastic resin composition of the disclosure.

5 The disclosure also relates to a method for producing a molded article including a molding step.

 The thermoplastic resin composition of the disclosure is suitable for a molded article in the form of tube, film, or sheet, and may be applicable to a molded article in a
10 different form.

[0245]

 The molding step is the same as that described for the method for producing a processing aid of the disclosure.

15 [0246]

 In the molding step, the molding temperature (extruding temperature) during molding is commonly equal to or higher than the melting point of the thermoplastic resin (B) and lower than the decomposition temperature of the
20 biodegradable polymer. To allow the processing aid to significantly exert its effects, the molding temperature preferably falls within a range of 160°C or higher and 270°C or lower.

 The molding temperature may also be referred to the
25 extrusion temperature in the case of extrusion molding.

[0247]

 Examples of applications of the film of the disclosure include, but are not limited to, bags, coating materials, dishware such as drink containers, electric
30 wires, cables, pipes, fibers, bottles, gasoline tanks, and other industrial molded articles.

[0248]

 It should be appreciated that a variety of modifications and changes in the structure and other
35 details may be made to the aforementioned embodiments

without departing from the spirit and scope of the claims.

EXAMPLES

[0249]

5 The disclosure is described with reference to, but not limited to, examples.

[0250]

 The following materials were used in the examples and the comparative examples.

10 (Additive (biodegradable polymer))

 PBS-1: polybutylene succinate (MFR: 22 g/10 min, melting point: 114°C)

 PBS-2: polybutylene succinate (MFR: 4 g/10 min, melting point: 85°C)

15 PBS-3: polybutylene succinate (MFR: 250 g/10 min, melting point: 114°C)

 PLA-1: polylactic acid (MFR: 3 g/10 min, melting point: 153°C)

20 PLA-2: polylactic acid (MFR: 30 g/10 min, melting point: 172°C)

 PLA-3: polylactic acid (MFR: 110 g/10 min, melting point: 174°C)

 PBAT: polybutylene adipate terephthalate (MFR: 4 g/10 min, melting point: 115°C)

25 (Additive (synergist))

 PCL: polycaprolactone (Mw: 80000, melting point: 55°C)

 PEG-1: polyethylene glycol (Mn: 8000, melting point: 63°C)

30 PEG-2: polyethylene glycol (Mn: 35000, melting point: 63°C)

 PEO-1: polyethylene oxide (Mv: 150000 to 400000, melting point: 64°C)

35 PEO-2: polyethylene oxide (Mv: 400000 to 600000, melting point: 65°C)

PEO-3: polyethylene oxide (Mv: 600000 to 1100000, melting point: 66°C)

MB50-002: silicone (ultra-high molecular weight silicone-containing masterbatch, available from Dupont)

5 GENIOPLAST PELLET S: silicone (ultra-high molecular weight silicone, available from Wacker Asahikasei Silicone Co., Ltd.)

Pebax MV1072: polyamide-polyether block copolymer (available from Arkema)

10 (Additive (ethylene-vinyl alcohol copolymer))

EVOH-1: ethylene-vinyl alcohol copolymer (ethylene content: 38 mol%, MFR: 1.5 g/10 min)

EVOH-2: ethylene-vinyl alcohol copolymer (ethylene content: 32 mol%, MFR: 1.6 g/10 min)

15 EVOH-3: ethylene-vinyl alcohol copolymer (ethylene content: 44 mol%, MFR: 1.6 g/10 min)

EVOH-4: ethylene-vinyl alcohol copolymer (ethylene content: 38 mol%, MFR: 50 g/10 min)
(Additive (lubricant (A)))

20 Polysorbate 60: polysorbate 60

Zn-St: zinc stearate (stearic acid zinc salt)

MG-C18(OH): magnesium 12-hydroxystearate

(Additive (degradation inhibitor))

25 Phenol-based: pentaerythritol tetrakis[3-(3,5-di-tert-butyl-4-hydroxyphenyl)propionate]

Phosphate-based: tris(2,4-di-tert-butylphenyl)phosphite

(Matrix resin and carrier resin)

30 LLDPE-1: metallocene catalyst linear low-density polyethylene (MFR: 0.7 g/10 min, melting point: 123°C, d = 0.926, MIR = 28.1)

LLDPE-2: metallocene catalyst linear low-density polyethylene (MFR: 2.0 g/10 min, melting point: 121°C, d = 0.925, MIR = 23.6)

35 LLDPE-3: Ziegler-Natta catalyst linear low-density

polyethylene (MFR: 0.8 g/10 min, melting point: 123°C, d = 0.925, MIR = 27.0)

LLDPE-4: Ziegler-Natta catalyst linear low-density polyethylene (MFR: 2.0 g/10 min, melting point: 121°C, d = 0.918, MIR = 23.2)

LDPE: low-density polyethylene (MFR: 2.0 g/10 min, melting point: 111°C, d = 0.924)
[0251]

MFR:

The MFRs (g/10 min) of the additives, matrix resins, and carrier resins were determined under conditions of 190°C and a 2.16 kgf load in conformity with ASTM D1238.
[0252]

MIR:

The MIRs of the matrix resins and carrier resins were determined by HLMI/MI.

HLMI: MFR (g/10 min) at 190°C and 21.6 kgf load in conformity with ASTM D1238

MI: MFR (g/10 min) at 190°C and 2.16 kgf load in conformity with ASTM D1238
[0253]

Melting point:

The melting point was defined as the temperature corresponding to the maximum value on a heat-of-fusion curve with a temperature-increasing rate of 10°C/min using a DSC device (available from Seiko Instruments Inc.).
[0254]

Examples A1 to A15 and Comparative Examples A1 to A10

The materials were each dry blended with a matrix resin (LLDPE-1) in the proportion shown in Table 1, whereby a thermoplastic resin composition was obtained. The processibility of the thermoplastic resin composition obtained was evaluated by the following extrusion evaluation. The results are shown in Table 1.

In Comparative Examples A3 to A10, extrusion was not

successfully performed due to slip.

[0255]

Examples B1 to B8 and Comparative Examples B1 to B6

Additives were dry blended at the ratio shown in
5 Table 2, whereby a processing aid was obtained. The
processing aid obtained was dry blended with a matrix resin
(LLDPE-1) in the proportion shown in Table 2, whereby a
thermoplastic resin composition was obtained. The
processibility of the thermoplastic resin composition
10 obtained was evaluated by the following extrusion
evaluation. The results are shown in Table 2.

In Comparative Examples B3 to B6, extrusion was not
successfully performed due to slip.

[0256]

15 Examples C1 to C15, Comparative Examples C1 to C10,
Examples D1 to D9, and Comparative Examples D1 to D11

First, the carrier resin and the additive(s) were
melt-kneaded in the proportions shown in Table 3 or 4 using
a twin-screw extruder (TEX α III available from Japan Steel
20 Works, Ltd.) under the conditions including a cylinder
temperature of 180°C to 200°C, a die temperature of 200°C,
and a screw rotational speed of 400 rpm, whereby a
masterbatch (MB) was obtained. The masterbatch obtained
was then dry blended with a matrix resin (LLDPE-1) in the
25 proportion shown in Table 3 or 4, whereby a thermoplastic
resin composition was obtained. The processibility of the
thermoplastic resin composition obtained was evaluated by
the following extrusion evaluation. The results are shown
in Table 3 or 4.

30 [0257]

Examples E1 to E13 and Comparative Example E1

Additives were dry blended at the ratio shown in
Table 5, whereby a processing aid was obtained. The
processing aid obtained was dry blended with a matrix resin
35 (LLDPE-1) in the proportion shown in Table 5, whereby a

thermoplastic resin composition was obtained. The processibility of the thermoplastic resin composition obtained was evaluated by the following extrusion evaluation. The results are shown in Table 5.

5 [0258]

Examples F1 to F16 and Comparative Example F1

First, the carrier resin and the additive(s) were melt-kneaded in the proportions shown in Table 6 using a twin-screw extruder (TEXαIII available from Japan Steel Works, Ltd.) under the conditions including a cylinder temperature of 180°C to 200°C, a die temperature of 200°C, and a screw rotational speed of 400 rpm, whereby a masterbatch (MB) was obtained. The masterbatch obtained was then dry blended with a matrix resin (LLDPE-1) in the proportion shown in Table 6, whereby a thermoplastic resin composition was obtained. The processibility of the thermoplastic resin composition obtained was evaluated by the following extrusion evaluation. The results are shown in Table 6.

20 [0259]

In Tables 1 to 4, the following examples have the same contents.

Examples A3 and B7

Examples A10 and B8

25 Examples C3 and D8

Examples C10 and D9

Comparative Examples A1, B1, C1, E1, and F1

Comparative Examples A2 and B2

[0260]

30 <Extrusion evaluation>

Each material was extruded for 60 minutes through a single screw extruder (Rheomex OS available from HAAKE, L/D: 33, screw diameter: 20 mm, die diameter: 2 mm) under the conditions including a cylinder temperature of 170°C to 200°C, a die temperature of 200°C, and a shear rate of

35

450/sec, which was evaluated for the following items.

Before each test operation, linear low-density polyethylene containing 15% by mass of silica was fed into a hopper and the screw rotational speed was increased to
 5 150 rpm to perform purging for about 15 minutes. The same LLDPE-1 as one to be used for the test was then fed to perform purging for about 15 minutes. The screw rotational speed was returned to 30 rpm and extrusion was performed until the temperature stabilized. After the pressure
 10 surely returned to the initial pressure, a next experiment was performed. If the pressure did not return to the initial value, the above purging process was repeated until the pressure returned to the initial value and a next experiment was then performed.

15 (Melt fracture (MF) state)

The matrix resin alone was extruded until the pressure was stabilized while melt fracture occurred on the entire surface. The point of time at which the screw appeared was defined as zero, and the matrix resin was then
 20 extruded for 60 minutes. In the examples where the processing aid or the masterbatch was used, they were fed to the hopper at the zero point. The appearance of a strand at an early stage of extrusion and the appearance of a strand at completion of extrusion were checked by visual
 25 and tactile inspection. A change in MF, which was observed at an early stage of extrusion, was evaluated by the following criteria. The smaller the value is, the better the MF state is.

- 1: MF completely disappeared.
- 30 2: MF reduced but not completely disappeared.
- 3: MF hardly changed or hardly reduced in comparison with the case of matrix resin alone.

(Pressure stability)

The extrusion pressure between 50 and 60 minutes from
 35 the start of extrusion was measured and the standard

deviation thereof was calculated. The closer the value is to 0, the better the pressure stability is.

(Die buildup (DBU))

The state of the die after extrusion was visually
5 observed and the presence of DBU (die drool) was evaluated.

In Tables 1 to 4, the DBU was evaluated in 3 grades by the following criteria. The smaller the value is, the better the DBU evaluation is.

1: No DBU occurred.

10 2: A little DBU occurred.

3: Much DBU occurred.

In Tables 5 and 6, the DBU was evaluated in 5 grades from 1 to 5. The smaller the value is, the smaller the amount of DBU occurred and the better the evaluation is,
15 with the grade 1 indicating no occurrence of DBU.

In Tables 1 to 4, both the 3 grade evaluation and the 5 grade evaluation are shown.

(Melt fracture (MF) disappearance time)

The period of time was measured from the zero point
20 of time described for the aforementioned MF state to the point when MF disappeared. The shorter the period of time is, the better the MF disappearance time is. The cases where MF did not disappear after 60 minutes from the extrusion are expressed with the symbol "-".

25 [0261]

[Table 1]

		Composition of processing aid	Concentration of additive in thermoplastic resin composition (mass%)	Extrusion evaluation				
				Additive	MF state	Pressure stability	DBU (3 grades)	DBU (5 grades)
Examples	A1	PBS-1	1.00	1	2.52	3	4	38
	A2	PBS-1	0.60	1	2.91	3	4	40
	A3	PBS-1	0.50	1	3.16	3	3	40
	A4	PBS-1	0.20	1	3.21	3	3	40
	A5	PBS-1	0.05	2	5.88	2	2	-
	A6	PBS-2	0.50	1	3.17	3	4	40
	A7	PBS-3	0.50	2	5.12	3	4	-
	A8	PLA-1	1.00	1	2.42	3	4	38
	A9	PLA-1	0.60	1	2.87	3	4	40
	A10	PLA-1	0.50	1	3.01	3	3	40
	A11	PLA-1	0.20	1	3.13	3	3	40
	A12	PLA-1	0.05	2	4.90	2	2	-
	A13	PLA-2	0.50	1	2.98	3	4	40
	A14	PLA-3	0.50	1	3.21	3	4	50
	A15	PBAT	1.00	2	5.78	3	4	-
Comparative Examples	A1	-	0.00	3	0.40	3	4	-
	A2	PCL	1.00	3	0.88	2	2	-
	A3	PEG-1	0.10	Extrusion not successfully performed (slip)				
	A4	PEG-1	0.50					
	A5	PEG-2	0.10					
	A6	PEG-2	0.50					
	A7	PEO-1	0.10					
	A8	PEG-1	0.50					
	A9	PEO-3	0.10					
	A10	PEO-3	0.50					

[0262]

[Table 2]

	Composition of processing aid			Concentration of additive 1 + additive 2 in thermoplastic resin composition (mass%)	Extrusion evaluation				
	Additive 1	Additive 2	Mass ratio (additive 1/2)		MF state	Pressure stability	DBU (3 grades)	DBU (5 grades)	MF disappearance time (min)
Examples	B1	PBS-1	PEG-1	95/5	0.50	1	2.81	2	35
	B2	PLA-1	PEG-1	95/5	0.50	1	2.12	2	30
	B3	PLA-1	PEG-1	99/1	0.50	1	2.32	2	35
	B4	PLA-1	PEO-1	90/10	0.50	1	2.56	2	35
	B5	PLA-1	PEO-1	95/5	0.50	1	2.80	2	35
	B6	PLA-1	PEO-3	95/5	0.50	1	2.99	3	40
	B7	PBS-1	-	100/0	0.50	1	3.16	3	40
	B8	PLA-1	-	100/0	0.50	1	3.01	3	40
Comparative Examples	B1	-	-	-	0.00	3	0.40	4	-
	B2	PCL	-	100/0	1.00	3	0.88	2	-
	B3	-	PEG-1	0/100	0.50	Extrusion not successfully performed (slip)			
	B4	-	PEO-1	0/100	0.50				
	B5	PEG-1	PEO-2	50/50	0.50				
	B6	PEG-1	PEO-3	50/50	0.50				

[0263]

[Table 3]

		Composition of masterbatch			Concentration of additive in thermoplastic resin composition (mass%)	Extrusion evaluation				
		Carrier resin	Additive	Concentration of additive in masterbatch (mass%)		MF state	Pressure stability	DBU (3 grades)	DBU (5 grades)	MF disappearance time (min)
Examples	C1	LLDPE-1	PBS-1	10	0.50	2	0.83	1	1	-
	C2	LLDPE-1	PBS-1	25	1.00	1	0.83	2	2	40
	C3	LLDPE-1	PBS-1	25	0.50	1	0.97	1	1	40
	C4	LLDPE-1	PBS-1	50	1.00	1	0.92	2	2	35
	C5	LLDPE-1	PBS-1	50	0.50	1	1.00	1	1	40
	C6	LLDPE-1	PBS-1	75	0.50	1	3.00	2	3	40
	C7	LLDPE-1	PBS-2	25	0.50	1	0.99	1	1	40
	C8	LLDPE-1	PLA-1	10	0.50	2	0.78	1	1	-
	C9	LLDPE-1	PLA-1	25	1.00	1	0.79	2	2	40
	C10	LLDPE-1	PLA-1	25	0.50	1	0.80	1	1	40
	C11	LLDPE-1	PLA-1	50	1.00	1	0.91	2	2	35
	C12	LLDPE-1	PLA-1	50	0.50	1	1.03	1	1	40
	C13	LLDPE-1	PLA-1	75	0.50	1	2.80	3	3	40
	C14	LLDPE-2	PLA-1	25	0.50	1	0.85	1	1	40
	C15	LLDPE-1	PLA-2	25	0.50	1	0.98	1	1	40
Comparative Examples	C1	-	-	-	0.00	3	0.40	3	4	-
	C2	LLDPE-1	PCL-1	25	0.50	3	0.70	2	3	-
	C3	LLDPE-1	PCL-1	50	0.50	3	0.81	2	3	-
	C4	LLDPE-1	PEG-1	5	0.50	2	3.27	2	3	-
	C5	LLDPE-1	PEG-2	5	0.15	2	2.50	2	3	-
	C6	LLDPE-1	PEG-2	5	0.50	2	2.70	2	3	-
	C7	LLDPE-1	PEO-1	5	0.10	3	2.01	2	3	-
	C8	LLDPE-1	PEO-1	5	0.50	2	2.50	2	3	-
	C9	LLDPE-1	PEO-3	5	0.10	3	1.98	2	3	-
	C10	LLDPE-1	PEO-3	5	0.50	3	2.40	2	3	-

[0264]

[Table 4]

	Composition of masterbatch						Concentration of additive 1 + additive 2 in thermoplastic resin composition (mass%)	Extrusion evaluation				
	Carrier resin	Additive 1	Additive 2	Mass ratio (additive 1/2)	Concentration of additive 1 + additive 2 in masterbatch (mass%)	MF state		Pressure stability	DBU (3 grades)	DBU (5 grades)	MF disappearance time (min)	
Examples	D1	LLDPE-1	PBS-1	PEG-1	95/5	25	0.50	1	0.85	1	1	35
	D2	LLDPE-1	PLA-1	PEG-1	95/5	25	0.50	1	0.78	1	1	30
	D3	LLDPE-1	PLA-1	PEG-1	99/1	25	0.50	1	0.90	1	1	40
	D4	LLDPE-1	PLA-1	PEO-1	90/10	25	0.50	1	0.85	1	1	35
	D5	LLDPE-1	PLA-1	PEO-1	95/5	25	0.50	1	0.80	1	1	35
	D6	LLDPE-1	PLA-1	PEO-3	95/5	25	0.50	1	0.95	1	1	40
	D7	LLDPE-1	PLA-1	PCL	95/5	25	0.50	1	0.96	1	1	40
	D8	LLDPE-1	PBS-1	-	100/0	25	0.50	1	0.97	1	1	40
	D9	LLDPE-1	PLA-1	-	100/0	25	0.50	1	0.80	1	1	40
Comparative Examples	D1	LLDPE-1	-	PEG-1	0/100	5	0.50	2	3.27	2	3	-
	D2	LLDPE-1	-	PEG-2	0/100	5	0.50	2	2.70	2	3	-
	D3	LLDPE-1	-	PEG-2	0/100	5	0.15	3	2.50	2	3	-
	D4	LLDPE-1	-	PEO-1	0/100	5	0.10	3	2.01	2	3	-
	D5	LLDPE-1	-	PEO-1	0/100	5	0.50	2	2.50	2	3	-
	D6	LLDPE-1	-	PEO-3	0/100	5	0.10	3	1.98	2	3	-
	D7	LLDPE-1	-	PEO-3	0/100	5	0.50	3	2.40	2	3	-
	D8	LLDPE-1	PEG-1	PEO-2	50/50	5	0.10	2	3.01	2	3	-
	D9	LLDPE-1	PEG-1	PEO-3	50/50	5	0.10	3	2.99	2	3	-
	D10	LLDPE-1	PEG-1	PEO-3	50/50	5	0.50	2	3.40	3	3	-
	D11	LLDPE-1	PCL	PEO-1	50/50	5	0.50	3	1.60	2	3	-

[0265]

[Table 5]

		Composition of processing aid			Concentration of additive 1 + additive 2 in thermoplastic resin composition (mass%)	Extrusion evaluation			
		Additive 1	Additive 2	Mass ratio (additive 1/2)		MF state	MF disappearance time (min)	DBU (5 grades)	Pressure stability
Examples	E1	PLA-1	EVOH-1	95/5	0.25	1	33	3	2.31
	E2	PLA-1	EVOH-1	90/10	0.25	1	30	3	1.95
	E3	PLA-1	EVOH-1	80/20	0.25	1	30	3	1.89
	E4	PLA-1	EVOH-1	50/50	0.25	1	30	3	1.74
	E5	PLA-1	EVOH-1	20/80	0.25	1	30	3	1.92
	E6	PLA-1	EVOH-1	80/20	0.10	1	32	3	2.11
	E7	PLA-1	EVOH-2	80/20	0.25	1	30	3	1.91
	E8	PLA-1	EVOH-3	80/20	0.25	1	30	3	1.92
	E9	PLA-1	EVOH-4	80/20	0.25	1	33	3	2.89
	E10	PLA-2	EVOH-1	80/20	0.25	1	30	3	1.91
	E11	PBS-1	EVOH-1	80/20	0.25	1	33	3	2.76
	E12	PLA-1	-	-	0.25	1	40	3	3.13
	E13	PBS-1	-	-	0.25	1	40	3	3.21
Comparative Example	E1	-	-	-	-	3	-	4	0.40

[0266]

[Table 6]

	Composition of masterbatch					Concentration of additive 1 + additive 2 in thermoplastic resin composition (mass%)	Extrusion evaluation				
	Carrier resin	Additive 1	Additive 2	Mass ratio (additive 1/2)	Concentration of additive 1 + additive 2 in masterbatch (mass%)		MF state	MF disappearance time (min)	DBU (5 grades)	Pressure stability	
Examples	F1	LLDPE-1	PLA-1	EVOH-1	95/5	25	0.25	1	38	1	0.55
	F2	LLDPE-1	PLA-1	EVOH-1	90/10	25	0.25	1	30	1	0.53
	F3	LLDPE-1	PLA-1	EVOH-1	80/20	25	0.25	1	30	1	0.53
	F4	LLDPE-1	PLA-1	EVOH-1	50/50	25	0.25	1	30	1	0.60
	F5	LLDPE-1	PLA-1	EVOH-1	20/80	25	0.25	1	30	2	0.61
	F6	LLDPE-1	PLA-1	EVOH-1	80/20	50	0.25	1	30	1	0.55
	F7	LLDPE-1	PLA-1	EVOH-1	80/20	70	0.25	1	30	2	0.98
	F8	LLDPE-1	PLA-1	EVOH-1	80/20	25	0.10	1	35	1	0.60
	F9	LLDPE-2	PLA-1	EVOH-1	80/20	25	0.25	1	30	1	0.55
	F10	LLDPE-1	PLA-1	EVOH-2	80/20	25	0.25	1	30	1	0.53
	F11	LLDPE-1	PLA-1	EVOH-3	80/20	25	0.25	1	35	1	0.52
	F12	LLDPE-1	PLA-1	EVOH-4	80/20	25	0.25	1	38	2	1.00
	F13	LLDPE-1	PLA-2	EVOH-1	80/20	25	0.25	1	30	1	0.53
	F14	LLDPE-1	PBS-1	EVOH-1	80/20	25	0.25	1	38	1	0.70
	F15	LLDPE-1	PLA-1	-	-	25	0.25	1	50	1	0.80
	F16	LLDPE-1	PBS-1	-	-	25	0.25	1	50	1	0.97
Comparative Example	F1	-	-	-	-	-	-	3	-	4	0.40

Examples 1 to 83 and Comparative Examples 1 to 3

First, the carrier resin and the additive(s) were melt-kneaded in the proportions shown in any of Tables 7 to 9 using a twin-screw extruder (TEXαIII available from Japan Steel Works, Ltd.) under the conditions including a cylinder temperature of 180°C to 200°C, a die temperature of 200°C, and a screw rotational speed of 400 rpm such that the concentration of the additive(s) was 25% by mass, whereby a masterbatch (MB) was obtained. The masterbatch obtained was then dry blended with a matrix resin in the proportion shown in any of Tables 7 to 9, and the processibility in this case was evaluated by the following extrusion evaluation. The results are shown in Tables 7 to 9. The materials of the additives used each contained no fluorine and the processing aid therefore had a fluorine content of 0% by mass.

[0267]

<Extrusion evaluation>

For Examples 1 to 72 and Comparative Examples 1 to 3, each material was extruded for 60 minutes through a single screw extruder (Rheomex OS available from HAAKE, L/D: 33, screw diameter: 20 mm, die diameter: 2 mm) under the conditions including a cylinder temperature of 170°C to 200°C, a die temperature of 200°C, and a shear rate of 450/sec, which was evaluated for the following items.

Before each test operation, linear low-density polyethylene containing 15% by mass of silica was fed into a hopper and the screw rotational speed was increased to 150 rpm to perform purging for about 15 minutes. The same matrix resin as one to be used for the test was then fed to perform purging for about 15 minutes. The screw rotational speed was returned to 30 rpm and extrusion was performed until the temperature stabilized. After the pressure surely returned to the initial pressure, a next experiment was performed. If the pressure did not return to the

initial value, the above purging process was repeated until the pressure returned to the initial value and a next experiment was then performed.

(Melt fracture (MF) state)

5 The matrix resin alone was extruded until the pressure was stabilized while melt fracture occurred on the entire surface. The point of time at which the screw appeared was defined as zero, and the matrix resin was then extruded for 60 minutes. In the examples where the
10 processing aid or the masterbatch was used, they were fed to the hopper at the zero point. The appearance of a strand at an early stage of extrusion and the appearance of a strand at completion of extrusion were checked by visual and tactile inspection. A change in MF, which was observed
15 at an early stage of extrusion, was evaluated by the following criteria. The smaller the value is, the better the MF state is.

Disappeared: MF completely disappeared.

20 Not disappeared: MF hardly changed, or MF reduced but not completely disappeared in comparison with the case of matrix resin alone.

(Die buildup (DBU))

25 The samples with MF completely disappeared were subjected to the extrusion evaluation during long-run molding (three hours). The state of the die after extrusion was visually observed and the presence of DBU (die drool) was evaluated.

30 The DBU was evaluated in 5 grades from 1 to 5. The smaller the value is, the smaller the amount of DBU occurred and the better the evaluation is, with the grade 1 indicating no occurrence of DBU.

(Storage stability test)

35 In Example 29, Example 36, Example 41, Example 46, and Example 47, long-run molding (three hours) was performed and a strand sample was collected, which was left

to stand at 80°C for 24 hours. After 24 hours had passed, the strand was subjected to sensory evaluation (tactile sensation) for the surface smoothness and the smoothness was evaluated before and after the test according to the following criteria. The results are shown in Table 8.

Yes: The smoothness after the test was higher than that before the test.

No: The smoothness did not change before and after the test.

10 [0268]

<Film formation>

For Examples 73 to 83, each material was extruded for 70 minutes through a monolayer inflation molding machine (inflation die diameter: 25 mm, die gap: 0.8 mm) under the conditions including a cylinder temperature of 170°C, a die temperature of 200°C, and a shear rate of 90/sec, which was evaluated for the following items. Before each test operation, linear low-density polyethylene containing 15% by mass of silica was fed into a hopper to perform purging for about 60 minutes. The same matrix resin as one used for the test was then fed to perform purging for about 60 minutes. After the pressure surely returned to the initial pressure, a next experiment was performed. If the pressure did not return to the initial value, the above purging process was repeated until the pressure returned to the initial value and a next experiment was then performed.

25 [0269]

(Melt fracture (MF) disappearance time)

The matrix resin alone was extruded until the pressure stabilized while melt fracture occurred on the entire surface. The point of time at which the screw appeared was defined as zero, and the matrix resin was then extruded for 70 minutes. In the examples where the processing aid or the masterbatch was used, they were fed to the hopper at the zero point. The appearance of a film

at an early stage of extrusion and the appearance of a film after start of extrusion were checked by visual and tactile inspection and the period of time until disappearance was recorded. The shorter the period of time is, the better the MF disappearance time is. The results are shown in Table 9.

[0270]

(Pressure stability)

After five minutes from the MF disappearance, the extrusion pressure was measured at 1-minute intervals for 20 minutes and the standard deviation thereof was calculated. The closer the value is to 0, the better the pressure stability is. The results are shown in Table 9.

[0271]

(Film thickness)

At the 50-minute, 60-minute, and 70-minute points from the start of film extrusion, the film was collected for three minutes. One measurement site was set in the TD direction of each collected film, and the film thickness was measured at 25 points (75 points in total) in the MD direction at 25°C. The average, the maximum, and the minimum were then calculated. The thickness unevenness was then calculated by the following formula. The results are shown in Table 9.

Thickness unevenness (%) = (maximum thickness (max) - minimum thickness (min)) / average thickness (average) × 100

[0272]

<MFR of masterbatch>

For Examples 84 to 91, the carrier resin and the additives were melt-kneaded in the proportions shown in Table 10 using a twin-screw extruder (TEXαIII available from Japan Steel Works, Ltd.) under the conditions including a cylinder temperature of 180°C to 200°C, a die temperature of 200°C, and a screw rotational speed of 400 rpm such that the concentration of the additives was 25% by

mass, whereby a masterbatch (MB) was obtained. The MFR (g/10 min) of the masterbatch obtained was measured (under conditions of 190°C and a 2.16 kgf load in conformity with ASTM D1238). The results are shown in Table 10.

5 [0273]

[Table 7]

	Matrix resin	Composition of masterbatch				Concentration of additives (ppm) *1	Extrusion evaluation	
		Carrier resin	Additive 1	Additive 2	Synergist	Mass ratio (additive 1/ additive 2/ Synergist)	MF state	DBU (5 grades)
Example 1	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PEG-1	76/19/5	Disappeared	1
Example 2	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PEG-1	56/14/30	Disappeared	1
Example 3	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PEG-1	85/10/5	Disappeared	1
Example 4	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PEG-1	63/7/30	Disappeared	1
Example 5	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PEO-1	76/19/5	Disappeared	1
Example 6	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PEO-1	56/14/30	Disappeared	1
Example 7	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PEO-1	85/10/5	Disappeared	1
Example 8	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PEO-1	63/7/30	Disappeared	1
Example 9	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PCL	76/19/5	Disappeared	2
Example 10	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PCL	56/14/30	Disappeared	2
Example 11	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PCL	85/10/5	Disappeared	2
Example 12	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	PCL	63/7/30	Disappeared	2
Example 13	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	MB50-002	76/19/5	Disappeared	2
Example 14	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	MB50-002	56/14/30	Disappeared	2
Example 15	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	MB50-002	85/10/5	Disappeared	2
Example 16	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	MB50-002	63/7/30	Disappeared	2
Example 17	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	Genioplast Pellet S	76/19/5	Disappeared	2
Example 18	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	Genioplast Pellet S	56/14/30	Disappeared	2
Example 19	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	Genioplast Pellet S	85/10/5	Disappeared	2
Example 20	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	Genioplast Pellet S	63/7/30	Disappeared	2
Example 21	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	Pebax MV1072	76/19/5	Disappeared	1
Example 22	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	Pebax MV1072	56/14/30	Disappeared	1
Example 23	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	Pebax MV1072	85/10/5	Disappeared	1
Example 24	LLDPE-1	LLDPE-2	PLA-1	EVOH-1	Pebax MV1072	63/7/30	Disappeared	1

*1: ((additive 1 + additive 2 + synergist)/(matrix resin + carrier resin + additive 1 + additive 2 + synergist)

[0274]

[Table 8-1]

	Matrix resin	Composition of masterbatch					Concentration of additives (ppm) *2	Extrusion evaluation		Storage stability
		Carrier resin	Additive 1	Additive 2	Additive 3	Mass ratio (additive 1/ additive 2/ additive 3)		MF state	DBU (5 grades)	
Comparative Example 1	LLDPE-1	LLDPE-2	-	-	-	-	-	Not disappeared	5	Bleed out
Comparative Example 2	LLDPE-1	LLDPE-2	Polysorbate60	-	-	100/0/0	1500	Not disappeared	-	
Comparative Example 3	LLDPE-1	LLDPE-2	Zn-St	-	-	100/0/0	1500	Not disappeared	-	
Example 25	LLDPE-1	LLDPE-2	PLA	Zn-St	-	90/10/0	1500	Disappeared	1	
Example 26	LLDPE-1	LLDPE-2	PLA	Zn-St	-	40/60/0	1500	Disappeared	3	
Example 27	LLDPE-1	LLDPE-2	PLA	Zn-St	-	80/20/0	1500	Disappeared	2	
Example 28	LLDPE-1	LLDPE-2	PLA	Zn-St	-	60/40/0	1500	Disappeared	2	
Example 29	LLDPE-1	LLDPE-2	PLA	Zn-St	-	70/30/0	1500	Disappeared	2	Yes
Example 30	LLDPE-1	LLDPE-2	PLA	Zn-St	-	70/30/0	1000	Disappeared	2	
Example 31	LLDPE-1	LLDPE-2	PLA	Zn-St	-	70/30/0	600	Disappeared	2	
Example 32	LLDPE-1	LLDPE-2	PLA	Mg-C18(OH)	-	90/10/0	1500	Disappeared	1	
Example 33	LLDPE-1	LLDPE-2	PLA	Mg-C18(OH)	-	40/60/0	1500	Disappeared	3	
Example 34	LLDPE-1	LLDPE-2	PLA	Mg-C18(OH)	-	80/20/0	1500	Disappeared	2	
Example 35	LLDPE-1	LLDPE-2	PLA	Mg-C18(OH)	-	60/40/0	1500	Disappeared	2	
Example 36	LLDPE-1	LLDPE-2	PLA	Mg-C18(OH)	-	70/30/0	1500	Disappeared	2	Yes
Example 37	LLDPE-1	LLDPE-2	PLA	Polysorbate60	-	90/10/0	1500	Disappeared	1	
Example 38	LLDPE-1	LLDPE-2	PLA	Polysorbate60	-	40/60/0	1500	Disappeared	3	
Example 39	LLDPE-1	LLDPE-2	PLA	Polysorbate60	-	80/20/0	1500	Disappeared	2	

*2: ((additive 1 + additive 2 + additive 3)/(matrix resin + carrier resin + additive 1 + additive 2 + additive 3)

[Table 8-2]

	Matrix resin	Composition of masterbatch					Concentration of additives (ppm) *2	Extrusion evaluation		Storage stability
		Carrier resin	Additive 1	Additive 2	Additive 3	Mass ratio (additive 1/ additive 2/ additive 3)		MF state	DBU (5 grades)	
<u>Example 40</u>	LLDPE-1	LLDPE-2	PLA	Polysorbate60	-	60/40/0	1500	Disappeared	2	
<u>Example 41</u>	LLDPE-1	LLDPE-2	PLA	Polysorbate60	-	70/30/0	1500	Disappeared	2	Yes
<u>Example 42</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	93/5/2	1500	Disappeared	2	
<u>Example 43</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	35/63/2	1500	Disappeared	2	
<u>Example 44</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	25/5/70	1500	Disappeared	3	
<u>Example 45</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	25/63/12	1500	Disappeared	2	
<u>Example 46</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	72/18/10	1500	Disappeared	1	No
<u>Example 47</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	77/19/4	1500	Disappeared	1	No
<u>Example 48</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	80/10/10	1500	Disappeared	1	
<u>Example 49</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	86/10/4	1500	Disappeared	1	
<u>Example 50</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	77/19/4	1000	Disappeared	1	
<u>Example 51</u>	LLDPE-1	LLDPE-2	PLA	EVOH-1	Zn-St	77/19/4	600	Disappeared	1	
<u>Example 52</u>	LLDPE-1	LLDPE-4	PLA	EVOH-1	Zn-St	77/19/4	1500	Disappeared	1	
<u>Example 53</u>	LLDPE-1	LDPE	PLA	EVOH-1	Zn-St	77/19/4	1500	Disappeared	1	
<u>Example 54</u>	LLDPE-3	LLDPE-4	PLA	EVOH-1	Zn-St	77/19/4	1500	Disappeared	1	
<u>Example 55</u>	LLDPE-3	LDPE	PLA	EVOH-1	Zn-St	77/19/4	1500	Disappeared	1	
<u>Example 56</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Zn-St	77/19/4	1500	Disappeared	1	
<u>Example 57</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Mg-C18(OH)	93/5/2	1500	Disappeared	2	
<u>Example 58</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Mg-C18(OH)	35/63/2	1500	Disappeared	2	
<u>Example 59</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Mg-C18(OH)	25/5/70	1500	Disappeared	3	

*2: ((additive 1 + additive 2 + additive 3)/(matrix resin + carrier resin + additive 1 + additive 2 + additive 3))

[Table 8-3]

	Matrix resin	Composition of masterbatch					Concentration of additives (ppm) *2	Extrusion evaluation		Storage stability
		Carrier resin	Additive 1	Additive 2	Additive 3	Mass ratio (additive 1/ additive 2/ additive 3)		MF state	DBU (5 grades)	
<u>Example 60</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Mg-C18(OH)	25/63/12	1500	Disappeared	2	
<u>Example 61</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Mg-C18(OH)	72/18/10	1500	Disappeared	1	
<u>Example 62</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Mg-C18(OH)	77/19/4	1500	Disappeared	1	
<u>Example 63</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Mg-C18(OH)	80/10/10	1500	Disappeared	1	
<u>Example 64</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Mg-C18(OH)	86/10/4	1500	Disappeared	1	
<u>Example 65</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Polysorbate60	93/5/2	1500	Disappeared	2	
<u>Example 66</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Polysorbate60	35/63/2	1500	Disappeared	2	
<u>Example 67</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Polysorbate60	25/5/70	1500	Disappeared	3	
<u>Example 68</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Polysorbate60	25/63/12	1500	Disappeared	2	
<u>Example 69</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Polysorbate60	72/18/10	1500	Disappeared	1	
<u>Example 70</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Polysorbate60	77/19/4	1500	Disappeared	1	
<u>Example 71</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Polysorbate60	80/10/10	1500	Disappeared	1	
<u>Example 72</u>	LLDPE-3	LLDPE-2	PLA	EVOH-1	Polysorbate60	86/10/4	1500	Disappeared	1	

*2: ((additive 1 + additive 2 + additive 3)/(matrix resin + carrier resin + additive 1 + additive 2 + additive 3)

[0275]

[Table 9]

	Matrix resin	Composition of masterbatch				Concentration of additives (ppm) *3	Concentration of additives (ppm) *4	Concentration of additives (ppm) *5	Film extrusion evaluation					
		Carrier resin	Additive 1	Additive 2	Degradation inhibitor				MF disappearance time (min)	Pressure stability	Film thickness			
											Average (μm)	Max (μm)	Min (μm)	Thickness unevenness (%)
<u>Example 73</u>	LLDPE-1	LLDPE-2	PLA	-	Phenol	2000	-	1000	40	0.538	68	73	64	13
<u>Example 74</u>	LLDPE-1	LLDPE-2	PLA	-	Phosphate	2000	-	1000	40	0.936	67	74	64	15
<u>Example 75</u>	LLDPE-1	LLDPE-2	PLA	-	Phenolphosphate =50:50	2000	-	1000	40	0.454	68	69	65	6
<u>Example 76</u>	LLDPE-1	LLDPE-2	PLA	-	Phenolphosphate =50:50	2000	-	500	40	0.722	65	73	64	14
<u>Example 77</u>	LLDPE-1	LLDPE-2	PLA	-	Phenolphosphate =50:50	2000	-	700	40	0.519	65	70	63	11
<u>Example 78</u>	LLDPE-1	LLDPE-2	PLA	-	Phenolphosphate =50:50	2000	-	1500	40	0.453	67	68	64	6
<u>Example 79</u>	LLDPE-1	LLDPE-2	PLA	-	Phenolphosphate =30:70	2000	-	1000	40	0.461	67	69	65	6
<u>Example 80</u>	LLDPE-1	LLDPE-2	PLA	-	Phenolphosphate =70:30	2000	-	1000	40	0.499	68	72	65	10
<u>Example 81</u>	LLDPE-1	LLDPE-2	PLA	EVOH	Phenolphosphate =50:50	1600	400	1000	20	0.451	70	73	69	6
<u>Example 82</u>	LLDPE-1	LLDPE-2	PLA	EVOH	Phenolphosphate =50:50	1800	200	1000	20	0.455	69	71	67	6
<u>Example 83</u>	LLDPE-1	LLDPE-2	PLA	-	-	2000	-	-	40	3.224	65	73	60	20

*3: (additive 1/(matrix resin + carrier resin + additive 1 + additive 2 + degradation inhibitor))

*4: (additive 2/(matrix resin + carrier resin + additive 1 + additive 2 + degradation inhibitor))

*5: (degradation inhibitor/(matrix resin + carrier resin + additive 1 + additive 2 + degradation inhibitor))

[0276]

[Table 10]

	Composition of masterbatch					Concentration of additives (wt%) (additive 1 + additive 2 + additive 3)/(carrier resin + additive 1 + additive 2 + additive 3)	MFR (g/10 min)
	Carrier resin	Additive 1	Additive 2	Additive 3	Mass ratio (additive 1/ additive 2/ additive 3)		
Example 84	LLDPE-2	PLA-1	EVOH-1	-	90/10/0	10	3.7
Example 85	LLDPE-2	PLA-1	EVOH-1	-	90/10/0	25	4.1
Example 86	LLDPE-2	PLA-1	EVOH-1	-	80/20/0	10	3.2
Example 87	LLDPE-2	PLA-1	EVOH-1	-	80/20/0	25	3.3
Example 88	LLDPE-2	PLA	Zn-St	-	90/10/0	10	5.1
Example 89	LLDPE-2	PLA	Zn-St	-	90/10/0	25	9.8
Example 90	LLDPE-2	PLA	EVOH-1	Zn-St	77/19/4	10	3.7
Example 91	LLDPE-2	PLA	EVOH-1	Zn-St	77/19/4	25	5.6

CLAIMS

Claim 1. A processing aid comprising a biodegradable polymer having a melting point of 65°C or higher.

5

Claim 2. The processing aid according to claim 1, wherein the melting point of the biodegradable polymer is 190°C or lower.

10 Claim 3. The processing aid according to claim 1 or 2,

wherein the biodegradable polymer includes an aliphatic polyester.

15 Claim 4. The processing aid according to claim 3, wherein the aliphatic polyester includes at least one selected from the group consisting of polylactic acid and polybutylene succinate.

20 Claim 5. The processing aid according to any one of claims 1 to 4, wherein the biodegradable polymer has a melt flow rate of 0.01 to 500 g/10 min at 190°C and a 2.16 kgf load.

25 Claim 6. The processing aid according to any one of claims 1 to 5, further comprising a synergist that includes at least one selected from the group consisting of polyol, polycaprolactone, silicone, and a polyamide-polyether block copolymer each of which has a melting point of 80°C or
30 lower.

Claim 7. The processing aid according to claim 6, wherein the polyol includes polyethylene glycol and/or polyethylene oxide.

35

Claim 8. The processing aid according to claim 7,
wherein the polyethylene glycol has a number average
molecular weight of 1000 to 50000, the polyethylene oxide
has a viscosity average molecular weight of 100000 to
5 10000000, and the polycaprolactone has a weight average
molecular weight of 2000 to 100000.

Claim 9. The processing aid according to any one of
claims 6 to 8,
10 wherein the biodegradable polymer and the synergist
have a mass ratio (biodegradable polymer:synergist) of
99.9:0.1 to 10:90.

Claim 10. The processing aid according to any one of
15 claims 1 to 9, further comprising an ethylene-vinyl alcohol
copolymer.

Claim 11. The processing aid according to claim 10,
wherein the ethylene-vinyl alcohol copolymer has a
20 melt flow rate of 40 g/10 min or lower at 190°C and a 2.16
kgf load.

Claim 12. The processing aid according to claim 10 or
11,
25 wherein the ethylene-vinyl alcohol copolymer has an
ethylene content of 10 to 50 mol%.

Claim 13. The processing aid according to any one of
claims 10 to 12,
30 wherein the biodegradable polymer and the ethylene-
vinyl alcohol copolymer have a mass ratio (biodegradable
polymer:ethylene-vinyl alcohol copolymer) of 95:5 to 10:90.

Claim 14. The processing aid according to any one of
35 claims 10 to 13,

wherein the biodegradable polymer and the ethylene-vinyl alcohol copolymer have a mass ratio (biodegradable polymer:ethylene-vinyl alcohol copolymer) of 92:8 to 70:30.

5 Claim 15. The processing aid according to any one of claims 10 to 14,

 wherein the biodegradable polymer, the ethylene-vinyl alcohol copolymer, and the synergist have a mass ratio (biodegradable polymer:ethylene-vinyl alcohol
10 copolymer:synergist) of (1 to 98):(1 to 98):(1 to 98).

 Claim 16. The processing aid according to any one of claims 10 to 15,

 wherein the biodegradable polymer, the ethylene-vinyl
15 alcohol copolymer, and the synergist have a mass ratio (biodegradable polymer:ethylene-vinyl alcohol copolymer:synergist) of (25 to 90):(5 to 70):(5 to 70).

 Claim 17. The processing aid according to any one of
20 claims 1 to 16, further comprising a lubricant (A) that includes at least one selected from the group consisting of a wax, an alcohol, and a surfactant.

 Claim 18. The processing aid according to claim 17,
25 wherein the biodegradable polymer and the lubricant (A) have a mass ratio (biodegradable polymer:lubricant (A)) of 99:1 to 1:99.

 Claim 19. The processing aid according to claim 17 or
30 18,

 wherein the biodegradable polymer and the lubricant (A) have a mass ratio (biodegradable polymer:lubricant (A)) of 90:10 to 40:60.

35 Claim 20. The processing aid according to any one of

claims 17 to 19,

wherein the biodegradable polymer, the ethylene-vinyl alcohol copolymer, and the lubricant (A) have a mass ratio (biodegradable polymer:ethylene-vinyl alcohol
5 copolymer:lubricant (A)) of (1 to 98):(1 to 98):(1 to 98).

Claim 21. The processing aid according to any one of claims 17 to 20,

wherein the biodegradable polymer, the ethylene-vinyl
10 alcohol copolymer, and the lubricant (A) have a mass ratio (biodegradable polymer:ethylene-vinyl alcohol
copolymer:lubricant (A)) of (25 to 93):(5 to 70):(2 to 70).

Claim 22. The processing aid according to any one of
15 claims 1 to 21,

wherein the processing aid is substantially free from fluorine.

Claim 23. A masterbatch comprising the processing aid
20 according to any one of claims 1 to 22 and a thermoplastic resin (A).

Claim 24. The masterbatch according to claim 23,
wherein the thermoplastic resin (A) includes a
25 polyolefin resin.

Claim 25. The masterbatch according to claim 24,
wherein the polyolefin resin includes polyethylene.

Claim 26. The masterbatch according to any one of
30 claims 23 to 25,

wherein the thermoplastic resin (A) and the processing aid have a mass ratio (thermoplastic resin
(A):processing aid) of 99:1 to 5:95.

35

Claim 27. The masterbatch according to any one of claims 23 to 26,

wherein the masterbatch has a melt flow rate of 0.01 to 100 g/10 min at 190°C and a 2.16 kgf load.

5

Claim 28. A thermoplastic resin composition comprising:

the processing aid according to any one of claims 1 to 22 and/or the masterbatch according to any one of claims 23 to 27; and

10

a thermoplastic resin (B).

Claim 29. The thermoplastic resin composition according to claim 28,

15

wherein the thermoplastic resin (B) includes a polyolefin resin.

Claim 30. The thermoplastic resin composition according to claim 29,

20

wherein the polyolefin resin includes polyethylene.

Claim 31. The thermoplastic resin composition according to any one of claims 28 to 30,

wherein the processing aid is contained in an amount of 0.001 to 5% by mass.

25

Claim 32. A film comprising the thermoplastic resin composition according to any one of claims 28 to 31.

30

Claim 33. A method for producing the processing aid according to any one of claims 1 to 22, comprising a mixing step and an ejecting step.

Claim 34. A method for producing the masterbatch according to any one of claims 23 to 27, comprising a

35

mixing step and an ejecting step.

Claim 35. A method for producing the thermoplastic
resin composition according to any one of claims 28 to 31,
5 comprising a mixing step and an ejecting step.

Claim 36. A method for producing the film according
to claim 32, comprising a molding step.